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November 23, 2022

Cynthia J. Kaleri  
Section Supervisor, Air Permits Section  
U.S. EPA, Region  
61201 Elm Street, Suite 500  
Dallas, Texas 75270

Re: Revised Application to Renew Part 71 Title V Operating Permit R6FOP-NM-04-R2  
Harvest Four Corners, LLC – Los Mestenos Compressor Station

Dear Ms. Kaleri,

Harvest Four Corners, LLC (Harvest) is pleased to submit to Region 6 of the Environmental Protection Agency (EPA) the attached revision to the Part 71 Title V permit renewal application (Permit Number R6FOP-NM-04-R2) for the Los Mestenos Compressor Station. Please note that this is the second revision to the original Title V renewal application submitted in February 2022. To avoid confusion, this revision of the application identifies what information is carried forward and what information is new.

Harvest appreciates the opportunity to submit the revised renewal application as well as EPA's commitment to continue processing the application. As requested by EPA, the revised application includes additional information addressing EPA's outstanding questions from October 19, 2022 as well as the October 31, 2022 rescission letter. Harvest's revised application seeks to address EPA's outstanding questions to the extent possible. Should EPA have any remaining concerns or need any additional information, Harvest remains committed to providing EPA the information it needs. For your convenience, Harvest has identified where in the application each response is provided.

- Provide the results EPA request that Harvest use the worst-case condensate sample analysis results over the 5-year time limit of the Los Mestenos Part 71 permit to calculate working and breathing losses and the flash emissions for the new TV application. Include the 2020 condensate analysis results when determining worst-case analysis and provide EPA a copy of these results. Also, revise all PTE calculations that utilize the condensate sample analysis to worst case scenario. **See Page 3 of Section 5.5.**
- Include information in the new application that reflect the changes to project scope and facility's process equipment. **See Page 3 of the Introduction.**
- Clarify in the new application if the condensate sample analysis is being used to calculate flash emission using VMGSYM for the pigging activities. If not, explain why? The worst-

case sample analysis results during the 5-year term of the permit should be used here as well. **See Page 2 of Section 5.8.**

- Harvest should not be using an outdated method to calculate tank emissions. Why is Harvest using an outdated method to calculate working and breathing losses of the tanks? Why is Harvest not using the same software to calculate working and breathing losses and the flash emissions? **See Pages 3 & 4 of Section 5.5.**
- Explain the use of emission factors from Colorado, meteorological data from Colorado, etc. instead of New Mexico. **See Page 4 of Section 5.5 & Page 2 of Section 5.9.**
- Provide recordkeeping to confirm the pigging activities number of events per week. **See Page 3 of Section 5.8.**
- Provide explanation for using 2010 TCEQ guidance for produced water emission factor and not more recent information. Also, use NMED guidance instead of, i.e., information specific to area where facility is located.. **See Page 2 of Section 5.9.**
- Provided an explanation on the meaning of “refinements” of VMGSym inputs. **See Page 4 of Section 5.5.**
- Revise process flow diagram to not include equipment that is out of service or decommissioned, and also submit documentation that this equipment is no longer an option for the facility. Usually when an operator has decommissioned equipment and wants to prove emission reductions, EPA requires proof that the supposedly decommissioned units are disconnected from the process and, if still on site, unable to be connected back up to the process and become emission units without significant reconstruction, requiring first evaluation for necessary pre-construction permitting. In fact, unless equipment has been removed from the site, we do not consider it “decommissioned,” but rather disconnected from the process and no longer an emission unit. To prove Harvest could provide photos of the disconnection (e.g., piping removed and blind flanged) and a project work order (or equivalent), *accompanied by a signed statement by the person responsible for CAA compliance.* **See Page 1 of Section 3.**
- Provide in the new application the methodologies throughout used to calculate PTE for each emission. Provide the model inputs i.e., characterization of the analysis as it is entered into the model and a characterization of the model outputs. Provide example calculation with the methodology used to calculate the pollutants emission rate that results in the total facility’s PTE. Provide all utilized methodologies and equations, assumptions, emission factors used for the emissions calculation. Information should allow for the public to follow and understand. **See Page 3 of the Introduction & Page 1 of Section 5**
- The revised Facility’s PTE calculations using worst case scenario of the condensate analysis over the 5-year term of the title V permit. **See Page 5 of Section 5.5.**
- The pigging activity emission calculations including an example calculation that aligns with an actual description of the activity as conducted at the Facility. **See Page 3 of Section 5.8.**
- An explanation of how VOC emissions are calculated using the well gas analysis for all the emission units that this analysis is used for and a calculation that demonstrates this description. **See Page 2 of Section 5.3, Page 2 of Section 5.4 & Page 3 of Section 5.8.**

- The complete characterization of the inputs and outputs to the VMGSym software used to calculate flash emissions and explanation why the model is being used separate of another model used for working and breathing losses from tanks – specifically explain how the different models, i.e., VMGSym and the outdated Tanks 4.09d, used together provide more accurate emission estimates for tank emissions instead of a single model like either VMGSym or TankESP that would account for all three types of emissions. **See Page 5 of Section 5.5.**
- Include the methodology/equations used to calculate the emissions for each emission unit with an example calculation of how the methodology is used. **See Page 2 of Section 5.**
- The Excel spreadsheets used to calculate the Facility emissions. **See Page 2 of Section 5.**

Thank you for your assistance. If you have questions or need any additional information, please contact me at (505) 632-4421.

Sincerely,



Oakley Hayes

Attachment

Los Mestenos Compressor Station Title V Operating Permit Renewal Application – Revision 2

**U.S ENVIRONMENTAL PROTECTION AGENCY (REGION 6)  
RENEWAL APPLICATION (REVISION 2)  
FOR PERMIT # R6FOP-NM-04-R2**

**LOS MESTENIOS COMPRESSOR STATION**

**Submitted By:**



**HARVEST FOUR CORNERS, LLC  
1755 Arroyo Drive  
Bloomfield, New Mexico 87413**

**Prepared By:**

**CIRRUS CONSULTING, LLC  
11139 Crisp Air Drive  
Colorado Springs, Colorado 80908  
(801) 294-3024**

**November 2022**



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## **Introduction**

The Harvest Four Corners, LLC (Harvest) Los Mestenios Compressor Station (Los Mestenios) currently operates under Part 71 Title V permit R6FOP-NM-04-R2, issued by EPA on August 8, 2017.

The facility is located on the Jicarilla Apache Indian Reservation, and as the Tribe has not developed their own rules and regulations concerning air emission sources, the facility is presently under the jurisdiction of the EPA.

### **Description of Facility**

The following description of the facility was taken from Revision 1 of this application.

The Los Mestenios Compressor Station is a natural gas compressor station that accepts produced natural gas gathered from various wellheads from the gas field surrounding the facility, and compresses this gas for delivery to natural gas processing facilities.

Under the existing Title V operating permit, the station is currently approved to operate a Solar Saturn T1200 natural gas fired turbine (Unit 1) and a Caterpillar G-399-TA 4 stroke rich burn (4SRB) reciprocating internal combustion engine (RICE) (Unit 2), both driving natural gas compressors. The existing permit also includes a 490-barrel (bbl) condensate storage tank (Unit T1) for which both flash and working/breathing losses are estimated, a 400-bbl condensate tank (Unit T2) with working/breathing losses only, fugitive emissions from valves, flanges, etc. (Unit F1), startup, shutdown, and maintenance emissions (Unit SSM) and miscellaneous insignificant emission sources.

### **Application History**

#### ***Original Application***

On January 21, 2022, a letter was submitted to the Environmental Protection Agency (EPA) Region 6 indicating that emissions at the Los Mestenios have dropped below the Title V major source thresholds. This occurred because the Caterpillar G-399-TA engine, a Title V major source by itself, was taken out of service and because flash emissions from the condensate storage tank dropped significantly.

At the request of EPA, a Title V permit renewal application was submitted in February 2022. In addition to renewing the Part 71 Title V permit, this original application identified several modifications to the facility:

- Unit 2 was to be replaced by a Waukesha L7042GL compressor engine. **Note that the Caterpillar engine is no longer operational and has been disconnected from the process as indicated in pictures provided to EPA;**
- The addition of **one Scania DS11 diesel emergency generator (Unit 3)**. The emergency generator was installed during the latter half of calendar year 2019; however, Harvest has not been able to find records indicating EPA was notified of startup. That being the case, this application is being used to provide notice of installation and startup.

### ***Revision 1***

Revision 1 of the application was submitted in September 2022 to include several corrections and modifications.

- The **490-bbl condensate tank was changed to a 400-bbl condensate tank**. The size indicated by previous applications was in error.
- Shortly after submittal of the original application it was learned that the most recent condensate analysis provided by **Noble Analytical Laboratory to Harvest, for Los Mestenos, did not include all the pertinent constituents. The revision updated the condensate storage tank emission calculations.** There was a slight drop in emissions from the two tanks.
- Harvest removed the Waukesha L7042GL compressor engine from the application. The Caterpillar engine would not be replaced. **With elimination of the engine there was an associated decrease in SSM and equipment leak emissions.**
- **The original application identified the tank heater (Unit 5) as having a rating of 0.30 million British Thermal Units per hour (mmBtu/hr). The revision correctly identified the rating at 0.012 mmBtu/hr. Note that the unit is still an insignificant source.**
- **Pig launching and pig receiving were added to the application as insignificant sources.**

### ***Revision 2***

Revision 2, this revision, is being submitted both to consolidate the additional information requested by EPA (at their request) and to modify the method of calculating the condensate storage tank emissions (also at EPA's request).

Additional information requested for the original application and Revision 1 was provided to EPA in February and August of 2022. Most of that information has been incorporated into this application. Pertinent information from those responses (including photos), not elsewhere included in this revision, are now provided in Section 8 of this application.

All additional information addressing EPA's outstanding questions from October 19, 2022 as well as the October 31, 2022 rescission letter, is provided in the body of this revision application, rather than in Section 8.

**Response to EPA request for additional information:**

- Include information in the new application that reflect the changes to project scope and facility's process equipment.

See the above written description.

**Response to EPA request for additional information:**

- Provide in the new application the methodologies throughout used to calculate PTE for each emission. Provide the model inputs i.e., characterization of the analysis as it is entered into the model and a characterization of the model outputs. Provide example calculation with the methodology used to calculate the pollutants emission rate that results in the total facility's PTE. Provide all utilized methodologies and equations, assumptions, emission factors used for the emissions calculation. Information should allow for the public to follow and understand.

Written explanations were provided in the previous versions of the application. These have been expanded so that the public might more easily follow and understand.

# **Section 1**

## **Application Forms**

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Application forms are provided in this section. Please see the following pages.

Federal Operating Permit Program (40 CFR Part 71)  
**GENERAL INFORMATION AND SUMMARY (GIS)**

**A. Mailing Address and Contact Information**

Facility name: Los Mestenos Compressor Station

Mailing address: Street or P.O. Box 1755 Arroyo Drive

City: Bloomfield State: NM ZIP: 87413 -

Contact person: Oakley Hayes Title Environmental Specialist

Telephone: (505) 632-4421 Ext.

Facsimile: (505) 632-4782 Ext.

**B. Facility Location**

Temporary source?  Yes X No Plant site location Section 2 5& 26, Township 26N, Range 5W  
(UTMH 292.3 km, UTMV 4,036.5 km, Zone 13)

City: ≈24 miles northwest of Gavilan State: NM County: Rio Arriba EPA Region: 6

Is the facility located within:

Indian lands? X YES  NO An offshore source in federal waters?  YES X NO

Non-attainment area?  YES X NO If yes, for what air pollutants? N/A

Within 50 miles of affected State? X YES  NO If yes, what state(s)? CO

**C. Owner**

Name: Hilcorp Energy Company Street/P.O. Box: 1111 Travis Street

City: Houston State: TX ZIP: 77002 -

Telephone: (713) 289 - 2630 Ext:

**D. Operator**

Name: Harvest Four Corners, LLC Street/P.O. Box: 1755 Arroyo Drive

City: Bloomfield State: NM ZIP: 87413 -

Telephone: (505) 632 - 4600 Ext:

**E. Application Type**

Mark only one permit application type and answer the supplementary question appropriate for the type marked.

☐ Initial Permit    ☒ Renewal    ☐ Significant Mod    ☐ Minor Permit Mod(MPM)

☐ Group Processing, MPM    ☐ Administrative Amendment

For initial permits, when did operations commence? \_\_\_\_ / \_\_\_\_ / \_\_\_\_

For permit renewal, what is the expiration date of current permit? 08 / 07 / 2022

**F. Applicable Requirement Summary**

Mark the types of applicable requirements that apply:

☐ SIP                      ☐ FIP/TIP                      ☐ PSD                      ☐ Non-attainment NSR

☐ Minor source NSR    ☐ Section 111                      ☐ Phase I acid rain    ☐ Phase II acid rain

☐ Stratospheric ozone    ☐ OCS regulations                      ☐ NESHAP                      ☐ Sec. 112(d) MACT

☒ Sec. 112(g) MACT    ☐ Early reduction of HAP    ☐ Sec 112(j) MACT    ☐ RMP [Sec.112(r)]

☐ Section 129                      ☐ NAAQS, increments or visibility but for temporary sources (This is rare)

Is the source subject to the Deepwater Port Act? ☐ YES ☒ NO

Has a risk management plan been registered? ☐ YES ☒ NO    Agency: \_\_\_\_\_

Phase II acid rain application submitted? ☐ YES ☒ NO    If YES, Permitting Authority: \_\_\_\_\_

**G. Source-Wide PTE Restrictions and Generic Applicable Requirements**

Cite and describe any emissions-limiting requirements and/or facility-wide "generic" applicable requirements.

Not applicable.



H. Process Description

List processes, products, and SIC codes for the facility.

| Process                 | Products               | SIC  |
|-------------------------|------------------------|------|
| Natural Gas Compression | Natural Gas            | 1389 |
| Condensate Storage      | Natural Gas Condensate | 1389 |
|                         |                        |      |
|                         |                        |      |

I. Emission Unit Identification

Assign an emissions unit ID and describe each emissions unit at the facility. Control equipment and/or alternative operating scenarios associated with emissions units should be listed on a separate line. Applicants may exclude from this list any insignificant emissions units or activities.

| Emissions Unit ID | Description of Unit                 |
|-------------------|-------------------------------------|
| 1                 | Solar Saturn 1200 Turbine           |
| 3                 | Scania DS11 Diesel Engine           |
| SSM               | Startup, Shutdown & Maintenance     |
| F1                | Piping Component Fugitive Emissions |
| T1                | 400 bbl Condensate Storage Tank     |
| T2                | 400 bbl Condensate Storage Tank     |
| L1                | Condensate Truck Loading            |
|                   |                                     |
|                   |                                     |
|                   |                                     |
|                   |                                     |
|                   |                                     |

**J. Facility Emissions Summary**

Enter potential to emit (PTE) for the facility as a whole for each regulated air pollutant listed below. Enter the name of the single HAP emitted in the greatest amount and its PTE. For all pollutants, stipulations to major source status may be indicated by entering "major" in the space for PTE. Indicate the total actual emissions for fee purposes for the facility in the space provided. Applications for permit modifications need not include actual emissions information.

NOx 20.21 tons/yr      VOC 140.92 tons/yr      SO2 0.21 tons/yr  
PM-10 0.38 tons/yr      CO 11.69 tons/yr      Lead 0.00 tons/yr  
Total HAP 14.60 tons/yr  
Single HAP with greatest amount n-Hexane      PTE 13.09 tons/yr  
Total of regulated pollutants (for fee calculation), Sec. F, line 5 of form FEE 173.42 tons/yr

**K. Existing Federally-Enforceable Permits**

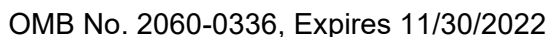
Permit number(s) R6FOP-NM-04-R2      Permit type Part 71      Permitting authority EPA  
Permit number(s) \_\_\_\_\_      Permit type \_\_\_\_\_      Permitting authority \_\_\_\_\_

**L. Emission Unit(s) Covered by General Permits – Not Applicable**

Emission unit(s) subject to general permit \_\_\_\_\_  
Check one: \_\_\_\_ Application made \_\_\_\_ Coverage granted  
General permit identifier \_\_\_\_\_      Expiration Date \_\_\_\_/\_\_\_\_/\_\_\_\_

**M. Cross-referenced Information**

Does this application cross-reference information? \_\_\_\_ YES      X NO (If yes, see instructions)



### A. General Information

SIC Code (4-digit): 1389      SCC Code 20200201

## B. Emissions Unit Description

Actual Heat Input      MM BTU/hr    Max. Design Heat Input 10.84 MM BTU/hr

**C. Fuel Data**

Primary fuel type(s): Natural Gas Standby fuel type(s): Not Applicable

Describe each fuel you expected to use during the term of the permit.

| Fuel Type   | Max. Sulfur Content (%) | Max. Ash Content (%) | BTU Value (cf, gal., or lb.) |
|-------------|-------------------------|----------------------|------------------------------|
| Natural Gas | Negligible              | Negligible           | 900 Btu/cf                   |
|             |                         |                      |                              |
|             |                         |                      |                              |

**D. Fuel Usage Rates**

| Fuel Type   | Annual Actual Usage | Maximum Usage |              |
|-------------|---------------------|---------------|--------------|
|             |                     | Hourly        | Annual       |
| Natural Gas | 105.51 MMscf        | 12,044 scf    | 105.51 MMscf |
|             |                     |               |              |

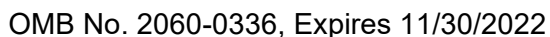
**E. Associated Air Pollution Control Equipment – Not Applicable**

|  |
|--|
| Emissions unit ID _____ Device type _____<br>Air pollutant(s) Controlled _____ Manufacturer _____<br>Model No. _____ Serial No. _____<br>Installation date ____/____/____ Control efficiency (%) _____<br>Efficiency estimation method _____ |
|--|

**F. Ambient Impact Assessment – Not Applicable**

This information must be completed by temporary sources or when ambient impact assessment is an applicable requirement for this emissions unit (this is not common).

|  |
|--|
| Stack height (ft) _____ Inside stack diameter (ft) _____<br>Stack temp (°F) _____ Design stack flow rate (ACFM) _____<br>Actual stack flow rate (ACFM) _____ Velocity (ft/sec) _____ |
|--|



### A. General Information

SIC Code (4-digit): 1389      SCC Code 20200102

## B. Emissions Unit Description

Actual Heat Input      MM BTU/hr    Max. Design Heat Input 0.69 MM BTU/hr

**C. Fuel Data**

Primary fuel type(s): Diesel Standby fuel type(s): Not Applicable

Describe each fuel you expected to use during the term of the permit.

| Fuel Type | Max. Sulfur Content (%) | Max. Ash Content (%) | BTU Value (cf, gal., or lb.) |
|-----------|-------------------------|----------------------|------------------------------|
| Diesel    | ≤0.0015%                | Unknown              | 138,000 Btu/gal              |
|           |                         |                      |                              |
|           |                         |                      |                              |

**D. Fuel Usage Rates**

| Fuel Type | Annual Actual Usage | Maximum Usage |           |
|-----------|---------------------|---------------|-----------|
|           |                     | Hourly        | Annual    |
| Diesel    | 2,500 gal           | 5 gal         | 2,500 gal |
|           |                     |               |           |

**E. Associated Air Pollution Control Equipment – Not Applicable**

Emissions unit ID \_\_\_\_\_ Device type \_\_\_\_\_

Air pollutant(s) Controlled \_\_\_\_\_ Manufacturer \_\_\_\_\_

Model No. \_\_\_\_\_ Serial No. \_\_\_\_\_

Installation date \_\_\_\_/\_\_\_\_/\_\_\_\_ Control efficiency (%) \_\_\_\_\_

Efficiency estimation method \_\_\_\_\_

**F. Ambient Impact Assessment – Not Applicable**

This information must be completed by temporary sources or when ambient impact assessment is an applicable requirement for this emissions unit (this is not common).

Stack height (ft) \_\_\_\_\_ Inside stack diameter (ft) \_\_\_\_\_

Stack temp (°F) \_\_\_\_\_ Design stack flow rate (ACFM) \_\_\_\_\_

Actual stack flow rate (ACFM) \_\_\_\_\_ Velocity (ft/sec) \_\_\_\_\_

## Federal Operating Permit Program (40 CFR Part 71)

**EMISSIONS UNIT DESCRIPTION FOR VOC EMITTING SOURCES (EUD-2)****A. General Information**Emissions unit ID SSM Description Startup, Shutdown & MaintenanceSIC Code (4-digit) 1389 SCC Code 2310021803**B. Emissions Unit Description**Equipment type SSM Emissions. Temporary source: ☐ Yes ☒ NoManufacturer N/A Model No. N/ASerial No. N/A Installation date N/AArticles being coated or degreased N/AApplication method N/AOverspray (surface coating) (%) N/A Drying method N/ANo. of dryers N/A Tank capacity (degreasers) (gal) N/A**C. Associated Air Pollution Control Equipment – Not Applicable**

Emissions unit ID \_\_\_\_\_ Device Type \_\_\_\_\_

Manufacturer \_\_\_\_\_ Model No \_\_\_\_\_

Serial No. \_\_\_\_\_ Installation date \_\_\_\_/\_\_\_\_/\_\_\_\_

Control efficiency (%) \_\_\_\_\_ Capture efficiency (%) \_\_\_\_\_

Air pollutant(s) controlled \_\_\_\_\_ Efficiency estimation method \_\_\_\_\_

**D. Ambient Impact Assessment – Not Applicable**

This information must be completed by temporary sources or when ambient impact assessment is an applicable requirement for this emissions unit (this is not common).

Stack height (ft) \_\_\_\_\_ Inside stack diameter (ft) \_\_\_\_\_

Stack temp (F) \_\_\_\_\_ Design stack flow rate (ACFM) \_\_\_\_\_

Actual stack flow rate (ACFM) \_\_\_\_\_ Velocity (ft/sec) \_\_\_\_\_

E. VOC-containing Substance Data

List each VOC-containing substance consumed, processed or produced at the emissions unit that is emitted into the air. In the name column, if providing a brand name, include the name of the manufacture; if the substance contains HAP, list the constituent HAP.

| Substance Name<br>(Chemical, Brand Name) | CAS No. | Substance Type | Actual Usage<br>(gal/yr) | Max Usage<br>(gal/day) | Max Usage<br>(gal/year) | VOC Content<br>(lb/gal) |
|--|---------|----------------|--------------------------|------------------------|-------------------------|-------------------------|
| Natural Gas                              | N/A     | Natural Gas    | N/A                      | N/A                    | N/A                     | N/A                     |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |



## Federal Operating Permit Program (40 CFR Part 71)

**EMISSIONS UNIT DESCRIPTION FOR VOC EMITTING SOURCES (EUD-2)****A. General Information**Emissions unit ID F1 Description Piping Component Fugitive EmissionsSIC Code (4-digit) 1389 SCC Code 2310021509**B. Emissions Unit Description**Equipment type Valves, Flanges, Seals, etc. Temporary source: ☐ Yes ☒ NoManufacturer Unknown Model No. UnknownSerial No. Unknown Installation date UnknownArticles being coated or degreased N/AApplication method N/AOverspray (surface coating) (%) N/A Drying method N/ANo. of dryers N/A Tank capacity (degreasers) (gal) N/A**C. Associated Air Pollution Control Equipment – Not Applicable**

Emissions unit ID \_\_\_\_\_ Device Type \_\_\_\_\_

Manufacturer \_\_\_\_\_ Model No \_\_\_\_\_

Serial No. \_\_\_\_\_ Installation date \_\_\_\_/\_\_\_\_/\_\_\_\_

Control efficiency (%) \_\_\_\_\_ Capture efficiency (%) \_\_\_\_\_

Air pollutant(s) controlled \_\_\_\_\_ Efficiency estimation method \_\_\_\_\_

**D. Ambient Impact Assessment – Not Applicable**

This information must be completed by temporary sources or when ambient impact assessment is an applicable requirement for this emissions unit (this is not common).

Stack height (ft) \_\_\_\_\_ Inside stack diameter (ft) \_\_\_\_\_

Stack temp (F) \_\_\_\_\_ Design stack flow rate (ACFM) \_\_\_\_\_

Actual stack flow rate (ACFM) \_\_\_\_\_ Velocity (ft/sec) \_\_\_\_\_

E. VOC-containing Substance Data

List each VOC-containing substance consumed, processed or produced at the emissions unit that is emitted into the air. In the name column, if providing a brand name, include the name of the manufacture; if the substance contains HAP, list the constituent HAP.

| Substance Name<br>(Chemical, Brand Name) | CAS No. | Substance Type | Actual Usage<br>(gal/yr) | Max Usage<br>(gal/day) | Max Usage<br>(gal/year) | VOC Content<br>(lb/gal) |
|--|---------|----------------|--------------------------|------------------------|-------------------------|-------------------------|
| Natural Gas                              | N/A     | Natural Gas    | N/A                      | N/A                    | N/A                     | N/A                     |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |
|  |         |                |                          |                        |                         |                         |

**Federal Operating Permit Program (40 CFR Part 71)****EMISSIONS UNIT DESCRIPTION FOR VOC EMITTING SOURCES (EUD-2)****A. General Information**Emissions unit ID T1 Description 400-bbl Condensate Storage TankSIC Code (4-digit) 1389 SCC Code 2310021010**B. Emissions Unit Description**Equipment type Condensate Storage Tank Temporary source: ☐ Yes ☒ NoManufacturer American Tank & Steel Model No. N/ASerial No. 2874 Installation date Unknown (Manufacture Date 06/1965)Articles being coated or degreased N/AApplication method N/AOverspray (surface coating) (%) N/A Drying method N/ANo. of dryers N/A Tank capacity (degreasers) (gal) N/A**C. Associated Air Pollution Control Equipment – Not Applicable**

Emissions unit ID \_\_\_\_\_ Device Type \_\_\_\_\_

Manufacturer \_\_\_\_\_ Model No \_\_\_\_\_

Serial No. \_\_\_\_\_ Installation date \_\_\_\_/\_\_\_\_/\_\_\_\_

Control efficiency (%) \_\_\_\_\_ Capture efficiency (%) \_\_\_\_\_

Air pollutant(s) controlled \_\_\_\_\_ Efficiency estimation method \_\_\_\_\_

**D. Ambient Impact Assessment – Not Applicable**

This information must be completed by temporary sources or when ambient impact assessment is an applicable requirement for this emissions unit (this is not common).

Stack height (ft) \_\_\_\_\_ Inside stack diameter (ft) \_\_\_\_\_

Stack temp (F) \_\_\_\_\_ Design stack flow rate (ACFM) \_\_\_\_\_

Actual stack flow rate (ACFM) \_\_\_\_\_ Velocity (ft/sec) \_\_\_\_\_

E. VOC-containing Substance Data

List each VOC-containing substance consumed, processed or produced at the emissions unit that is emitted into the air. In the name column, if providing a brand name, include the name of the manufacture; if the substance contains HAP, list the constituent HAP.

| Substance Name<br>(Chemical,<br>Brand Name) | CAS No. | Substance Type         | Actual Usage<br>(gal/yr) | Max Usage<br>(gal/day) | Max Usage<br>(gal/year) | VOC Content<br>(lb/gal) |
|---|---------|------------------------|--------------------------|------------------------|-------------------------|-------------------------|
| Natural Gas Condensate                      | N/A     | Natural Gas Condensate | N/A                      | 2,548                  | 929,922                 | ≈5.7                    |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |

## Federal Operating Permit Program (40 CFR Part 71)

**EMISSIONS UNIT DESCRIPTION FOR VOC EMITTING SOURCES (EUD-2)****A. General Information**Emissions unit ID T2 Description 400 bbl Condensate Storage TankSIC Code (4-digit) 1389 SCC Code 2310021010**B. Emissions Unit Description**Equipment type Condensate Storage Tank Temporary source: ☐ Yes ☒ NoManufacturer American Tank & Steel Model No. N/ASerial No. 831-2918 Installation date 2014 (Manufacture Date 1965)Articles being coated or degreased N/AApplication method N/AOverspray (surface coating) (%) N/A Drying method N/ANo. of dryers N/A Tank capacity (degreasers) (gal) N/A**C. Associated Air Pollution Control Equipment – Not Applicable**

Emissions unit ID \_\_\_\_\_ Device Type \_\_\_\_\_

Manufacturer \_\_\_\_\_ Model No \_\_\_\_\_

Serial No. \_\_\_\_\_ Installation date \_\_\_\_/\_\_\_\_/\_\_\_\_

Control efficiency (%) \_\_\_\_\_ Capture efficiency (%) \_\_\_\_\_

Air pollutant(s) controlled \_\_\_\_\_ Efficiency estimation method \_\_\_\_\_

**D. Ambient Impact Assessment – Not Applicable**

This information must be completed by temporary sources or when ambient impact assessment is an applicable requirement for this emissions unit (this is not common).

Stack height (ft) \_\_\_\_\_ Inside stack diameter (ft) \_\_\_\_\_

Stack temp (F) \_\_\_\_\_ Design stack flow rate (ACFM) \_\_\_\_\_

Actual stack flow rate (ACFM) \_\_\_\_\_ Velocity (ft/sec) \_\_\_\_\_

E. VOC-containing Substance Data

List each VOC-containing substance consumed, processed or produced at the emissions unit that is emitted into the air. In the name column, if providing a brand name, include the name of the manufacture; if the substance contains HAP, list the constituent HAP.

| Substance Name<br>(Chemical, Brand Name) | CAS No. | Substance Type         | Actual Usage<br>(gal/yr) | Max Usage<br>(gal/day) | Max Usage<br>(gal/year) | VOC Content<br>(lb/gal) |
|--|---------|------------------------|--------------------------|------------------------|-------------------------|-------------------------|
| Natural Gas Condensate                   | N/A     | Natural Gas Condensate | N/A                      | 1,274                  | 464,961                 | ≈5.7                    |
|  |         |                        |                          |                        |                         |                         |
|  |         |                        |                          |                        |                         |                         |
|  |         |                        |                          |                        |                         |                         |
|  |         |                        |                          |                        |                         |                         |
|  |         |                        |                          |                        |                         |                         |
|  |         |                        |                          |                        |                         |                         |
|  |         |                        |                          |                        |                         |                         |

## Federal Operating Permit Program (40 CFR Part 71)

**EMISSIONS UNIT DESCRIPTION FOR VOC EMITTING SOURCES (EUD-2)****A. General Information**Emissions unit ID L1 Description Condensate Truck LoadingSIC Code (4-digit) 1389 SCC Code 2310021030**B. Emissions Unit Description**Equipment type Condensate Truck Loading Temporary source: ☐ Yes ☒ NoManufacturer N/A Model No. N/ASerial No. N/A Installation date N/AArticles being coated or degreased N/AApplication method N/AOverspray (surface coating) (%) N/A Drying method N/ANo. of dryers N/A Tank capacity (degreasers) (gal) N/A**C. Associated Air Pollution Control Equipment – Not Applicable**

Emissions unit ID \_\_\_\_\_ Device Type \_\_\_\_\_

Manufacturer \_\_\_\_\_ Model No \_\_\_\_\_

Serial No. \_\_\_\_\_ Installation date \_\_\_\_/\_\_\_\_/\_\_\_\_

Control efficiency (%) \_\_\_\_\_ Capture efficiency (%) \_\_\_\_\_

Air pollutant(s) controlled \_\_\_\_\_ Efficiency estimation method \_\_\_\_\_

**D. Ambient Impact Assessment – Not Applicable**

This information must be completed by temporary sources or when ambient impact assessment is an applicable requirement for this emissions unit (this is not common).

Stack height (ft) \_\_\_\_\_ Inside stack diameter (ft) \_\_\_\_\_

Stack temp (F) \_\_\_\_\_ Design stack flow rate (ACFM) \_\_\_\_\_

Actual stack flow rate (ACFM) \_\_\_\_\_ Velocity (ft/sec) \_\_\_\_\_

E. VOC-containing Substance Data

List each VOC-containing substance consumed, processed or produced at the emissions unit that is emitted into the air. In the name column, if providing a brand name, include the name of the manufacture; if the substance contains HAP, list the constituent HAP.

| Substance Name<br>(Chemical,<br>Brand Name) | CAS No. | Substance Type         | Actual Usage<br>(gal/yr) | Max Usage<br>(gal/day) | Max Usage<br>(gal/year) | VOC Content<br>(lb/gal) |
|---|---------|------------------------|--------------------------|------------------------|-------------------------|-------------------------|
| Natural Gas Condensate                      | N/A     | Natural Gas Condensate | N/A                      | 2,548                  | 929,922                 | ≈5.7                    |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |
|   |         |                        |                          |                        |                         |                         |



Federal Operating Permit Program (40 CFR Part 71)  
**INSIGNIFICANT EMISSIONS (IE)**

On this page list each insignificant activity or emission unit. In the "number" column, indicate the number of units in this category. Descriptions should be brief but unique. Indicate which emissions criterion of part 71 is the basis for the exemption.

| Number | Description of Activities or Emissions Units | RAP<br>(except HAP) | HAP |
|--------|--|---------------------|-----|
| 4      | Fuel Gas Heater (0.3 MMBtu/hr)               | X                   | X   |
| 5      | Tank Heater (0.012 MMBtu/hr)                 | X                   | X   |
| PL     | Pig Launcher                                 | X                   | X   |
| PR     | Pig Receiver                                 | X                   | X   |
| T3     | Produced Water Storage Tank (70 bbl)         | X                   | X   |
| L2     | Truck Loading (Produced Water)               | X                   | X   |
| T4     | Lube Oil Storage Tank (500 gal)              | X                   | X   |
| T5     | Lube Oil Storage Tank (500 bbl)              | X                   | X   |
| T6     | Ambitrol Storage Tank (350 gal)              | X                   | X   |
| T7     | Methanol Storage Tank (500 gal)              | X                   | X   |
|        |  |                     |     |

Federal Operating Permit Program (40 CFR Part 71)  
**EMISSION CALCULATIONS (EMISS)**

Calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit, control device, or alternative operating scenario identified in section I of form **GIS**. If form **FEE** does not need to be submitted with the application, do not calculate actual emissions.

**A. Emissions Unit ID**   1  

**B. Identification and Quantification of Emissions**

For each emissions unit identified above, list each regulated air pollutant or other pollutant for which the source is major, then list any other regulated pollutant (for fee calculation) not already listed. HAP may be simply listed as "HAP." Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each pollutant. Do not calculate PTE for air pollutants listed solely for fee purposes. Include all fugitives for fee purposes. See instructions concerning GHGs. Values should be reported to the nearest tenth (0.1) of a ton for yearly values or tenth (0.1) of a pound for hourly values.

| Air Pollutants | Emission Rates                    |                   |                  | CAS No. |
|----------------|-----------------------------------|-------------------|------------------|---------|
|                | Actual Annual Emissions (tons/yr) | Potential to Emit |                  |         |
|                |                                   | Hourly (lb/hr)    | Annual (tons/yr) |         |
| NO2            | 19.3                              | 4.4               | 19.3             |         |
| CO             | 11.4                              | 2.6               | 11.4             |         |
| VOC            | 0.4                               | 0.1               | 0.4              |         |
| SO2            | 0.2                               | --                | 0.2              |         |
| TSP            | 0.3                               | 0.1               | 0.3              |         |
| PM10           | 0.3                               | 0.1               | 0.3              |         |
| PM2.5          | 0.3                               | 0.1               | 0.3              |         |
| Acetaldehyde   | --                                | --                | 0.2              | 75070   |
| Formaldehyde   | --                                | --                | 0.2              | 50000   |
| Total HAPs     | --                                | 0.1               | 0.5              |         |
| CO2            | --                                | --                | 5544.6           |         |
| CH4            | --                                | --                | 0.1              |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |

Federal Operating Permit Program (40 CFR Part 71)  
**EMISSION CALCULATIONS (EMISS)**

Calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit, control device, or alternative operating scenario identified in section I of form **GIS**. If form **FEE** does not need to be submitted with the application, do not calculate actual emissions.

**A. Emissions Unit ID**   3  

**B. Identification and Quantification of Emissions**

For each emissions unit identified above, list each regulated air pollutant or other pollutant for which the source is major, then list any other regulated pollutant (for fee calculation) not already listed. HAP may be simply listed as "HAP." Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each pollutant. Do not calculate PTE for air pollutants listed solely for fee purposes. Include all fugitives for fee purposes. See instructions concerning GHGs. Values should be reported to the nearest tenth (0.1) of a ton for yearly values or tenth (0.1) of a pound for hourly values.

| Air Pollutants | Emission Rates                    |                   |                  | CAS No. |
|----------------|-----------------------------------|-------------------|------------------|---------|
|                | Actual Annual Emissions (tons/yr) | Potential to Emit |                  |         |
|                |                                   | Hourly (lb/hr)    | Annual (tons/yr) |         |
| NO2            | 0.2                               | 3.0               | 0.8              |         |
| CO             | --                                | 0.7               | 0.2              |         |
| VOC            | --                                | 0.2               | 0.1              |         |
| SO2            | --                                | 0.2               | 0.1              |         |
| TSP            | --                                | 0.2               | 0.1              |         |
| PM10           | --                                | 0.2               | 0.1              |         |
| PM2.5          | --                                | 0.2               | 0.1              |         |
| Total HAPs     | --                                | --                | --               |         |
| CO2            | --                                | --                | 31.2             |         |
| CH4            | --                                | --                | --               |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |

Federal Operating Permit Program (40 CFR Part 71)  
**EMISSION CALCULATIONS (EMISS)**

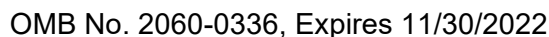
Calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit, control device, or alternative operating scenario identified in section I of form **GIS**. If form **FEE** does not need to be submitted with the application, do not calculate actual emissions.

**A. Emissions Unit ID** SSM

**B. Identification and Quantification of Emissions**

For each emissions unit identified above, list each regulated air pollutant or other pollutant for which the source is major, then list any other regulated pollutant (for fee calculation) not already listed. HAP may be simply listed as "HAP." Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each pollutant. Do not calculate PTE for air pollutants listed solely for fee purposes. Include all fugitives for fee purposes. See instructions concerning GHGs. Values should be reported to the nearest tenth (0.1) of a ton for yearly values or tenth (0.1) of a pound for hourly values.

| Air Pollutants | Emission Rates                    |                   |                  | CAS No. |
|----------------|-----------------------------------|-------------------|------------------|---------|
|                | Actual Annual Emissions (tons/yr) | Potential to Emit |                  |         |
|                |                                   | Hourly (lb/hr)    | Annual (tons/yr) |         |
| VOC            | 0.0                               | --                | 11.9             | 110543  |
| n-Hexane       | --                                | --                | 0.3              |         |
| Total HAPs     | --                                | --                | 0.3              |         |
| CO2            | --                                | --                | 0.9              |         |
| CH4            | --                                | --                | 30.3             |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |



Calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit, control device, or alternative operating scenario identified in section I of form **GIS**. If form **FEE** does not need to be submitted with the application, do not calculate actual emissions.

## B. Identification and Quantification of Emissions

For each emissions unit identified above, list each regulated air pollutant or other pollutant for which the source is major, then list any other regulated pollutant (for fee calculation) not already listed. HAP may be simply listed as "HAP." Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each pollutant. Do not calculate PTE for air pollutants listed solely for fee purposes. Include all fugitives for fee purposes. See instructions concerning GHGs. Values should be reported to the nearest tenth (0.1) of a ton for yearly values or tenth (0.1) of a pound for hourly values.

[illegible]

Federal Operating Permit Program (40 CFR Part 71)  
**EMISSION CALCULATIONS (EMISS)**

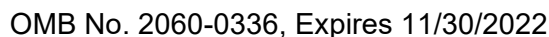
Calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit, control device, or alternative operating scenario identified in section I of form **GIS**. If form **FEE** does not need to be submitted with the application, do not calculate actual emissions.

**A. Emissions Unit ID** T1

**B. Identification and Quantification of Emissions**

For each emissions unit identified above, list each regulated air pollutant or other pollutant for which the source is major, then list any other regulated pollutant (for fee calculation) not already listed. HAP may be simply listed as "HAP." Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each pollutant. Do not calculate PTE for air pollutants listed solely for fee purposes. Include all fugitives for fee purposes. See instructions concerning GHGs. Values should be reported to the nearest tenth (0.1) of a ton for yearly values or tenth (0.1) of a pound for hourly values.

| Air Pollutants | Emission Rates                    |                   |                  | CAS No. |
|----------------|-----------------------------------|-------------------|------------------|---------|
|                | Actual Annual Emissions (tons/yr) | Potential to Emit |                  |         |
|                |                                   | Hourly (lb/hr)    | Annual (tons/yr) |         |
| VOC            | 7.1                               | --                | 115.6            |         |
| Benzene        | --                                | --                | 0.5              | 71432   |
| n-Hexane       | 0.6                               | --                | 11.7             | 110543  |
| Toluene        | --                                | --                | 0.3              | 108883  |
| Total HAPs     | 0.6                               | --                | 12.5             |         |
| CO2            | --                                | --                | 0.7              |         |
| CH4            | --                                | --                | 10.7             |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |
|                |                                   |                   |                  |         |

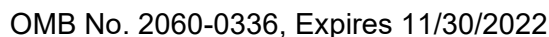


Calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit, control device, or alternative operating scenario identified in section I of form **GIS**. If form **FEE** does not need to be submitted with the application, do not calculate actual emissions.

## B. Identification and Quantification of Emissions

For each emissions unit identified above, list each regulated air pollutant or other pollutant for which the source is major, then list any other regulated pollutant (for fee calculation) not already listed. HAP may be simply listed as "HAP." Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each pollutant. Do not calculate PTE for air pollutants listed solely for fee purposes. Include all fugitives for fee purposes. See instructions concerning GHGs. Values should be reported to the nearest tenth (0.1) of a ton for yearly values or tenth (0.1) of a pound for hourly values.

[illegible]



Calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit, control device, or alternative operating scenario identified in section I of form **GIS**. If form **FEE** does not need to be submitted with the application, do not calculate actual emissions.

## B. Identification and Quantification of Emissions

For each emissions unit identified above, list each regulated air pollutant or other pollutant for which the source is major, then list any other regulated pollutant (for fee calculation) not already listed. HAP may be simply listed as "HAP." Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each pollutant. Do not calculate PTE for air pollutants listed solely for fee purposes. Include all fugitives for fee purposes. See instructions concerning GHGs. Values should be reported to the nearest tenth (0.1) of a ton for yearly values or tenth (0.1) of a pound for hourly values.

[illegible]



**Federal Operating Permit Program (40 CFR Part 71)**  
**POTENTIAL TO EMIT (PTE)**

For each emissions unit at the facility, list the unit ID and the PTE of each air pollutant listed below and sum the values to determine the total PTE for the facility. It may be helpful to complete form **EMISS** before completing this form. Report each pollutant at each unit to the nearest tenth (0.1) of a ton; values may be reported with greater precision (i.e., more decimal places) if desired. Report facility total PTE for each listed pollutant on this form and in section **J** of form **GIS**. The HAP column is for the PTE of all HAPs for each unit. You may use an attachment to show any pollutants that may be present in major amounts that are not already listed on the form (this is not common).

| Emissions Unit ID       | Regulated Air Pollutants and Pollutants for which Source is Major<br>(PTE in tons/yr) |              |            |            |             |            |             |
|-------------------------|---|--------------|------------|------------|-------------|------------|-------------|
|                         | NOx   | VOC          | SO2        | PM10       | CO          | Lead       | HAP         |
| 1                       | 19.3  | 0.4          | 0.2        | 0.3        | 11.4        | 0.0        | 0.5         |
| 3                       | 0.8   | 0.1          | 0.0        | 0.1        | 0.2         | 0.0        | 0.0         |
| SSM                     |   | 11.9         |            |            |             |            | 0.3         |
| F1                      |   | 3.9          |            |            |             |            | 0.1         |
| T1                      |   | 115.6        |            |            |             |            | 12.5        |
| T2                      |   | 5.0          |            |            |             |            | 0.7         |
| L1                      |   | 2.5          |            |            |             |            | 0.4         |
|                         |   |              |            |            |             |            |             |
|                         |   |              |            |            |             |            |             |
|                         |   |              |            |            |             |            |             |
| <b>FACILITY TOTALS:</b> | <b>20.2</b>   | <b>140.9</b> | <b>0.2</b> | <b>0.4</b> | <b>11.7</b> | <b>0.0</b> | <b>14.6</b> |

## **Section 2**

### **Description of the Routine Operation of the Facility**

---

The following description of operations at the facility was taken from Revision 1 of the application.

The Los Mestenos Compressor Station is located in northwestern New Mexico, within the boundaries of the Jicarilla Apache Reservation, and therefore falls within the jurisdiction of United States Environmental Protection Agency, Region 6. The facility compresses natural gas for pipeline transmission. The natural gas is received from pipelines that are fed by upstream natural gas wells.

Once at the facility, the natural gas passes through the liquids receiver (VR-1013) and then through the inlet suction scrubber (VSC-1022). There are no emissions from these vessels. Their purpose is to separate liquids from the natural gas stream. Liquids are separated from the gas stream in both vessels and sent to the facility condensate tank (T-1023), which can then overflow into the second facility condensate tank (T-1024), if needed. Flash emissions will occur in the first tank where the liquid is discharged and working and breathing emissions will occur from both tanks. All tank emissions are vented to atmosphere, as there are currently no applicable requirements to control tank emissions at the facility. Water is separated off the condensate and drained into the facility's produced water tank. Liquids are removed from the facility via truck. There are loadout emissions associated with this action. During the winter months, a small tank heater is used to prevent the liquids in the tanks from freezing. There are a small amount of combustion emissions associated with this unit.

After the natural gas passes through the inlet suction scrubber (VSC-1022), it is compressed by the Solar Turbine (GT-1031) from approximately 95 psi to 210 psi (this is the primary purpose of the turbine). The turbine fires natural gas that is heated with a fuel gas heater during the winter months to prevent any condensables from freezing. There are a small amount of combustion emissions associated with the fuel gas heater. The turbine does not have any emission controls and emits to atmosphere. After compression, the gas passes through the facility discharge cooler (AC-1021) before exiting the facility and being discharged to Harvest's Dogie Compressor Station. There are no emissions associated with the discharge cooler.

There is also a pig launcher (VR-1014) and pig receiver (VR-1011) located within a quarter mile of the facility. Pigs are launched in pipelines to clean out any buildups of liquid and other material in the pipe. There are small amounts of emissions when a pig is launched and when a

pig is received. Emissions are dependent on the volume of the launcher/receiver. Multiple pigs can be caught in a receiver before it is opened and vents emissions to atmosphere, so not every pig receiving event results in emissions. For the pigs that are received at Los Mestenos, smaller diameter pigs are used in one pipeline and drop into a different larger pipeline. The pig used in this larger pipeline then pushes the smaller pigs into the facility receiver. So multiple pigs are caught in the receiver simultaneously, resulting in the receiver only being opened once for multiple pigs. This common industry practice reduces emissions by limiting how many times the receiver is opened. Liquids from the pigging operations are sent to the condensate storage tanks. Any flash emissions that might occur are accounted for in the condensate tank flash emission calculations.

An emergency diesel powered generator engine provides electricity to the site if the facility loses power.

Methanol is injected into the natural gas stream to prevent pipeline freezes in the winter. Methanol works as an anti-freeze by joining with the natural gas and water vapor to lower the freezing point of the vapor. The Ambitrol tank contains anti-freeze.

# Section 3

## Process Flow Sheet

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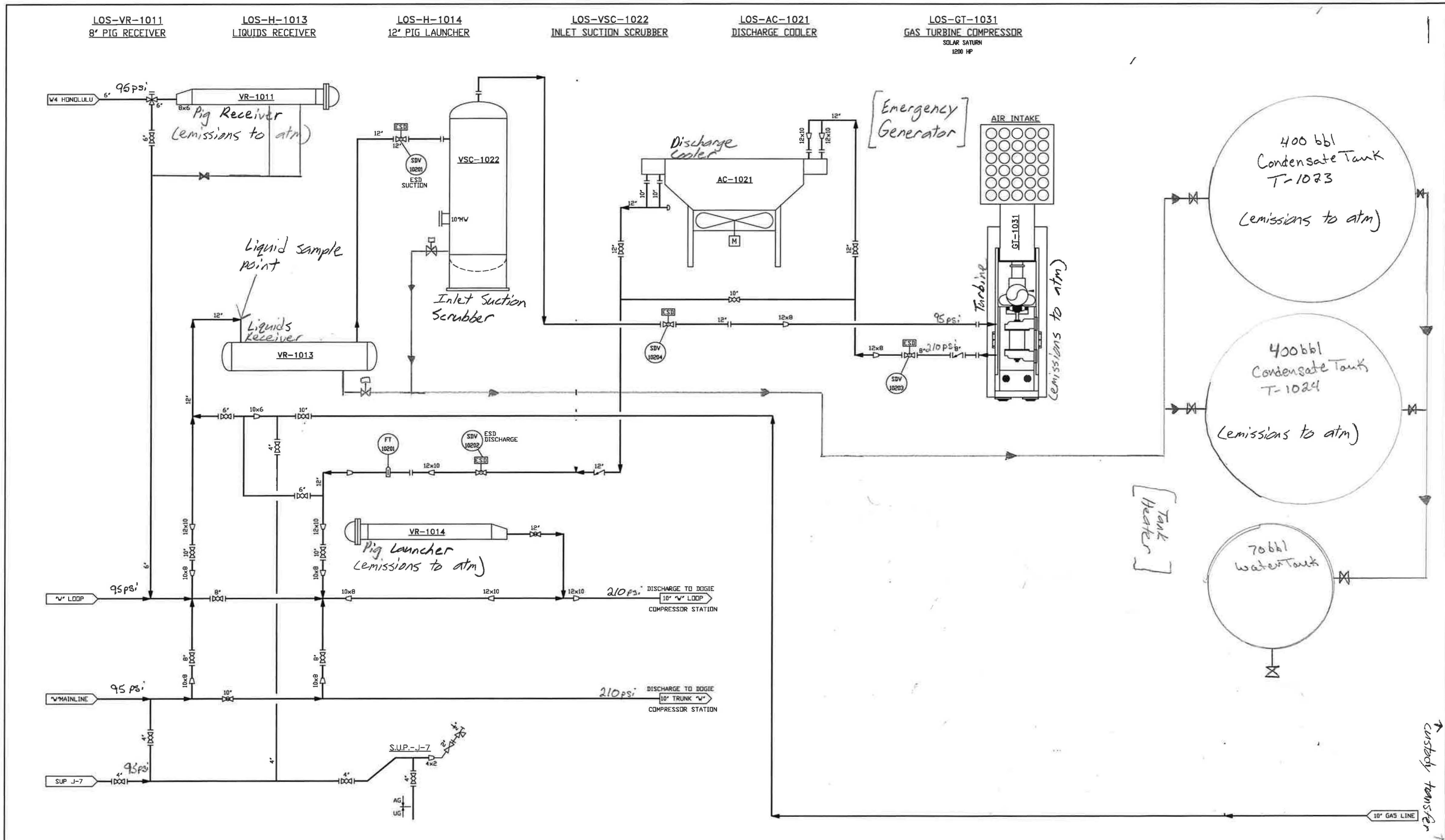
A process flow sheet is provided in this section. It has been updated to incorporate suggestions made by EPA. Please see the following page.

### Response to EPA request for additional information:

- Revise process flow diagram to not include equipment that is out of service or decommissioned, and also submit documentation that this equipment is no longer an option for the facility. Usually when an operator has decommissioned equipment and wants to prove emission reductions, EPA requires proof that the supposedly decommissioned units are disconnected from the process and, if still on site, unable to be connected back up to the process and become emission units without significant reconstruction, requiring first evaluation for necessary pre-construction permitting. In fact, unless equipment has been removed from the site, we do not consider it “decommissioned,” but rather disconnected from the process and no longer an emission unit. To prove Harvest could provide photos of the disconnection (e.g., piping removed and blind flanged) and a project work order (or equivalent), *accompanied by a signed statement by the person responsible for CAA compliance.*

The process flow sheet submitted with Revision 1 of the application has been revised so as to exclude equipment that is out of service or decommissioned. Photographs were previously provided to EPA showing that the engine has been disconnected. They are included in Section 8. The certification of this application by the responsible official constitutes a signed statement declaring the unit is no longer in service.





# **Section 4**

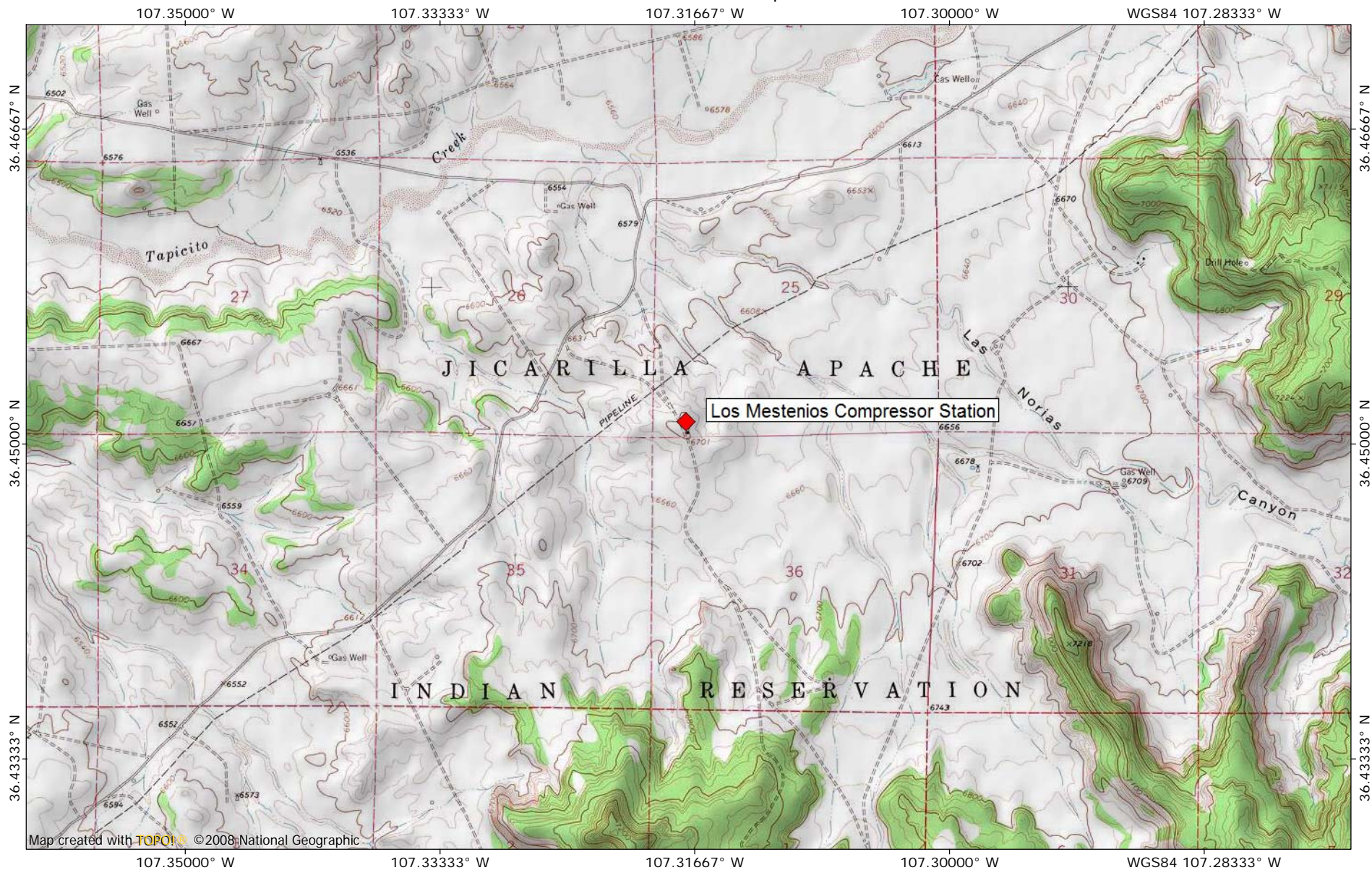
## **Topographic Map**

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A topographic map is provided in this section. Please see the following page.



HARVEST FOUR CORNERS, LLC - LOS MESTENIOS COMPRESSOR STATION - Jicarilla Apache Reservation, Rio Arriba Co., NM T 26 N, R 05 W, Sec. 25/36



0.0 0.5 1.0 miles  
0.0 0.5 1.0 1.5 km

TN MN  
8½°  
02/02/22

# Section 5

## Emission Calculations

---

### *General*

Per EPA's request in an October 24<sup>th</sup> meeting, Harvest is providing a more detailed written explanation of the methodologies used to calculate emissions. Where changes have been made to the calculations, explanations are provided.

Note that this Section 5 is divided into 12 subsections: Turbine, Generator, Startup, Shutdown & Maintenance, Equipment Leaks, Condensate Storage Tanks, Condensate Truck Loading, Heaters, Pig Launcher & Receiver, Produced Water Storage Tanks, Produced Water Truck Loading, Miscellaneous Tanks, and GHG Emissions. Each of the 12 subparts begins with a written description of the calculations. Then PTE emissions calculations are provided. Finally, for significant source types, actual emissions calculations are provided.

This general section provides tables summarizing both the PTE and actual emissions calculations from the other subsections.

In each of the 12 subsections, supporting documentation for the calculations is provided with the PTE emissions calculations.

### **Response to EPA request for additional information:**

- Provide in the new application the methodologies throughout used to calculate PTE for each emission. Provide the model inputs i.e., characterization of the analysis as it is entered into the model and a characterization of the model outputs. Provide example calculation with the methodology used to calculate the pollutants emission rate that results in the total facility's PTE. Provide all utilized methodologies and equations, assumptions, emission factors used for the emissions calculation. Information should allow for the public to follow and understand.

In both the original application submitted in February 2022 and Revision 1 of the application submitted in September 2022, Harvest provided detailed calculations for all equipment. They identified the methodologies used, input and output data, emission factors, assumptions, equations used, etc. This application contains those same calculations, with any changes as noted in the descriptions in the various subsections.



**Response to EPA request for additional information:**

- Include the methodology/equations used to calculate the emissions for each emission unit with an example calculation of how the methodology is used.

See the response above.

**Response to EPA request for additional information:**

- The Excel spreadsheets used to calculate the Facility emissions.

Two Excel workbooks are being provided with this revision of the application: one for the PTE calculations and one for the actual calculations.

## Facility Total PTE Emissions (Criteria Pollutants)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number  | Description                  | NOX,     |          | CO,      |          | VOC,     |          | SOX,     |          | TSP,     |          | PM10,    |          | PM2.5,   |          |
|--------------|------------------------------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|
|              |                              | pph      | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      |
| 1            | Solar Saturn T1200           | 4.41     | 19.30    | 2.60     | 11.40    | 9.13E-02 | 4.00E-01 | 3.69E-02 | 1.61E-01 | 7.15E-02 | 3.13E-01 | 7.15E-02 | 3.13E-01 | 7.15E-02 | 3.13E-01 |
| 3            | Scania DS11                  | 3.04     | 7.61E-01 | 6.56E-01 | 1.64E-01 | 2.48E-01 | 6.21E-02 | 2.00E-01 | 5.00E-02 | 2.14E-01 | 5.35E-02 | 2.14E-01 | 5.35E-02 | 2.14E-01 | 5.35E-02 |
| SSM          | SSM                          | -        | -        | -        | -        | -        | 11.88    | -        | -        | -        | -        | -        | -        | -        | -        |
| F1           | Leaks                        | -        | -        | -        | -        | 8.79E-01 | 3.85     | -        | -        | -        | -        | -        | -        | -        | -        |
| T1           | Condensate Tank - 400 bbl    | -        | -        | -        | -        | -        | 115.61   | -        | -        | -        | -        | -        | -        | -        | -        |
| T2           | Condensate Tank - 400 bbl    | -        | -        | -        | -        | -        | 4.97     | -        | -        | -        | -        | -        | -        | -        | -        |
| L1           | Truck Loading (Condensate)   | -        | -        | -        | -        | -        | 2.49     | -        | -        | -        | -        | -        | -        | -        | -        |
| 4            | Fuel Gas Heater              | 3.33E-02 | 1.46E-01 | 2.80E-02 | 1.23E-01 | 1.83E-03 | 8.03E-03 | 2.00E-04 | 8.76E-04 | 2.53E-03 | 1.11E-02 | 2.53E-03 | 1.11E-02 | 2.53E-03 | 1.11E-02 |
| 5            | Tank Heater                  | 1.33E-03 | 5.84E-03 | 1.12E-03 | 4.91E-03 | 7.33E-05 | 3.21E-04 | 8.00E-06 | 3.50E-05 | 1.01E-04 | 4.44E-04 | 1.01E-04 | 4.44E-04 | 1.01E-04 | 4.44E-04 |
| PL           | Pig Launcher                 | -        | -        | -        | -        | -        | 2.84E-01 | -        | -        | -        | -        | -        | -        | -        | -        |
| PR           | Pig Reciever                 | -        | -        | -        | -        | -        | 1.23     | -        | -        | -        | -        | -        | -        | -        | -        |
| T3           | Produced H2O Tank - 70 bbl   | -        | -        | -        | -        | -        | 1.10E-01 | -        | -        | -        | -        | -        | -        | -        | -        |
| L2           | Truck Loading (Produced H2O) | -        | -        | -        | -        | -        | 1.38E-03 | -        | -        | -        | -        | -        | -        | -        | -        |
| T4           | Lube Oil Tank - 500 gal      | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        |
| T5           | Used Oil Tank - 500 gal      | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        |
| T6           | Ambitrol Tank - 350 gal      | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        | -        |
| T7           | Methanol Tank - 500 gal      | -        | -        | -        | -        | -        | 2.24E-02 | -        | -        | -        | -        | -        | -        | -        | -        |
| <b>Total</b> |                              | 7.48     | 20.21    | 3.29     | 11.69    | 1.22     | 140.92   | 2.37E-01 | 2.12E-01 | 2.88E-01 | 3.78E-01 | 2.88E-01 | 3.78E-01 | 2.88E-01 | 3.78E-01 |

## Facility Total PTE Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                  | Total HAPs, |          | 1,3-Butadiene, |          | Acetaldehyde, |          | Acrolein, |          | Benzene, |          |
|-------------|------------------------------|-------------|----------|----------------|----------|---------------|----------|-----------|----------|----------|----------|
|             |                              | pph         | tpy      | pph            | tpy      | pph           | tpy      | pph       | tpy      | pph      | tpy      |
| 1           | Solar Saturn T1200           | 1.04E-01    | 4.55E-01 | 1.60E-04       | 7.00E-04 | 4.34E-02      | 1.90E-01 | 6.39E-04  | 2.80E-03 | 1.35E-03 | 5.90E-03 |
| 3           | Scania DS11                  | 2.52E-03    | 6.31E-04 |                |          | 5.29E-04      | 1.32E-04 |           |          | 6.44E-04 | 1.61E-04 |
| SSM         | SSM                          |             | 3.41E-01 |                |          |               |          |           |          |          | 2.30E-02 |
| F1          | Leaks                        | 2.53E-02    | 1.11E-01 |                |          |               |          |           |          | 1.70E-03 | 7.46E-03 |
| T1          | Condensate Tank - 400 bbl    |             | 12.53    |                |          |               |          |           |          |          | 5.13E-01 |
| T2          | Condensate Tank - 400 bbl    |             | 7.10E-01 |                |          |               |          |           |          |          | 1.81E-02 |
| L1          | Truck Loading (Condensate)   |             | 3.56E-01 |                |          |               |          |           |          |          | 9.05E-03 |
| 4           | Fuel Gas Heater              | 4.29E-03    | 1.88E-02 | 9.13E-05       | 4.00E-04 | 2.28E-04      | 1.00E-03 |           |          | 2.28E-04 | 1.00E-03 |
| 5           | Tank Heater                  | 1.14E-04    | 5.00E-04 |                |          |               |          |           |          |          |          |
| PL          | Pig Launcher                 |             | 8.16E-03 |                |          |               |          |           |          |          | 5.51E-04 |
| PR          | Pig Reciever                 |             | 3.52E-02 |                |          |               |          |           |          |          | 2.38E-03 |
| T3          | Produced H2O Tank - 70 bbl   |             | 1.88E-02 |                |          |               |          |           |          |          | 2.94E-03 |
| L2          | Truck Loading (Produced H2O) |             | 2.35E-06 |                |          |               |          |           |          |          | 3.69E-07 |
| T4          | Lube Oil Tank - 500 gal      |             |          |                |          |               |          |           |          |          |          |
| T5          | Used Oil Tank - 500 gal      |             |          |                |          |               |          |           |          |          |          |
| T6          | Ambitrol Tank - 350 gal      |             |          |                |          |               |          |           |          |          |          |
| T7          | Methanol Tank - 500 gal      |             | 2.24E-02 |                |          |               |          |           |          |          |          |
|             | Total                        | 1.36E-01    | 14.60    | 2.51E-04       | 1.10E-03 | 4.41E-02      | 1.91E-01 | 6.39E-04  | 2.80E-03 | 3.92E-03 | 5.83E-01 |

## Facility Total PTE Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                  | Biphenyl, |          | Chromium, |          | Ethylbenzene, |          | Formaldehyde, |          | n-Hexane, |          |
|-------------|------------------------------|-----------|----------|-----------|----------|---------------|----------|---------------|----------|-----------|----------|
|             |                              | pph       | tpy      | pph       | tpy      | pph           | tpy      | pph           | tpy      | pph       | tpy      |
| 1           | Solar Saturn T1200           | 8.22E-04  | 3.60E-03 | 6.85E-05  | 3.00E-04 | 2.51E-04      | 1.10E-03 | 4.24E-02      | 1.86E-01 | 3.77E-03  | 1.65E-02 |
| 3           | Scania DS11                  |           |          |           |          |               |          | 8.14E-04      | 2.04E-04 |           |          |
| SSM         | SSM                          |           |          |           |          | 5.09E-04      |          |               |          | 2.68E-01  |          |
| F1          | Leaks                        |           |          |           |          | 3.76E-05      | 1.65E-04 |               |          | 1.98E-02  | 8.69E-02 |
| T1          | Condensate Tank - 400 bbl    |           |          |           |          |               | 6.42E-03 |               |          |           | 11.66    |
| T2          | Condensate Tank - 400 bbl    |           |          |           |          |               | 2.60E-04 |               |          |           | 6.77E-01 |
| L1          | Truck Loading (Condensate)   |           |          |           |          |               | 1.32E-04 |               |          |           | 3.40E-01 |
| 4           | Fuel Gas Heater              |           |          |           |          | 6.39E-04      | 2.80E-03 | 2.51E-04      | 1.10E-03 | 4.11E-04  | 1.80E-03 |
| 5           | Tank Heater                  |           |          |           |          | 2.28E-05      | 1.00E-04 |               |          | 2.28E-05  | 1.00E-04 |
| PL          | Pig Launcher                 |           |          |           |          |               | 1.22E-05 |               |          |           | 6.42E-03 |
| PR          | Pig Reciever                 |           |          |           |          |               | 5.26E-05 |               |          |           | 2.77E-02 |
| T3          | Produced H2O Tank - 70 bbl   |           |          |           |          |               | 2.94E-04 |               |          |           | 9.24E-03 |
| L2          | Truck Loading (Produced H2O) |           |          |           |          |               | 3.69E-08 |               |          |           | 1.16E-06 |
| T4          | Lube Oil Tank - 500 gal      |           |          |           |          |               |          |               |          |           |          |
| T5          | Used Oil Tank - 500 gal      |           |          |           |          |               |          |               |          |           |          |
| T6          | Ambitrol Tank - 350 gal      |           |          |           |          |               |          |               |          |           |          |
| T7          | Methanol Tank - 500 gal      |           |          |           |          |               |          |               |          |           |          |
|             | Total                        | 8.22E-04  | 3.60E-03 | 6.85E-05  | 3.00E-04 | 9.51E-04      | 1.18E-02 | 4.34E-02      | 1.87E-01 | 2.40E-02  | 13.09    |

## Facility Total PTE Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                  | Isooctane |          | Manganese, |          | Methanol, |          | Naphthalene, |          | Nickel,  |          |
|-------------|------------------------------|-----------|----------|------------|----------|-----------|----------|--------------|----------|----------|----------|
|             |                              | pph       | tpy      | pph        | tpy      | pph       | tpy      | pph          | tpy      | pph      | tpy      |
| 1           | Solar Saturn T1200           | 4.02E-03  | 1.76E-02 | 4.57E-05   | 2.00E-04 |           |          | 2.28E-05     | 1.00E-04 | 2.28E-05 | 1.00E-04 |
| 3           | Scania DS11                  |           |          |            |          |           |          | 5.85E-05     | 1.46E-05 |          |          |
| SSM         | SSM                          |           | 6.72E-03 |            |          |           |          |              |          |          |          |
| F1          | Leaks                        | 5.67E-04  | 2.48E-03 |            |          |           |          |              |          |          |          |
| T1          | Condensate Tank - 400 bbl    |           | 0.00E+00 |            |          |           |          |              |          |          |          |
| T2          | Condensate Tank - 400 bbl    |           | 0.00E+00 |            |          |           |          |              |          |          |          |
| L1          | Truck Loading (Condensate)   |           | 0.00E+00 |            |          |           |          |              |          |          |          |
| 4           | Fuel Gas Heater              | 8.45E-04  | 3.70E-03 |            |          | 2.97E-04  | 1.30E-03 |              |          |          |          |
| 5           | Tank Heater                  | 2.28E-05  | 1.00E-04 |            |          |           |          |              |          |          |          |
| PL          | Pig Launcher                 |           | 1.61E-04 |            |          |           |          |              |          |          |          |
| PR          | Pig Reciever                 |           | 6.95E-04 |            |          |           |          |              |          |          |          |
| T3          | Produced H2O Tank - 70 bbl   |           |          |            |          |           |          |              |          |          |          |
| L2          | Truck Loading (Produced H2O) |           |          |            |          |           |          |              |          |          |          |
| T4          | Lube Oil Tank - 500 gal      |           |          |            |          |           |          |              |          |          |          |
| T5          | Used Oil Tank - 500 gal      |           |          |            |          |           |          |              |          |          |          |
| T6          | Ambitrol Tank - 350 gal      |           |          |            |          |           |          |              |          |          |          |
| T7          | Methanol Tank - 500 gal      |           |          |            |          | 2.24E-02  |          |              |          |          |          |
|             | Total                        | 5.45E-03  | 3.15E-02 | 4.57E-05   | 2.00E-04 | 2.97E-04  | 2.37E-02 | 8.13E-05     | 1.15E-04 | 2.28E-05 | 1.00E-04 |

## Facility Total PTE Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                  | Phenol,  |          | Phosphorous, |          | Propionaldehyde, |          | Propylene Oxide, |          | Styrene, |          |
|-------------|------------------------------|----------|----------|--------------|----------|------------------|----------|------------------|----------|----------|----------|
|             |                              | pph      | tpy      | pph          | tpy      | pph              | tpy      | pph              | tpy      | pph      | tpy      |
| 1           | Solar Saturn T1200           | 2.74E-04 | 1.20E-03 | 1.60E-04     | 7.00E-04 | 2.17E-03         | 9.50E-03 | 3.20E-04         | 1.40E-03 |          |          |
| 3           | Scania DS11                  |          |          |              |          |                  |          |                  |          |          |          |
| SSM         | SSM                          |          |          |              |          |                  |          |                  |          |          |          |
| F1          | Leaks                        |          |          |              |          |                  |          |                  |          |          |          |
| T1          | Condensate Tank - 400 bbl    |          |          |              |          |                  |          |                  |          |          |          |
| T2          | Condensate Tank - 400 bbl    |          |          |              |          |                  |          |                  |          |          |          |
| L1          | Truck Loading (Condensate)   |          |          |              |          |                  |          |                  |          |          |          |
| 4           | Fuel Gas Heater              |          |          |              |          |                  |          |                  |          | 6.16E-04 | 2.70E-03 |
| 5           | Tank Heater                  |          |          |              |          |                  |          |                  |          | 2.28E-05 | 1.00E-04 |
| PL          | Pig Launcher                 |          |          |              |          |                  |          |                  |          |          |          |
| PR          | Pig Reciever                 |          |          |              |          |                  |          |                  |          |          |          |
| T3          | Produced H2O Tank - 70 bbl   |          |          |              |          |                  |          |                  |          |          |          |
| L2          | Truck Loading (Produced H2O) |          |          |              |          |                  |          |                  |          |          |          |
| T4          | Lube Oil Tank - 500 gal      |          |          |              |          |                  |          |                  |          |          |          |
| T5          | Used Oil Tank - 500 gal      |          |          |              |          |                  |          |                  |          |          |          |
| T6          | Ambitrol Tank - 350 gal      |          |          |              |          |                  |          |                  |          |          |          |
| T7          | Methanol Tank - 500 gal      |          |          |              |          |                  |          |                  |          |          |          |
|             | Total                        | 2.74E-04 | 1.20E-03 | 1.60E-04     | 7.00E-04 | 2.17E-03         | 9.50E-03 | 3.20E-04         | 1.40E-03 | 6.39E-04 | 2.80E-03 |

## Facility Total PTE Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                  | Toluene, |          | Xylenes, |          |
|-------------|------------------------------|----------|----------|----------|----------|
|             |                              | pph      | tpy      | pph      | tpy      |
| 1           | Solar Saturn T1200           | 1.03E-03 | 4.50E-03 | 3.11E-03 | 1.36E-02 |
| 3           | Scania DS11                  | 2.82E-04 | 7.06E-05 | 1.97E-04 | 4.92E-05 |
| SSM         | SSM                          |          | 3.64E-02 |          | 6.11E-03 |
| F1          | Leaks                        | 2.69E-03 | 1.18E-02 | 4.51E-04 | 1.98E-03 |
| T1          | Condensate Tank - 400 bbl    |          | 3.16E-01 |          | 3.22E-02 |
| T2          | Condensate Tank - 400 bbl    |          | 1.31E-02 |          | 1.50E-03 |
| L1          | Truck Loading (Condensate)   |          | 6.54E-03 |          | 7.50E-04 |
| 4           | Fuel Gas Heater              | 2.97E-04 | 1.30E-03 | 3.88E-04 | 1.70E-03 |
| 5           | Tank Heater                  |          |          | 2.28E-05 | 1.00E-04 |
| PL          | Pig Launcher                 |          | 8.72E-04 |          | 1.46E-04 |
| PR          | Pig Reciever                 |          | 3.76E-03 |          | 6.31E-04 |
| T3          | Produced H2O Tank - 70 bbl   |          | 3.78E-03 |          | 2.52E-03 |
| L2          | Truck Loading (Produced H2O) |          | 4.74E-07 |          | 3.16E-07 |
| T4          | Lube Oil Tank - 500 gal      |          |          |          |          |
| T5          | Used Oil Tank - 500 gal      |          |          |          |          |
| T6          | Ambitrol Tank - 350 gal      |          |          |          |          |
| T7          | Methanol Tank - 500 gal      |          |          |          |          |
|             | Total                        | 4.30E-03 | 3.98E-01 | 4.16E-03 | 6.13E-02 |

## Facility Total Actual Emissions (Criteria Pollutants)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit<br>Number | Description                | NOX, |          | CO,      |          | VOC,     |          | SOX,     |          | TSP,     |          | PM10,    |          | PM2.5,   |          |
|----------------|----------------------------|------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|----------|
|                |                            | pph  | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      | pph      | tpy      |
| 1              | Solar Saturn T1200         | 4.41 | 19.30    | 2.60     | 11.40    | 9.13E-02 | 4.00E-01 | 3.69E-02 | 1.61E-01 | 7.15E-02 | 3.13E-01 | 7.15E-02 | 3.13E-01 | 7.15E-02 | 3.13E-01 |
| 3              | Scania DS11                | 3.04 | 1.85E-01 | 6.56E-01 | 3.99E-02 | 2.48E-01 | 1.51E-02 | 2.00E-01 | 1.22E-02 | 2.14E-01 | 1.30E-02 | 2.14E-01 | 1.30E-02 | 2.14E-01 | 1.30E-02 |
| SSM            | SSM                        | -    | -        | -        | -        | -        | 0.00     | -        | -        | -        | -        | -        | -        | -        | -        |
| F1             | Equipment Leaks            | -    | -        | -        | -        | 8.79E-01 | 3.85     | -        | -        | -        | -        | -        | -        | -        | -        |
| T1             | Condensate Tank - 400 bbl  | -    | -        | -        | -        | -        | 7.12     | -        | -        | -        | -        | -        | -        | -        | -        |
| T2             | Condensate Tank - 400 bbl  | -    | -        | -        | -        | -        | 1.63     | -        | -        | -        | -        | -        | -        | -        | -        |
| L1             | Truck Loading (Condensate) | -    | -        | -        | -        | -        | 0.26     | -        | -        | -        | -        | -        | -        | -        | -        |
|                | <b>Total</b>               | 7.45 | 19.49    | 3.26     | 11.44    | 1.22     | 13.28    | 2.37E-01 | 1.74E-01 | 2.85E-01 | 3.26E-01 | 2.85E-01 | 3.26E-01 | 2.85E-01 | 3.26E-01 |



## Facility Total Actual Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                | Total HAPs, |          | 1,3-Butadiene, |          | Acetaldehyde, |          | Acrolein, |          | Benzene, |          |
|-------------|----------------------------|-------------|----------|----------------|----------|---------------|----------|-----------|----------|----------|----------|
|             |                            | pph         | tpy      | pph            | tpy      | pph           | tpy      | pph       | tpy      | pph      | tpy      |
| 1           | Solar Saturn T1200         | 1.04E-01    | 4.55E-01 | 1.60E-04       | 7.00E-04 | 4.34E-02      | 1.90E-01 | 6.39E-04  | 2.80E-03 | 1.35E-03 | 5.90E-03 |
| 3           | Scania DS11                | 2.52E-03    | 1.54E-04 |                |          | 5.29E-04      | 3.22E-05 |           |          | 6.44E-04 | 3.92E-05 |
| SSM         | SSM                        |             | 0.00E+00 |                |          |               |          |           |          |          | 0.00E+00 |
| F1          | Leaks                      | 2.53E-02    | 1.11E-01 |                |          |               |          |           |          | 1.70E-03 | 7.46E-03 |
| T1          | Condensate Tank - 400 bbl  |             | 6.44E-01 |                |          |               |          |           |          |          | 4.79E-02 |
| T2          | Condensate Tank - 400 bbl  |             | 1.55E-01 |                |          |               |          |           |          |          | 9.04E-03 |
| L1          | Truck Loading (Condensate) |             | 2.50E-02 |                |          |               |          |           |          |          | 1.46E-03 |
|             | Total                      | 1.32E-01    | 1.39     | 1.60E-04       | 7.00E-04 | 4.39E-02      | 1.90E-01 | 6.39E-04  | 2.80E-03 | 3.69E-03 | 7.17E-02 |

## Facility Total Actual Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                | Biphenyl, |          | Chromium, |          | Ethylbenzene, |          | Formaldehyde, |          | n-Hexane, |          |
|-------------|----------------------------|-----------|----------|-----------|----------|---------------|----------|---------------|----------|-----------|----------|
|             |                            | pph       | tpy      | pph       | tpy      | pph           | tpy      | pph           | tpy      | pph       | tpy      |
| 1           | Solar Saturn T1200         | 8.22E-04  | 3.60E-03 | 6.85E-05  | 3.00E-04 | 2.51E-04      | 1.10E-03 | 4.24E-02      | 1.86E-01 | 3.77E-03  | 1.65E-02 |
| 3           | Scania DS11                |           |          |           |          |               |          | 8.14E-04      | 4.96E-05 |           |          |
| SSM         | SSM                        |           |          |           |          | 0.00E+00      |          |               |          | 0.00E+00  |          |
| F1          | Leaks                      |           |          |           |          | 3.76E-05      | 1.65E-04 |               |          | 1.98E-02  | 8.69E-02 |
| T1          | Condensate Tank - 400 bbl  |           |          |           |          |               | 2.41E-03 |               |          |           | 5.70E-01 |
| T2          | Condensate Tank - 400 bbl  |           |          |           |          |               | 4.95E-04 |               |          |           | 1.41E-01 |
| L1          | Truck Loading (Condensate) |           |          |           |          |               | 7.96E-05 |               |          |           | 2.27E-02 |
|             | Total                      | 8.22E-04  | 3.60E-03 | 6.85E-05  | 3.00E-04 | 2.89E-04      | 4.24E-03 | 4.32E-02      | 1.86E-01 | 2.36E-02  | 8.37E-01 |

## Facility Total Actual Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                | Isooctane |          | Manganese, |          | Naphthalene, |          | Nickel,  |          | Phenol,  |          |
|-------------|----------------------------|-----------|----------|------------|----------|--------------|----------|----------|----------|----------|----------|
|             |                            | pph       | tpy      | pph        | tpy      | pph          | tpy      | pph      | tpy      | pph      | tpy      |
| 1           | Solar Saturn T1200         | 4.02E-03  | 1.76E-02 | 4.57E-05   | 2.00E-04 | 2.28E-05     | 1.00E-04 | 2.28E-05 | 1.00E-04 | 2.74E-04 | 1.20E-03 |
| 3           | Scania DS11                |           |          |            |          | 5.85E-05     | 3.56E-06 |          |          |          |          |
| SSM         | SSM                        |           | 0.00E+00 |            |          |              |          |          |          |          |          |
| F1          | Leaks                      | 5.67E-04  | 2.48E-03 |            |          |              |          |          |          |          |          |
| T1          | Condensate Tank - 400 bbl  |           | 6.84E-03 |            |          |              |          |          |          |          |          |
| T2          | Condensate Tank - 400 bbl  |           | 1.77E-03 |            |          |              |          |          |          |          |          |
| L1          | Truck Loading (Condensate) |           | 2.85E-04 |            |          |              |          |          |          |          |          |
|             | Total                      | 4.59E-03  | 2.90E-02 | 4.57E-05   | 2.00E-04 | 8.13E-05     | 1.04E-04 | 2.28E-05 | 1.00E-04 | 2.74E-04 | 1.20E-03 |

## Facility Total Actual Emissions (HAPs)

Company: Harvest Four Corners, LLC

Facility: Los Mestenos Compressor Station

Date / Rev: November 2022 / Rev 2

| Unit Number | Description                | Phosphorous, |          | Propionaldehyde, |          | Propylene Oxide, |          | Toluene, |          | Xylenes, |          |
|-------------|----------------------------|--------------|----------|------------------|----------|------------------|----------|----------|----------|----------|----------|
|             |                            | pph          | tpy      | pph              | tpy      | pph              | tpy      | pph      | tpy      | pph      | tpy      |
| 1           | Solar Saturn T1200         | 1.60E-04     | 7.00E-04 | 2.17E-03         | 9.50E-03 | 3.20E-04         | 1.40E-03 | 1.03E-03 | 4.50E-03 | 3.11E-03 | 1.36E-02 |
| 3           | Scania DS11                |              |          |                  |          |                  |          | 2.82E-04 | 1.72E-05 | 1.97E-04 | 1.20E-05 |
| SSM         | SSM                        |              |          |                  |          |                  |          |          | 0.00E+00 |          | 0.00E+00 |
| F1          | Leaks                      |              |          |                  |          |                  |          | 2.69E-03 | 1.18E-02 | 4.51E-04 | 1.98E-03 |
| T1          | Condensate Tank - 400 bbl  |              |          |                  |          |                  |          |          | 5.66E-03 |          | 1.13E-02 |
| T2          | Condensate Tank - 400 bbl  |              |          |                  |          |                  |          |          | 1.19E-03 |          | 1.98E-03 |
| L1          | Truck Loading (Condensate) |              |          |                  |          |                  |          |          | 1.91E-04 |          | 3.19E-04 |
|             | Total                      | 1.60E-04     | 7.00E-04 | 2.17E-03         | 9.50E-03 | 3.20E-04         | 1.40E-03 | 4.00E-03 | 2.34E-02 | 3.75E-03 | 2.92E-02 |

# **Section 5.1**

## **Turbine (Unit 1)**

### **Written Description**

### ***Turbine (Unit 1)***

The nitrogen oxide (NO<sub>x</sub>), carbon monoxide (CO), and volatile organic compound (VOC) emissions from the Solar Saturn T1200 turbine (Unit 1) were taken from previous applications and permits. Sulfur dioxide (SO<sub>2</sub>) and particulate emissions were calculated using the AP-42 emission factors from Table 3.1-2a. Hazardous air pollutant (HAP) emissions were calculated using GRI-HAPCalc 3.0. Potential to Emit (PTE) and 2021 actual emissions were calculated assuming the turbine operates at full site capacity for 8,760 hours per year (hr/yr). There were no shutdowns during 2021.

In this application, there are no changes to the calculations as they were presented in the either of the previous applications.

# **Section 5.1**

## **Turbine (Unit 1)**

### **PTE Emission Calculations**

## Turbine Exhaust PTE Emissions Calculations

Unit Number: **1**

Description: Solar Saturn T1200

### Horsepower Calculations

**6,715** ft above MSL**1,200** hp**1,136** hp

Elevation

Nameplate hp

Site-rated hp

Mfg. data

Mfg. data

### Fuel Consumption

10.84 MMBtu/hr

12,044 scf/hr

**8,760** hr/yr

94,958 MMBtu/yr

105.51 MMscf/yr

**900** Btu/scf

Hourly fuel consumption

Hourly fuel consumption

Annual operating time

Annual fuel consumption

Annual fuel consumption

Field gas heating value

Btu/hp-hr x NMAQB site-rated hp / 1,000,000

MMBtu/hr x 1,000,000 / Btu/scf

Harvest Four Corners, LLC

MMBtu/hr x hr/yr

scf/hr x hr/yr / 1,000,000

Nominal heat content

### Steady-State Emission Rates

| Pollutants | Uncontrolled Emission Rates, |              |
|------------|------------------------------|--------------|
|            | pph                          | tpy          |
| NOX        | <b>4.41</b>                  | <b>19.30</b> |
| CO         | <b>2.60</b>                  | <b>11.40</b> |
| VOC        | 9.13E-02                     | 4.00E-01     |

Emissions brought forward from Part 71 TV permit R6NM-04-10-M1

| Pollutants | Emission Factors,<br>lb/MMBtu | Uncontrolled Emission Rates, |          |
|------------|-------------------------------|------------------------------|----------|
|            |                               | pph                          | tpy      |
| SO2        | <b>3.40E-03</b>               | 3.69E-02                     | 1.61E-01 |
| TSP        | <b>6.60E-03</b>               | 7.15E-02                     | 3.13E-01 |
| PM10       | <b>6.60E-03</b>               | 7.15E-02                     | 3.13E-01 |
| PM2.5      | <b>6.60E-03</b>               | 7.15E-02                     | 3.13E-01 |

Emission factors taken from AP-42, Table 3.1-2a

Uncontrolled Emission Rates (pph) = lb/MMBtu x MMBtu/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton



**GRI-HAPCalc® 3.0**  
**Turbine Report**

Facility ID: LOS MESTENIOS  
Operation Type: COMPRESSOR STATION  
Facility Name: LOS MESTENIOS COMPRESSOR  
User Name: Harvest Four Corners, LLC  
Units of Measure: U.S. STANDARD

Notes:

Note: Emissions less than 5.00E-09 tons (or tonnes) per year are considered insignificant and are treated as zero.  
These emissions are indicated on the report with a "0".  
Emissions between 5.00E-09 and 5.00E-05 tons (or tonnes) per year are represented on the report with "0.0000".

**Turbine Unit**

Unit Name: T1200

Hours of Operation: 8,760 Yearly  
Rate Power: 1136 hp  
Fuel Type: NATURAL GAS  
Emission Factor Set: FIELD > EPA > LITERATURE  
Additional EF Set: -NONE-

**Calculated Emissions (ton/yr)**

| <u>Chemical Name</u>   | <u>Emissions</u> | <u>Emission Factor</u> | <u>Emission Factor Set</u> |
|------------------------|------------------|------------------------|----------------------------|
| <b>HAPs</b>            |                  |                        |                            |
| Formaldehyde           | 0.1856           | 0.01693680 g/bhp-hr    | GRI Field                  |
| Acetaldehyde           | 0.1900           | 0.01733570 g/bhp-hr    | GRI Field                  |
| 1,3-Butadiene          | 0.0007           | 0.00006160 g/bhp-hr    | GRI Field                  |
| Acrolein               | 0.0028           | 0.00026000 g/bhp-hr    | GRI Field                  |
| Propional              | 0.0095           | 0.00086500 g/bhp-hr    | GRI Field                  |
| Propylene Oxide        | 0.0014           | 0.00012480 g/bhp-hr    | EPA                        |
| n-Nitrosodimethylamine | 0.0000           | 0.00000100 g/bhp-hr    | EPA                        |
| Benzene                | 0.0059           | 0.00053840 g/bhp-hr    | GRI Field                  |
| Toluene                | 0.0045           | 0.00041100 g/bhp-hr    | GRI Field                  |
| Ethylbenzene           | 0.0011           | 0.00010330 g/bhp-hr    | EPA                        |
| Xylenes(m,p,o)         | 0.0136           | 0.00124410 g/bhp-hr    | GRI Field                  |
| 2,2,4-Trimethylpentane | 0.0176           | 0.00160530 g/bhp-hr    | GRI Field                  |
| n-Hexane               | 0.0165           | 0.00150580 g/bhp-hr    | GRI Field                  |
| Phenol                 | 0.0012           | 0.00011010 g/bhp-hr    | GRI Field                  |
| n-Nitrosomorpholine    | 0.0000           | 0.00000100 g/bhp-hr    | EPA                        |
| Naphthalene            | 0.0001           | 0.00000760 g/bhp-hr    | GRI Field                  |
| 2-Methylnaphthalene    | 0.0000           | 0.00000130 g/bhp-hr    | GRI Field                  |
| Biphenyl               | 0.0036           | 0.00033050 g/bhp-hr    | GRI Field                  |
| Phenanthrene           | 0.0000           | 0.00000050 g/bhp-hr    | GRI Field                  |
| Chrysene               | 0.0000           | 0.00000100 g/bhp-hr    | GRI Field                  |
| Beryllium              | 0.0000           | 0.00000010 g/bhp-hr    | GRI Field                  |
| Phosphorous            | 0.0007           | 0.00006520 g/bhp-hr    | GRI Field                  |
| Chromium               | 0.0001           | 0.00000820 g/bhp-hr    | GRI Field                  |
| Chromium               | 0.0001           | 0.00000560 g/bhp-hr    | EPA                        |
| Manganese              | 0.0002           | 0.00001750 g/bhp-hr    | GRI Field                  |
| Nickel                 | 0.0001           | 0.00000610 g/bhp-hr    | GRI Field                  |
| Cobalt                 | 0.0000           | 0.00000160 g/bhp-hr    | GRI Field                  |

|          |        |                     |           |
|----------|--------|---------------------|-----------|
| Arsenic  | 0.0000 | 0.00000060 g/bhp-hr | GRI Field |
| Selenium | 0.0000 | 0.00000030 g/bhp-hr | GRI Field |
| Cadmium  | 0.0000 | 0.00000020 g/bhp-hr | GRI Field |
| Mercury  | 0.0000 | 0.00000270 g/bhp-hr | GRI Field |
| Lead     | 0.0000 | 0.00000340 g/bhp-hr | GRI Field |

|              |       |        |  |
|--------------|-------|--------|--|
| <b>Total</b> | <hr/> | 0.4553 |  |
|--------------|-------|--------|--|

### Criteria Pollutants

|       |         |                     |           |
|-------|---------|---------------------|-----------|
| PM    | 0.3490  | 0.03184680 g/bhp-hr | EPA       |
| CO    | 23.1061 | 2.10828420 g/bhp-hr | GRI Field |
| NMHC  | 2.1248  | 0.19387800 g/bhp-hr | GRI Field |
| NMEHC | 0.1321  | 0.01205010 g/bhp-hr | EPA       |
| NOx   | 13.7233 | 1.25216290 g/bhp-hr | GRI Field |
| SO2   | 0.0113  | 0.00102720 g/bhp-hr | GRI Field |

### Other Pollutants

|                           |            |                       |           |
|---------------------------|------------|-----------------------|-----------|
| Methane                   | 10.8193    | 0.98719230 g/bhp-hr   | GRI Field |
| Acetylene                 | 0.0785     | 0.00716540 g/bhp-hr   | GRI Field |
| Ethylene                  | 0.1529     | 0.01395450 g/bhp-hr   | GRI Field |
| Ethane                    | 1.6449     | 0.15008370 g/bhp-hr   | GRI Field |
| Propane                   | 0.1754     | 0.01600000 g/bhp-hr   | GRI Field |
| Isobutane                 | 0.0526     | 0.00480000 g/bhp-hr   | GRI Field |
| Butane                    | 0.0570     | 0.00520000 g/bhp-hr   | GRI Field |
| Trimethylamine            | 0.0000     | 0.00000070 g/bhp-hr   | EPA       |
| Cyclopentane              | 0.0181     | 0.00165110 g/bhp-hr   | GRI Field |
| Butyrald/Isobutyraldehyde | 0.0147     | 0.00134000 g/bhp-hr   | GRI Field |
| n-Pentane                 | 0.8894     | 0.08115000 g/bhp-hr   | GRI Field |
| Cyclohexane               | 0.0671     | 0.00612400 g/bhp-hr   | GRI Field |
| Methylcyclohexane         | 0.0968     | 0.00883120 g/bhp-hr   | GRI Field |
| n-Octane                  | 0.0349     | 0.00318890 g/bhp-hr   | GRI Field |
| 1,3,5-Trimethylbenzene    | 0.0329     | 0.00300000 g/bhp-hr   | GRI Field |
| n-Nonane                  | 0.0058     | 0.00053260 g/bhp-hr   | GRI Field |
| CO2                       | 5,188.2765 | 473.39811550 g/bhp-hr | EPA       |
| Vanadium                  | 0.0000     | 0.00000070 g/bhp-hr   | GRI Field |
| Copper                    | 0.0002     | 0.00002050 g/bhp-hr   | GRI Field |
| Molybdenum                | 0.0002     | 0.00002030 g/bhp-hr   | GRI Field |
| Barium                    | 0.0003     | 0.00002290 g/bhp-hr   | GRI Field |

Table 3.1-2a. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASES FROM STATIONARY GAS TURBINES

| Emission Factors <sup>a</sup> - Uncontrolled |   |                           |  |                           |
|--|---|---------------------------|--|---------------------------|
| Pollutant                                    | Natural Gas-Fired Turbines <sup>b</sup> |                           | Distillate Oil-Fired Turbines <sup>d</sup> |                           |
|  | (lb/MMBtu) <sup>c</sup><br>(Fuel Input) | Emission Factor<br>Rating | (lb/MMBtu) <sup>c</sup><br>(Fuel Input)    | Emission Factor<br>Rating |
| CO <sub>2</sub> <sup>f</sup>                 | 110                                     | A                         | 157  | A                         |
| N <sub>2</sub> O                             | 0.003 <sup>g</sup>                      | E                         | ND   | NA                        |
| Lead   | ND                                      | NA                        | 1.4 E-05                                   | C                         |
| SO <sub>2</sub>                              | 0.94S <sup>h</sup>                      | B                         | 1.01S <sup>h</sup>                         | B                         |
| Methane                                      | 8.6 E-03                                | C                         | ND   | NA                        |
| VOC  | 2.1 E-03                                | D                         | 4.1 E-04 <sup>j</sup>                      | E                         |
| TOC <sup>k</sup>                             | 1.1 E-02                                | B                         | 4.0 E-03 <sup>l</sup>                      | C                         |
| PM (condensable)                             | 4.7 E-03 <sup>l</sup>                   | C                         | 7.2 E-03 <sup>l</sup>                      | C                         |
| PM (filterable)                              | 1.9 E-03 <sup>l</sup>                   | C                         | 4.3 E-03 <sup>l</sup>                      | C                         |
| PM (total)                                   | 6.6 E-03 <sup>l</sup>                   | C                         | 1.2 E-02 <sup>l</sup>                      | C                         |

<sup>a</sup> Factors are derived from units operating at high loads ( $\geq 80$  percent load) only. For information on units operating at other loads, consult the background report for this chapter (Reference 16), available at “www.epa.gov/ttn/chief”. ND = No Data, NA = Not Applicable.

<sup>b</sup> SCCs for natural gas-fired turbines include 2-01-002-01, 2-02-002-01 & 03, and 2-03-002-02 & 03.

<sup>c</sup> Emission factors based on an average natural gas heating value (HHV) of 1020 Btu/scf at 60°F. To convert from (lb/MMBtu) to (lb/10<sup>6</sup> scf), multiply by 1020. Similarly, these emission factors can be converted to other natural gas heating values.

<sup>d</sup> SCCs for distillate oil-fired turbines are 2-01-001-01, 2-02-001-01, 2-02-001-03, and 2-03-001-02.

<sup>e</sup> Emission factors based on an average distillate oil heating value of 139 MMBtu/10<sup>3</sup> gallons. To convert from (lb/MMBtu) to (lb/10<sup>3</sup> gallons), multiply by 139.

<sup>f</sup> Based on 99.5% conversion of fuel carbon to CO<sub>2</sub> for natural gas and 99% conversion of fuel carbon to CO<sub>2</sub> for distillate oil. CO<sub>2</sub> (Natural Gas) [lb/MMBtu] = (0.0036 scf/Btu)(%CON)(C)(D), where %CON = weight percent conversion of fuel carbon to CO<sub>2</sub>, C = carbon content of fuel by weight, and D = density of fuel. For natural gas, C is assumed at 75%, and D is assumed at 4.1 E+04 lb/10<sup>6</sup>scf. For distillate oil, CO<sub>2</sub> (Distillate Oil) [lb/MMBtu] = (26.4 gal/MMBtu) (%CON)(C)(D), where C is assumed at 87%, and the D is assumed at 6.9 lb/gallon.

<sup>g</sup> Emission factor is carried over from the previous revision to AP-42 (Supplement B, October 1996) and is based on limited source tests on a single turbine with water-steam injection (Reference 5).

<sup>h</sup> All sulfur in the fuel is assumed to be converted to SO<sub>2</sub>. S = percent sulfur in fuel. Example, if sulfur content in the fuel is 3.4 percent, then S = 3.4. If S is not available, use 3.4 E-03 lb/MMBtu for natural gas turbines, and 3.3 E-02 lb/MMBtu for distillate oil turbines (the equations are more accurate).

<sup>j</sup> VOC emissions are assumed equal to the sum of organic emissions.

<sup>k</sup> Pollutant referenced as THC in the gathered emission tests. It is assumed as TOC, because it is based on EPA Test Method 25A.

<sup>l</sup> Emission factors are based on combustion turbines using water-steam injection.

# **Section 5.1**

## **Turbine (Unit 1)**

### **Actual Emission Calculations**

## Turbine Exhaust Actual Emissions Calculations

Unit Number: **1**

Description: Solar Saturn T1200

### Horsepower Calculations

**6,715** ft above MSL**1,200** hp**1,136** hp

Elevation

Nameplate hp

Site-rated hp

Mfg. data

Mfg. data

### Fuel Consumption

10.84 MMBtu/hr

12,044 scf/hr

**8,760** hr/yr

94,958 MMBtu/yr

105.51 MMscf/yr

**900** Btu/scf

Hourly fuel consumption

Hourly fuel consumption

Annual operating time

Annual fuel consumption

Annual fuel consumption

Field gas heating value

Btu/hp-hr x NMAQB site-rated hp / 1,000,000

MMBtu/hr x 1,000,000 / Btu/scf

Harvest Four Corners, LLC

MMBtu/hr x hr/yr

scf/hr x hr/yr / 1,000,000

Nominal heat content

### Steady-State Emission Rates

| Pollutants | Uncontrolled Emission Rates, |              |
|------------|------------------------------|--------------|
|            | pph                          | tpy          |
| NOX        | <b>4.41</b>                  | <b>19.30</b> |
| CO         | <b>2.60</b>                  | <b>11.40</b> |
| VOC        | 9.13E-02                     | 4.00E-01     |

Emissions brought forward from Part 71 TV permit R6NM-04-10-M1

| Pollutants | Emission Factors,<br>lb/MMBtu | Uncontrolled Emission Rates, |          |
|------------|-------------------------------|------------------------------|----------|
|            |                               | pph                          | tpy      |
| SO2        | <b>3.40E-03</b>               | 3.69E-02                     | 1.61E-01 |
| TSP        | <b>6.60E-03</b>               | 7.15E-02                     | 3.13E-01 |
| PM10       | <b>6.60E-03</b>               | 7.15E-02                     | 3.13E-01 |
| PM2.5      | <b>6.60E-03</b>               | 7.15E-02                     | 3.13E-01 |

Emission factors taken from AP-42, Table 3.1-2a

Uncontrolled Emission Rates (pph) = lb/MMBtu x MMBtu/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

**Section 5.2**  
**Generator (Unit 3)**  
**Written Description**

### ***Generator (Unit 2)***

Emissions from the Waukesha Scania DS11 emergency generator engine were calculated using AP-42 emission factors from Tables 3.3-1 & 3.3-2. PTE emissions were calculated assuming the engine operates at full site capacity for 500 hr/yr. During 2021, the generator was in operation for a total of 121.8 hours. Actual 2021 emissions were calculated assuming the engine operates at full site capacity during that time.

In this application, there are no changes to the calculations as they were presented in the either of the previous applications.

## **Section 5.2**

### **Generator (Unit 2)**

#### **PTE Emission Calculations**



## Engine Exhaust PTE Emissions Calculations

Unit Number: **3**  
 Description: Scania DS11 Diesel Generator (Emergency)

### Horsepower

**250** hp

Nameplate hp

Mfg. data

The data sheet shows the DS11 has a horsepower rating of 250+. Since the associated alternator is rated at 130 kW, the assumption of a site rating at 250 hp should be conservative.

### Fuel Consumption

**0.69** MMBtu/hr  
**138,000** Btu/gal  
 5.00 gal/hr  
**500** hr/yr  
 2,500 gal/yr  
 345 MMBtu/yr

Hourly fuel consumption  
 Field gas heating value  
 Hourly fuel consumption  
 Annual operating time  
 Hourly fuel consumption  
 Annual fuel consumption

Mfg. data  
 Nominal heat content  
 MMBtu/hr x 1,000,000 / Btu/gal  
 Harvest Four Corners, LLC  
 gal/hr x hr/yr  
 MMBtu/hr x hr/yr

### Steady-State Emission Rates

| Pollutants        | Emission Factors, lb/MMBtu | Uncontrolled Emission Rates, |          |
|-------------------|----------------------------|------------------------------|----------|
|                   |                            | pph                          | tpy      |
| NO <sub>2</sub>   | <b>4.41</b>                | 3.04                         | 7.61E-01 |
| CO                | <b>9.50E-01</b>            | 6.56E-01                     | 1.64E-01 |
| VOC               | <b>3.60E-01</b>            | 2.48E-01                     | 6.21E-02 |
| SO <sub>2</sub>   | <b>2.90E-01</b>            | 2.00E-01                     | 5.00E-02 |
| TSP               | <b>3.10E-01</b>            | 2.14E-01                     | 5.35E-02 |
| PM <sub>10</sub>  | <b>3.10E-01</b>            | 2.14E-01                     | 5.35E-02 |
| PM <sub>2.5</sub> | <b>3.10E-01</b>            | 2.14E-01                     | 5.35E-02 |
| Acetaldehyde      | <b>7.67E-04</b>            | 5.29E-04                     | 1.32E-04 |
| Benzene           | <b>9.33E-04</b>            | 6.44E-04                     | 1.61E-04 |
| Formaldehyde      | <b>1.18E-03</b>            | 8.14E-04                     | 2.04E-04 |
| Naphthalene       | <b>8.48E-05</b>            | 5.85E-05                     | 1.46E-05 |
| Toluene           | <b>4.09E-04</b>            | 2.82E-04                     | 7.06E-05 |
| Xylene            | <b>2.85E-04</b>            | 1.97E-04                     | 4.92E-05 |

Emission factors taken from AP-42, Tables 3.3-1 & 3.3-2

Uncontrolled Emission Rates (pph) = lb/MMBtu x MMBtu/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Table 3.3-1. EMISSION FACTORS FOR UNCONTROLLED GASOLINE AND DIESEL INDUSTRIAL ENGINES<sup>a</sup>

| Pollutant                    | Gasoline Fuel<br>(SCC 2-02-003-01, 2-03-003-01) |   | Diesel Fuel<br>(SCC 2-02-001-02, 2-03-001-01)   |   | EMISSION<br>FACTOR<br>RATING |
|------------------------------|---|---|---|---|------------------------------|
|                              | Emission Factor<br>(lb/hp-hr)<br>(power output) | Emission Factor<br>(lb/MMBtu)<br>(fuel input) | Emission Factor<br>(lb/hp-hr)<br>(power output) | Emission Factor<br>(lb/MMBtu)<br>(fuel input) |                              |
| NO <sub>x</sub>              | 0.011   | 1.63  | 0.031   | 4.41  | D                            |
| CO                           | 6.96 E-03 <sup>d</sup>                          | 0.99 <sup>d</sup>                             | 6.68 E-03                                       | 0.95  | D                            |
| SO <sub>x</sub>              | 5.91 E-04                                       | 0.084   | 2.05 E-03                                       | 0.29  | D                            |
| PM-10 <sup>b</sup>           | 7.21 E-04                                       | 0.10  | 2.20 E-03                                       | 0.31  | D                            |
| CO <sub>2</sub> <sup>c</sup> | 1.08  | 154   | 1.15  | 164   | B                            |
| Aldehydes                    | 4.85 E-04                                       | 0.07  | 4.63 E-04                                       | 0.07  | D                            |
| TOC                          |   |   |   |   |                              |
| Exhaust                      | 0.015   | 2.10  | 2.47 E-03                                       | 0.35  | D                            |
| Evaporative                  | 6.61 E-04                                       | 0.09  | 0.00  | 0.00  | E                            |
| Crankcase                    | 4.85 E-03                                       | 0.69  | 4.41 E-05                                       | 0.01  | E                            |
| Refueling                    | 1.08 E-03                                       | 0.15  | 0.00  | 0.00  | E                            |

<sup>a</sup> References 2,5-6,9-14. When necessary, an average brake-specific fuel consumption (BSFC) of 7,000 Btu/hp-hr was used to convert from lb/MMBtu to lb/hp-hr. To convert from lb/hp-hr to kg/kw-hr, multiply by 0.608. To convert from lb/MMBtu to ng/J, multiply by 430. SCC = Source Classification Code. TOC = total organic compounds.


<sup>b</sup> PM-10 = particulate matter less than or equal to 10 µm aerodynamic diameter. All particulate is assumed to be ≤ 1 µm in size.

<sup>c</sup> Assumes 99% conversion of carbon in fuel to CO<sub>2</sub> with 87 weight % carbon in diesel, 86 weight % carbon in gasoline, average BSFC of 7,000 Btu/hp-hr, diesel heating value of 19,300 Btu/lb, and gasoline heating value of 20,300 Btu/lb.

<sup>d</sup> Instead of 0.439 lb/hp-hr (power output) and 62.7 lb/mmBtu (fuel input), the correct emissions factors values are 6.96 E-03 lb/hp-hr (power output) and 0.99 lb/mmBtu (fuel input), respectively. This is an editorial correction. March 24, 2009

Table 3.3-2. SPECIATED ORGANIC COMPOUND EMISSION  
FACTORS FOR UNCONTROLLED DIESEL ENGINES<sup>a</sup>

EMISSION FACTOR RATING: E

| Pollutant   | Emission Factor<br>(Fuel Input)<br>(lb/MMBtu) |
|---|---|
| Benzene <sup>b</sup>  | 9.33 E-04                                     |
| Toluene <sup>b</sup>  | 4.09 E-04                                     |
| Xylenes <sup>b</sup>  | 2.85 E-04                                     |
| Propylene  | 2.58 E-03                                     |
| 1,3-Butadiene <sup>b,c</sup>  | <3.91 E-05                                    |
| Formaldehyde <sup>b</sup>   | 1.18 E-03                                     |
| Acetaldehyde <sup>b</sup>   | 7.67 E-04                                     |
| Acrolein <sup>b</sup>   | <9.25 E-05                                    |
| Polycyclic aromatic hydrocarbons (PAH)  |   |
| Naphthalene <sup>b</sup>  | 8.48 E-05                                     |
| Acenaphthylene  | <5.06 E-06                                    |
| Acenaphthene  | <1.42 E-06                                    |
| Fluorene  | 2.92 E-05                                     |
| Phenanthrene  | 2.94 E-05                                     |
| Anthracene  | 1.87 E-06                                     |
| Fluoranthene  | 7.61 E-06                                     |
| Pyrene  | 4.78 E-06                                     |
| Benzo(a)anthracene  | 1.68 E-06                                     |
| Chrysene  | 3.53 E-07                                     |
| Benzo(b)fluoranthene  | <9.91 E-08                                    |
| Benzo(k)fluoranthene  | <1.55 E-07                                    |
| Benzo(a)pyrene  | <1.88 E-07                                    |
| Indeno(1,2,3-cd)pyrene  | <3.75 E-07                                    |
| Dibenz(a,h)anthracene   | <5.83 E-07                                    |
| Benzo(g,h,i)perylene  | <4.89 E-07                                    |
| TOTAL PAH   | 1.68 E-04                                     |

<sup>a</sup> Based on the uncontrolled levels of 2 diesel engines from References 6-7. Source Classification Codes 2-02-001-02, 2-03-001-01. To convert from lb/MMBtu to ng/J, multiply by 430.

<sup>b</sup> Hazardous air pollutant listed in the *Clean Air Act*.

<sup>c</sup> Based on data from 1 engine.


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## Scania DS11 Diesel (11.0)

### Quick Overview

Engine type: DS11 Diesel - Scania

Construction Year: 1970-1995

Number of cylinders: 6


Bore ø: 127 mm

Engine content: 11022 CC

Compression ratio: 15 : 1

HP: 250+

### Parts

|                      |  |   |
|----------------------|--|---|
| Fuel                 |  | Diesel  |
| Construction Year    |  | 1970-1995   |
| Bore                 |  | 127 x 145   |
| Number of cylinders  |  | 6   |
| Compression ratio    |  | 15 : 1  |
| Engine content CC    |  | 11022  |
| Engine type          |  | DS11 Diesel - Scania  |
| Car type             |  | Scania DS11 11.0 Diesel series - Scania DS 11 (11.0)                                      |
| HP                   |  | 250+  |
| Piston               | <input type="text" value="0"/>             | MKP op aanvraag - 127mm - std (3480)  |
| Piston Rings         | <input type="text" value="0"/>             | MKPR 3480 - ø 127mm - 2,385 - 2,385 - 2,385 - 4,747 mm std                                |
| Small end bearings   | <input type="text" value="0"/>             | MKSB S 6597 L - std 127mm   |
| Cylinder Liner       | <input type="text" value="0"/>             | MKL op aanvraag - std 127mm   |
| Kitset / Assembly    | <input type="text" value="0"/>             | MKASS 612790 - std  |
| Conrod Bearings      | <input type="text" value="0"/>             | MKCB VPR 747 - std  |
| Main Bearings        | <input type="text" value="0"/>             | MKMB VPM 748 - std  |
| Camshaft bearing set | <input type="text" value="0"/>             | VPW 100 - std   |
| Valve intake         | <input type="text" value="0"/>             | MKIV op aanvraag - std  |
| Exhaust Valve        | <input type="text" value="0"/>             | MKEV op aanvraag - std  |
| Valve guide intake   | <input type="text" value="0"/>             | MKIG op aanvraag - std  |
| Valve guide exhaust  | <input type="text" value="0"/>             | MKEG op aanvraag - std  |
| Head gasket set      | <input type="text" value="0"/>             | MKHS op aanvraag - std  |
| Headgasket           | <input type="text" value="0"/>             | MKHG op aanvraag - std  |
| Piston Pin Bushings  | <input type="text" value="0"/>             | MKSB S 6597 L - std 127mm   |
| Parts                | Components not found? Request at comments! |   |

## **Section 5.2**

### **Generator (Unit 2)**

#### **Actual Emission Calculations**

## Engine Exhaust Actual Emissions Calculations

Unit Number: **3**  
 Description: Scania DS11 Diesel Generator (Emergency)

### Horsepower

**250** hp

Nameplate hp

Mfg. data

The data sheet shows the DS11 has a horsepower rating of 250+. Since the associated alternator is rated at 130 kW, the assumption of a site rating at 250 hp should be conservative.

### Fuel Consumption

**0.69** MMBtu/hr  
**138,000** Btu/gal  
 5.00 gal/hr  
**121.8** hr/yr  
 609 gal/yr  
 84 MMBtu/yr

Hourly fuel consumption  
 Field gas heating value  
 Hourly fuel consumption  
 Annual operating time  
 Hourly fuel consumption  
 Annual fuel consumption

Mfg. data  
 Nominal heat content  
 MMBtu/hr x 1,000,000 / Btu/gal  
 Harvest Four Corners, LLC  
 gal/hr x hr/yr  
 MMBtu/hr x hr/yr

### Steady-State Emission Rates

| Pollutants        | Emission Factors, lb/MMBtu | Uncontrolled Emission Rates, |          |
|-------------------|----------------------------|------------------------------|----------|
|                   |                            | pph                          | tpy      |
| NO <sub>2</sub>   | <b>4.41</b>                | 3.04                         | 1.85E-01 |
| CO                | <b>9.50E-01</b>            | 6.56E-01                     | 3.99E-02 |
| VOC               | <b>3.60E-01</b>            | 2.48E-01                     | 1.51E-02 |
| SO <sub>2</sub>   | <b>2.90E-01</b>            | 2.00E-01                     | 1.22E-02 |
| TSP               | <b>3.10E-01</b>            | 2.14E-01                     | 1.30E-02 |
| PM <sub>10</sub>  | <b>3.10E-01</b>            | 2.14E-01                     | 1.30E-02 |
| PM <sub>2.5</sub> | <b>3.10E-01</b>            | 2.14E-01                     | 1.30E-02 |
| Acetaldehyde      | <b>7.67E-04</b>            | 5.29E-04                     | 3.22E-05 |
| Benzene           | <b>9.33E-04</b>            | 6.44E-04                     | 3.92E-05 |
| Formaldehyde      | <b>1.18E-03</b>            | 8.14E-04                     | 4.96E-05 |
| Naphthalene       | <b>8.48E-05</b>            | 5.85E-05                     | 3.56E-06 |
| Toluene           | <b>4.09E-04</b>            | 2.82E-04                     | 1.72E-05 |
| Xylene            | <b>2.85E-04</b>            | 1.97E-04                     | 1.20E-05 |

Emission factors taken from AP-42, Tables 3.3-1 & 3.3-2

Uncontrolled Emission Rates (pph) = lb/MMBtu x MMBtu/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

## **Section 5.3**

### **Startup Shutdown & Maintenance (Unit SSM)**

#### **Written Description**

### ***Startup, Shutdown & Maintenance (Unit SSM)***

Emissions associated with startups, shutdowns and routine maintenance (SSM) of the turbine (Unit 1) and associated piping are vented to the atmosphere.

The VOC and HAP emissions from blowdowns of the compressor and piping associated with the facility were calculated from the quantity of gas vented during each event, the composition of the gas, and the number of events. The quantity of gas vented during each event was estimated by Harvest. The composition of the gas was based on a recent gas analysis from the facility. The estimated annual number of blowdown events includes an added safety factor because emissions from each blowdown event are dependent on the composition of the gas in the pipeline and the number of blowdowns in a year may vary. Experience indicates the composition of the gas will vary.

Four extended gas analyses (collected during the last five years, 2017 - 2021) were available for use in the application: April 2017, April 2018, October 2019, and May 2021. Harvest calculated SSM emissions using the analysis that predicted the highest VOC emission rate, the May 2021 analysis.

PTE emissions were calculated assuming a maximum of 100 blowdowns per year. There were no turbine startups or shutdowns during 2021. Therefore, actual 2021 emissions were calculated assuming zero blowdowns per year.

The SSM emissions identified in this application are routine or predictable startup/shutdown and scheduled maintenance and do not include malfunctions or upsets.

In this application, there are no changes to the calculations as they were presented in the either of the previous applications.

#### **Response to EPA request for additional information:**

- An explanation of how VOC emissions are calculated using the well gas analysis for all the emission units that this analysis is used for and a calculation that demonstrates this description.

The gas passing through the facility is a blend of gas from wells throughout the area. See the written description above and the calculation spreadsheets.



## **Section 5.3**

**Startup Shutdown & Maintenance (Unit SSM)**

**PTE Emission Calculations**

## Turbine & Compressor Blowdown PTE Emissions Calculations

Unit Number: **SSM**

Description: Turbine, Compressor &amp; Piping Associated With Station

### Throughput

**1** # of units  
**100** events/yr/unit  
**5,780** scf/event  
**12,400** scf/event  
 1,818,000 scf/yr

Number of units  
 Blowdowns per year per unit  
 Gas loss per blowdown (compressor)  
 Gas loss per blowdown (turbine)  
 Annual gas loss

Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 # of units x events/yr/unit  
     x [scf/event (compressor)  
     + scf/event (turbine)]

### Emission Rates

| Pollutants   | Emission Factors, lb/scf | Uncontrolled, Emission Rates, tpy |
|--------------|--------------------------|-----------------------------------|
| VOC          | 1.307E-02                | 11.88                             |
| Benzene      | 2.533E-05                | 2.30E-02                          |
| Ethylbenzene | 5.598E-07                | 5.09E-04                          |
| n-Hexane     | 2.951E-04                | 2.68E-01                          |
| Isooctane    | 7.398E-06                | 6.72E-03                          |
| Toluene      | 4.008E-05                | 3.64E-02                          |
| Xylene       | 6.718E-06                | 6.11E-03                          |

Emission factors calculated from gas composition (see table below)

Uncontrolled Emission Rates (tpy) = scf/yr x lb/scf / 2,000 lb/ton

### Gas Composition

| Components        | Mole Percents, % | Molecular Weights, lb/lb-mole | Emission Factors, lb/scf |
|-------------------|------------------|-------------------------------|--------------------------|
| Carbon dioxide    | 0.8632           | 44.01                         | 1.002E-03                |
| Hydrogen sulfide  | 0.0000           | 34.07                         | 0.000E+00                |
| Nitrogen          | 0.4462           | 28.01                         | 3.295E-04                |
| Methane           | 78.7294          | 16.04                         | 3.329E-02                |
| Ethane            | 10.7901          | 30.07                         | 8.554E-03                |
| Propane           | 5.0734           | 44.09                         | 5.897E-03                |
| Isobutane         | 0.8940           | 58.12                         | 1.370E-03                |
| n-Butane          | 1.5609           | 58.12                         | 2.392E-03                |
| Isopentane        | 0.5577           | 72.15                         | 1.061E-03                |
| n-Pentane         | 0.4298           | 72.15                         | 8.176E-04                |
| Cyclopentane      | 0.0189           | 70.14                         | 3.495E-05                |
| n-Hexane          | 0.1299           | 86.17                         | 2.951E-04                |
| Cyclohexane       | 0.0389           | 84.16                         | 8.631E-05                |
| Other hexanes     | 0.2872           | 86.18                         | 6.525E-04                |
| Heptanes          | 0.0720           | 100.20                        | 1.902E-04                |
| Methylcyclohexane | 0.0556           | 98.19                         | 1.439E-04                |
| Isooctane         | 0.0028           | 100.21                        | 7.398E-06                |
| Benzene           | 0.0123           | 78.11                         | 2.533E-05                |
| Toluene           | 0.0165           | 92.14                         | 4.008E-05                |
| Ethylbenzene      | 0.0002           | 106.17                        | 5.598E-07                |
| Xylenes           | 0.0024           | 106.17                        | 6.718E-06                |
| C8+ Heavies       | 0.0187           | 110.00                        | 5.423E-05                |
| Total             | 100.0001         |                               |                          |
| Total VOC         |                  |                               | 1.307E-02                |

Gas stream composition obtained from **Los Mestenos** extended gas analysis dated **05/06/2021**

Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.3 scf/lb-mole



2030 Afton Place  
Farmington, NM 87401  
(505) 325-6622

Analysis No: HM2021049  
Cust No: 33700-10375

### Well/Lease Information

Customer Name: HARVEST MIDSTREAM  
Well Name: Los Mestenios CDP  
County/State:  
Location:  
Lease/PA/CA:  
Formation:  
Cust. Stn. No.:

Source: METER RUN  
Well Flowing: Y  
Pressure: 80 PSIG  
Flow Temp: 60 DEG. F  
Ambient Temp: 72 DEG. F  
Flow Rate: MCF/D  
Sample Method: Purge & Fill  
Sample Date: 05/06/2021  
Sample Time: 2.10 PM  
Sampled By:  
Sampled by (CO): Harvest Mid.

Heat Trace: N  
Remarks: Calculated Molecular Weight = 21.3865

### Analysis

| Component:             | Mole%:  | Unnormalized %: | **GPM:  | *BTU:  | *SP Gravity: |
|------------------------|---------|-----------------|---------|--------|--------------|
| Nitrogen               | 0.4462  | 0.4456          | 0.0490  | 0.00   | 0.0043       |
| CO2                    | 0.8632  | 0.8621          | 0.1480  | 0.00   | 0.0131       |
| Methane                | 78.7294 | 78.6321         | 13.3930 | 795.17 | 0.4361       |
| Ethane                 | 10.7901 | 10.7768         | 2.8960  | 190.95 | 0.1120       |
| Propane                | 5.0734  | 5.0671          | 1.4030  | 127.65 | 0.0772       |
| Iso-Butane             | 0.8940  | 0.8929          | 0.2940  | 29.07  | 0.0179       |
| N-Butane               | 1.5609  | 1.5590          | 0.4940  | 50.92  | 0.0313       |
| Neopentane 2,2 dmc3    | 0.0000  | 0.0000          | 0.0000  | 0.00   | 0.0000       |
| I-Pentane              | 0.5577  | 0.5570          | 0.2050  | 22.31  | 0.0139       |
| N-Pentane              | 0.4298  | 0.4293          | 0.1560  | 17.23  | 0.0107       |
| Neohexane              | 0.0117  | N/R             | 0.0050  | 0.55   | 0.0003       |
| 2-3-Dimethylbutane     | 0.0181  | N/R             | 0.0070  | 0.86   | 0.0005       |
| Cyclopentane           | 0.0189  | N/R             | 0.0060  | 0.71   | 0.0005       |
| 2-Methylpentane        | 0.1220  | N/R             | 0.0510  | 5.79   | 0.0036       |
| 3-Methylpentane        | 0.0464  | N/R             | 0.0190  | 2.20   | 0.0014       |
| C6                     | 0.1299  | 0.6545          | 0.0540  | 6.18   | 0.0039       |
| Methylcyclopentane     | 0.0890  | N/R             | 0.0320  | 4.01   | 0.0026       |
| Benzene                | 0.0123  | N/R             | 0.0030  | 0.46   | 0.0003       |
| Cyclohexane            | 0.0389  | N/R             | 0.0130  | 1.74   | 0.0011       |
| 2-Methylhexane         | 0.0143  | N/R             | 0.0070  | 0.78   | 0.0005       |
| 3-Methylhexane         | 0.0156  | N/R             | 0.0070  | 0.85   | 0.0005       |
| 2-2-4-Trimethylpentane | 0.0028  | N/R             | 0.0010  | 0.17   | 0.0001       |
| i-heptanes             | 0.0091  | N/R             | 0.0040  | 0.48   | 0.0003       |
| Heptane                | 0.0330  | N/R             | 0.0150  | 1.82   | 0.0011       |

|                         |               |               |               |                |               |
|-------------------------|---------------|---------------|---------------|----------------|---------------|
| Methylcyclohexane       | 0.0556        | N/R           | 0.0220        | 2.90           | 0.0019        |
| Toluene                 | 0.0165        | N/R           | 0.0060        | 0.74           | 0.0005        |
| 2-Methylheptane         | 0.0064        | N/R           | 0.0030        | 0.40           | 0.0003        |
| 4-Methylheptane         | 0.0033        | N/R           | 0.0020        | 0.20           | 0.0001        |
| i-Octanes               | 0.0026        | N/R           | 0.0010        | 0.16           | 0.0001        |
| Octane                  | 0.0056        | N/R           | 0.0030        | 0.35           | 0.0002        |
| Ethylbenzene            | 0.0002        | N/R           | 0.0000        | 0.01           | 0.0000        |
| m, p Xylene             | 0.0022        | N/R           | 0.0010        | 0.11           | 0.0001        |
| o Xylene (& 2,2,4 tmc7) | 0.0002        | N/R           | 0.0000        | 0.01           | 0.0000        |
| i-C9                    | 0.0002        | N/R           | 0.0000        | 0.01           | 0.0000        |
| C9                      | 0.0003        | N/R           | 0.0000        | 0.02           | 0.0000        |
| i-C10                   | 0.0001        | N/R           | 0.0000        | 0.01           | 0.0000        |
| C10                     | 0.0001        | N/R           | 0.0000        | 0.01           | 0.0000        |
| i-C11                   | 0.0000        | N/R           | 0.0000        | 0.00           | 0.0000        |
| C11                     | 0.0001        | N/R           | 0.0000        | 0.01           | 0.0000        |
| C12P                    | 0.0000        | N/R           | 0.0000        | 0.00           | 0.0000        |
| <b>Total</b>            | <b>100.00</b> | <b>99.876</b> | <b>19.300</b> | <b>1264.86</b> | <b>0.7368</b> |

\* @ 14.730 PSIA DRY & UNCORRECTED FOR COMPRESSIBILITY

\*\*@ 14.730 PSIA & 60 DEG. F.

|                                      |        |
|--------------------------------------|--------|
| COMPRESSIBILITY FACTOR (1/Z):        | 1.0037 |
| BTU/CU.FT IDEAL:                     | 1267.8 |
| BTU/CU.FT (DRY) CORRECTED FOR (1/Z): | 1272.5 |
| BTU/CU.FT (WET) CORRECTED FOR (1/Z): | 1250.4 |
| DRY BTU @ 15.025:                    | 1298.0 |
| REAL SPECIFIC GRAVITY:               | 0.7392 |

|                    |               |
|--------------------|---------------|
| CYLINDER #:        | 16            |
| CYLINDER PRESSURE: | 66 PSIG       |
| ANALYSIS DATE:     | 05/07/2021    |
| ANALYSIS TIME:     | 11:17:24 AM   |
| ANALYSIS RUN BY:   | PATRICIA KING |

**GPM, BTU, and SPG calculations as shown above are based on current GPA constants.**

**GPA Standard: GPA 2286-14**

**GC: SRI Instruments 8610      Last Cal/Verify: 05/11/2021**

**GC Method: C12+BTEX Gas**

## **Section 5.3**

**Startup Shutdown & Maintenance (Unit SSM)**

**Actual Emission Calculations**

## Turbine & Compressor Blowdown Actual Emissions Calculations

Unit Number: **SSM**

Description: Turbine, Compressor &amp; Piping Associated With Station

### Throughput

**1** # of units  
**0** events/yr/unit  
**5,780** scf/event  
**12,400** scf/event  
**0** scf/yr

Number of units  
 Blowdowns per year per unit  
 Gas loss per blowdown (compressor)  
 Gas loss per blowdown (turbine)  
 Annual gas loss

Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 # of units x events/yr/unit  
 x [scf/event (compressor)  
 + scf/event (turbine)]

### Emission Rates

| Pollutants   | Emission Factors, lb/scf | Uncontrolled, Emission Rates, tpy |
|--------------|--------------------------|-----------------------------------|
| VOC          | 1.307E-02                | 0.00E+00                          |
| Benzene      | 2.533E-05                | 0.00E+00                          |
| Ethylbenzene | 5.598E-07                | 0.00E+00                          |
| n-Hexane     | 2.951E-04                | 0.00E+00                          |
| Isooctane    | 7.398E-06                | 0.00E+00                          |
| Toluene      | 4.008E-05                | 0.00E+00                          |
| Xylene       | 6.718E-06                | 0.00E+00                          |

Emission factors calculated from gas composition (see table below)

Uncontrolled Emission Rates (tpy) = scf/yr x lb/scf / 2,000 lb/ton

### Gas Composition

| Components        | Mole Percents, % | Molecular Weights, lb/lb-mole | Emission Factors, lb/scf |
|-------------------|------------------|-------------------------------|--------------------------|
| Carbon dioxide    | <b>0.8632</b>    | 44.01                         | 1.002E-03                |
| Hydrogen sulfide  | <b>0.0000</b>    | 34.07                         | 0.000E+00                |
| Nitrogen          | <b>0.4462</b>    | 28.01                         | 3.295E-04                |
| Methane           | <b>78.7294</b>   | 16.04                         | 3.329E-02                |
| Ethane            | <b>10.7901</b>   | 30.07                         | 8.554E-03                |
| Propane           | <b>5.0734</b>    | 44.09                         | 5.897E-03                |
| Isobutane         | <b>0.8940</b>    | 58.12                         | 1.370E-03                |
| n-Butane          | <b>1.5609</b>    | 58.12                         | 2.392E-03                |
| Isopentane        | <b>0.5577</b>    | 72.15                         | 1.061E-03                |
| n-Pentane         | <b>0.4298</b>    | 72.15                         | 8.176E-04                |
| Cyclopentane      | <b>0.0189</b>    | 70.14                         | 3.495E-05                |
| n-Hexane          | <b>0.1299</b>    | 86.17                         | 2.951E-04                |
| Cyclohexane       | <b>0.0389</b>    | 84.16                         | 8.631E-05                |
| Other hexanes     | <b>0.2872</b>    | 86.18                         | 6.525E-04                |
| Heptanes          | <b>0.0720</b>    | 100.20                        | 1.902E-04                |
| Methylcyclohexane | <b>0.0556</b>    | 98.19                         | 1.439E-04                |
| Isooctane         | <b>0.0028</b>    | 100.21                        | 7.398E-06                |
| Benzene           | <b>0.0123</b>    | 78.11                         | 2.533E-05                |
| Toluene           | <b>0.0165</b>    | 92.14                         | 4.008E-05                |
| Ethylbenzene      | <b>0.0002</b>    | 106.17                        | 5.598E-07                |
| Xylenes           | <b>0.0024</b>    | 106.17                        | 6.718E-06                |
| C8+ Heavies       | <b>0.0186</b>    | 110.00                        | 5.394E-05                |
| Total             | 100.0000         |                               |                          |
| Total VOC         |                  |                               | 1.307E-02                |

Gas stream composition obtained from **Los Mestenos** extended gas analysis dated **05/06/2021**

Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.3 scf/lb-mole

## **Section 5.4**

### **Equipment Leaks (Unit F1)**

#### **Written Description**

### ***Equipment Leaks (F-1)***

Fugitive emissions from equipment leaks (valves, flanges, seals, etc.) were calculated using emission factors from the *1995 Protocol for Equipment Leak Emission Estimates* published by the Environmental Protection Agency (EPA), component counts provided by Harvest, and the gas composition provided by a recent extended gas analysis. First, total organic compound (TOC) emissions were estimated using the component count and EPA emission factors. Then, the gas composition from the extended gas analysis (converted from mole fraction to weight percent) was used to estimate the percentage of VOC and HAP in the TOC.

Four extended gas analyses (collected during the last five years, 2017 - 2021) were available for use in the application: April 2017, April 2018, October 2019, and May 2021. Harvest calculated equipment leak emissions using the analysis that predicted the highest VOC emission rate, the May 2021 analysis.

PTE and 2021 actual emissions were calculated assuming all the equipment operated 8,760 hours during the year.

In this application, there are no changes to the calculations as they were presented in the either of the previous applications.

### **Response to EPA request for additional information:**

- An explanation of how VOC emissions are calculated using the well gas analysis for all the emission units that this analysis is used for and a calculation that demonstrates this description.

See the written description above and the calculation spreadsheets provided in this subsection.



## **Section 5.4**

**Equipment Leaks (Unit F1)**

**PTE Emission Calculations**

## Equipment Leaks PTE Emissions Calculations

Unit Number: **F1**

Description: Valves, Connectors, Seals &amp; Open-Ended Lines

### Steady-State Emission Rates

| Equipment              | Number of Components, # of sources | Emission Factors, kg/hr/source | Emission Factors, lb/hr/source | Uncontrolled TOC Emission Rates, |              |
|------------------------|------------------------------------|--------------------------------|--------------------------------|----------------------------------|--------------|
|                        |                                    |                                |                                | pph                              | tpy          |
| Valves                 | 252                                | 0.0045                         | 0.0099                         | 2.49                             | 10.93        |
| Connectors             | 187                                | 0.0002                         | 0.0004                         | 0.08                             | 0.36         |
| Pump Seals             | 0                                  | 0.0024                         | 0.0053                         | 0.00                             | 0.00         |
| Compressor Seals       | 28                                 | 0.0088                         | 0.0194                         | 0.54                             | 2.37         |
| Pressure Relief Valves | 13                                 | 0.0088                         | 0.0194                         | 0.25                             | 1.10         |
| Open-Ended Lines       | 73                                 | 0.0020                         | 0.0044                         | 0.32                             | 1.41         |
| <b>Total</b>           |                                    |                                |                                | <b>3.69</b>                      | <b>16.17</b> |

Number of components based on the numbers of compressors and dehydrators at the station (see next page)

Emission factors taken from the EPA "1995 Protocol for Equipment Leak Emission Estimates"

Emission factors (lb/hr/source) = Emission factors (kg/hr/source) x 2.2 lb/kg

Uncontrolled TOC Emission Rates (pph) = lb/hr/source x # of sources

Uncontrolled TOC Emission Rates (tpy) = Uncontrolled TOC Emission Rates (pph) x 8,760 hr/yr / 2,000 lb/ton

| Components        | Mole Percents, % | Molecular Weights, lb/lb-mole | Component Weights, lb/lb-mole | Weight Percent of TOC, % | Uncontrolled Emission Rates, |          |
|-------------------|------------------|-------------------------------|-------------------------------|--------------------------|------------------------------|----------|
|                   |                  |                               |                               |                          | pph                          | tpy      |
| Carbon dioxide    | 0.8632           | 44.010                        |                               |                          |                              |          |
| Hydrogen sulfide  | 0.0000           | 34.070                        |                               |                          |                              |          |
| Nitrogen          | 0.4462           | 28.013                        |                               |                          |                              |          |
| Methane           | 78.7294          | 16.043                        | 1263.056                      | 60.619                   |                              |          |
| Ethane            | 10.7901          | 30.070                        | 324.458                       | 15.572                   |                              |          |
| Propane           | 5.0734           | 44.097                        | 223.722                       | 10.737                   | 3.96E-01                     | 1.74E+00 |
| Isobutane         | 0.8940           | 58.123                        | 51.962                        | 2.494                    | 9.21E-02                     | 4.03E-01 |
| n-Butane          | 1.5609           | 58.123                        | 90.724                        | 4.354                    | 1.61E-01                     | 7.04E-01 |
| Isopentane        | 0.5577           | 72.150                        | 40.238                        | 1.931                    | 7.13E-02                     | 3.12E-01 |
| n-Pentane         | 0.4298           | 72.150                        | 31.010                        | 1.488                    | 5.49E-02                     | 2.41E-01 |
| Cyclopentane      | 0.0189           | 70.134                        | 1.326                         | 0.064                    | 2.35E-03                     | 1.03E-02 |
| n-Hexane          | 0.1299           | 86.177                        | 11.194                        | 0.537                    | 1.98E-02                     | 8.69E-02 |
| Cyclohexane       | 0.0389           | 84.161                        | 3.274                         | 0.157                    | 5.80E-03                     | 2.54E-02 |
| Other hexanes     | 0.2872           | 86.177                        | 24.750                        | 1.188                    | 4.39E-02                     | 1.92E-01 |
| Heptanes          | 0.0720           | 100.204                       | 7.215                         | 0.346                    | 1.28E-02                     | 5.60E-02 |
| Methylcyclohexane | 0.0556           | 98.188                        | 5.459                         | 0.262                    | 9.67E-03                     | 4.24E-02 |
| Isooctane         | 0.0028           | 114.231                       | 0.320                         | 0.015                    | 5.67E-04                     | 2.48E-03 |
| Benzene           | 0.0123           | 78.114                        | 0.961                         | 0.046                    | 1.70E-03                     | 7.46E-03 |
| Toluene           | 0.0165           | 92.141                        | 1.520                         | 0.073                    | 2.69E-03                     | 1.18E-02 |
| Ethylbenzene      | 0.0002           | 106.167                       | 0.021                         | 0.001                    | 3.76E-05                     | 1.65E-04 |
| Xylenes           | 0.0024           | 106.167                       | 0.255                         | 0.012                    | 4.51E-04                     | 1.98E-03 |
| C8+ Heavies       | 0.0187           | 114.231                       | 2.136                         | 0.103                    | 3.79E-03                     | 1.66E-02 |
| <b>Total</b>      | 100.0001         |                               | 2083.601                      |                          |                              |          |
| <b>Total VOC</b>  |                  |                               |                               | 23.809                   | 8.79E-01                     | 3.85     |

Gas stream composition obtained from **Los Mestenos** extended gas analysis dated **05/06/2021**

Component Weights (lb/lb-mole) = (% / 100) \* Molecular Weights (lb/lb-mole)

Weight Percent of TOC (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)

Uncontrolled Emission Rates (pph) = Total Uncontrolled TOC Emission Rate (pph) x (% / 100)

Uncontrolled Emission Rates (tpy) = Total Uncontrolled TOC Emission Rate (tpy) x (% / 100)

## Equipment Leaks PTE Emissions Calculations

Unit Number: **F1**

Description: Valves, Connectors, Seals &amp; Lines

Number of Compression Units at the Facility: **1**Number of Dehydrators at the Facility: **0**

| Process Equipment Description                               | Equipment Count |            |            |                  |                        |          | Instrument Count |       |          |
|---|-----------------|------------|------------|------------------|------------------------|----------|------------------|-------|----------|
|   | Valves          | Connectors | Pump Seals | Compressor Seals | Pressure Relief Valves | Open-end | Flow             | Level | Pressure |
| Station inlet, meter run to pulsation dampener              | 17              | 14         | 0          | 0                | 1                      | 13       | 3                | 0     | 3        |
| Pulsation dampener  | 12              | 8          | 0          | 0                | 0                      | 2        | 0                | 4     | 1        |
| Compressor suction header                                   | 7               | 4          | 0          | 0                | 0                      | 3        | 0                | 0     | 1        |
| Suction header feed to instrument gas header                | 3               | 1          | 0          | 0                | 0                      | 1        | 0                | 0     | 0        |
| Compressor discharge header and bypass to station discharge | 6               | 5          | 0          | 0                | 0                      | 3        | 0                | 1     | 1        |
| Compressor discharge header and suction header bypass lines | 4               | 2          | 0          | 0                | 0                      | 2        | 0                | 0     | 1        |
| Fuel gas header   | 2               | 2          | 0          | 0                | 1                      | 2        | 0                | 0     | 1        |
| Instrument gas header                                       | 2               | 2          | 0          | 0                | 1                      | 2        | 0                | 0     | 0        |
| Station discharge header                                    | 9               | 5          | 0          | 0                | 1                      | 6        | 0                | 0     | 2        |
| Fuel gas recovery header                                    | 2               | 2          | 0          | 0                | 1                      | 2        | 0                | 0     | 0        |
| Fuel gas feed and filter loop                               | 15              | 9          | 0          | 0                | 0                      | 1        | 0                | 4     | 1        |
| Instrument gas feed and filter loop                         | 9               | 11         | 0          | 0                | 0                      | 3        | 0                | 0     | 0        |
| Produced water storage tank                                 | 1               | 0          | 0          | 0                | 0                      | 1        | 0                | 1     | 0        |
| ESD panel   | 12              | 0          | 0          | 0                | 0                      | 0        | 0                | 0     | 0        |
| Starting gas header   | 6               | 2          | 0          | 0                | 1                      | 3        | 0                | 0     | 0        |
| Hot gas header  | 2               | 2          | 0          | 0                | 0                      | 2        | 0                | 0     | 0        |
| Volume bottle lop   | 12              | 4          | 0          | 24               | 1                      | 2        | 0                | 0     | 1        |
| Components from Compressors                                 | 44              | 59         | 0          | 4                | 6                      | 11       | 0                | 4     | 9        |
| Components from dehydrators                                 | 0               | 0          | 0          | 0                | 0                      | 0        | 0                | 0     | 0        |
| Total   | 165             | 132        | 0          | 28               | 13                     | 59       | 3                | 14    | 21       |
| Adjusted Total  | 252             | 187        | 0          | 28               | 13                     | 73       |                  |       |          |

The following additions are included in the Adjusted Total:

- 1 valve is added for each open end line
- 2 connectors are added for each flow meter
- 2 valves, 2 connectors and 1 open end line are added for each level gauge
- 1 connector is added for each pressure gauge

The component count is based on an evaluation of the typical configuration of a Harvest compressor station (two stage compression)

TABLE 2-4. OIL AND GAS PRODUCTION OPERATIONS AVERAGE EMISSION FACTORS (kg/hr/source)

| Equipment Type      | Service <sup>a</sup> | Emission Factor (kg/hr/source) <sup>b</sup> |
|---------------------|----------------------|---|
| Valves              | Gas                  | 4.5E-03                                     |
|                     | Heavy Oil            | 8.4E-06                                     |
|                     | Light Oil            | 2.5E-03                                     |
|                     | Water/Oil            | 9.8E-05                                     |
| Pump seals          | Gas                  | 2.4E-03                                     |
|                     | Heavy Oil            | NA  |
|                     | Light Oil            | 1.3E-02                                     |
|                     | Water/Oil            | 2.4E-05                                     |
| Others <sup>c</sup> | Gas                  | 8.8E-03                                     |
|                     | Heavy Oil            | 3.2E-05                                     |
|                     | Light Oil            | 7.5E-03                                     |
|                     | Water/Oil            | 1.4E-02                                     |
| Connectors          | Gas                  | 2.0E-04                                     |
|                     | Heavy Oil            | 7.5E-06                                     |
|                     | Light Oil            | 2.1E-04                                     |
|                     | Water/Oil            | 1.1E-04                                     |
| Flanges             | Gas                  | 3.9E-04                                     |
|                     | Heavy Oil            | 3.9E-07                                     |
|                     | Light Oil            | 1.1E-04                                     |
|                     | Water/Oil            | 2.9E-06                                     |
| Open-ended lines    | Gas                  | 2.0E-03                                     |
|                     | Heavy Oil            | 1.4E-04                                     |
|                     | Light Oil            | 1.4E-03                                     |
|                     | Water/Oil            | 2.5E-04                                     |

<sup>a</sup>Water/Oil emission factors apply to water streams in oil service with a water content greater than 50%, from the point of origin to the point where the water content reaches 99%. For water streams with a water content greater than 99%, the emission rate is considered negligible.

<sup>b</sup>These factors are for total organic compound emission rates (including non-VOC's such as methane and ethane) and apply to light crude, heavy crude, gas plant, gas production, and off shore facilities. "NA" indicates that not enough data were available to develop the indicated emission factor.

<sup>c</sup>The "other" equipment type was derived from compressors, diaphragms, drains, dump arms, hatches, instruments, meters, pressure relief valves, polished rods, relief valves, and vents. This "other" equipment type should be applied for any equipment type other than connectors, flanges, open-ended lines, pumps, or valves.

## **Section 5.4**

**Equipment Leaks (Unit F1)**

**Actual Emission Calculations**

## Equipment Leaks Actual Emissions Calculations

Unit Number: **F1**

Description: Valves, Connectors, Seals &amp; Open-Ended Lines

### Steady-State Emission Rates

| Equipment              | Number of Components, # of sources | Emission Factors, kg/hr/source | Emission Factors, lb/hr/source | Uncontrolled TOC Emission Rates, |              |
|------------------------|------------------------------------|--------------------------------|--------------------------------|----------------------------------|--------------|
|                        |                                    |                                |                                | pph                              | tpy          |
| Valves                 | 252                                | 0.0045                         | 0.0099                         | 2.49                             | 10.93        |
| Connectors             | 187                                | 0.0002                         | 0.0004                         | 0.08                             | 0.36         |
| Pump Seals             | 0                                  | 0.0024                         | 0.0053                         | 0.00                             | 0.00         |
| Compressor Seals       | 28                                 | 0.0088                         | 0.0194                         | 0.54                             | 2.37         |
| Pressure Relief Valves | 13                                 | 0.0088                         | 0.0194                         | 0.25                             | 1.10         |
| Open-Ended Lines       | 73                                 | 0.0020                         | 0.0044                         | 0.32                             | 1.41         |
| <b>Total</b>           |                                    |                                |                                | <b>3.69</b>                      | <b>16.17</b> |

Number of components based on the numbers of compressors and dehydrators at the station (see next page)

Emission factors taken from the EPA "1995 Protocol for Equipment Leak Emission Estimates"

Emission factors (lb/hr/source) = Emission factors (kg/hr/source) x 2.2 lb/kg

Uncontrolled TOC Emission Rates (pph) = lb/hr/source x # of sources

Uncontrolled TOC Emission Rates (tpy) = Uncontrolled TOC Emission Rates (pph) x 8,760 hr/yr / 2,000 lb/ton

| Components        | Mole Percents, % | Molecular Weights, lb/lb-mole | Component Weights, lb/lb-mole | Weight Percent of TOC, % | Uncontrolled Emission Rates, |          |
|-------------------|------------------|-------------------------------|-------------------------------|--------------------------|------------------------------|----------|
|                   |                  |                               |                               |                          | pph                          | tpy      |
| Carbon dioxide    | 0.8632           | 44.010                        |                               |                          |                              |          |
| Hydrogen sulfide  | 0.0000           | 34.070                        |                               |                          |                              |          |
| Nitrogen          | 0.4462           | 28.013                        |                               |                          |                              |          |
| Methane           | 78.7294          | 16.043                        | 1263.056                      | 60.619                   |                              |          |
| Ethane            | 10.7901          | 30.070                        | 324.458                       | 15.572                   |                              |          |
| Propane           | 5.0734           | 44.097                        | 223.722                       | 10.737                   | 3.96E-01                     | 1.74E+00 |
| Isobutane         | 0.8940           | 58.123                        | 51.962                        | 2.494                    | 9.21E-02                     | 4.03E-01 |
| n-Butane          | 1.5609           | 58.123                        | 90.724                        | 4.354                    | 1.61E-01                     | 7.04E-01 |
| Isopentane        | 0.5577           | 72.150                        | 40.238                        | 1.931                    | 7.13E-02                     | 3.12E-01 |
| n-Pentane         | 0.4298           | 72.150                        | 31.010                        | 1.488                    | 5.49E-02                     | 2.41E-01 |
| Cyclopentane      | 0.0189           | 70.134                        | 1.326                         | 0.064                    | 2.35E-03                     | 1.03E-02 |
| n-Hexane          | 0.1299           | 86.177                        | 11.194                        | 0.537                    | 1.98E-02                     | 8.69E-02 |
| Cyclohexane       | 0.0389           | 84.161                        | 3.274                         | 0.157                    | 5.80E-03                     | 2.54E-02 |
| Other hexanes     | 0.2872           | 86.177                        | 24.750                        | 1.188                    | 4.39E-02                     | 1.92E-01 |
| Heptanes          | 0.0720           | 100.204                       | 7.215                         | 0.346                    | 1.28E-02                     | 5.60E-02 |
| Methylcyclohexane | 0.0556           | 98.188                        | 5.459                         | 0.262                    | 9.67E-03                     | 4.24E-02 |
| Isooctane         | 0.0028           | 114.231                       | 0.320                         | 0.015                    | 5.67E-04                     | 2.48E-03 |
| Benzene           | 0.0123           | 78.114                        | 0.961                         | 0.046                    | 1.70E-03                     | 7.46E-03 |
| Toluene           | 0.0165           | 92.141                        | 1.520                         | 0.073                    | 2.69E-03                     | 1.18E-02 |
| Ethylbenzene      | 0.0002           | 106.167                       | 0.021                         | 0.001                    | 3.76E-05                     | 1.65E-04 |
| Xylenes           | 0.0024           | 106.167                       | 0.255                         | 0.012                    | 4.51E-04                     | 1.98E-03 |
| C8+ Heavies       | 0.0186           | 114.231                       | 2.125                         | 0.102                    | 3.76E-03                     | 1.65E-02 |
| <b>Total</b>      | 100.0000         |                               | 2083.590                      |                          |                              |          |
| <b>Total VOC</b>  |                  |                               |                               | 23.809                   | 8.79E-01                     | 3.85     |

Gas stream composition obtained from **Los Mestenos** extended gas analysis dated **05/06/2021**

Component Weights (lb/lb-mole) = (% / 100) \* Molecular Weights (lb/lb-mole)

Weight Percent of TOC (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)

Uncontrolled Emission Rates (pph) = Total Uncontrolled TOC Emission Rate (pph) x (% / 100)

Uncontrolled Emission Rates (tpy) = Total Uncontrolled TOC Emission Rate (tpy) x (% / 100)

## Equipment Leaks Actual Emissions Calculations

Unit Number: **F1**

Description: Valves, Connectors, Seals &amp; Lines

Number of Compression Units at the Facility: **1**Number of Dehydrators at the Facility: **0**

| Process Equipment Description                               | Equipment Count |            |            |                  |                        |          | Instrument Count |       |          |
|---|-----------------|------------|------------|------------------|------------------------|----------|------------------|-------|----------|
|   | Valves          | Connectors | Pump Seals | Compressor Seals | Pressure Relief Valves | Open-end | Flow             | Level | Pressure |
| Station inlet, meter run to pulsation dampener              | 17              | 14         | 0          | 0                | 1                      | 13       | 3                | 0     | 3        |
| Pulsation dampener  | 12              | 8          | 0          | 0                | 0                      | 2        | 0                | 4     | 1        |
| Compressor suction header                                   | 7               | 4          | 0          | 0                | 0                      | 3        | 0                | 0     | 1        |
| Suction header feed to instrument gas header                | 3               | 1          | 0          | 0                | 0                      | 1        | 0                | 0     | 0        |
| Compressor discharge header and bypass to station discharge | 6               | 5          | 0          | 0                | 0                      | 3        | 0                | 1     | 1        |
| Compressor discharge header and suction header bypass lines | 4               | 2          | 0          | 0                | 0                      | 2        | 0                | 0     | 1        |
| Fuel gas header   | 2               | 2          | 0          | 0                | 1                      | 2        | 0                | 0     | 1        |
| Instrument gas header                                       | 2               | 2          | 0          | 0                | 1                      | 2        | 0                | 0     | 0        |
| Station discharge header                                    | 9               | 5          | 0          | 0                | 1                      | 6        | 0                | 0     | 2        |
| Fuel gas recovery header                                    | 2               | 2          | 0          | 0                | 1                      | 2        | 0                | 0     | 0        |
| Fuel gas feed and filter loop                               | 15              | 9          | 0          | 0                | 0                      | 1        | 0                | 4     | 1        |
| Instrument gas feed and filter loop                         | 9               | 11         | 0          | 0                | 0                      | 3        | 0                | 0     | 0        |
| Produced water storage tank                                 | 1               | 0          | 0          | 0                | 0                      | 1        | 0                | 1     | 0        |
| ESD panel   | 12              | 0          | 0          | 0                | 0                      | 0        | 0                | 0     | 0        |
| Starting gas header   | 6               | 2          | 0          | 0                | 1                      | 3        | 0                | 0     | 0        |
| Hot gas header  | 2               | 2          | 0          | 0                | 0                      | 2        | 0                | 0     | 0        |
| Volume bottle lop   | 12              | 4          | 0          | 24               | 1                      | 2        | 0                | 0     | 1        |
| Components from Compressors                                 | 44              | 59         | 0          | 4                | 6                      | 11       | 0                | 4     | 9        |
| Components from dehydrators                                 | 0               | 0          | 0          | 0                | 0                      | 0        | 0                | 0     | 0        |
| Total   | 165             | 132        | 0          | 28               | 13                     | 59       | 3                | 14    | 21       |
| Adjusted Total  | 252             | 187        | 0          | 28               | 13                     | 73       |                  |       |          |

The following additions are included in the Adjusted Total:

- 1 valve is added for each open end line
- 2 connectors are added for each flow meter
- 2 valves, 2 connectors and 1 open end line are added for each level gauge
- 1 connector is added for each pressure gauge

The component count is based on an evaluation of the typical configuration of a Harvest compressor station (two stage compression)

## **Section 5.5**

### **Condensate Storage Tanks (Units T1 & T2)**

#### **Written Description**



### ***Condensate Storage Tanks (Units T1 & T2)***

The facility is equipped with two condensate storage tanks. Unit T1 receives the condensate when it first enters the facility and all flashing occurs in this tank. Unit T2 is permitted to prevent overflows from T1 during times when haul truck access is limited due to outside factors such as weather and/or road conditions. Flashing does not occur in this tank, only working/breathing losses.

Flash emissions from the condensate storage tank (Unit T1) were calculated using VMGSim. Flashing typically occurs when high pressure liquids are dropped to lower pressures, in this case when high pressure condensate empties into the atmospheric condensate storage tanks. VMGSim is an effective tool for estimating these flash emissions. Using the composition of the condensate and the applicable pressures and temperatures for the facility, VMGSim can predict the amounts of different pollutants that will be emitted from the tanks. The inputs and outputs are identified on Page 3 of each VMGSim output.

Using molecular weights, the VMGSim flash gas output compositions from the condensate storage tanks were converted from mole fractions to weight percent. See the table on Page 2 of each of the Condensate Storage Tank Emissions Data and Calculations spreadsheets. These weight percentages were used to calculate HAP emissions, as percentages of the VOC emissions.

For consistency with the previous application and revision, the PTE flash emission calculations were prepared using a condensate throughput rate of 22,141 bbl/yr. Note that the highest 12-month rolling total condensate throughput occurred in May 2017 and was only 9,109.8 bbl/yr. Four condensate analyses (collected during the last five years, 2017 - 2021) were available for use in the application: December 2017, December 2018, November 2019, and August 2021. Harvest ran VMGSim using each of these analyses and prepared the PTE flash emission calculations in this application using the analysis that predicted the highest VOC emission rate, the December 2018 analysis.

Actual flash emissions were calculated using the condensate throughput from 2021 (3,667.8 bbl/yr) and the condensate analysis from August 2021.

Working/breathing losses from the condensate storage tanks were calculated using TANKS 4.0.9d. Using molecular weights the post-flash condensate composition (excluding water), provided by VMGSim, was converted from mole fractions to weight percentages. See the table on Page 3 of each of the Condensate Storage Tank Emissions Data and Calculations spreadsheets. These weight percentages, in turn, were input into the TANKS program, along with the appropriate tank dimensions and throughputs. The Unit T1 throughput was estimated at 22,141 bbl/yr. Since Unit T2 is a backup tank, its throughput was estimated at 11,070 bbl/yr,

half the throughput seen by Unit T1. The TANKS inputs and outputs can be seen on the TANKS output file, included with the calculations in this section.

The working/breathing losses and flash emissions from the condensate storage tanks were combined. See the table on Page 1 of each of the Condensate Storage Tank Emissions Data and Calculations spreadsheets.

This method of calculating condensate storage tank emissions is a change from what was submitted in the previous two versions of the application.

**Response to EPA request for additional information:**

- Provide the results EPA request that Harvest use the worst-case condensate sample analysis results over the 5-year time limit of the Los Mestenos Part 71 permit to calculate working and breathing losses and the flash emissions for the new TV application. Include the 2020 condensate analysis results when determining worst-case analysis and provide EPA a copy of these results. Also, revise all PTE calculations that utilize the condensate sample analysis to worst case scenario.

See the written description above. Harvest did not sample the condensate in 2020. Note that there is not requirement for annual condensate sampling.

**Response to EPA request for additional information:**

- Harvest should not be using an outdated method to calculate tank emissions. Why is Harvest using an outdated method to calculate working and breathing losses of the tanks? Why is Harvest not using the same software to calculate working and breathing losses and the flash emissions?

Harvest did not use an outdated method for calculating working breathing losses. TANKS 4.0.9d was selected both because its use is standard industry practice accepted in all the states in which Harvest operates and because the model uses the EPA recommended equations/algorithms specified in AP-42 Chapter 7 to calculate working/breathing losses. From the EPA website:

\*\*\*IMPORTANT NOTE - The TANKS model was developed using a software that is now outdated. Because of this, the model is not reliably functional on computers using certain operating systems such as Windows Vista or Windows 7. We are anticipating that additional problems will arise as PCs switch to the other operating systems. Therefore, we can no longer provide assistance to users of TANKs 4.09d. The model will remain on the website to be used at your discretion and at your own risk. We will continue to recommend the use of the equations/algorithms specified in AP-42 Chapter 7 for estimating VOC emissions from storage tanks. The equations specified in AP-42 Chapter

7 (<https://www.epa.gov/ttn/chief/ap42/ch07/index.html>) can be employed with many current spreadsheet/software programs.

Windows Vista and Windows 7 were not used when running the model. TANKS 4.0.9d has been operating reliably using the Windows 10 operating system. As EPA notes, the software that was used in the development of the model has become outdated. However, the underlying calculation methodology used in the program, which is based on Chapter 7 of AP-42, still follows EPA's recommendation for estimating emissions from storage tanks. Therefore, the TANKS 4.0.9d software remains a valid option for calculating working and breathing losses from storage tanks.

Note that Promax and VMGSim both use the AP-42 Chapter 7 equations/algorithms to calculate working/breathing losses. If VMGSim had been used to calculate the losses, results would have been essentially the same, except that unlike TANKS 4.0.9d, VMGSim does not provide access to the Albuquerque meteorological data.

**Response to EPA request for additional information:**

- Explain the use of emission factors from Colorado, meteorological data from Colorado, etc. instead of New Mexico.

The TANKS 4.0.9d meteorological data from Albuquerque, New Mexico was used in the original application and Revision 1. Working/breathing losses in this application were also calculated using Albuquerque, New Mexico meteorological data.

**Response to EPA request for additional information:**

- Provided an explanation on the meaning of “refinements” of VMGSym inputs.

Harvest was referring to conducting the modeling internally (rather than using an outside consultant) and using actual data from their operation of the facility rather than data Williams Four Corners, LLC may have been using.

As noted in previous responses to EPA, Harvest cannot compare the current calculations with previous applications. Harvest did not own or operate the facility at that time and does not have access to detailed information showing how past emissions were calculated. Harvest can only state that the emissions calculations in this application represent operations as they exist today.

**Response to EPA request for additional information:**

- The revised Facility's PTE calculations using worst case scenario of the condensate analysis over the 5-year term of the title V permit.

See the written description above and the calculations in this section.

**Response to EPA request for additional information:**

- The complete characterization of the inputs and outputs to the VMGSym software used to calculate flash emissions and explanation why the model is being used separate of another model used for working and breathing losses from tanks – specifically explain how the different models, i.e., VMGSym and the outdated Tanks 4.09d, used together provide more accurate emission estimates for tank emissions instead of a single model like either VMGSym or TankESP that would account for all three types of emissions.

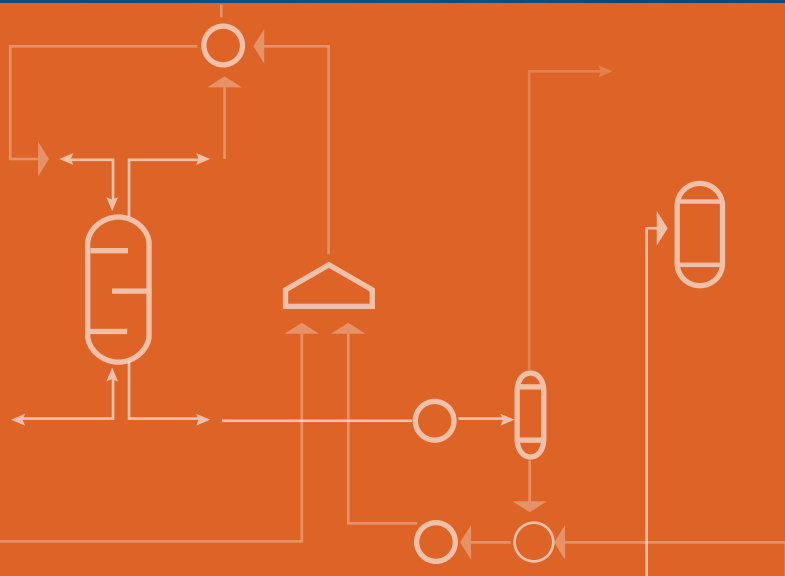
For VMGSim inputs and outputs, please see Page 3 of each of the VMGSim output files provided in this section (there is one output file for the PTE calculations and one for the actual emissions calculations).

VMGSim was selected because it is a sophisticated model that provides accurate estimates of flash emissions. From Schlumberger (the provider of VMGSim):

The Symmetry platform is powered by a best-in-class thermodynamic engine used for fluid representation, which is extensively validated against experimental data. The built-in database includes more than 20,000 chemicals, 80 thermodynamic property packages, and hundreds of unit operations, providing unparalleled model sophistication and precision.

Please see the attached brochure and VMG technical paper.

As noted above, Promax and VMGSim both use the AP-42 Chapter 7 equations/algorithms to calculate working/breathing losses. If VMGSim had been used to calculate the losses, results would have been essentially the same, except that unlike TANKS 4.0.9d, VMGSim does not provide access to the Albuquerque meteorological data.



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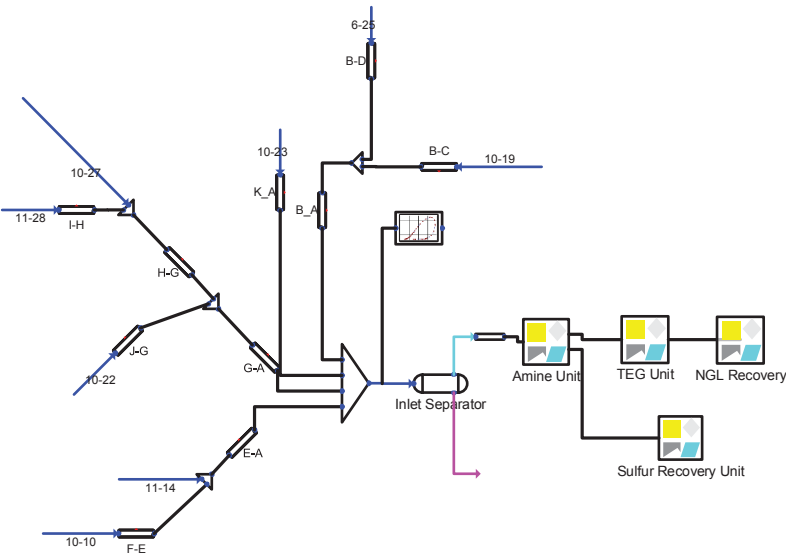
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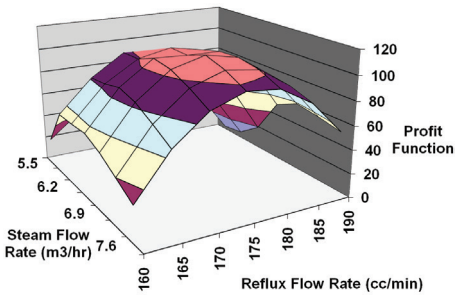


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# APPLICATIONS

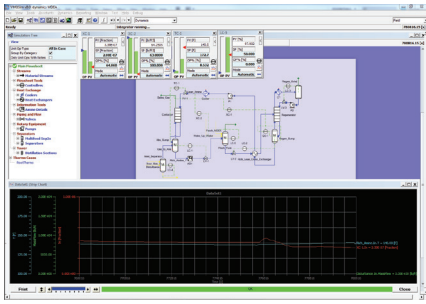
With VMGSim™, you get world-class simulation software capable of modeling various processes and applications:

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# Virtual Materials Group

## Overview and Products

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### Introduction

Virtual Materials Group (VMG) is focused on developing high quality and cost-effective software for the Process Industries. VMG provides its clients with proven, validated and robust thermo-physical property prediction packages for the hydrocarbon, chemicals and petrochemical industry. VMG's thermodynamic models are backed by extensive experimental data and development support provided by the VMG technical support team.

More recently, VMG developed a new steady-state, process flowsheet simulation called VMGSim. This simulator uses the same interactive calculation principles of non-sequential, unit operation calculations with partial data flow, which were developed in the late 1970's in Calgary and which are used today by most process engineers in the oil & gas production industry. The steady-state process simulator integrates a state of the art steady state process simulation kernel combined with Microsoft Visio for extensive graphics capabilities and Excel for spreadsheet calculations. VMGSim provides affordable steady-state process simulation with uncompromising quality.

Virtual Materials Group also provides high level consulting in custom process simulator development, custom process model building, operator training simulator development and thermodynamic model development.

### Background to VMG People

Most of the people involved in VMG have had extensive (15-25 years each) experience in thermodynamics and process simulation. One of the VMG partners founded Hyprotech and another developed and wrote most of HYSIM and then the original basis of HYSYS. The VMG development group has many years of writing, teaching and applying thermodynamic models to process simulation.

VMG's development team have been involved in thermodynamic modelling and creation of the software packages associated with thermodynamic modelling. VMG also has a close working relationship with the thermodynamic research group at NIST in the USA.

The basis of the flowsheet simulation program incorporates new ideas in flowsheet simulation relating to integrated tower models and sub-flowsheeting.

VMG's Associates around the world were all involved in marketing of, support of and user-training for HYSIM and HYSYS during the past 15-20 years. Most were involved in pioneering the move of process engineering software to personal computers and have remained involved as personal computers became the standard computer used for engineering calculations in the process industries. VMG's European Associate introduced PC-based process engineering to the European oil & gas industry in late 1984. The first



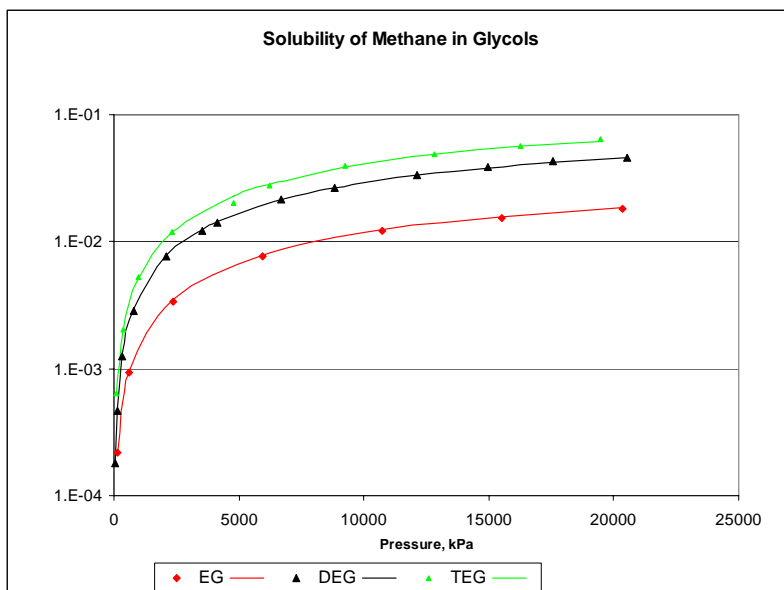
licenses of such software in Europe were delivered in 1984. VMG's Associates in the USA, Japan, Far and Middle East were all involved in pioneering PC-based and interactive process simulation in their respective countries.

## Oil & Gas Industry Applications

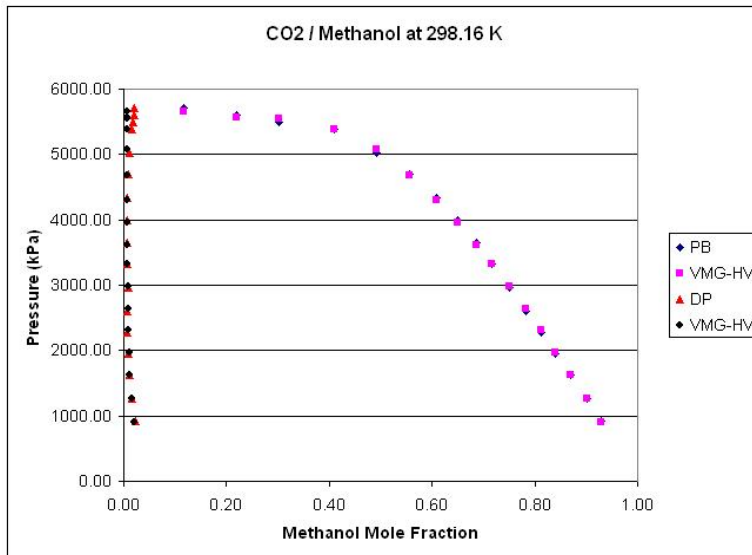
VMG have developed an advanced Peng-Robinson model within their thermodynamic package VMGThermo and initial work on VMG's steady-state process flowsheet simulator called VMGSim has been concentrated on the oil & gas production industry.

In addition to modelling "standard" hydrocarbon systems, VMG have recently paid special attention to extending their thermodynamic models towards accurate modelling of acid gas, mercury, glycols and hydrocarbons dissolved in glycols over wide operating ranges as well as taking salinity into account in the water phase for hydrate and hydrocarbon solubility predictions. The intention is to provide the oil & gas production industry with more accurate thermodynamic modelling than has been possible up to now.

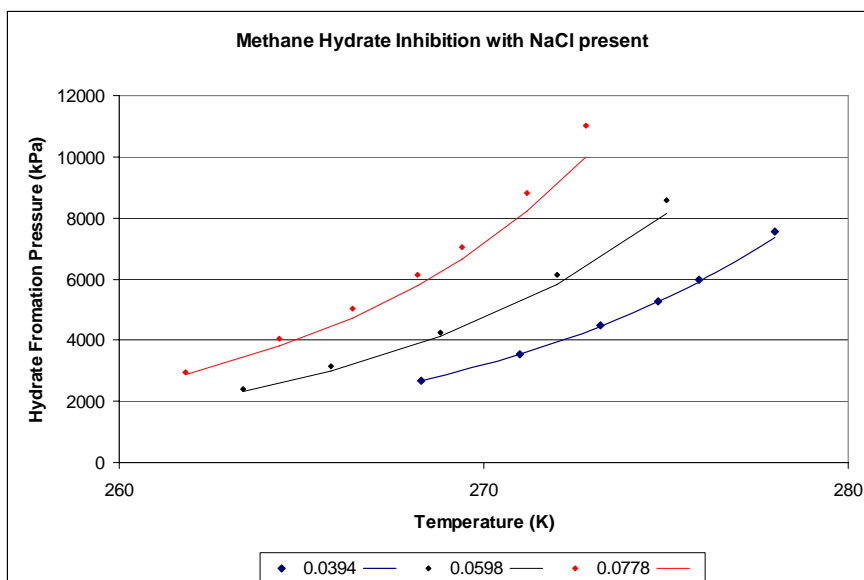
An example showing the experimental versus calculated values for solubility of methane in various glycols is shown below. This has been achieved by accurate fitting of vapour pressures for the components over wide ranges of temperatures then collection and validation of binary data which was then used to determine the thermodynamic model parameters.



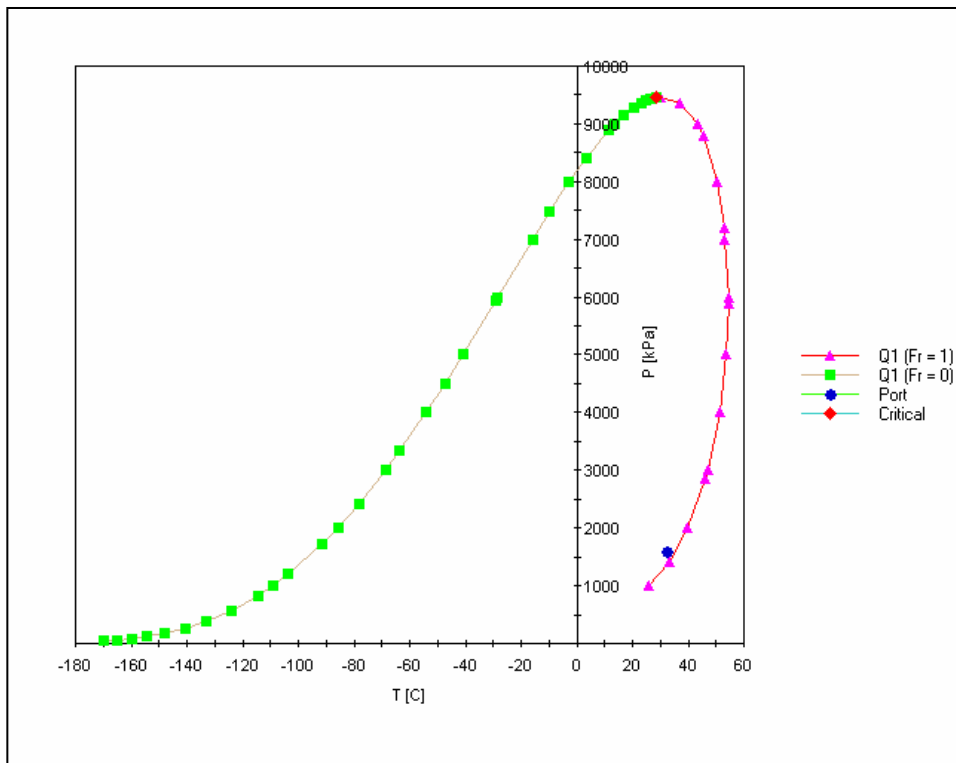
The Peng-Robinson model was extended to include a free energy term by Huron-Vidal and VMG's version of this powerful model is identified as GE-PR within the VMGThermo package. Calculation of the phase behaviour of CO<sub>2</sub>-methanol at 25°C over a range of pressures is shown in the diagram below with comparison to literature data.



Gas hydrates form in natural gas systems if water is present. The salinity of the water affects the hydrate formation temperature as the water activity is altered by the presence of salt. It is possible to predict this effect as shown below.



A phase envelope showing the dew and bubble point lines of a stream being produced from a reservoir is shown below. This was calculated within VMGSim using VMG's Advanced Peng Robinson thermodynamic model.

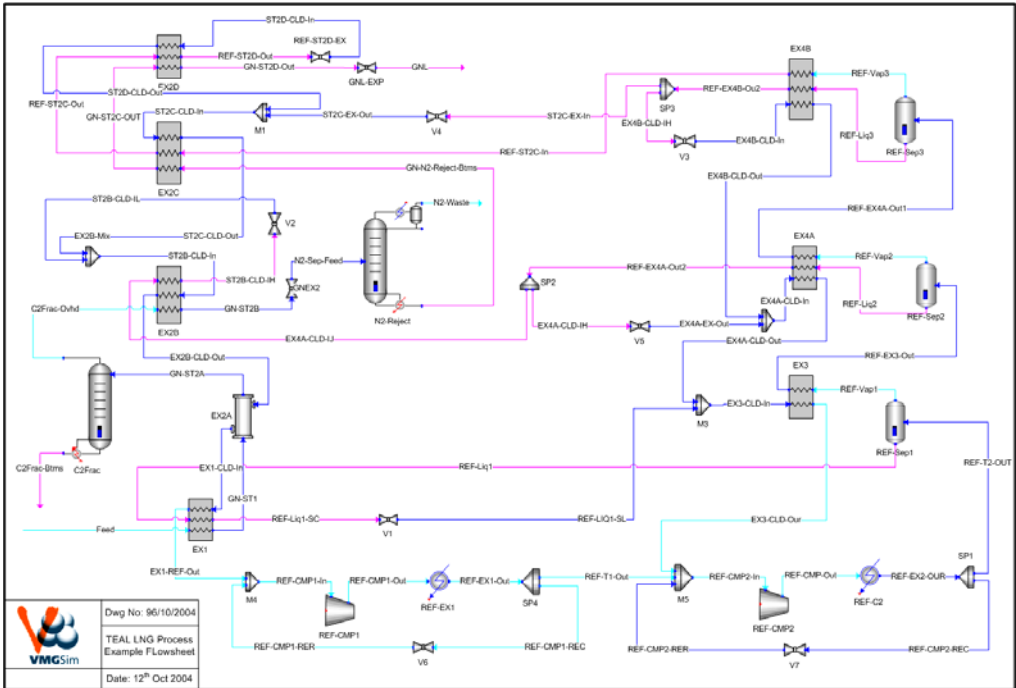


The true critical temperature and pressure of the stream as well as the cricondentherm and cricondenbar are also calculated and reported and shown below.

|                | P [kPa] | T [C] |
|----------------|---------|-------|
| Cricondenbar   | 9466.3  | 30.09 |
| Cricondentherm | 5886.9  | 54.44 |
| Crit_P         | 9455.2  |       |
| Crit_T         |         | 28.34 |

# Multi-stage Compression

| Name                | /Feed      | /S1        | /S2        | /HP-Gas    | /KO3Liq-to-M2 | /KO2liq-to-M1 | /KO1-OLiq | /KO1-Water |
|---------------------|------------|------------|------------|------------|---------------|---------------|-----------|------------|
| T [C]               | 30         | 30         | 30         | 40         | 23.445        | 25.915        | 29.059    | 29.059     |
| P [kPa]             | 1500       | 3000       | 6000       | 12000      | 3000          | 1500          | 1500      | 1500       |
| MoleFlow [kgmole/h] | 3526.92    | 3167.998   | 3115.929   | 3081.772   | 34.158        | 86.228        | 127.051   | 318.099    |
| Component Mole Flow |            |            |            |            |               |               |           |            |
| WATER               | 320.62909  | 8.68602    | 4.63057    | 2.58449    | 2.04608       | 6.10152       | 0.07558   | 317.96901  |
| NITROGEN            | 76.84413   | 76.87661   | 76.87373   | 76.76464   | 0.10908       | 0.11196       | 0.07811   | 0.00138    |
| CARBON DIOXIDE      | 44.82574   | 44.86541   | 44.74493   | 44.45844   | 0.28643       | 0.40692       | 0.34007   | 0.02718    |
| HYDROGEN SULFIDE    | 0          | 0          | 0          | 0          | 0             | 0             | 0         | 0          |
| METHANE             | 2432.26953 | 2434.52245 | 2432.72067 | 2424.62629 | 8.09499       | 9.89684       | 7.55996   | 0.08396    |
| ETHANE              | 276.47018  | 276.99342  | 274.90496  | 271.62742  | 3.27784       | 5.36634       | 4.83202   | 0.01109    |
| PROPANE             | 117.21781  | 117.22633  | 114.14951  | 111.01609  | 3.13365       | 6.21052       | 6.19809   | 0.00391    |
| ISOBUTANE           | 55.1793    | 54.56717   | 50.99928   | 48.32669   | 2.67263       | 6.24056       | 6.85227   | 0.00042    |
| n-BUTANE            | 50.93474   | 49.55673   | 45.0513    | 42.1068    | 2.94466       | 7.45014       | 8.82688   | 0.00127    |
| ISOPENTANE          | 38.20105   | 34.44107   | 28.23126   | 25.13192   | 3.09951       | 9.30939       | 13.06916  | 0.00022    |
| n-PENTANE           | 36.50323   | 31.25407   | 24.37901   | 21.28462   | 3.09443       | 9.96957       | 15.21855  | 0.00019    |
| n-HEXANE            | 77.84519   | 39.00876   | 19.24365   | 13.8447    | 5.39881       | 25.16383      | 64.00024  | 0.00002    |
| Total               | 3526.92    | 3167.998   | 3115.929   | 3081.772   | 34.158        | 86.228        | 127.051   | 318.099    |

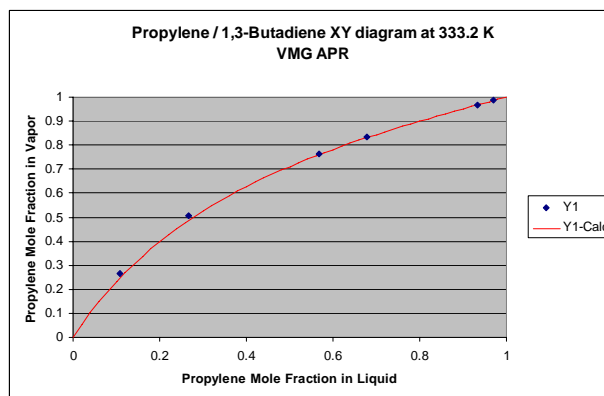
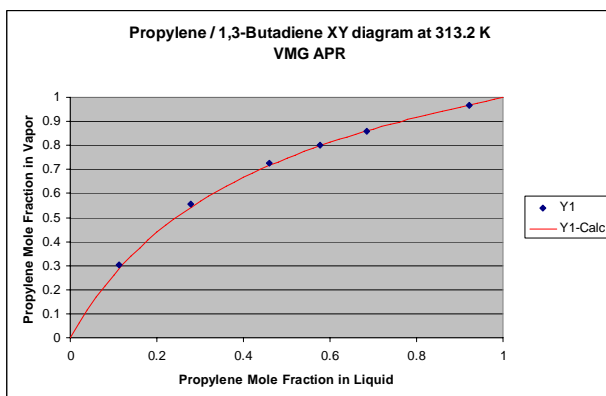


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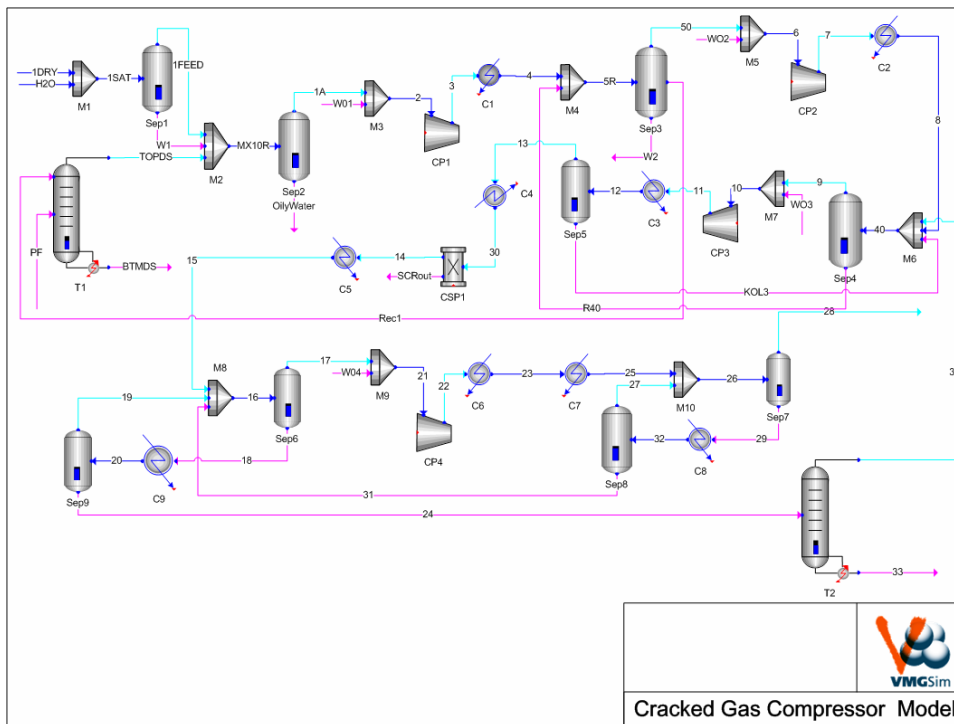
## Petrochemical Applications

VMGThermo and VMGSim have also been applied to petrochemical applications such as modelling of ethylene and propylene plants.

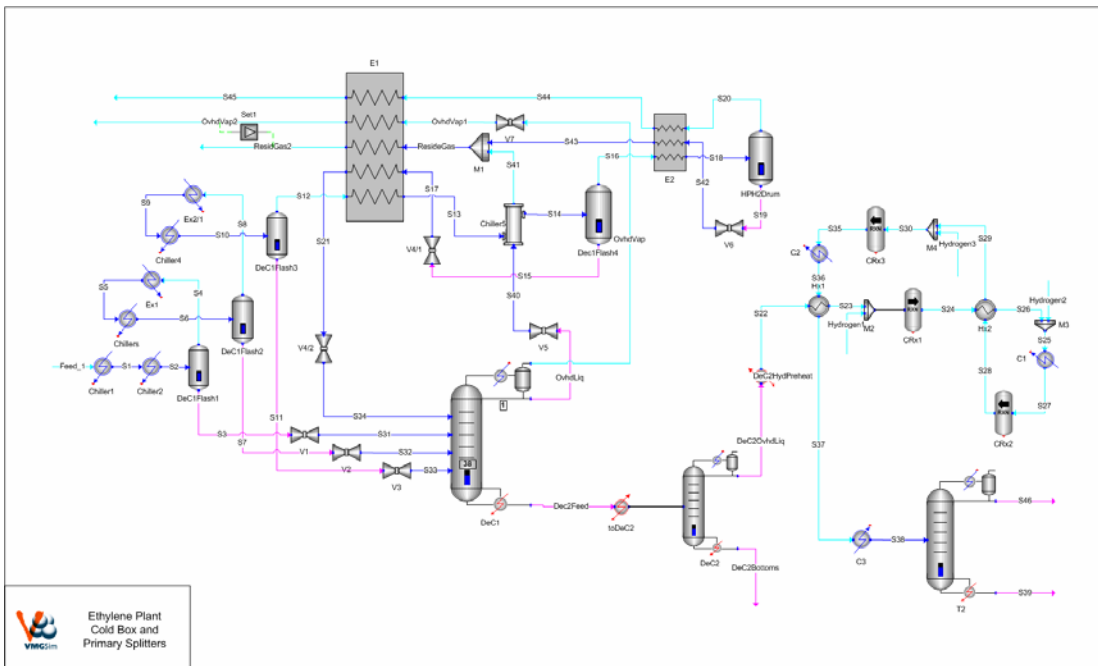
An accurate phase behaviour prediction for the fractionation in such plants is vital to achieve correct prediction of the compositions of products, particularly in mixtures such as propylene and butadiene. A couple of validation curves (XY diagrams) at two different temperatures are shown below.



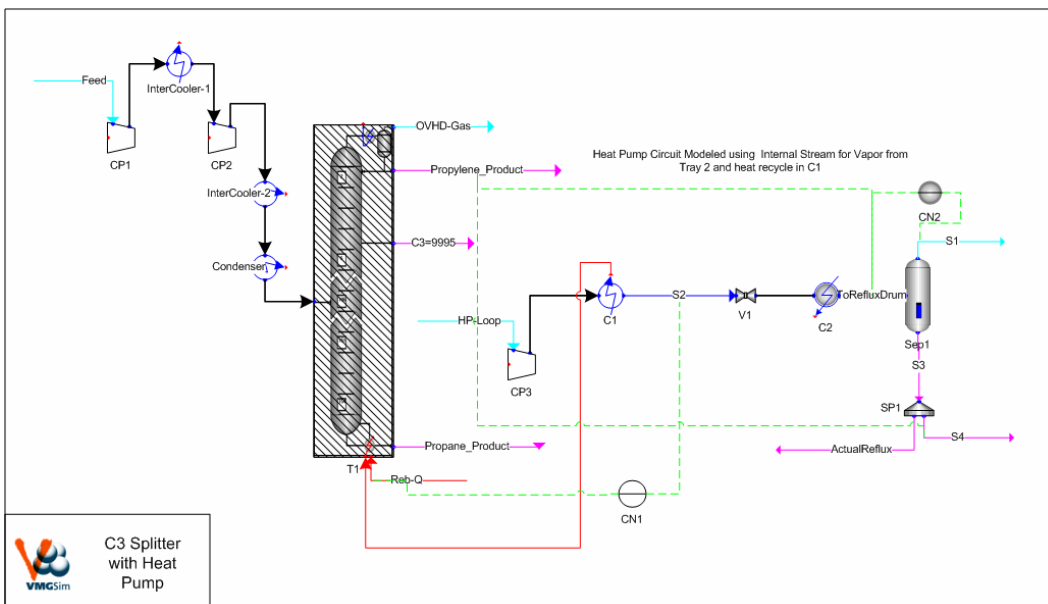
A series of example steady-state flowsheet models of sections from a typical ethylene plant were then developed:



The gas from the cracked gas compressor section is fed to the demethanizer section then the C2 components are split from the C2-rich liquid and in turn split into ethane and ethylene.



A simulation model schematic of a propane-propylene splitter with a heat pump system used to provide energy for the tower reboiler is shown below.

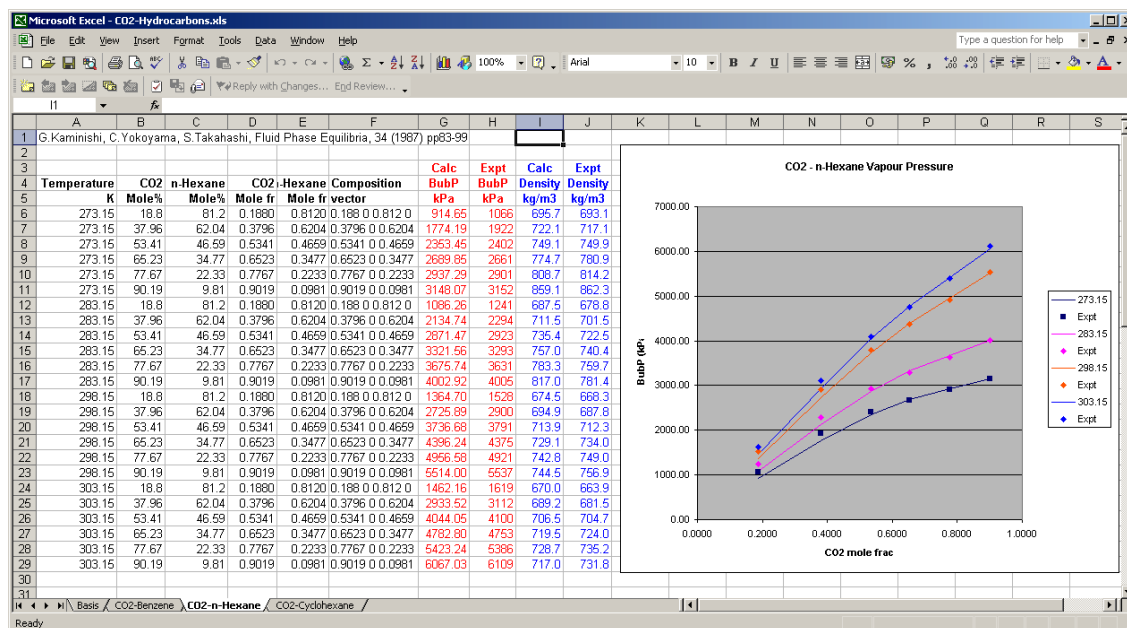




## Other Applications of VMGThermo

VMGThermo is now being used by a number of software vendors in the process industries for thermodynamic property calculations within their own software. The vendor list includes HTRI (heat exchanger design), Ariel Compressors, Schmart (relief valves) and Neotec (multiphase flow and production forecasting).

VMGThermo may also be run directly from Excel. An example showing the calculation of vapour pressure of a range of CO<sub>2</sub>-n-Hexane mixtures for a series of temperatures is shown below.



VMG will be developing a CAPE-OPEN interface for VMGThermo so that VMGThermo will be available for use with any CAPE-OPEN software package.

VMGThermo is also linked to IDEAS from IDEAS Simulation and formed the thermodynamic engine for a very large operator training system for an oil sands extraction plant in Alberta, which used a new solvent-based bitumen recovery process. During the process of development of the OTS the customer was also to check out the large process control system as well as identify and resolve problems in design of the control philosophy.

## **Conclusion**

VMGThermo is a general thermodynamic package which applies to mixture of components found in the oil & gas, petrochemical and chemical process industries as well as certain specialised processes such as fatty acid production, sulphuric acid manufacture and urea fertilizer plants. VMGThermo is wrapped in a generalised callable package and may be used from programs written in FORTRAN, C++, Python and Visual Basic as well as having a direct link to Excel.

VMGThermo has been extensively tested and validated by VMG and a number of partner companies. VMGThermo has been used in many industrial applications. VMGThermo is linked to several equipment design programs to provide accurate thermophysical properties for use in design calculations.

VMGSim is a new interactive steady-state flowsheet simulator driven by VMGThermo. VMGSim offers some interesting new features, flexibility and capabilities to process engineers in the process engineering industry.

## **Section 5.5**

**Condensate Storage Tanks (Units T1 & T2)**

**PTE Emission Calculations**

## Condensate Storage Tank PTE Emissions Data and Calculations

Unit Number: **T1 & T2**

Description: Condensate Storage Tanks

### Emission Rates

| Source/Pollutants | Working/Breathing Losses,<br>ppy tpy |          | Flash<br>Losses,<br>tpy | Uncontrolled<br>Emission<br>Rates,<br>tpy | 10%<br>Safety Factor<br>tpy |
|-------------------|--------------------------------------|----------|-------------------------|---|-----------------------------|
| <b>T1</b>         |                                      |          |                         |   |                             |
| VOC               | 9,458.83                             | 4.73     | 100.38                  | 105.10                                    | 115.61                      |
| Benzene           | 34.39                                | 1.72E-02 | 4.49E-01                | 4.66E-01                                  | 5.13E-01                    |
| Ethylbenzene      | 0.50                                 | 2.50E-04 | 5.59E-03                | 5.84E-03                                  | 6.42E-03                    |
| n-Hexane          | 1,289.93                             | 6.45E-01 | 9.95                    | 10.60                                     | 11.66                       |
| Isooctane         | 0.00                                 | 0.00E+00 | 0.00E+00                | 0.00E+00                                  | 0.00E+00                    |
| Toluene           | 24.86                                | 1.24E-02 | 2.75E-01                | 2.87E-01                                  | 3.16E-01                    |
| Xylene            | 2.85                                 | 1.43E-03 | 2.79E-02                | 2.93E-02                                  | 3.22E-02                    |
| <b>T2</b>         |                                      |          |                         |   |                             |
| VOC               | 9,932.45                             | 4.97     | --                      | 4.97                                      |                             |
| Benzene           | 36.11                                | 1.81E-02 | --                      | 1.81E-02                                  |                             |
| Ethylbenzene      | 0.52                                 | 2.60E-04 | --                      | 2.60E-04                                  |                             |
| n-Hexane          | 1,354.52                             | 6.77E-01 | --                      | 6.77E-01                                  |                             |
| Isooctane         | 0.00                                 | 0.00E+00 | --                      | 0.00E+00                                  |                             |
| Toluene           | 26.11                                | 1.31E-02 | --                      | 1.31E-02                                  |                             |
| Xylene            | 2.99                                 | 1.50E-03 | --                      | 1.50E-03                                  |                             |

Working/breathing losses taken from TANKS 4.0 results

Flash VOC emissions taken from VMGSim results

Flash HAP emissions calculated from the flash VOC emissions and the weight % HAP (calculated in the table below)

Unit T2 does not have flash emissions because it is an overflow tank for Unit T1. All flashing occurs in Unit T1.

## Condensate Storage Tank PTE Emissions Data and Calculations

Unit Number: T1 &amp; T2

Description: Condensate Storage Tanks

### Flash Emissions Composition (To Determine HAP Emissions)

| Components        | Mole<br>Percents,<br>% | Molecular<br>Weights,<br>lb/lb-mole | Component<br>Weights,<br>lb/lb-mole | Weight<br>Percent,<br>% |
|-------------------|------------------------|-------------------------------------|-------------------------------------|-------------------------|
| Carbon dioxide    | 0.5433                 | 44.010                              |                                     |                         |
| Hydrogen sulfide  | 0.0000                 | 34.070                              |                                     |                         |
| Nitrogen          | 0.4004                 | 28.013                              |                                     |                         |
| Water             | 0.0000                 | 18.015                              |                                     |                         |
| Methane           | 21.6866                | 16.043                              |                                     |                         |
| Ethane            | 20.2810                | 30.070                              |                                     |                         |
| Propane           | 25.1557                | 44.097                              | 1109.289                            | 33.965                  |
| Isobutane         | 6.1816                 | 58.123                              | 359.293                             | 11.001                  |
| n-Butane          | 11.4648                | 58.123                              | 666.370                             | 20.403                  |
| Isopentane        | 4.5748                 | 72.150                              | 330.073                             | 10.106                  |
| n-Pentane         | 3.8944                 | 72.150                              | 280.979                             | 8.603                   |
| Cyclopentane      | 0.0000                 | 70.134                              | 0.000                               | 0.000                   |
| n-Hexane          | 3.7581                 | 86.177                              | 323.859                             | 9.916                   |
| Cyclohexane       | 0.5328                 | 84.161                              | 44.839                              | 1.373                   |
| Other hexanes     | 0.0000                 | 86.177                              | 0.000                               | 0.000                   |
| Heptanes          | 1.0165                 | 100.204                             | 101.853                             | 3.119                   |
| Methylcyclohexane | 0.0000                 | 98.188                              | 0.000                               | 0.000                   |
| Isooctane         | 0.0000                 | 114.231                             | 0.000                               | 0.000                   |
| Benzene           | 0.1870                 | 78.114                              | 14.604                              | 0.447                   |
| Toluene           | 0.0970                 | 92.141                              | 8.940                               | 0.274                   |
| Ethylbenzene      | 0.0017                 | 106.167                             | 0.182                               | 0.006                   |
| Xylenes           | 0.0085                 | 106.167                             | 0.907                               | 0.028                   |
| n-Octane          | 0.2071                 | 114.232                             | 23.657                              | 0.724                   |
| n-Nonane          | 0.0085                 | 128.259                             | 1.085                               | 0.033                   |
| n-Decane          | 0.0003                 | 142.286                             | 0.041                               | 0.001                   |
| Total             | 100.0000               |                                     | 3265.971                            | 100.000                 |

Gas stream composition obtained from VGMSym output

Component Weights (lb/lb-mole) = (% / 100) \* Molecular Weights (lb/lb-mole)

Weight Percent of TOC (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)

## Condensate Storage Tank PTE Emissions Data and Calculations

Unit Number: **T1 & T2**

Description: Condensate Storage Tanks

### Condensate Composition (To Determine Working/Breathing Losses)

| Components        | Mole<br>Percents,<br>% | Molecular<br>Weights,<br>lb/lb-mole | Component<br>Weights,<br>lb/lb-mole | Weight<br>Percent,<br>% |
|-------------------|------------------------|-------------------------------------|-------------------------------------|-------------------------|
| Carbon dioxide    | 0.0078                 | 44.010                              |                                     |                         |
| Hydrogen sulfide  | 0.0000                 | 34.070                              |                                     |                         |
| Nitrogen          | 0.0005                 | 28.013                              |                                     |                         |
| Water             | 0.0000                 | 18.015                              |                                     |                         |
| Methane           | 0.1027                 | 16.043                              |                                     |                         |
| Ethane            | 0.6729                 | 30.070                              |                                     |                         |
| Propane           | 3.1038                 | 44.097                              | 136.8685                            | 1.5414                  |
| Isobutane         | 2.0276                 | 58.123                              | 117.8498                            | 1.3272                  |
| n-Butane          | 5.6863                 | 58.123                              | 330.5053                            | 3.7221                  |
| Isopentane        | 6.1242                 | 72.150                              | 441.8645                            | 4.9762                  |
| n-Pentane         | 6.7464                 | 72.150                              | 486.7492                            | 5.4817                  |
| Cyclopentane      | 0.0000                 | 70.134                              | 0.0000                              | 0.0000                  |
| n-Hexane          | 25.4671                | 86.177                              | 2194.6743                           | 24.7159                 |
| Cyclohexane       | 4.9821                 | 84.161                              | 419.2976                            | 4.7220                  |
| Other hexanes     | 0.0000                 | 86.177                              | 0.0000                              | 0.0000                  |
| Heptanes          | 23.0538                | 100.204                             | 2310.0869                           | 26.0157                 |
| Methylcyclohexane | 0.0000                 | 98.188                              | 0.0000                              | 0.0000                  |
| Isooctane         | 0.0000                 | 114.231                             | 0.0000                              | 0.0000                  |
| Benzene           | 1.2121                 | 78.114                              | 94.6820                             | 1.0663                  |
| Toluene           | 2.5643                 | 92.141                              | 236.2760                            | 2.6609                  |
| Ethylbenzene      | 0.1322                 | 106.167                             | 14.0390                             | 0.1581                  |
| Xylenes           | 0.9039                 | 106.167                             | 95.9682                             | 1.0808                  |
| n-Octane          | 14.9754                | 114.232                             | 1710.6720                           | 19.2652                 |
| n-Nonane          | 2.0107                 | 128.259                             | 257.8897                            | 2.9043                  |
| n-Decane          | 0.2262                 | 142.286                             | 32.1815                             | 0.3624                  |
| Total             | 100.0000               |                                     | 8879.6046                           | 100.0000                |

Gas stream composition obtained from VGMSym output

Component Weights (lb/lb-mole) = (% / 100) \* Molecular Weights (lb/lb-mole)

Weight Percent of TOC (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)

In TANKS 4, the propane percentage is included with isobutane and n-butane (an even distribution)

## Simulation Report



# Symmetry

**File Name:** 2018 Los Mestenos Emissions Flash Model 22141 bpy  
**Company:** VMG, a Schlumberger Technology  
**Customer:**  
**Project:**  
**Job No:**  
**Prepared By:**  
**Report Date:** Friday, October 21, 2022  
**Unit Set:** Field

File: U:\Environmental\Condensate Flash Calcs\Los Mestenos 17755 BBL 2017 to 2022\2018 Los Mestenos

Symmetry

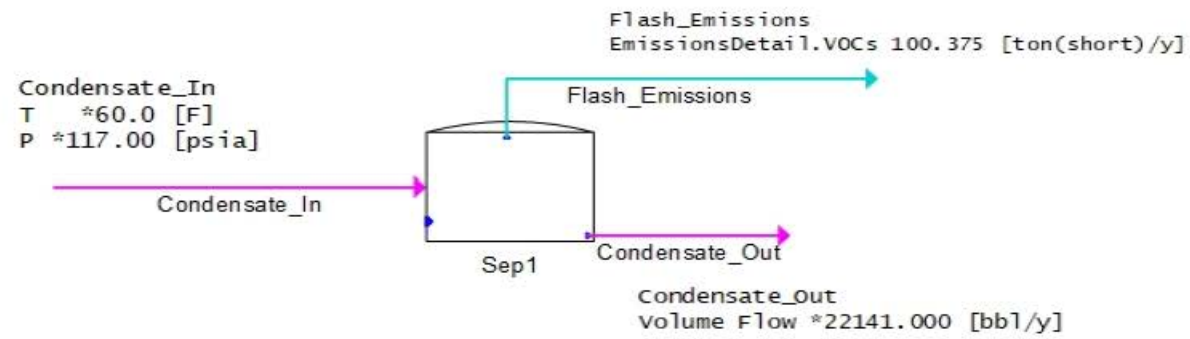
[Main Flowsheet](#)

[Material Stream \(3\)](#)

[2ph Separator \(1\)](#)

\*Bold face throughout the report denotes specified values.

\*Italic face throughout the report denotes recycle values.





Input Condensate Temperature: 60 °F  
 Input Condensate Pressure: 117 psia  
 Output Condensate Flow: 22,141 bbl/yr  
 Output Condensate Flow: 60.66 bbl/day  
 VOC Emission Rate: 100.38 tpy

| /Condensate_In (Material Stream) |                |                     |          |          |
|----------------------------------|----------------|---------------------|----------|----------|
| Thermo Model: APRNGL2            |                |                     |          |          |
| Connections                      |                |                     |          |          |
| Material Inlets                  |                |                     |          |          |
|                                  | Connection     | Up Stream Unit Op   |          |          |
| In                               | <Disconnected> | ---                 |          |          |
| Material Outlets                 |                |                     |          |          |
|                                  | Connection     | Down Stream Unit Op |          |          |
| Out                              | Sep1.In0       | ---                 |          |          |
| Allocation / Product Allocation  |                |                     |          |          |
| Auto Calculate                   | False          | Is Up To Date       |          | False    |
| Status                           | Y?No Results   |                     |          |          |
| Equilibrium Results              |                |                     |          |          |
|                                  | Bulk           | Vap                 | Liq0     | Liq1     |
| Phase Frac [Fraction]            | 1.00           | 0.00                | 1.00     | 0.00     |
| T [F]                            | 60.0           | 60.0                | 60.0     | 60.0     |
| P [psia]                         | 117.00         | 117.00              | 117.00   | 117.00   |
| Mole Flow [lbmol/h]              | 7.49           | 0.00                | 7.49     | 0.00     |
| Mass Flow [lb/h]                 | 633.74         | 0.00                | 633.74   | 0.00     |
| Fraction [Fraction]              |                |                     |          |          |
| NITROGEN                         | 3.80E-04       | 0.0441              | 3.80E-04 | 3.80E-04 |
| METHANE                          | 0.0213         | 0.6940              | 0.0213   | 0.0213   |
| CARBON DIOXIDE                   | 5.80E-04       | 0.0064              | 5.80E-04 | 5.80E-04 |
| ETHANE                           | 0.0251         | 0.1236              | 0.0251   | 0.0251   |
| PROPANE                          | 0.0517         | 0.0712              | 0.0517   | 0.0517   |
| ISOBUTANE                        | 0.0242         | 0.0129              | 0.0242   | 0.0242   |
| n-BUTANE                         | 0.0623         | 0.0223              | 0.0623   | 0.0623   |
| ISOPENTANE                       | 0.0598         | 0.0082              | 0.0598   | 0.0598   |
| n-PENTANE                        | 0.0648         | 0.0069              | 0.0648   | 0.0648   |
| CYCLOPENTANE                     | 0.00           | 0.00                | 0.00     | 0.00     |
| n-HEXANE                         | 0.2343         | 0.0067              | 0.2343   | 0.2343   |
| METHYLCYCLOHEXANE                | 0.00           | 0.00                | 0.00     | 0.00     |
| 2,2,4-TRIMETHYLPENTANE           | 0.00           | 0.00                | 0.00     | 0.00     |
| BENZENE                          | 0.0112         | 3.26E-04            | 0.0112   | 0.0112   |
| CYCLOHEXANE                      | 0.0457         | 9.41E-04            | 0.0457   | 0.0457   |
| n-HEPTANE                        | 0.2099         | 0.0019              | 0.2099   | 0.2099   |
| TOLUENE                          | 0.0233         | 1.74E-04            | 0.0233   | 0.0233   |
| n-OCTANE                         | 0.1359         | 3.94E-04            | 0.1359   | 0.1359   |
| ETHYLBENZENE                     | 0.0012         | 3.21E-06            | 0.0012   | 0.0012   |
| m-XYLENE                         | 0.0082         | 1.60E-05            | 0.0082   | 0.0082   |
| o-XYLENE                         | 0.00           | 0.00E+00            | 0.00     | 0.00     |
| n-NONANE                         | 0.0182         | 1.67E-05            | 0.0182   | 0.0182   |
| n-DECANE                         | 0.0021         | 5.98E-07            | 0.0021   | 0.0021   |
| n-UNDECANE                       | 0.00           | 0.00E+00            | 0.00     | 0.00     |
| n-DODECANE                       | 0.00           | 0.00E+00            | 0.00     | 0.00     |
| WATER                            | 0.00           | 0.00E+00            | 0.00     | 0.00     |

| /Condensate_Out (Material Stream) |                |                     |          |      |
|-----------------------------------|----------------|---------------------|----------|------|
| Thermo Model: APRNGL2             |                |                     |          |      |
| Connections                       |                |                     |          |      |
| Material Inlets                   |                |                     |          |      |
|                                   | Connection     | Up Stream Unit Op   |          |      |
| In                                | Sep1.Liq0      | ---                 |          |      |
| Material Outlets                  |                |                     |          |      |
|                                   | Connection     | Down Stream Unit Op |          |      |
| Out                               | <Disconnected> | ---                 |          |      |
| Allocation / Product Allocation   |                |                     |          |      |
| Auto Calculate                    | False          | Is Up To Date       | False    |      |
| Status                            | Y?No Results   |                     |          |      |
| Equilibrium Results               |                |                     |          |      |
|                                   | Bulk           | Vap                 | Liq0     | Liq1 |
| Phase Frac [Fraction]             | 1.00           | 0.00                | 1.00     |      |
| T [F]                             | 60.0           | 60.0                | 60.0     |      |
| P [psia]                          | 13.00          | 13.00               | 13.00    |      |
| Mole Flow [lbmol/h]               | 6.78           | 0.00                | 6.78     |      |
| Mass Flow [lb/h]                  | 603.86         | 0.00                | 603.86   |      |
| Fraction [Fraction]               |                |                     |          |      |
| NITROGEN                          | 5.16E-06       | 0.0040              | 5.16E-06 |      |
| METHANE                           | 0.0010         | 0.2169              | 0.0010   |      |
| CARBON DIOXIDE                    | 7.80E-05       | 0.0054              | 7.80E-05 |      |
| ETHANE                            | 0.0067         | 0.2028              | 0.0067   |      |
| PROPANE                           | 0.0310         | 0.2516              | 0.0310   |      |
| ISOBUTANE                         | 0.0203         | 0.0618              | 0.0203   |      |
| n-BUTANE                          | 0.0569         | 0.1146              | 0.0569   |      |
| ISOPENTANE                        | 0.0612         | 0.0457              | 0.0612   |      |
| n-PENTANE                         | 0.0675         | 0.0389              | 0.0675   |      |
| CYCLOPENTANE                      | 0.00           | 0.00                | 0.00     |      |
| n-HEXANE                          | 0.2547         | 0.0376              | 0.2547   |      |
| METHYLCYCLOHEXANE                 | 0.00           | 0.00                | 0.00     |      |
| 2,2,4-TRIMETHYLPENTANE            | 0.00           | 0.00                | 0.00     |      |
| BENZENE                           | 0.0121         | 0.0019              | 0.0121   |      |
| CYCLOHEXANE                       | 0.0498         | 0.0053              | 0.0498   |      |
| n-HEPTANE                         | 0.2305         | 0.0102              | 0.2305   |      |
| TOLUENE                           | 0.0256         | 9.70E-04            | 0.0256   |      |
| n-OCTANE                          | 0.1498         | 0.0021              | 0.1498   |      |
| ETHYLBENZENE                      | 0.0013         | 1.71E-05            | 0.0013   |      |
| m-XYLENE                          | 0.0090         | 8.54E-05            | 0.0090   |      |
| o-XYLENE                          | 0.00           | 0.00E+00            | 0.00     |      |
| n-NONANE                          | 0.0201         | 8.46E-05            | 0.0201   |      |
| n-DECANE                          | 0.0023         | 2.91E-06            | 0.0023   |      |
| n-UNDECANE                        | 0.00           | 0.00E+00            | 0.00     |      |
| n-DODECANE                        | 0.00           | 0.00E+00            | 0.00     |      |
| WATER                             | 0.00           | 0.00E+00            | 0.00     |      |

| /Flash_Emissions (Material Stream) |                |                     |          |      |
|------------------------------------|----------------|---------------------|----------|------|
| Thermo Model: APRNGL2              |                |                     |          |      |
| Connections                        |                |                     |          |      |
| Material Inlets                    |                |                     |          |      |
|                                    | Connection     | Up Stream Unit Op   |          |      |
| In                                 | Sep1.Vap       | ---                 |          |      |
| Material Outlets                   |                |                     |          |      |
|                                    | Connection     | Down Stream Unit Op |          |      |
| Out                                | <Disconnected> | ---                 |          |      |
| Allocation / Product Allocation    |                |                     |          |      |
| Auto Calculate                     | False          | Is Up To Date       | False    |      |
| Status                             | Y?No Results   |                     |          |      |
| Equilibrium Results                |                |                     |          |      |
|                                    | Bulk           | Vap                 | Liq0     | Liq1 |
| Phase Frac [Fraction]              | 1.00           | 1.00                | 0.00E+00 |      |
| T [F]                              | 60.0           | 60.0                | 60.0     |      |
| P [psia]                           | 13.00          | 13.00               | 13.00    |      |
| Mole Flow [lbmol/h]                | 0.70           | 0.70                | 0.00     |      |
| Mass Flow [lb/h]                   | 29.88          | 29.88               | 0.00     |      |
| Fraction [Fraction]                |                |                     |          |      |
| NITROGEN                           | 0.0040         | 0.0040              | 5.16E-06 |      |
| METHANE                            | 0.2169         | 0.2169              | 0.0010   |      |
| CARBON DIOXIDE                     | 0.0054         | 0.0054              | 7.80E-05 |      |
| ETHANE                             | 0.2028         | 0.2028              | 0.0067   |      |
| PROPANE                            | 0.2516         | 0.2516              | 0.0310   |      |
| ISOBUTANE                          | 0.0618         | 0.0618              | 0.0203   |      |
| n-BUTANE                           | 0.1146         | 0.1146              | 0.0569   |      |
| ISOPENTANE                         | 0.0457         | 0.0457              | 0.0612   |      |
| n-PENTANE                          | 0.0389         | 0.0389              | 0.0675   |      |
| CYCLOPENTANE                       | 0.00           | 0.00                | 0.00     |      |
| n-HEXANE                           | 0.0376         | 0.0376              | 0.2547   |      |
| METHYLCYCLOHEXANE                  | 0.00           | 0.00                | 0.00     |      |
| 2,2,4-TRIMETHYLPENTANE             | 0.00           | 0.00                | 0.00     |      |
| BENZENE                            | 0.0019         | 0.0019              | 0.0121   |      |
| CYCLOHEXANE                        | 0.0053         | 0.0053              | 0.0498   |      |
| n-HEPTANE                          | 0.0102         | 0.0102              | 0.2305   |      |
| TOLUENE                            | 9.70E-04       | 9.70E-04            | 0.0256   |      |
| n-OCTANE                           | 0.0021         | 0.0021              | 0.1498   |      |
| ETHYLBENZENE                       | 1.71E-05       | 1.71E-05            | 0.0013   |      |
| m-XYLENE                           | 8.54E-05       | 8.54E-05            | 0.0090   |      |
| o-XYLENE                           | 0.00E+00       | 0.00E+00            | 0.00     |      |
| n-NONANE                           | 8.46E-05       | 8.46E-05            | 0.0201   |      |
| n-DECANE                           | 2.91E-06       | 2.91E-06            | 0.0023   |      |
| n-UNDECANE                         | 0.00E+00       | 0.00E+00            | 0.00     |      |
| n-DODECANE                         | 0.00E+00       | 0.00E+00            | 0.00     |      |
| WATER                              | 0.00E+00       | 0.00E+00            | 0.00     |      |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

|                      |                                      |
|----------------------|--------------------------------------|
| User Identification: | Los Mestenos - T1 - Condensate (PTE) |
| City:                | Gavilan                              |
| State:               | New Mexico                           |
| Company:             | Harvest Four Corners, LLC            |
| Type of Tank:        | Vertical Fixed Roof Tank             |
| Description:         | 400 Barrel Condensate Storage Tank   |

**Tank Dimensions**

|                          |            |
|--------------------------|------------|
| Shell Height (ft):       | 20.00      |
| Diameter (ft):           | 12.00      |
| Liquid Height (ft) :     | 19.00      |
| Avg. Liquid Height (ft): | 9.50       |
| Volume (gallons):        | 16,075.00  |
| Turnovers:               | 57.85      |
| Net Throughput(gal/yr):  | 929,922.00 |
| Is Tank Heated (y/n):    | N          |

**Paint Characteristics**

|                    |             |
|--------------------|-------------|
| Shell Color/Shade: | Gray/Medium |
| Shell Condition    | Good        |
| Roof Color/Shade:  | Gray/Medium |
| Roof Condition:    | Good        |

**Roof Characteristics**

|                         |       |
|-------------------------|-------|
| Type:                   | Dome  |
| Height (ft)             | 0.00  |
| Radius (ft) (Dome Roof) | 12.00 |

**Breather Vent Settings**

|                          |       |
|--------------------------|-------|
| Vacuum Settings (psig):  | -0.03 |
| Pressure Settings (psig) | 0.03  |

Meterological Data used in Emissions Calculations: Albuquerque, New Mexico (Avg Atmospheric Pressure = 12.15 psia)

# **TANKS 4.0.9d** **Emissions Report - Detail Format** **Liquid Contents of Storage Tank**

## **Los Mestenios - T1 - Condensate (PTE) - Vertical Fixed Roof Tank** **Gavilan, New Mexico**

| Mixture/Component       | Month | Daily Liquid Surf.<br>Temperature (deg F) |       |       | Liquid<br>Bulk<br>Temp<br>(deg F) | Vapor Pressure (psia) |         |         | Vapor<br>Mol.<br>Weight. | Liquid<br>Mass<br>Fract. | Vapor<br>Mass<br>Fract. | Mol.<br>Weight | Basis for Vapor Pressure<br>Calculations |
|-------------------------|-------|---|-------|-------|-----------------------------------|-----------------------|---------|---------|--------------------------|--------------------------|-------------------------|----------------|--|
|                         |       | Avg.                                      | Min.  | Max.  |                                   | Avg.                  | Min.    | Max.    |                          |                          |                         |                |  |
| Condensate              | All   | 67.36                                     | 53.93 | 80.79 | 59.23                             | 5.6924                | 4.3318  | 7.1442  | 66.3202                  |                          |                         | 90.18          |  |
| Benzene                 |       |   |       |       |                                   | 1.4274                | 0.9846  | 2.0237  | 78.1100                  | 0.0107                   | 0.0036                  | 78.11          | Option 2: A=6.905, B=1211.033, C=220.79  |
| Butane (-n)             |       |   |       |       |                                   | 29.9357               | 23.3576 | 34.6684 | 58.1230                  | 0.0449                   | 0.3213                  | 58.12          | Option 1: VP60 = 26.1 VP70 = 31.31       |
| Cyclohexane             |       |   |       |       |                                   | 1.4738                | 1.0254  | 2.0729  | 84.1600                  | 0.0472                   | 0.0166                  | 84.16          | Option 2: A=6.841, B=1201.53, C=222.65   |
| Decane (-n)             |       |   |       |       |                                   | 0.0395                | 0.0291  | 0.0536  | 142.2900                 | 0.0036                   | 0.0000                  | 142.29         | Option 1: VP60 = .033211 VP70 = .041762  |
| Ethylbenzene            |       |   |       |       |                                   | 0.1396                | 0.0876  | 0.2162  | 106.1700                 | 0.0016                   | 0.0001                  | 106.17         | Option 2: A=6.975, B=1424.255, C=213.21  |
| Heptane (-n)            |       |   |       |       |                                   | 0.7600                | 0.5088  | 1.1128  | 100.2000                 | 0.2602                   | 0.0472                  | 100.20         | Option 3: A=37358, B=8.2585              |
| Hexane (-n)             |       |   |       |       |                                   | 2.3100                | 1.6303  | 3.2059  | 86.1700                  | 0.2472                   | 0.1364                  | 86.17          | Option 2: A=6.876, B=1171.17, C=224.41   |
| Iso-Butane              |       |   |       |       |                                   | 43.3083               | 34.4026 | 53.8185 | 58.1230                  | 0.0210                   | 0.2170                  | 58.12          | Option 1: VP60 = 38.14 VP70 = 45.16      |
| Isopentane              |       |   |       |       |                                   | 11.8640               | 8.7212  | 15.5743 | 72.1500                  | 0.0498                   | 0.1410                  | 72.15          | Option 1: VP60 = 10.005 VP70 = 12.53     |
| Nonane (-n)             |       |   |       |       |                                   | 0.0784                | 0.0568  | 0.1080  | 128.2600                 | 0.0290                   | 0.0005                  | 128.26         | Option 1: VP60 = .065278 VP70 = .08309   |
| Octane (-n)             |       |   |       |       |                                   | 0.1769                | 0.1254  | 0.2493  | 114.2300                 | 0.1927                   | 0.0081                  | 114.23         | Option 1: VP60 = .145444 VP70 = .188224  |
| Pentane (-n)            |       |   |       |       |                                   | 8.0308                | 5.9649  | 10.6537 | 72.1500                  | 0.0548                   | 0.1052                  | 72.15          | Option 3: A=27691, B=7.558               |
| Toluene                 |       |   |       |       |                                   | 0.4136                | 0.2726  | 0.6120  | 92.1300                  | 0.0266                   | 0.0026                  | 92.13          | Option 2: A=6.954, B=1344.8, C=219.48    |
| Xylenes (mixed isomers) |       |   |       |       |                                   | 0.1165                | 0.0728  | 0.1813  | 106.1700                 | 0.0108                   | 0.0003                  | 106.17         | Option 2: A=7.009, B=1462.266, C=215.11  |

## TANKS 4.0.9d

### Emissions Report - Detail Format

### Detail Calculations (AP-42)

#### Los Mestenos - T1 - Condensate (PTE) - Vertical Fixed Roof Tank Gavilan, New Mexico

|  |            |
|--|------------|
| <b>Annual Emission Calculations</b>                                |            |
| Standing Losses (lb):  | 3,731.0793 |
| Vapor Space Volume (cu ft):  | 1,280.6108 |
| Vapor Density (lb/cu ft):  | 0.0668     |
| Vapor Space Expansion Factor:                                      | 0.5281     |
| Vented Vapor Saturation Factor:                                    | 0.2264     |
| <b>Tank Vapor Space Volume:</b>                                    |            |
| Vapor Space Volume (cu ft):  | 1,280.6108 |
| Tank Diameter (ft):  | 12.0000    |
| Vapor Space Outage (ft):   | 11.3231    |
| Tank Shell Height (ft):  | 20.0000    |
| Average Liquid Height (ft):  | 9.5000     |
| Roof Outage (ft):  | 0.8231     |
| <b>Roof Outage (Dome Roof)</b>                                     |            |
| Roof Outage (ft):  | 0.8231     |
| Dome Radius (ft):  | 12.0000    |
| Shell Radius (ft):   | 6.0000     |
| <b>Vapor Density</b>   |            |
| Vapor Density (lb/cu ft):  | 0.0668     |
| Vapor Molecular Weight (lb/lb-mole):                               | 66.3202    |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 5.6924     |
| Daily Avg. Liquid Surface Temp. (deg. R):                          | 527.0322   |
| Daily Average Ambient Temp. (deg. F):                              | 56.1542    |
| Ideal Gas Constant R (psia cu ft / (lb-mol-deg R)):                | 10.731     |
| Liquid Bulk Temperature (deg. R):                                  | 518.9042   |
| Tank Paint Solar Absorptance (Shell):                              | 0.6800     |
| Tank Paint Solar Absorptance (Roof):                               | 0.6800     |
| Daily Total Solar Insulation Factor (Btu/sqft day):                | 1,765.3167 |
| <b>Vapor Space Expansion Factor</b>                                |            |
| Vapor Space Expansion Factor:                                      | 0.5281     |
| Daily Vapor Temperature Range (deg. R):                            | 53.7176    |
| Daily Vapor Pressure Range (psia):                                 | 2.8124     |
| Breather Vent Press. Setting Range(psia):                          | 0.0600     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 5.6924     |
| Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia): | 4.3318     |
| Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia): | 7.1442     |
| Daily Avg. Liquid Surface Temp. (deg R):                           | 527.0322   |
| Daily Min. Liquid Surface Temp. (deg R):                           | 513.6028   |
| Daily Max. Liquid Surface Temp. (deg R):                           | 540.4617   |
| Daily Ambient Temp. Range (deg. R):                                | 27.9250    |
| <b>Vented Vapor Saturation Factor</b>                              |            |
| Vented Vapor Saturation Factor:                                    | 0.2264     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 5.6924     |
| Vapor Space Outage (ft):   | 11.3231    |
| Working Losses (lb):   | 5,727.7476 |

|  |              |
|--|--------------|
| Vapor Molecular Weight (lb/lb-mole):   | 66.3202      |
| Vapor Pressure at Daily Average Liquid |              |
| Surface Temperature (psia):            | 5.6924       |
| Annual Net Throughput (gal/yr.):       | 929,922.0000 |
| Annual Turnovers:                      | 57.8500      |
| Turnover Factor:                       | 0.6852       |
| Maximum Liquid Volume (gal):           | 16,075.0000  |
| Maximum Liquid Height (ft):            | 19.0000      |
| Tank Diameter (ft):                    | 12.0000      |
| Working Loss Product Factor:           | 1.0000       |
|  |              |
| Total Losses (lb):                     | 9,458.8269   |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Los Mestenos - T1 - Condensate (PTE) - Vertical Fixed Roof Tank**  
**Gavilan, New Mexico**

|                         | Losses(lbs)  |                |                 |
|-------------------------|--------------|----------------|-----------------|
| Components              | Working Loss | Breathing Loss | Total Emissions |
| Condensate              | 5,727.75     | 3,731.08       | 9,458.83        |
| Iso-Butane              | 1,242.99     | 809.69         | 2,052.68        |
| Butane (-n)             | 1,840.05     | 1,198.62       | 3,038.67        |
| Pentane (-n)            | 602.29       | 392.34         | 994.63          |
| Hexane (-n)             | 781.11       | 508.82         | 1,289.93        |
| Cyclohexane             | 95.21        | 62.02          | 157.24          |
| Heptane (-n)            | 270.52       | 176.22         | 446.73          |
| Benzene                 | 20.82        | 13.57          | 34.39           |
| Toluene                 | 15.06        | 9.81           | 24.86           |
| Ethylbenzene            | 0.30         | 0.20           | 0.50            |
| Xylenes (mixed isomers) | 1.72         | 1.12           | 2.85            |
| Octane (-n)             | 46.64        | 30.38          | 77.02           |
| Nonane (-n)             | 3.11         | 2.03           | 5.14            |
| Decane (-n)             | 0.20         | 0.13           | 0.32            |
| Isopentane              | 807.72       | 526.15         | 1,333.87        |



**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

|                      |                                      |
|----------------------|--------------------------------------|
| User Identification: | Los Mestenos - T2 - Condensate (PTE) |
| City:                | Gavilan                              |
| State:               | New Mexico                           |
| Company:             | Harvest Four Corners, LLC            |
| Type of Tank:        | Vertical Fixed Roof Tank             |
| Description:         | 400 Barrel Condensate Storage Tank   |

**Tank Dimensions**

|                          |            |
|--------------------------|------------|
| Shell Height (ft):       | 12.83      |
| Diameter (ft):           | 15.50      |
| Liquid Height (ft) :     | 11.83      |
| Avg. Liquid Height (ft): | 6.00       |
| Volume (gallons):        | 16,800.00  |
| Turnovers:               | 27.68      |
| Net Throughput(gal/yr):  | 464,961.00 |
| Is Tank Heated (y/n):    | N          |

**Paint Characteristics**

|                    |             |
|--------------------|-------------|
| Shell Color/Shade: | Gray/Medium |
| Shell Condition    | Good        |
| Roof Color/Shade:  | Gray/Medium |
| Roof Condition:    | Good        |

**Roof Characteristics**

|                         |       |
|-------------------------|-------|
| Type:                   | Dome  |
| Height (ft)             | 0.00  |
| Radius (ft) (Dome Roof) | 12.00 |

**Breather Vent Settings**

|                          |       |
|--------------------------|-------|
| Vacuum Settings (psig):  | -0.03 |
| Pressure Settings (psig) | 0.03  |

Meterological Data used in Emissions Calculations: Albuquerque, New Mexico (Avg Atmospheric Pressure = 12.15 psia)

## TANKS 4.0.9d

### Emissions Report - Detail Format

### Liquid Contents of Storage Tank

#### Los Mestenos - T2 - Condensate (PTE) - Vertical Fixed Roof Tank Gavilan, New Mexico

| Mixture/Component       | Month | Daily Liquid Surf.<br>Temperature (deg F) |       |       | Liquid<br>Bulk<br>Temp<br>(deg F) | Vapor Pressure (psia) |         |         | Vapor<br>Mol.<br>Weight. | Liquid<br>Mass<br>Fract. | Vapor<br>Mass<br>Fract. | Mol.<br>Weight | Basis for Vapor Pressure<br>Calculations |
|-------------------------|-------|---|-------|-------|-----------------------------------|-----------------------|---------|---------|--------------------------|--------------------------|-------------------------|----------------|--|
|                         |       | Avg.                                      | Min.  | Max.  |                                   | Avg.                  | Min.    | Max.    |                          |                          |                         |                |  |
| Condensate              | All   | 67.36                                     | 53.93 | 80.79 | 59.23                             | 5.6924                | 4.3318  | 7.1442  | 66.3202                  |                          |                         | 90.18          |  |
| Benzene                 |       |   |       |       |                                   | 1.4274                | 0.9846  | 2.0237  | 78.1100                  | 0.0107                   | 0.0036                  | 78.11          | Option 2: A=6.905, B=1211.033, C=220.79  |
| Butane (-n)             |       |   |       |       |                                   | 29.9357               | 23.3576 | 34.6684 | 58.1230                  | 0.0449                   | 0.3213                  | 58.12          | Option 1: VP60 = 26.1 VP70 = 31.31       |
| Cyclohexane             |       |   |       |       |                                   | 1.4738                | 1.0254  | 2.0729  | 84.1600                  | 0.0472                   | 0.0166                  | 84.16          | Option 2: A=6.841, B=1201.53, C=222.65   |
| Decane (-n)             |       |   |       |       |                                   | 0.0395                | 0.0291  | 0.0536  | 142.2900                 | 0.0036                   | 0.0000                  | 142.29         | Option 1: VP60 = .033211 VP70 = .041762  |
| Ethylbenzene            |       |   |       |       |                                   | 0.1396                | 0.0876  | 0.2162  | 106.1700                 | 0.0016                   | 0.0001                  | 106.17         | Option 2: A=6.975, B=1424.255, C=213.21  |
| Heptane (-n)            |       |   |       |       |                                   | 0.7600                | 0.5088  | 1.1128  | 100.2000                 | 0.2602                   | 0.0472                  | 100.20         | Option 3: A=37358, B=8.2585              |
| Hexane (-n)             |       |   |       |       |                                   | 2.3100                | 1.6303  | 3.2059  | 86.1700                  | 0.2472                   | 0.1364                  | 86.17          | Option 2: A=6.876, B=1171.17, C=224.41   |
| Iso-Butane              |       |   |       |       |                                   | 43.3083               | 34.4026 | 53.8185 | 58.1230                  | 0.0210                   | 0.2170                  | 58.12          | Option 1: VP60 = 38.14 VP70 = 45.16      |
| Isopentane              |       |   |       |       |                                   | 11.8640               | 8.7212  | 15.5743 | 72.1500                  | 0.0498                   | 0.1410                  | 72.15          | Option 1: VP60 = 10.005 VP70 = 12.53     |
| Nonane (-n)             |       |   |       |       |                                   | 0.0784                | 0.0568  | 0.1080  | 128.2600                 | 0.0290                   | 0.0005                  | 128.26         | Option 1: VP60 = .065278 VP70 = .08309   |
| Octane (-n)             |       |   |       |       |                                   | 0.1769                | 0.1254  | 0.2493  | 114.2300                 | 0.1927                   | 0.0081                  | 114.23         | Option 1: VP60 = .145444 VP70 = .188224  |
| Pentane (-n)            |       |   |       |       |                                   | 8.0308                | 5.9649  | 10.6537 | 72.1500                  | 0.0548                   | 0.1052                  | 72.15          | Option 3: A=27691, B=7.558               |
| Toluene                 |       |   |       |       |                                   | 0.4136                | 0.2726  | 0.6120  | 92.1300                  | 0.0266                   | 0.0026                  | 92.13          | Option 2: A=6.954, B=1344.8, C=219.48    |
| Xylenes (mixed isomers) |       |   |       |       |                                   | 0.1165                | 0.0728  | 0.1813  | 106.1700                 | 0.0108                   | 0.0003                  | 106.17         | Option 2: A=7.009, B=1462.266, C=215.11  |

## TANKS 4.0.9d

### Emissions Report - Detail Format

### Detail Calculations (AP-42)

#### Los Mestenos - T2 - Condensate (PTE) - Vertical Fixed Roof Tank Gavilan, New Mexico

|  |            |
|--|------------|
| <b>Annual Emission Calculations</b>                                |            |
| Standing Losses (lb):  | 5,753.1321 |
| Vapor Space Volume (cu ft):  | 1,568.5156 |
| Vapor Density (lb/cu ft):  | 0.0668     |
| Vapor Space Expansion Factor:                                      | 0.5281     |
| Vented Vapor Saturation Factor:                                    | 0.2851     |
| <b>Tank Vapor Space Volume:</b>                                    |            |
| Vapor Space Volume (cu ft):  | 1,568.5156 |
| Tank Diameter (ft):  | 15.5000    |
| Vapor Space Outage (ft):   | 8.3126     |
| Tank Shell Height (ft):  | 12.8300    |
| Average Liquid Height (ft):  | 6.0000     |
| Roof Outage (ft):  | 1.4826     |
| <b>Roof Outage (Dome Roof)</b>                                     |            |
| Roof Outage (ft):  | 1.4826     |
| Dome Radius (ft):  | 12.0000    |
| Shell Radius (ft):   | 7.7500     |
| <b>Vapor Density</b>   |            |
| Vapor Density (lb/cu ft):  | 0.0668     |
| Vapor Molecular Weight (lb/lb-mole):                               | 66.3202    |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 5.6924     |
| Daily Avg. Liquid Surface Temp. (deg. R):                          | 527.0322   |
| Daily Average Ambient Temp. (deg. F):                              | 56.1542    |
| Ideal Gas Constant R (psia cu ft / (lb-mol-deg R)):                | 10.731     |
| Liquid Bulk Temperature (deg. R):                                  | 518.9042   |
| Tank Paint Solar Absorptance (Shell):                              | 0.6800     |
| Tank Paint Solar Absorptance (Roof):                               | 0.6800     |
| Daily Total Solar Insulation Factor (Btu/sqft day):                | 1,765.3167 |
| <b>Vapor Space Expansion Factor</b>                                |            |
| Vapor Space Expansion Factor:                                      | 0.5281     |
| Daily Vapor Temperature Range (deg. R):                            | 53.7176    |
| Daily Vapor Pressure Range (psia):                                 | 2.8124     |
| Breather Vent Press. Setting Range (psia):                         | 0.0600     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 5.6924     |
| Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia): | 4.3318     |
| Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia): | 7.1442     |
| Daily Avg. Liquid Surface Temp. (deg R):                           | 527.0322   |
| Daily Min. Liquid Surface Temp. (deg R):                           | 513.6028   |
| Daily Max. Liquid Surface Temp. (deg R):                           | 540.4617   |
| Daily Ambient Temp. Range (deg. R):                                | 27.9250    |
| <b>Vented Vapor Saturation Factor</b>                              |            |
| Vented Vapor Saturation Factor:                                    | 0.2851     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 5.6924     |
| Vapor Space Outage (ft):   | 8.3126     |
| Working Losses (lb):   | 4,179.3172 |

|  |              |
|--|--------------|
| Vapor Molecular Weight (lb/lb-mole):   | 66.3202      |
| Vapor Pressure at Daily Average Liquid |              |
| Surface Temperature (psia):            | 5.6924       |
| Annual Net Throughput (gal/yr.):       | 464,961.0000 |
| Annual Turnovers:                      | 27.6800      |
| Turnover Factor:                       | 1.0000       |
| Maximum Liquid Volume (gal):           | 16,800.0000  |
| Maximum Liquid Height (ft):            | 11.8300      |
| Tank Diameter (ft):                    | 15.5000      |
| Working Loss Product Factor:           | 1.0000       |
|  |              |
| Total Losses (lb):                     | 9,932.4493   |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Los Mestenos - T2 - Condensate (PTE) - Vertical Fixed Roof Tank**  
**Gavilan, New Mexico**

|                         | Losses(lbs)  |                |                 |
|-------------------------|--------------|----------------|-----------------|
| Components              | Working Loss | Breathing Loss | Total Emissions |
| Condensate              | 4,179.32     | 5,753.13       | 9,932.45        |
| Iso-Butane              | 906.96       | 1,248.50       | 2,155.46        |
| Butane (-n)             | 1,342.61     | 1,848.21       | 3,190.82        |
| Isopentane              | 589.36       | 811.30         | 1,400.66        |
| Benzene                 | 15.19        | 20.92          | 36.11           |
| Toluene                 | 10.99        | 15.12          | 26.11           |
| Pentane (-n)            | 439.47       | 604.96         | 1,044.43        |
| Hexane (-n)             | 569.95       | 784.57         | 1,354.52        |
| Ethylbenzene            | 0.22         | 0.30           | 0.52            |
| Xylenes (mixed isomers) | 1.26         | 1.73           | 2.99            |
| Octane (-n)             | 34.03        | 46.84          | 80.87           |
| Nonane (-n)             | 2.27         | 3.13           | 5.40            |
| Decane (-n)             | 0.14         | 0.20           | 0.34            |
| Cyclohexane             | 69.47        | 95.64          | 165.11          |
| Heptane (-n)            | 197.38       | 271.71         | 469.10          |

## **Section 5.5**

**Condensate Storage Tanks (Units T1 & T2)**

**Actual Emission Calculations**

## Condensate Storage Tank Actual Emissions Data and Calculations

Unit Number: **T1 & T2**

Description: Condensate Storage Tanks

### Emission Rates

| Source/Pollutants | Working/Breathing Losses,<br>ppy tpy |          | Flash<br>Losses,<br>tpy | Uncontrolled<br>Emission<br>Rates,<br>tpy |
|-------------------|--------------------------------------|----------|-------------------------|---|
| <b>T1</b>         |                                      |          |                         |   |
| VOC               | 2,803.84                             | 1.40     | 5.72                    | 7.12                                      |
| Benzene           | 15.56                                | 7.78E-03 | 4.01E-02                | 4.79E-02                                  |
| Ethylbenzene      | 0.85                                 | 4.25E-04 | 1.98E-03                | 2.41E-03                                  |
| n-Hexane          | 242.18                               | 1.21E-01 | 4.49E-01                | 5.70E-01                                  |
| Isooctane         | 3.04                                 | 1.52E-03 | 5.32E-03                | 6.84E-03                                  |
| Toluene           | 2.04                                 | 1.02E-03 | 4.64E-03                | 5.66E-03                                  |
| Xylene            | 3.40                                 | 1.70E-03 | 9.60E-03                | 1.13E-02                                  |
| <b>T2</b>         |                                      |          |                         |   |
| VOC               | 3,257.57                             | 1.63     | --                      | 1.63                                      |
| Benzene           | 18.08                                | 9.04E-03 | --                      | 9.04E-03                                  |
| Ethylbenzene      | 0.99                                 | 4.95E-04 | --                      | 4.95E-04                                  |
| n-Hexane          | 281.37                               | 1.41E-01 | --                      | 1.41E-01                                  |
| Isooctane         | 3.54                                 | 1.77E-03 | --                      | 1.77E-03                                  |
| Toluene           | 2.37                                 | 1.19E-03 | --                      | 1.19E-03                                  |
| Xylene            | 3.95                                 | 1.98E-03 | --                      | 1.98E-03                                  |

Working/breathing losses taken from TANKS 4.0 results

Flash VOC emissions taken from VMGSim results

Flash HAP emissions calculated from the flash VOC emissions and the weight % HAP (calculated in the table below)

Unit T2 does not have flash emissions because it is an overflow tank for Unit T1. All flashing occurs in Unit T1.

## Condensate Storage Tank Actual Emissions Data and Calculations

Unit Number: **T1 & T2**

Description: Condensate Storage Tanks

### Flash Emissions Composition (To Determine HAP Emissions)

| Components        | Mole<br>Percents,<br>% | Molecular<br>Weights,<br>lb/lb-mole | Component<br>Weights,<br>lb/lb-mole | Weight<br>Percent,<br>% |
|-------------------|------------------------|-------------------------------------|-------------------------------------|-------------------------|
| Carbon dioxide    | 0.1288                 | 44.010                              |                                     |                         |
| Hydrogen sulfide  | 0.0000                 | 34.070                              |                                     |                         |
| Nitrogen          | 1.6104                 | 28.013                              |                                     |                         |
| Water             | 0.0000                 | 18.015                              |                                     |                         |
| Methane           | 62.5659                | 16.043                              |                                     |                         |
| Ethane            | 9.7156                 | 30.070                              |                                     |                         |
| Propane           | 2.9900                 | 44.097                              | 131.850                             | 7.865                   |
| Isobutane         | 4.4177                 | 58.123                              | 256.770                             | 15.316                  |
| n-Butane          | 8.4598                 | 58.123                              | 491.706                             | 29.329                  |
| Isopentane        | 4.0103                 | 72.150                              | 289.346                             | 17.259                  |
| n-Pentane         | 2.7352                 | 72.150                              | 197.345                             | 11.771                  |
| Cyclopentane      | 0.0141                 | 70.134                              | 0.986                               | 0.059                   |
| n-Hexane          | 1.5277                 | 86.177                              | 131.652                             | 7.853                   |
| Cyclohexane       | 0.4003                 | 84.161                              | 33.686                              | 2.009                   |
| Other hexanes     | 0.0000                 | 86.177                              | 0.000                               | 0.000                   |
| Heptanes          | 1.0140                 | 100.204                             | 101.608                             | 6.061                   |
| Methylcyclohexane | 0.0000                 | 98.188                              | 0.000                               | 0.000                   |
| Isooctane         | 0.0137                 | 114.231                             | 1.560                               | 0.093                   |
| Benzene           | 0.1504                 | 78.114                              | 11.747                              | 0.701                   |
| Toluene           | 0.0148                 | 92.141                              | 1.359                               | 0.081                   |
| Ethylbenzene      | 0.0055                 | 106.167                             | 0.580                               | 0.035                   |
| Xylenes           | 0.0265                 | 106.167                             | 2.816                               | 0.168                   |
| n-Octane          | 0.1540                 | 114.232                             | 17.595                              | 1.049                   |
| n-Nonane          | 0.0409                 | 128.259                             | 5.250                               | 0.313                   |
| n-Decane          | 0.0045                 | 142.286                             | 0.641                               | 0.038                   |
| Total             | 100.0000               |                                     | 1676.497                            | 100.000                 |

Gas stream composition obtained from VGMSym output

Component Weights (lb/lb-mole) = (% / 100) \* Molecular Weights (lb/lb-mole)

Weight Percent of TOC (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)



## Condensate Storage Tank Actual Emissions Data and Calculations

Unit Number: **T1 & T2**

Description: Condensate Storage Tanks

### Condensate Composition (To Determine Working/Breathing Losses)

| Components        | Mole<br>Percents,<br>% | Molecular<br>Weights,<br>lb/lb-mole | Component<br>Weights,<br>lb/lb-mole | Weight<br>Percent,<br>% |
|-------------------|------------------------|-------------------------------------|-------------------------------------|-------------------------|
| Carbon dioxide    | 0.0019                 | 44.010                              |                                     |                         |
| Hydrogen sulfide  | 0.0000                 | 34.070                              |                                     |                         |
| Nitrogen          | 0.0020                 | 28.013                              |                                     |                         |
| Water             | 0.0000                 | 18.015                              |                                     |                         |
| Methane           | 0.2919                 | 16.043                              |                                     |                         |
| Ethane            | 0.3081                 | 30.070                              |                                     |                         |
| Propane           | 0.3598                 | 44.097                              | 15.8642                             | 0.1520                  |
| Isobutane         | 1.4337                 | 58.123                              | 83.3327                             | 0.7985                  |
| n-Butane          | 4.1675                 | 58.123                              | 242.2289                            | 2.3211                  |
| Isopentane        | 5.4021                 | 72.150                              | 389.7591                            | 3.7348                  |
| n-Pentane         | 4.8392                 | 72.150                              | 349.1468                            | 3.3457                  |
| Cyclopentane      | 0.0485                 | 70.134                              | 3.4002                              | 0.0326                  |
| n-Hexane          | 10.3589                | 86.177                              | 892.6951                            | 8.5542                  |
| Cyclohexane       | 4.2658                 | 84.161                              | 359.0121                            | 3.4402                  |
| Other hexanes     | 0.0000                 | 86.177                              | 0.0000                              | 0.0000                  |
| Heptanes          | 22.7383                | 100.204                             | 2278.4709                           | 21.8333                 |
| Methylcyclohexane | 0.0000                 | 98.188                              | 0.0000                              | 0.0000                  |
| Isooctane         | 0.3093                 | 114.231                             | 35.3280                             | 0.3385                  |
| Benzene           | 1.1881                 | 78.114                              | 92.8089                             | 0.8893                  |
| Toluene           | 0.4562                 | 92.141                              | 42.0352                             | 0.4028                  |
| Ethylbenzene      | 0.4896                 | 106.167                             | 51.9800                             | 0.4981                  |
| Xylenes           | 2.3418                 | 106.167                             | 248.6262                            | 2.3824                  |
| n-Octane          | 12.2941                | 114.232                             | 1404.3772                           | 13.4573                 |
| n-Nonane          | 9.7927                 | 128.259                             | 1256.0008                           | 12.0355                 |
| n-Decane          | 18.9106                | 142.286                             | 2690.7109                           | 25.7835                 |
| Total             | 100.0000               |                                     | 10435.7771                          | 100.0000                |

Gas stream composition obtained from VGMSym output

Component Weights (lb/lb-mole) = (% / 100) \* Molecular Weights (lb/lb-mole)

Weight Percent of TOC (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)

In TANKS 4, the propane percentage is included with isobutane and n-butane (an even distribution)

## Simulation Report



# Symmetry

**File Name:** 2021 Los Mestenos Emissions Actual 11.21.2022  
**Company:** VMG, a Schlumberger Technology  
**Customer:**  
**Project:**  
**Job No:**  
**Prepared By:**  
**Report Date:** Monday, November 21, 2022  
**Unit Set:** Field

File: C:\Users\nwork.HEC-HOU\OneDrive - Hilcorp\Environmental\Condensate Flash Calcs\Los Mestenos 1

Symmetry

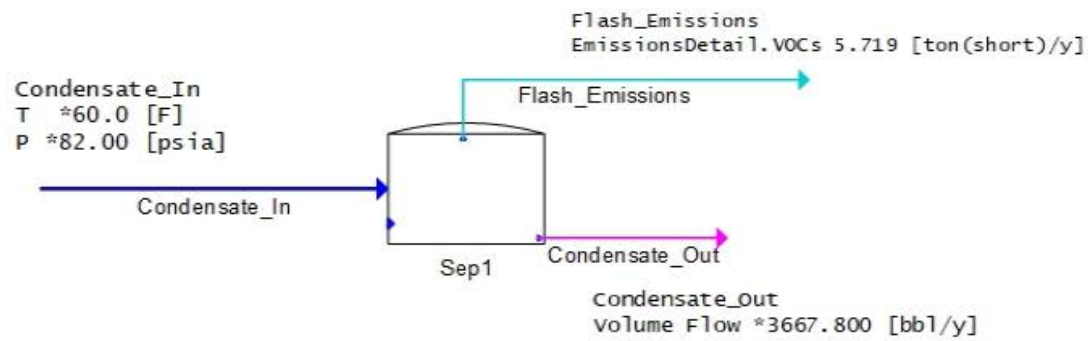
[Main Flowsheet](#)

[Material Stream \(3\)](#)

[2ph Separator \(1\)](#)

\*Bold face throughout the report denotes specified values.

\*Italic face throughout the report denotes recycle values.



Input Condensate Temperature: 60 °F  
 Input Condensate Pressure: 82 psia  
 Output Condensate Flow: 3,668 bbl/yr  
 Output Condensate Flow: 10.05 bbl/day  
 VOC Emission Rate: 5.72 tpy

| /Condensate_In (Material Stream) |                |                     |          |          |
|----------------------------------|----------------|---------------------|----------|----------|
| Thermo Model: APRNL2             |                |                     |          |          |
| Connections                      |                |                     |          |          |
| Material Inlets                  |                |                     |          |          |
|                                  | Connection     | Up Stream Unit Op   |          |          |
| In                               | <Disconnected> | ---                 |          |          |
| Material Outlets                 |                |                     |          |          |
|                                  | Connection     | Down Stream Unit Op |          |          |
| Out                              | Sep1.In0       | ---                 |          |          |
| Allocation / Product Allocation  |                |                     |          |          |
| Auto Calculate                   | False          | Is Up To Date       | False    |          |
| Status                           | Y?No Results   |                     |          |          |
| Equilibrium Results              |                |                     |          |          |
|                                  | Bulk           | Vap                 | Liq0     | Liq1     |
| Phase Frac [Fraction]            | 1.00           | 0.0289              | 0.9711   | 0.00     |
| T [F]                            | 60.0           | 60.0                | 60.0     | 60.0     |
| P [psia]                         | 82.00          | 82.00               | 82.00    | 82.00    |
| Mole Flow [lbmol/h]              | 1.04           | 0.03                | 1.01     | 0.00     |
| Mass Flow [lb/h]                 | 106.48         | 0.59                | 105.90   | 0.00     |
| Fraction [Fraction]              |                |                     |          |          |
| NITROGEN                         | 0.0012         | 0.0336              | 2.62E-04 | 0.0012   |
| METHANE                          | 0.0496         | 0.8677              | 0.0252   | 0.0496   |
| CARBON DIOXIDE                   | 1.14E-04       | 9.83E-04            | 8.81E-05 | 1.14E-04 |
| ETHANE                           | 0.0101         | 0.0471              | 0.0090   | 0.0101   |
| PROPANE                          | 0.0056         | 0.0077              | 0.0055   | 0.0056   |
| ISOBUTANE                        | 0.0166         | 0.0089              | 0.0168   | 0.0166   |
| n-BUTANE                         | 0.0449         | 0.0161              | 0.0458   | 0.0449   |
| ISOPENTANE                       | 0.0530         | 0.0071              | 0.0543   | 0.0530   |
| n-PENTANE                        | 0.0468         | 0.0048              | 0.0481   | 0.0468   |
| CYCLOPENTANE                     | 4.59E-04       | 2.43E-05            | 4.72E-04 | 4.59E-04 |
| n-HEXANE                         | 0.0970         | 0.0027              | 0.0998   | 0.0970   |
| METHYLCYCLOHEXANE                | 0.00           | 0.00                | 0.00     | 0.00     |
| 2,2,4-TRIMETHYLPENTANE           | 0.0029         | 2.43E-05            | 0.0030   | 0.0029   |
| BENZENE                          | 0.0111         | 2.60E-04            | 0.0114   | 0.0111   |
| CYCLOHEXANE                      | 0.0398         | 6.96E-04            | 0.0409   | 0.0398   |
| n-HEPTANE                        | 0.2111         | 0.0018              | 0.2173   | 0.2111   |
| TOLUENE                          | 0.0042         | 2.59E-05            | 0.0044   | 0.0042   |
| n-OCTANE                         | 0.1041         | 2.79E-04            | 0.1072   | 0.1041   |
| ETHYLBENZENE                     | 0.0045         | 9.81E-06            | 0.0047   | 0.0045   |
| m-XYLENE                         | 0.0217         | 3.53E-05            | 0.0223   | 0.0217   |
| o-XYLENE                         | 0.0098         | 1.23E-05            | 0.0101   | 0.0098   |
| n-NONANE                         | 0.0906         | 7.56E-05            | 0.0933   | 0.0906   |
| n-DECANE                         | 0.00           | 0.00E+00            | 0.00     | 0.00     |
| n-UNDECANE                       | 0.0875         | 6.63E-06            | 0.0901   | 0.0875   |
| n-DODECANE                       | 0.0875         | 2.13E-06            | 0.0901   | 0.0875   |
| WATER                            | 0.00           | 0.00E+00            | 0.00     | 0.00     |

| /Condensate_Out (Material Stream) |                |                     |          |      |
|-----------------------------------|----------------|---------------------|----------|------|
| Thermo Model: APRNGL2             |                |                     |          |      |
| Connections                       |                |                     |          |      |
| Material Inlets                   |                |                     |          |      |
|                                   | Connection     | Up Stream Unit Op   |          |      |
| In                                | Sep1.Liq0      | ---                 |          |      |
| Material Outlets                  |                |                     |          |      |
|                                   | Connection     | Down Stream Unit Op |          |      |
| Out                               | <Disconnected> | ---                 |          |      |
| Allocation / Product Allocation   |                |                     |          |      |
| Auto Calculate                    | False          | Is Up To Date       | False    |      |
| Status                            | Y?No Results   |                     |          |      |
| Equilibrium Results               |                |                     |          |      |
|                                   | Bulk           | Vap                 | Liq0     | Liq1 |
| Phase Frac [Fraction]             | 1.00           | 0.00                | 1.00     |      |
| T [F]                             | 60.0           | 60.0                | 60.0     |      |
| P [psia]                          | 13.00          | 13.00               | 13.00    |      |
| Mole Flow [lbmol/h]               | 0.96           | 0.00                | 0.96     |      |
| Mass Flow [lb/h]                  | 104.13         | 0.00                | 104.13   |      |
| Fraction [Fraction]               |                |                     |          |      |
| NITROGEN                          | 1.98E-05       | 0.0161              | 1.98E-05 |      |
| METHANE                           | 0.0029         | 0.6257              | 0.0029   |      |
| CARBON DIOXIDE                    | 1.88E-05       | 0.0013              | 1.88E-05 |      |
| ETHANE                            | 0.0031         | 0.0972              | 0.0031   |      |
| PROPANE                           | 0.0036         | 0.0299              | 0.0036   |      |
| ISOBUTANE                         | 0.0143         | 0.0442              | 0.0143   |      |
| n-BUTANE                          | 0.0417         | 0.0846              | 0.0417   |      |
| ISOPENTANE                        | 0.0540         | 0.0401              | 0.0540   |      |
| n-PENTANE                         | 0.0484         | 0.0274              | 0.0484   |      |
| CYCLOPENTANE                      | 4.85E-04       | 1.41E-04            | 4.85E-04 |      |
| n-HEXANE                          | 0.1036         | 0.0153              | 0.1036   |      |
| METHYLCYCLOHEXANE                 | 0.00           | 0.00                | 0.00     |      |
| 2,2,4-TRIMETHYLPENTANE            | 0.0031         | 1.37E-04            | 0.0031   |      |
| BENZENE                           | 0.0119         | 0.0015              | 0.0119   |      |
| CYCLOHEXANE                       | 0.0427         | 0.0040              | 0.0427   |      |
| n-HEPTANE                         | 0.2274         | 0.0101              | 0.2274   |      |
| TOLUENE                           | 0.0046         | 1.48E-04            | 0.0046   |      |
| n-OCTANE                          | 0.1124         | 0.0015              | 0.1124   |      |
| ETHYLBENZENE                      | 0.0049         | 5.47E-05            | 0.0049   |      |
| m-XYLENE                          | 0.0234         | 1.97E-04            | 0.0234   |      |
| o-XYLENE                          | 0.0106         | 6.84E-05            | 0.0106   |      |
| n-NONANE                          | 0.0979         | 4.09E-04            | 0.0979   |      |
| n-DECANE                          | 0.00           | 0.00E+00            | 0.00     |      |
| n-UNDECANE                        | 0.0946         | 3.43E-05            | 0.0946   |      |
| n-DODECANE                        | 0.0946         | 1.08E-05            | 0.0946   |      |
| WATER                             | 0.00           | 0.00E+00            | 0.00     |      |

| /Flash_Emissions (Material Stream) |                |                     |          |      |
|------------------------------------|----------------|---------------------|----------|------|
| Thermo Model: APRNGL2              |                |                     |          |      |
| Connections                        |                |                     |          |      |
| Material Inlets                    |                |                     |          |      |
|                                    | Connection     | Up Stream Unit Op   |          |      |
| In                                 | Sep1.Vap       | ---                 |          |      |
| Material Outlets                   |                |                     |          |      |
|                                    | Connection     | Down Stream Unit Op |          |      |
| Out                                | <Disconnected> | ---                 |          |      |
| Allocation / Product Allocation    |                |                     |          |      |
| Auto Calculate                     | False          | Is Up To Date       | False    |      |
| Status                             | Y?No Results   |                     |          |      |
| Equilibrium Results                |                |                     |          |      |
|                                    | Bulk           | Vap                 | Liq0     | Liq1 |
| Phase Frac [Fraction]              | 1.00           | 1.00                | 0.00E+00 |      |
| T [F]                              | 60.0           | 60.0                | 60.0     |      |
| P [psia]                           | 13.00          | 13.00               | 13.00    |      |
| Mole Flow [lbmol/h]                | 0.08           | 0.08                | 0.00     |      |
| Mass Flow [lb/h]                   | 2.35           | 2.35                | 0.00     |      |
| Fraction [Fraction]                |                |                     |          |      |
| NITROGEN                           | 0.0161         | 0.0161              | 1.98E-05 |      |
| METHANE                            | 0.6257         | 0.6257              | 0.0029   |      |
| CARBON DIOXIDE                     | 0.0013         | 0.0013              | 1.88E-05 |      |
| ETHANE                             | 0.0972         | 0.0972              | 0.0031   |      |
| PROPANE                            | 0.0299         | 0.0299              | 0.0036   |      |
| ISOBUTANE                          | 0.0442         | 0.0442              | 0.0143   |      |
| n-BUTANE                           | 0.0846         | 0.0846              | 0.0417   |      |
| ISOPENTANE                         | 0.0401         | 0.0401              | 0.0540   |      |
| n-PENTANE                          | 0.0274         | 0.0274              | 0.0484   |      |
| CYCLOPENTANE                       | 1.41E-04       | 1.41E-04            | 4.85E-04 |      |
| n-HEXANE                           | 0.0153         | 0.0153              | 0.1036   |      |
| METHYLCYCLOHEXANE                  | 0.00           | 0.00                | 0.00     |      |
| 2,2,4-TRIMETHYLPENTANE             | 1.37E-04       | 1.37E-04            | 0.0031   |      |
| BENZENE                            | 0.0015         | 0.0015              | 0.0119   |      |
| CYCLOHEXANE                        | 0.0040         | 0.0040              | 0.0427   |      |
| n-HEPTANE                          | 0.0101         | 0.0101              | 0.2274   |      |
| TOLUENE                            | 1.48E-04       | 1.48E-04            | 0.0046   |      |
| n-OCTANE                           | 0.0015         | 0.0015              | 0.1124   |      |
| ETHYLBENZENE                       | 5.47E-05       | 5.47E-05            | 0.0049   |      |
| m-XYLENE                           | 1.97E-04       | 1.97E-04            | 0.0234   |      |
| o-XYLENE                           | 6.84E-05       | 6.84E-05            | 0.0106   |      |
| n-NONANE                           | 4.09E-04       | 4.09E-04            | 0.0979   |      |
| n-DECANE                           | 0.00E+00       | 0.00E+00            | 0.00     |      |
| n-UNDECANE                         | 3.43E-05       | 3.43E-05            | 0.0946   |      |
| n-DODECANE                         | 1.08E-05       | 1.08E-05            | 0.0946   |      |
| WATER                              | 0.00E+00       | 0.00E+00            | 0.00     |      |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

|                      |                                      |
|----------------------|--------------------------------------|
| User Identification: | Los Mestenos - T1 - Condensate (ACT) |
| City:                | Gavilan                              |
| State:               | New Mexico                           |
| Company:             | Harvest Four Corners, LLC            |
| Type of Tank:        | Vertical Fixed Roof Tank             |
| Description:         | 400 Barrel Condensate Storage Tank   |

**Tank Dimensions**

|                          |            |
|--------------------------|------------|
| Shell Height (ft):       | 20.00      |
| Diameter (ft):           | 12.00      |
| Liquid Height (ft) :     | 19.00      |
| Avg. Liquid Height (ft): | 9.50       |
| Volume (gallons):        | 16,075.00  |
| Turnovers:               | 9.58       |
| Net Throughput(gal/yr):  | 154,048.00 |
| Is Tank Heated (y/n):    | N          |

**Paint Characteristics**

|                    |             |
|--------------------|-------------|
| Shell Color/Shade: | Gray/Medium |
| Shell Condition    | Good        |
| Roof Color/Shade:  | Gray/Medium |
| Roof Condition:    | Good        |

**Roof Characteristics**

|                         |       |
|-------------------------|-------|
| Type:                   | Dome  |
| Height (ft)             | 0.00  |
| Radius (ft) (Dome Roof) | 12.00 |

**Breather Vent Settings**

|                          |       |
|--------------------------|-------|
| Vacuum Settings (psig):  | -0.03 |
| Pressure Settings (psig) | 0.03  |

Meterological Data used in Emissions Calculations: Albuquerque, New Mexico (Avg Atmospheric Pressure = 12.15 psia)

## TANKS 4.0.9d

### Emissions Report - Detail Format

### Liquid Contents of Storage Tank

#### Los Mestenos - T1 - Condensate (ACT) - Vertical Fixed Roof Tank Gavilan, New Mexico

| Mixture/Component                  | Month | Daily Liquid Surf.<br>Temperature (deg F) |       |       | Liquid<br>Bulk<br>Temp<br>(deg F) | Vapor Pressure (psia) |         |         | Vapor<br>Mol.<br>Weight | Liquid<br>Mass<br>Fract. | Vapor<br>Mass<br>Fract. | Mol.<br>Weight | Basis for Vapor Pressure<br>Calculations |
|------------------------------------|-------|---|-------|-------|-----------------------------------|-----------------------|---------|---------|-------------------------|--------------------------|-------------------------|----------------|--|
|                                    |       | Avg.                                      | Min.  | Max.  |                                   | Avg.                  | Min.    | Max.    |                         |                          |                         |                |  |
| Condensate                         | All   | 67.36                                     | 53.93 | 80.79 | 59.23                             | 3.5613                | 2.6970  | 4.4885  | 67.5024                 |                          |                         | 105.08         |  |
| 2,2,4-Trimethylpentane (isooctane) |       |   |       |       |                                   | 0.7338                | 0.4989  | 1.0546  | 114.2300                | 0.0034                   | 0.0011                  | 114.23         | Option 2: A=6.8118, B=1257.84, C=220.74  |
| Benzene                            |       |   |       |       |                                   | 1.4274                | 0.9846  | 2.0237  | 78.1100                 | 0.0089                   | 0.0055                  | 78.11          | Option 2: A=6.905, B=1211.033, C=220.79  |
| Butane (-n)                        |       |   |       |       |                                   | 29.9357               | 23.3576 | 34.6684 | 58.1230                 | 0.0240                   | 0.3137                  | 58.12          | Option 1: VP60 = 26.1 VP70 = 31.31       |
| Cyclohexane                        |       |   |       |       |                                   | 1.4738                | 1.0254  | 2.0729  | 84.1600                 | 0.0344                   | 0.0222                  | 84.16          | Option 2: A=6.841, B=1201.53, C=222.65   |
| Cyclopentane                       |       |   |       |       |                                   | 4.9596                | 3.6370  | 6.6394  | 70.1300                 | 0.0003                   | 0.0007                  | 70.13          | Option 1: VP60 = 4.177 VP70 = 5.24       |
| Decane (-n)                        |       |   |       |       |                                   | 0.0395                | 0.0291  | 0.0536  | 142.2900                | 0.2578                   | 0.0045                  | 142.29         | Option 1: VP60 = .033211 VP70 = .041762  |
| Ethylbenzene                       |       |   |       |       |                                   | 0.1396                | 0.0876  | 0.2162  | 106.1700                | 0.0050                   | 0.0003                  | 106.17         | Option 2: A=6.975, B=1424.255, C=213.21  |
| Heptane (-n)                       |       |   |       |       |                                   | 0.7600                | 0.5088  | 1.1128  | 100.2000                | 0.2183                   | 0.0725                  | 100.20         | Option 3: A=37358, B=8.2585              |
| Hexane (-n)                        |       |   |       |       |                                   | 2.3100                | 1.6303  | 3.2059  | 86.1700                 | 0.0855                   | 0.0864                  | 86.17          | Option 2: A=6.876, B=1171.17, C=224.41   |
| Iso-Butane                         |       |   |       |       |                                   | 43.3083               | 34.4026 | 53.8185 | 58.1230                 | 0.0087                   | 0.1656                  | 58.12          | Option 1: VP60 = 38.14 VP70 = 45.16      |
| Isopentane                         |       |   |       |       |                                   | 11.8640               | 8.7212  | 15.5743 | 72.1500                 | 0.0373                   | 0.1937                  | 72.15          | Option 1: VP60 = 10.005 VP70 = 12.53     |
| Nonane (-n)                        |       |   |       |       |                                   | 0.0784                | 0.0568  | 0.1080  | 128.2600                | 0.1204                   | 0.0041                  | 128.26         | Option 1: VP60 = .065278 VP70 = .08309   |
| Octane (-n)                        |       |   |       |       |                                   | 0.1769                | 0.1254  | 0.2493  | 114.2300                | 0.1346                   | 0.0104                  | 114.23         | Option 1: VP60 = .145444 VP70 = .188224  |
| Pentane (-n)                       |       |   |       |       |                                   | 8.0308                | 5.9649  | 10.6537 | 72.1500                 | 0.0335                   | 0.1174                  | 72.15          | Option 3: A=27691, B=7.558               |
| Toluene                            |       |   |       |       |                                   | 0.4136                | 0.2726  | 0.6120  | 92.1300                 | 0.0040                   | 0.0007                  | 92.13          | Option 2: A=6.954, B=1344.8, C=219.48    |
| Xylenes (mixed isomers)            |       |   |       |       |                                   | 0.1165                | 0.0728  | 0.1813  | 106.1700                | 0.0238                   | 0.0012                  | 106.17         | Option 2: A=7.009, B=1462.266, C=215.11  |



## TANKS 4.0.9d

### Emissions Report - Detail Format

### Detail Calculations (AP-42)

#### Los Mestenios - T1 - Condensate (ACT) - Vertical Fixed Roof Tank Gavilan, New Mexico

|  |            |
|--|------------|
| <b>Annual Emission Calculations</b>                                |            |
| Standing Losses (lb):  | 1,922.1111 |
| Vapor Space Volume (cu ft):  | 1,280.6108 |
| Vapor Density (lb/cu ft):  | 0.0425     |
| Vapor Space Expansion Factor:                                      | 0.3035     |
| Vented Vapor Saturation Factor:                                    | 0.3188     |
| <b>Tank Vapor Space Volume:</b>                                    |            |
| Vapor Space Volume (cu ft):  | 1,280.6108 |
| Tank Diameter (ft):  | 12.0000    |
| Vapor Space Outage (ft):   | 11.3231    |
| Tank Shell Height (ft):  | 20.0000    |
| Average Liquid Height (ft):  | 9.5000     |
| Roof Outage (ft):  | 0.8231     |
| <b>Roof Outage (Dome Roof)</b>                                     |            |
| Roof Outage (ft):  | 0.8231     |
| Dome Radius (ft):  | 12.0000    |
| Shell Radius (ft):   | 6.0000     |
| <b>Vapor Density</b>   |            |
| Vapor Density (lb/cu ft):  | 0.0425     |
| Vapor Molecular Weight (lb/lb-mole):                               | 67.5024    |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 3.5613     |
| Daily Avg. Liquid Surface Temp. (deg. R):                          | 527.0322   |
| Daily Average Ambient Temp. (deg. F):                              | 56.1542    |
| Ideal Gas Constant R (psia cu ft / (lb-mol-deg R)):                | 10.731     |
| Liquid Bulk Temperature (deg. R):                                  | 518.9042   |
| Tank Paint Solar Absorptance (Shell):                              | 0.6800     |
| Tank Paint Solar Absorptance (Roof):                               | 0.6800     |
| Daily Total Solar Insulation Factor (Btu/sqft day):                | 1,765.3167 |
| <b>Vapor Space Expansion Factor</b>                                |            |
| Vapor Space Expansion Factor:                                      | 0.3035     |
| Daily Vapor Temperature Range (deg. R):                            | 53.7176    |
| Daily Vapor Pressure Range (psia):                                 | 1.7915     |
| Breather Vent Press. Setting Range(psia):                          | 0.0600     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 3.5613     |
| Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia): | 2.6970     |
| Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia): | 4.4885     |
| Daily Avg. Liquid Surface Temp. (deg R):                           | 527.0322   |
| Daily Min. Liquid Surface Temp. (deg R):                           | 513.6028   |
| Daily Max. Liquid Surface Temp. (deg R):                           | 540.4617   |
| Daily Ambient Temp. Range (deg. R):                                | 27.9250    |
| <b>Vented Vapor Saturation Factor</b>                              |            |
| Vented Vapor Saturation Factor:                                    | 0.3188     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 3.5613     |
| Vapor Space Outage (ft):   | 11.3231    |
| Working Losses (lb):   | 881.7326   |

|  |              |
|--|--------------|
| Vapor Molecular Weight (lb/lb-mole):   | 67.5024      |
| Vapor Pressure at Daily Average Liquid |              |
| Surface Temperature (psia):            | 3.5613       |
| Annual Net Throughput (gal/yr.):       | 154,048.0000 |
| Annual Turnovers:                      | 9.5800       |
| Turnover Factor:                       | 1.0000       |
| Maximum Liquid Volume (gal):           | 16,075.0000  |
| Maximum Liquid Height (ft):            | 19.0000      |
| Tank Diameter (ft):                    | 12.0000      |
| Working Loss Product Factor:           | 1.0000       |
|  |              |
| Total Losses (lb):                     | 2,803.8438   |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Los Mestenos - T1 - Condensate (ACT) - Vertical Fixed Roof Tank**  
**Gavilan, New Mexico**

|                                    | Losses(lbs)  |                |                 |
|------------------------------------|--------------|----------------|-----------------|
| Components                         | Working Loss | Breathing Loss | Total Emissions |
| Condensate                         | 881.73       | 1,922.11       | 2,803.84        |
| Iso-Butane                         | 145.97       | 318.21         | 464.18          |
| Butane (-n)                        | 276.57       | 602.91         | 879.49          |
| Isopentane                         | 170.78       | 372.28         | 543.06          |
| Pentane (-n)                       | 103.56       | 225.75         | 329.31          |
| Cyclopentane                       | 0.62         | 1.36           | 1.98            |
| Hexane (-n)                        | 76.16        | 166.02         | 242.18          |
| Cyclohexane                        | 19.54        | 42.60          | 62.14           |
| Heptane (-n)                       | 63.96        | 139.42         | 203.37          |
| Benzene                            | 4.89         | 10.67          | 15.56           |
| Toluene                            | 0.64         | 1.40           | 2.04            |
| Ethylbenzene                       | 0.27         | 0.58           | 0.85            |
| Xylenes (mixed isomers)            | 1.07         | 2.33           | 3.40            |
| Octane (-n)                        | 9.18         | 20.01          | 29.18           |
| Nonane (-n)                        | 3.64         | 7.93           | 11.56           |
| Decane (-n)                        | 3.93         | 8.56           | 12.48           |
| 2,2,4-Trimethylpentane (isooctane) | 0.96         | 2.09           | 3.04            |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

|                      |                                      |
|----------------------|--------------------------------------|
| User Identification: | Los Mestenos - T2 - Condensate (ACT) |
| City:                | Gavilan                              |
| State:               | New Mexico                           |
| Company:             | Harvest Four Corners, LLC            |
| Type of Tank:        | Vertical Fixed Roof Tank             |
| Description:         | 400 Barrel Condensate Storage Tank   |

**Tank Dimensions**

|                          |           |
|--------------------------|-----------|
| Shell Height (ft):       | 12.83     |
| Diameter (ft):           | 15.50     |
| Liquid Height (ft) :     | 11.83     |
| Avg. Liquid Height (ft): | 6.00      |
| Volume (gallons):        | 16,800.00 |
| Turnovers:               | 4.58      |
| Net Throughput(gal/yr):  | 77,024.00 |
| Is Tank Heated (y/n):    | N         |

**Paint Characteristics**

|                    |             |
|--------------------|-------------|
| Shell Color/Shade: | Gray/Medium |
| Shell Condition    | Good        |
| Roof Color/Shade:  | Gray/Medium |
| Roof Condition:    | Good        |

**Roof Characteristics**

|                         |       |
|-------------------------|-------|
| Type:                   | Dome  |
| Height (ft)             | 0.00  |
| Radius (ft) (Dome Roof) | 15.50 |

**Breather Vent Settings**

|                          |       |
|--------------------------|-------|
| Vacuum Settings (psig):  | -0.03 |
| Pressure Settings (psig) | 0.03  |

Meterological Data used in Emissions Calculations: Albuquerque, New Mexico (Avg Atmospheric Pressure = 12.15 psia)

# **TANKS 4.0.9d** **Emissions Report - Detail Format** **Liquid Contents of Storage Tank**

## **Los Mestenios - T2 - Condensate (ACT) - Vertical Fixed Roof Tank** **Gavilan, New Mexico**

| Mixture/Component                  | Month | Daily Liquid Surf.<br>Temperature (deg F) |       |       | Liquid<br>Bulk<br>Temp<br>(deg F) | Vapor Pressure (psia) |         |         | Vapor<br>Mol.<br>Weight | Liquid<br>Mass<br>Fract. | Vapor<br>Mass<br>Fract. | Mol.<br>Weight | Basis for Vapor Pressure<br>Calculations |
|------------------------------------|-------|---|-------|-------|-----------------------------------|-----------------------|---------|---------|-------------------------|--------------------------|-------------------------|----------------|--|
|                                    |       | Avg.                                      | Min.  | Max.  |                                   | Avg.                  | Min.    | Max.    |                         |                          |                         |                |  |
| Condensate                         | All   | 67.36                                     | 53.93 | 80.79 | 59.23                             | 3.5613                | 2.6970  | 4.4885  | 67.5024                 |                          |                         | 105.08         |  |
| 2,2,4-Trimethylpentane (isooctane) |       |   |       |       |                                   | 0.7338                | 0.4989  | 1.0546  | 114.2300                | 0.0034                   | 0.0011                  | 114.23         | Option 2: A=6.8118, B=1257.84, C=220.74  |
| Benzene                            |       |   |       |       |                                   | 1.4274                | 0.9846  | 2.0237  | 78.1100                 | 0.0089                   | 0.0055                  | 78.11          | Option 2: A=6.905, B=1211.033, C=220.79  |
| Butane (-n)                        |       |   |       |       |                                   | 29.9357               | 23.3576 | 34.6684 | 58.1230                 | 0.0240                   | 0.3137                  | 58.12          | Option 1: VP60 = 26.1 VP70 = 31.31       |
| Cyclohexane                        |       |   |       |       |                                   | 1.4738                | 1.0254  | 2.0729  | 84.1600                 | 0.0344                   | 0.0222                  | 84.16          | Option 2: A=6.841, B=1201.53, C=222.65   |
| Cyclopentane                       |       |   |       |       |                                   | 4.9596                | 3.6370  | 6.6394  | 70.1300                 | 0.0003                   | 0.0007                  | 70.13          | Option 1: VP60 = 4.177 VP70 = 5.24       |
| Decane (-n)                        |       |   |       |       |                                   | 0.0395                | 0.0291  | 0.0536  | 142.2900                | 0.2578                   | 0.0045                  | 142.29         | Option 1: VP60 = .033211 VP70 = .041762  |
| Ethylbenzene                       |       |   |       |       |                                   | 0.1396                | 0.0876  | 0.2162  | 106.1700                | 0.0050                   | 0.0003                  | 106.17         | Option 2: A=6.975, B=1424.255, C=213.21  |
| Heptane (-n)                       |       |   |       |       |                                   | 0.7600                | 0.5088  | 1.1128  | 100.2000                | 0.2183                   | 0.0725                  | 100.20         | Option 3: A=37358, B=8.2585              |
| Hexane (-n)                        |       |   |       |       |                                   | 2.3100                | 1.6303  | 3.2059  | 86.1700                 | 0.0855                   | 0.0864                  | 86.17          | Option 2: A=6.876, B=1171.17, C=224.41   |
| Iso-Butane                         |       |   |       |       |                                   | 43.3083               | 34.4026 | 53.8185 | 58.1230                 | 0.0087                   | 0.1656                  | 58.12          | Option 1: VP60 = 38.14 VP70 = 45.16      |
| Isopentane                         |       |   |       |       |                                   | 11.8640               | 8.7212  | 15.5743 | 72.1500                 | 0.0373                   | 0.1937                  | 72.15          | Option 1: VP60 = 10.005 VP70 = 12.53     |
| Nonane (-n)                        |       |   |       |       |                                   | 0.0784                | 0.0568  | 0.1080  | 128.2600                | 0.1204                   | 0.0041                  | 128.26         | Option 1: VP60 = .065278 VP70 = .08309   |
| Octane (-n)                        |       |   |       |       |                                   | 0.1769                | 0.1254  | 0.2493  | 114.2300                | 0.1346                   | 0.0104                  | 114.23         | Option 1: VP60 = .145444 VP70 = .188224  |
| Pentane (-n)                       |       |   |       |       |                                   | 8.0308                | 5.9649  | 10.6537 | 72.1500                 | 0.0335                   | 0.1174                  | 72.15          | Option 3: A=27691, B=7.558               |
| Toluene                            |       |   |       |       |                                   | 0.4136                | 0.2726  | 0.6120  | 92.1300                 | 0.0040                   | 0.0007                  | 92.13          | Option 2: A=6.954, B=1344.8, C=219.48    |
| Xylenes (mixed isomers)            |       |   |       |       |                                   | 0.1165                | 0.0728  | 0.1813  | 106.1700                | 0.0238                   | 0.0012                  | 106.17         | Option 2: A=7.009, B=1462.266, C=215.11  |

## TANKS 4.0.9d

### Emissions Report - Detail Format

### Detail Calculations (AP-42)

#### Los Mestenios - T2 - Condensate (ACT) - Vertical Fixed Roof Tank Gavilan, New Mexico

|  |            |
|--|------------|
| <b>Annual Emission Calculations</b>                                |            |
| Standing Losses (lb):  | 2,816.7067 |
| Vapor Space Volume (cu ft):  | 1,489.3739 |
| Vapor Density (lb/cu ft):  | 0.0425     |
| Vapor Space Expansion Factor:                                      | 0.3035     |
| Vented Vapor Saturation Factor:                                    | 0.4016     |
| <b>Tank Vapor Space Volume:</b>                                    |            |
| Vapor Space Volume (cu ft):  | 1,489.3739 |
| Tank Diameter (ft):  | 15.5000    |
| Vapor Space Outage (ft):   | 7.8932     |
| Tank Shell Height (ft):  | 12.8300    |
| Average Liquid Height (ft):  | 6.0000     |
| Roof Outage (ft):  | 1.0632     |
| <b>Roof Outage (Dome Roof)</b>                                     |            |
| Roof Outage (ft):  | 1.0632     |
| Dome Radius (ft):  | 15.5000    |
| Shell Radius (ft):   | 7.7500     |
| <b>Vapor Density</b>   |            |
| Vapor Density (lb/cu ft):  | 0.0425     |
| Vapor Molecular Weight (lb/lb-mole):                               | 67.5024    |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 3.5613     |
| Daily Avg. Liquid Surface Temp. (deg. R):                          | 527.0322   |
| Daily Average Ambient Temp. (deg. F):                              | 56.1542    |
| Ideal Gas Constant R (psia cu ft / (lb-mol-deg R)):                | 10.731     |
| Liquid Bulk Temperature (deg. R):                                  | 518.9042   |
| Tank Paint Solar Absorptance (Shell):                              | 0.6800     |
| Tank Paint Solar Absorptance (Roof):                               | 0.6800     |
| Daily Total Solar Insulation Factor (Btu/sqft day):                | 1,765.3167 |
| <b>Vapor Space Expansion Factor</b>                                |            |
| Vapor Space Expansion Factor:                                      | 0.3035     |
| Daily Vapor Temperature Range (deg. R):                            | 53.7176    |
| Daily Vapor Pressure Range (psia):                                 | 1.7915     |
| Breather Vent Press. Setting Range (psia):                         | 0.0600     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 3.5613     |
| Vapor Pressure at Daily Minimum Liquid Surface Temperature (psia): | 2.6970     |
| Vapor Pressure at Daily Maximum Liquid Surface Temperature (psia): | 4.4885     |
| Daily Avg. Liquid Surface Temp. (deg R):                           | 527.0322   |
| Daily Min. Liquid Surface Temp. (deg R):                           | 513.6028   |
| Daily Max. Liquid Surface Temp. (deg R):                           | 540.4617   |
| Daily Ambient Temp. Range (deg. R):                                | 27.9250    |
| <b>Vented Vapor Saturation Factor</b>                              |            |
| Vented Vapor Saturation Factor:                                    | 0.4016     |
| Vapor Pressure at Daily Average Liquid Surface Temperature (psia): | 3.5613     |
| Vapor Space Outage (ft):   | 7.8932     |
| Working Losses (lb):   | 440.8663   |

|  |             |
|--|-------------|
| Vapor Molecular Weight (lb/lb-mole):   | 67.5024     |
| Vapor Pressure at Daily Average Liquid |             |
| Surface Temperature (psia):            | 3.5613      |
| Annual Net Throughput (gal/yr.):       | 77,024.0000 |
| Annual Turnovers:                      | 4.5800      |
| Turnover Factor:                       | 1.0000      |
| Maximum Liquid Volume (gal):           | 16,800.0000 |
| Maximum Liquid Height (ft):            | 11.8300     |
| Tank Diameter (ft):                    | 15.5000     |
| Working Loss Product Factor:           | 1.0000      |
|  |             |
| Total Losses (lb):                     | 3,257.5730  |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Los Mestenos - T2 - Condensate (ACT) - Vertical Fixed Roof Tank**  
**Gavilan, New Mexico**

|                                    | Losses(lbs)  |                |                 |
|------------------------------------|--------------|----------------|-----------------|
| Components                         | Working Loss | Breathing Loss | Total Emissions |
| Condensate                         | 440.87       | 2,816.71       | 3,257.57        |
| Iso-Butane                         | 72.99        | 466.31         | 539.29          |
| Butane (-n)                        | 138.29       | 883.52         | 1,021.81        |
| Hexane (-n)                        | 38.08        | 243.29         | 281.37          |
| Cyclohexane                        | 9.77         | 62.43          | 72.20           |
| Heptane (-n)                       | 31.98        | 204.31         | 236.29          |
| Benzene                            | 2.45         | 15.63          | 18.08           |
| Toluene                            | 0.32         | 2.05           | 2.37            |
| Ethylbenzene                       | 0.13         | 0.86           | 0.99            |
| Xylenes (mixed isomers)            | 0.54         | 3.42           | 3.95            |
| Octane (-n)                        | 4.59         | 29.32          | 33.91           |
| Nonane (-n)                        | 1.82         | 11.62          | 13.43           |
| Decane (-n)                        | 1.96         | 12.54          | 14.50           |
| 2,2,4-Trimethylpentane (isooctane) | 0.48         | 3.06           | 3.54            |
| Isopentane                         | 85.39        | 545.56         | 630.94          |
| Pentane (-n)                       | 51.78        | 330.82         | 382.60          |
| Cyclopentane                       | 0.31         | 1.99           | 2.30            |



## **Section 5.6**

### **Condensate Truck Loading (Unit L1)**

#### **Written Description**

### ***Condensate Truck Loading (L1)***

Emissions from condensate truck loading were calculated using the emission factor equation from AP-42, Section 5.2, *Transportation and Marketing of Petroleum Liquids*. The TANKS 4.0.9d predicted pressure, molecular weight, and temperature (from the condensate working/breathing losses output file) were used to calculate the emission factor. The inputs and calculated emission factor are identified on the Condensate Truck Loading Emissions Calculations spreadsheets.

With the change in condensate composition (switching from the 2021 analysis to the 2018 analysis), TANKS adjusted the predicted pressure and molecular weight. These changes increased the emission factor used to calculate the truck loading emissions. As a result, condensate truck loading is now a significant source.

PTE emissions were calculated using an annual condensate throughput rate of 22,141 bbl/yr.

Actual emissions were calculated using the 2021 condensate throughput rate of 3,667.8 bbl/yr.

## **Section 5.6**

**Condensate Truck Loading (Unit L1)**

**PTE Emission Calculations**

## Condensate Truck Loading PTE Emissions Calculations

Unit Number: **L1**

Description: Truck Loading

### Emission Factor

|                             |                                  |  |
|-----------------------------|----------------------------------|--|
| <b>0.6</b>                  | Saturation factor, S             | AP-42, Table 5.2-1 (submerged loading & dedicated service) |
| <b>5.6924</b> psia          | True vapor pressure of liquid, P | TANKS 4.0 output file                                      |
| <b>66.3202</b> lb/lb-mole   | Molecular weight of vapors, M    | TANKS 4.0 output file                                      |
| <b>67.36</b> °F             | Temperature of liquid            | TANKS 4.0 output file                                      |
| 527.0 °R                    | Temperature of liquid, T         | °F + 459.67  |
| 5.36 lb/10 <sup>3</sup> gal | Emission factor, L               | AP-42, Section 5.2, Equation 1<br>L = 12.46 (SPM/T)        |

### Production Rate

**929.92** 10<sup>3</sup> gal/yr

Maximum annual production rate

Harvest Four Corners, LLC

(= 22,141 bbl/yr, which is approx. max historical throughput plus 10%)

### Steady-State Emission Rates

| Pollutant | Emission Rates, tpy |
|-----------|---------------------|
| VOC       | 2.49                |

Emission Rate (tpy) = lb/10<sup>3</sup> gal x 10<sup>3</sup> gal/yr / 2,000 lb/ton

| Pollutants   | Percent of VOC, % | Emission Rates, tpy |
|--------------|-------------------|---------------------|
| Benzene      | <b>0.36</b>       | 9.05E-03            |
| Ethylbenzene | <b>0.01</b>       | 1.32E-04            |
| n-Hexane     | <b>13.64</b>      | 3.40E-01            |
| Isooctane    | <b>0.00</b>       | 0.00E+00            |
| Toluene      | <b>0.26</b>       | 6.54E-03            |
| m-Xylene     | <b>0.03</b>       | 7.50E-04            |

Liquid percent of VOC calculated from the TANKS 4.0 results

Percent of VOC (%) = 100 x Pollutant Emission Rate (lb/yr) / Total VOC Emission Rate (lb/yr)

Emission Rates (tpy) = VOC Emission Rate (tpy) x (%) / 100

loading operation, resulting in high levels of vapor generation and loss. If the turbulence is great enough, liquid droplets will be entrained in the vented vapors.

A second method of loading is submerged loading. Two types are the submerged fill pipe method and the bottom loading method. In the submerged fill pipe method, the fill pipe extends almost to the bottom of the cargo tank. In the bottom loading method, a permanent fill pipe is attached to the cargo tank bottom. During most of submerged loading by both methods, the fill pipe opening is below the liquid surface level. Liquid turbulence is controlled significantly during submerged loading, resulting in much lower vapor generation than encountered during splash loading.

The recent loading history of a cargo carrier is just as important a factor in loading losses as the method of loading. If the carrier has carried a nonvolatile liquid such as fuel oil, or has just been cleaned, it will contain vapor-free air. If it has just carried gasoline and has not been vented, the air in the carrier tank will contain volatile organic vapors, which will be expelled during the loading operation along with newly generated vapors.

Cargo carriers are sometimes designated to transport only one product, and in such cases are practicing "dedicated service". Dedicated gasoline cargo tanks return to a loading terminal containing air fully or partially saturated with vapor from the previous load. Cargo tanks may also be "switch loaded" with various products, so that a nonvolatile product being loaded may expel the vapors remaining from a previous load of a volatile product such as gasoline. These circumstances vary with the type of cargo tank and with the ownership of the carrier, the petroleum liquids being transported, geographic location, and season of the year.

One control measure for vapors displaced during liquid loading is called "vapor balance service", in which the cargo tank retrieves the vapors displaced during product unloading at bulk plants or service stations and transports the vapors back to the loading terminal. Figure 5.2-5 shows a tank truck in vapor balance service filling a service station underground tank and taking on displaced gasoline vapors for return to the terminal. A cargo tank returning to a bulk terminal in vapor balance service normally is saturated with organic vapors, and the presence of these vapors at the start of submerged loading of the tanker truck results in greater loading losses than encountered during nonvapor balance, or "normal", service. Vapor balance service is usually not practiced with marine vessels, although some vessels practice emission control by means of vapor transfer within their own cargo tanks during ballasting operations, discussed below.

Emissions from loading petroleum liquid can be estimated (with a probable error of  $\pm 30$  percent)<sup>4</sup> using the following expression:

$$L_L = 12.46 \frac{SPM}{T} \quad (1)$$

where:

$L_L$  = loading loss, pounds per 1000 gallons ( $\text{lb}/10^3 \text{ gal}$ ) of liquid loaded

$S$  = a saturation factor (see Table 5.2-1)

$P$  = true vapor pressure of liquid loaded, pounds per square inch absolute (psia)  
(see Figure 7.1-5, Figure 7.1-6, and Table 7.1-2)

$M$  = molecular weight of vapors, pounds per pound-mole ( $\text{lb}/\text{lb-mole}$ ) (see Table 7.1-2)

$T$  = temperature of bulk liquid loaded,  $^{\circ}\text{R}$  ( $^{\circ}\text{F} + 460$ )

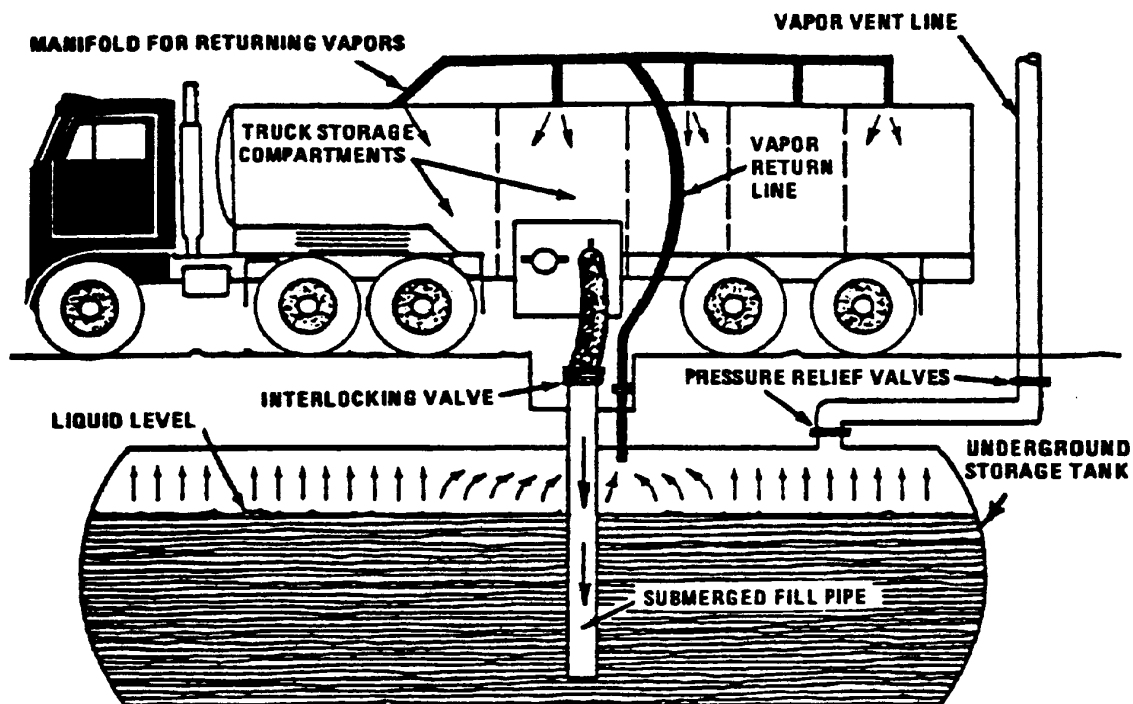


Figure 5.2-5. Tank truck unloading into a service station underground storage tank and practicing "vapor balance" form of emission control.

Table 5.2-1. SATURATION (S) FACTORS FOR CALCULATING PETROLEUM LIQUID LOADING LOSSES

| Cargo Carrier                  | Mode Of Operation                                  | S Factor |
|--------------------------------|--|----------|
| Tank trucks and rail tank cars | Submerged loading of a clean cargo tank            | 0.50     |
|                                | Submerged loading: dedicated normal service        | 0.60     |
|                                | Submerged loading: dedicated vapor balance service | 1.00     |
|                                | Splash loading of a clean cargo tank               | 1.45     |
|                                | Splash loading: dedicated normal service           | 1.45     |
|                                | Splash loading: dedicated vapor balance service    | 1.00     |
|                                |  |          |
| Marine vessels <sup>a</sup>    | Submerged loading: ships                           | 0.2      |
|                                | Submerged loading: barges                          | 0.5      |

<sup>a</sup> For products other than gasoline and crude oil. For marine loading of gasoline, use factors from Table 5.2-2. For marine loading of crude oil, use Equations 2 and 3 and Table 5.2-3.

The saturation factor, S, represents the expelled vapor's fractional approach to saturation, and it accounts for the variations observed in emission rates from the different unloading and loading methods. Table 5.2-1 lists suggested saturation factors.

Emissions from controlled loading operations can be calculated by multiplying the uncontrolled emission rate calculated in Equation 1 by an overall reduction efficiency term:

$$\left( 1 - \frac{\text{eff}}{100} \right)$$

The overall reduction efficiency should account for the capture efficiency of the collection system as well as both the control efficiency and any downtime of the control device. Measures to reduce loading emissions include selection of alternate loading methods and application of vapor recovery equipment. The latter captures organic vapors displaced during loading operations and recovers the vapors by the use of refrigeration, absorption, adsorption, and/or compression. The recovered product is piped back to storage. Vapors can also be controlled through combustion in a thermal oxidation unit, with no product recovery. Figure 5.2-6 demonstrates the recovery of gasoline vapors from tank trucks during loading operations at bulk terminals. Control efficiencies for the recovery units range from 90 to over 99 percent, depending on both the nature of the vapors and the type of control equipment used.<sup>5-6</sup> However, not all of the displaced vapors reach the control device, because of leakage from both the tank truck and collection system. The collection efficiency should be assumed to be 99.2 percent for tanker trucks passing the MACT-level annual leak test (not more than 1 inch water column pressure change in 5 minutes after pressurizing to 18 inches water followed by pulling a vacuum of 6 inches water).<sup>7</sup> A collection efficiency of 98.7 percent (a 1.3 percent leakage rate) should be assumed for trucks passing the NSPS-level annual test (3 inches pressure change). A collection efficiency of 70 percent should be assumed for trucks not passing one of these annual leak tests.<sup>6</sup>

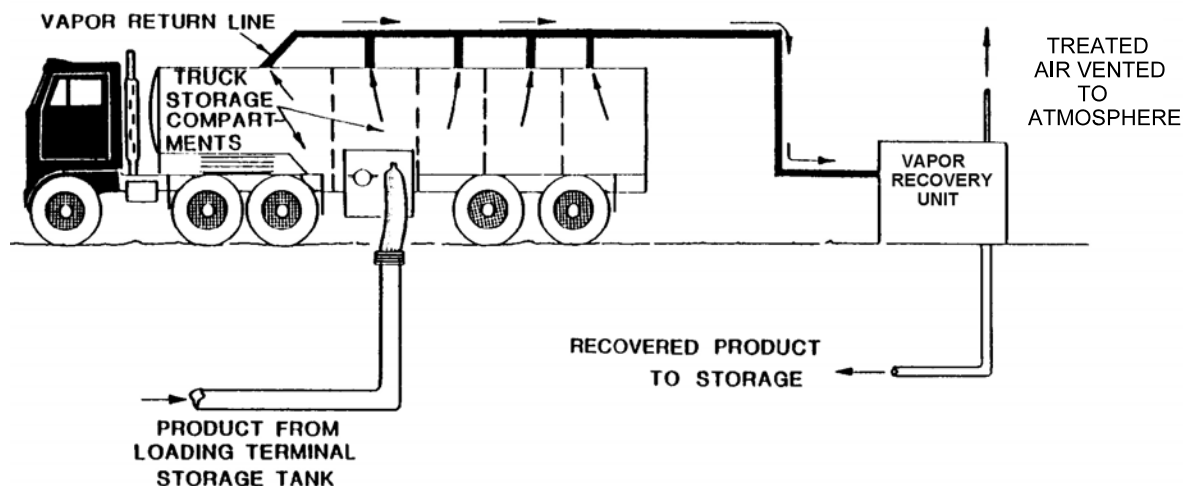


Figure 5.2-6. Tank truck loading with vapor recovery.

## **Section 5.6**

### **Condensate Truck Loading (Unit L1)**

#### **Actual Emission Calculations**



## Condensate Truck Loading Actual Emissions Calculations

Unit Number: **L1**

Description: Truck Loading

### Emission Factor

**0.6**

Saturation factor, S

AP-42, Table 5.2-1 (submerged loading  
& dedicated service)**3.5613** psia

True vapor pressure of liquid, P

TANKS 4.0 output file

**67.5024** lb/lb-mole

Molecular weight of vapors, M

TANKS 4.0 output file

**67.36** °F

Temperature of liquid

TANKS 4.0 output file

527.0 °R

Temperature of liquid, T

°F + 459.67

3.41 lb/10<sup>3</sup> gal

Emission factor, L

AP-42, Section 5.2, Equation 1

L = 12.46 (SPM/T)

### Production Rate

**154.05** 10<sup>3</sup> gal/yrMaximum annual production rate  
(= 3,667.8 bbl/yr)

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### Steady-State Emission Rates

| Pollutant | Emission Rates, tpy |
|-----------|---------------------|
| VOC       | 2.63E-01            |

Emission Rate (tpy) = lb/10<sup>3</sup> gal x 10<sup>3</sup> gal/yr / 2,000 lb/ton

| Pollutants   | Percent of VOC, % | Emission Rates, tpy |
|--------------|-------------------|---------------------|
| Benzene      | <b>0.55</b>       | 1.46E-03            |
| Ethylbenzene | <b>0.03</b>       | 7.96E-05            |
| n-Hexane     | <b>8.64</b>       | 2.27E-02            |
| Isooctane    | <b>0.11</b>       | 2.85E-04            |
| Toluene      | <b>0.07</b>       | 1.91E-04            |
| m-Xylene     | <b>0.12</b>       | 3.19E-04            |

Liquid percent of VOC calculated from the TANKS 4.0 results

Percent of VOC (%) = 100 x Pollutant Emission Rate (lb/yr) / Total VOC Emission Rate (lb/yr)

Emission Rates (tpy) = VOC Emission Rate (tpy) x (%) / 100

## **Section 5.7**

**Heaters (Units 4 & 5)**

**Written Description**

### ***Heaters (Units 4 & 5)***

Emissions from the heaters were calculated using AP-42 emission factors from Tables 1.4-1 & 1.4-2. PTE and emissions were calculated assuming the heaters operate at full capacity for 8,760 hours per year.

In this application, there are no changes to the calculations as they were presented in Revision 1 of the application.

The calculations demonstrate the heaters are insignificant sources. Therefore, actual emissions were not calculated.

## **Section 5.7**

**Heaters (Units 4 & 5)**

**PTE Emission Calculations**

## Heater Exhaust PTE Emissions Calculations

Unit Number: **4**

Description: Fuel Gas Heater

### Fuel Consumption

**0.30** MMBtu/hr

333 scf/hr

**8,760** hr/yr

2,628 MMBtu/yr

2.92 MMscf/yr

**900** Btu/scf

Capacity

Hourly fuel consumption

Annual operating time

Annual fuel consumption

Annual fuel consumption

Field gas heating value

Mfg. data

MMBtu/hr x 1,000,000 / Btu/scf

Harvest Four Corners, LLC

MMBtu/hr x hr/yr

scf/hr x hr/yr / 1,000,000

Nominal heat content

### Steady-State Emission Rates

| Pollutants | Emission Factors,<br>lb/MMscf | Uncontrolled Emission Rates, |          |
|------------|-------------------------------|------------------------------|----------|
|            |                               | pph                          | tpy      |
| NOX        | <b>100</b>                    | 3.33E-02                     | 1.46E-01 |
| CO         | <b>84</b>                     | 2.80E-02                     | 1.23E-01 |
| VOC        | <b>5.5</b>                    | 1.83E-03                     | 8.03E-03 |
| SO2        | <b>0.6</b>                    | 2.00E-04                     | 8.76E-04 |
| TSP        | <b>7.60</b>                   | 2.53E-03                     | 1.11E-02 |
| PM10       | <b>7.60</b>                   | 2.53E-03                     | 1.11E-02 |
| PM2.5      | <b>7.60</b>                   | 2.53E-03                     | 1.11E-02 |

Emission factors taken from AP-42, Tables 1.4-1 &amp; 1.4-2

Uncontrolled Emission Rates (pph) = lb/MMscf x MMscf/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

## Heater Exhaust PTE Emissions Calculations

Unit Number: **5**  
 Description: Tank Heater

### Fuel Consumption

**0.012** MMBtu/hr  
 13 scf/hr  
**8,760** hr/yr  
 105 MMBtu/yr  
 0.12 MMscf/yr  
**900** Btu/scf

Capacity  
 Hourly fuel consumption  
 Annual operating time  
 Annual fuel consumption  
 Annual fuel consumption  
 Field gas heating value

Mfg. data  
 MMBtu/hr x 1,000,000 / Btu/scf  
 Harvest Four Corners, LLC  
 MMBtu/hr x hr/yr  
 scf/hr x hr/yr / 1,000,000  
 Nominal heat content

### Steady-State Emission Rates

| Pollutants | Emission Factors,<br>lb/MMscf | Uncontrolled Emission Rates, |          |
|------------|-------------------------------|------------------------------|----------|
|            |                               | pph                          | tpy      |
| NOX        | <b>100</b>                    | 1.33E-03                     | 5.84E-03 |
| CO         | <b>84</b>                     | 1.12E-03                     | 4.91E-03 |
| VOC        | <b>5.5</b>                    | 7.33E-05                     | 3.21E-04 |
| SO2        | <b>0.6</b>                    | 8.00E-06                     | 3.50E-05 |
| TSP        | <b>7.60</b>                   | 1.01E-04                     | 4.44E-04 |
| PM10       | <b>7.60</b>                   | 1.01E-04                     | 4.44E-04 |
| PM2.5      | <b>7.60</b>                   | 1.01E-04                     | 4.44E-04 |

Emission factors taken from AP-42, Tables 1.4-1 & 1.4-2

Uncontrolled Emission Rates (pph) = lb/MMscf x MMscf/hr

Uncontrolled Emission Rates (tpy) = Uncontrolled Emission Rates (pph) x hr/yr / 2,000 lb/ton

Table 1.4-1. EMISSION FACTORS FOR NITROGEN OXIDES (NO<sub>x</sub>) AND CARBON MONOXIDE (CO)  
FROM NATURAL GAS COMBUSTION<sup>a</sup>

| Combustor Type<br>(MMBtu/hr Heat Input)<br>[SCC]                                | NO <sub>x</sub> <sup>b</sup>                |                              | CO  |                              |
|---|---|------------------------------|---|------------------------------|
|   | Emission Factor<br>(lb/10 <sup>6</sup> scf) | Emission<br>Factor<br>Rating | Emission Factor<br>(lb/10 <sup>6</sup> scf) | Emission<br>Factor<br>Rating |
| Large Wall-Fired Boilers<br>(>100)<br>[1-01-006-01, 1-02-006-01, 1-03-006-01]   |   |                              |   |                              |
| Uncontrolled (Pre-NSPS) <sup>c</sup>  | 280   | A                            | 84  | B                            |
| Uncontrolled (Post-NSPS) <sup>c</sup>   | 190   | A                            | 84  | B                            |
| Controlled - Low NO <sub>x</sub> burners  | 140   | A                            | 84  | B                            |
| Controlled - Flue gas recirculation   | 100   | D                            | 84  | B                            |
| Small Boilers<br>(≤100)<br>[1-01-006-02, 1-02-006-02, 1-03-006-02, 1-03-006-03] |   |                              |   |                              |
| Uncontrolled  | 100   | B                            | 84  | B                            |
| Controlled - Low NO <sub>x</sub> burners  | 50  | D                            | 84  | B                            |
| Controlled - Low NO <sub>x</sub> burners/Flue gas recirculation                 | 32  | C                            | 84  | B                            |
| Tangential-Fired Boilers<br>(All Sizes)<br>[1-01-006-04]                        |   |                              |   |                              |
| Uncontrolled  | 170   | A                            | 24  | C                            |
| Controlled - Flue gas recirculation   | 76  | D                            | 98  | D                            |
| Residential Furnaces<br>(≤0.3)<br>[No SCC]                                      |   |                              |   |                              |
| Uncontrolled  | 94  | B                            | 40  | B                            |

<sup>a</sup> Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. To convert from lb/10<sup>6</sup> scf to kg/10<sup>6</sup> m<sup>3</sup>, multiply by 16. Emission factors are based on an average natural gas higher heating value of 1,020 Btu/scf. To convert from lb/10<sup>6</sup> scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable.

<sup>b</sup> Expressed as NO<sub>2</sub>. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO<sub>x</sub> emission factor. For tangential-fired boilers with SNCR control, apply a 13 percent reduction to the appropriate NO<sub>x</sub> emission factor.

<sup>c</sup> NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of heat input that commenced construction modification, or reconstruction after August 17, 1971, and units with heat input capacities between 100 and 250 MMBtu/hr that commenced construction modification, or reconstruction after June 19, 1984.

TABLE 1.4-2. EMISSION FACTORS FOR CRITERIA POLLUTANTS AND GREENHOUSE GASES FROM NATURAL GAS COMBUSTION<sup>a</sup>

| Pollutant  | Emission Factor<br>(lb/10 <sup>6</sup> scf) | Emission Factor Rating |
|--|---|------------------------|
| CO <sub>2</sub> <sup>b</sup>                             | 120,000                                     | A                      |
| Lead   | 0.0005                                      | D                      |
| N <sub>2</sub> O (Uncontrolled)                          | 2.2   | E                      |
| N <sub>2</sub> O (Controlled-low-NO <sub>x</sub> burner) | 0.64  | E                      |
| PM (Total) <sup>c</sup>                                  | 7.6   | D                      |
| PM (Condensable) <sup>c</sup>                            | 5.7   | D                      |
| PM (Filterable) <sup>c</sup>                             | 1.9   | B                      |
| SO <sub>2</sub> <sup>d</sup>                             | 0.6   | A                      |
| TOC  | 11  | B                      |
| Methane  | 2.3   | B                      |
| VOC  | 5.5   | C                      |

<sup>a</sup> Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from lb/10<sup>6</sup> scf to kg/10<sup>6</sup> m<sup>3</sup>, multiply by 16. To convert from lb/10<sup>6</sup> scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. TOC = Total Organic Compounds.

VOC = Volatile Organic Compounds.

<sup>b</sup> Based on approximately 100% conversion of fuel carbon to CO<sub>2</sub>. CO<sub>2</sub>[lb/10<sup>6</sup> scf] = (3.67) (CON) (C)(D), where CON = fractional conversion of fuel carbon to CO<sub>2</sub>, C = carbon content of fuel by weight (0.76), and D = density of fuel, 4.2x10<sup>4</sup> lb/10<sup>6</sup> scf.

<sup>c</sup> All PM (total, condensable, and filterable) is assumed to be less than 1.0 micrometer in diameter. Therefore, the PM emission factors presented here may be used to estimate PM<sub>10</sub>, PM<sub>2.5</sub> or PM<sub>1</sub> emissions. Total PM is the sum of the filterable PM and condensable PM. Condensable PM is the particulate matter collected using EPA Method 202 (or equivalent). Filterable PM is the particulate matter collected on, or prior to, the filter of an EPA Method 5 (or equivalent) sampling train.

<sup>d</sup> Based on 100% conversion of fuel sulfur to SO<sub>2</sub>.

Assumes sulfur content is natural gas of 2,000 grains/10<sup>6</sup> scf. The SO<sub>2</sub> emission factor in this table can be converted to other natural gas sulfur contents by multiplying the SO<sub>2</sub> emission factor by the ratio of the site-specific sulfur content (grains/10<sup>6</sup> scf) to 2,000 grains/10<sup>6</sup> scf.



## **Section 5.8**

**Pig Launcher & Receiver (Units PL & PR)**

**Written Description**

### ***Pig Launcher & Receiver (PL & PR)***

Harvest recently updated their estimate of the pig receiver blowdown volume. The volume released was calculated from the receiver dimensions and pipeline pressure. The new calculations are included on the pig launcher and receiver emissions calculations spreadsheets.

Emissions from pig receiving occur when the receiver is opened to remove the pigging devices. The emissions were calculated from the number of events, the volume of gas released per event, and composition of the gas. The quantity of gas vented during each event was calculated by Harvest (see paragraph above). The composition of the gas was based on a recent gas analysis from the facility. It was conservatively estimated by operations that pig launching will occur once per month and pig receiving will occur 116 times per year (twice per week plus once per month as a safety factor).

Four extended gas analyses (collected during the last five years, 2017 - 2021) were available for use in the application: April 2017, April 2018, October 2019, and May 2021. Harvest calculated pig launcher and receiver emissions using the analysis that predicted the highest VOC emission rates, the May 2021 analysis.

In this application, there are no changes to the calculations as they were presented in Revision 1 of the application.

Calculations demonstrate that both the pig launcher and the pig receiver are insignificant sources. Therefore, actual emissions were not calculated.

### **Response to EPA request for additional information:**

- Clarify in the new application if the condensate sample analysis is being used to calculate flash emission using VMGSYm for the pigging activities. If not, explain why? The worst-case sample analysis results during the 5-year term of the permit should be used here as well.

A condensate analysis was not used to calculate pigging emissions. As stated above, emissions were calculated using a recent extended gas analysis, the analysis from the last five years that produced the highest VOC emission rate. A gas sample from the facility is the best available representation of the composition. Note that liquids from the pigging operations are sent to the condensate tanks and any flash emissions from that liquid are accounted for in the condensate tank flash emissions calculations.

**Response to EPA request for additional information:**

- Provide recordkeeping to confirm the pigging activities number of events per week.

Though Harvest is not required to keep records of pigging activities, a listing of the 2021 events is included in Section 8.

**Response to EPA request for additional information:**

- The pigging activity emission calculations including an example calculation that aligns with an actual description of the activity as conducted at the Facility.

In Revision 1 of the application, Harvest provided detailed calculations for the pigging activities. This application contains those same calculations.

**Response to EPA request for additional information:**

- An explanation of how VOC emissions are calculated using the well gas analysis for all the emission units that this analysis is used for and a calculation that demonstrates this description.

The gas passing through the facility is a blend of gas from wells throughout the area. See the written description above and the calculation spreadsheets.

## **Section 5.8**

**Pig Launcher & Receiver (Units PL & PR)**

**PTE Emission Calculations**

## Pig Launcher PTE Emissions Calculations

Unit Number: **PL**  
 Description: Pig Launcher

### Blowdown Volume

| Outside Diameter, in | Wall Thickness, in | Tube Length, ft | Port Size, in | Pressure, psig | Purge Duration, min | Gas Loss, mscf |
|----------------------|--------------------|-----------------|---------------|----------------|---------------------|----------------|
| <b>16</b>            | <b>0.375</b>       | <b>7</b>        | <b>1</b>      | <b>210</b>     | <b>1</b>            | 3.627          |

Blowdown Gas Loss

$$(((\text{Outside diameter (in)} - 2 * [\text{Wall thickness (in)}])^2) * [\text{Pressure (psig)}] * [\text{Pipeline length (ft)}] * 0.372 / 1000000$$

Purge Gas Loss

$$([\text{Port size (in)}]^2 * [\text{Pressure (psig)}] * ([\text{Purge duration (min)}] / 60)$$

### Throughput

**12** events/yr  
 3,627 scf/event  
 43,526 scf/yr

Blowdowns per year  
 Gas loss per blowdown  
 Annual gas loss

Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 events/yr x scf/event

### Emission Rates

| Pollutants   | Emission Factors, lb/scf | Uncontrolled, Emission Rates, tpy |
|--------------|--------------------------|-----------------------------------|
| VOC          | 1.307E-02                | 2.84E-01                          |
| Benzene      | 2.532E-05                | 5.51E-04                          |
| Ethylbenzene | 5.597E-07                | 1.22E-05                          |
| n-Hexane     | 2.950E-04                | 6.42E-03                          |
| Isooctane    | 7.396E-06                | 1.61E-04                          |
| Toluene      | 4.007E-05                | 8.72E-04                          |
| Xylene       | 6.716E-06                | 1.46E-04                          |

Emission factors calculated from gas composition (see table below)

Uncontrolled Emission Rates (tpy) = scf/yr x lb/scf / 2,000 lb/ton

### Gas Composition

| Components        | Mole Percents, % | Molecular Weights, lb/lb-mole | Emission Factors, lb/scf |
|-------------------|------------------|-------------------------------|--------------------------|
| Carbon dioxide    | <b>0.8632</b>    | 44.01                         | 1.001E-03                |
| Hydrogen sulfide  | <b>0.0000</b>    | 34.07                         | 0.000E+00                |
| Nitrogen          | <b>0.4462</b>    | 28.01                         | 3.294E-04                |
| Methane           | <b>78.7294</b>   | 16.04                         | 3.328E-02                |
| Ethane            | <b>10.7901</b>   | 30.07                         | 8.552E-03                |
| Propane           | <b>5.0734</b>    | 44.09                         | 5.896E-03                |
| Isobutane         | <b>0.8940</b>    | 58.12                         | 1.370E-03                |
| n-Butane          | <b>1.5609</b>    | 58.12                         | 2.391E-03                |
| Isopentane        | <b>0.5577</b>    | 72.15                         | 1.061E-03                |
| n-Pentane         | <b>0.4298</b>    | 72.15                         | 8.173E-04                |
| Cyclopentane      | <b>0.0189</b>    | 70.14                         | 3.494E-05                |
| n-Hexane          | <b>0.1299</b>    | 86.17                         | 2.950E-04                |
| Cyclohexane       | <b>0.0389</b>    | 84.16                         | 8.629E-05                |
| Other hexanes     | <b>0.2872</b>    | 86.18                         | 6.524E-04                |
| Heptanes          | <b>0.0720</b>    | 100.20                        | 1.902E-04                |
| Methylcyclohexane | <b>0.0556</b>    | 98.19                         | 1.439E-04                |
| Isooctane         | <b>0.0028</b>    | 100.21                        | 7.396E-06                |
| Benzene           | <b>0.0123</b>    | 78.11                         | 2.532E-05                |
| Toluene           | <b>0.0165</b>    | 92.14                         | 4.007E-05                |
| Ethylbenzene      | <b>0.0002</b>    | 106.17                        | 5.597E-07                |
| Xylenes           | <b>0.0024</b>    | 106.17                        | 6.716E-06                |
| C8+ Heavies       | <b>0.0187</b>    | 110.00                        | 5.422E-05                |
| Total             | 100.0001         |                               |                          |
| Total VOC         |                  |                               | 1.307E-02                |

Gas stream composition obtained from **Los Mestenos** extended gas analysis dated **05/06/2021**

Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole

## Pig Receiver PTE Emissions Calculations

Unit Number: **PR**  
 Description: Pig Receiver

### Blowdown Volume

| Outside Diameter, in | Wall Thickness, in | Tube Length, ft | Port Size, in | Pressure, psig | Purge Duration, min | Gas Loss, mcf |
|----------------------|--------------------|-----------------|---------------|----------------|---------------------|---------------|
| <b>12</b>            | <b>0.375</b>       | <b>8</b>        | <b>1</b>      | <b>95</b>      | <b>1</b>            | 1.619         |

Blowdown Gas Loss

$(([\text{Outside diameter (in)}] - 2 * [\text{Wall thickness (in)}])^2 * [\text{Pressure (psig)}] * [\text{Pipeline length (ft)}] * 0.372 / 1000000$

Purge Gas Loss

$([\text{Port size (in)}]^2 * [\text{Pressure (psig)}] * ([\text{Purge duration (min)}] / 60)$

### Throughput

**116** events/yr  
 1,619 scf/event  
 187,817 scf/yr

Blowdowns per year  
 Gas loss per blowdown  
 Annual gas loss

Harvest Four Corners, LLC  
 Harvest Four Corners, LLC  
 events/yr x scf/event

### Emission Rates

| Pollutants   | Emission Factors, lb/scf | Uncontrolled, Emission Rates, tpy |
|--------------|--------------------------|-----------------------------------|
| VOC          | 1.307E-02                | 1.23                              |
| Benzene      | 2.532E-05                | 2.38E-03                          |
| Ethylbenzene | 5.597E-07                | 5.26E-05                          |
| n-Hexane     | 2.950E-04                | 2.77E-02                          |
| Isooctane    | 7.396E-06                | 6.95E-04                          |
| Toluene      | 4.007E-05                | 3.76E-03                          |
| Xylene       | 6.716E-06                | 6.31E-04                          |

Emission factors calculated from gas composition (see table below)

Uncontrolled Emission Rates (tpy) = scf/yr x lb/scf / 2,000 lb/ton

### Gas Composition

| Components        | Mole Percents, % | Molecular Weights, lb/lb-mole | Emission Factors, lb/scf |
|-------------------|------------------|-------------------------------|--------------------------|
| Carbon dioxide    | <b>0.8632</b>    | 44.01                         | 1.001E-03                |
| Hydrogen sulfide  | <b>0.0000</b>    | 34.07                         | 0.000E+00                |
| Nitrogen          | <b>0.4462</b>    | 28.01                         | 3.294E-04                |
| Methane           | <b>78.7294</b>   | 16.04                         | 3.328E-02                |
| Ethane            | <b>10.7901</b>   | 30.07                         | 8.552E-03                |
| Propane           | <b>5.0734</b>    | 44.09                         | 5.896E-03                |
| Isobutane         | <b>0.8940</b>    | 58.12                         | 1.370E-03                |
| n-Butane          | <b>1.5609</b>    | 58.12                         | 2.391E-03                |
| Isopentane        | <b>0.5577</b>    | 72.15                         | 1.061E-03                |
| n-Pentane         | <b>0.4298</b>    | 72.15                         | 8.173E-04                |
| Cyclopentane      | <b>0.0189</b>    | 70.14                         | 3.494E-05                |
| n-Hexane          | <b>0.1299</b>    | 86.17                         | 2.950E-04                |
| Cyclohexane       | <b>0.0389</b>    | 84.16                         | 8.629E-05                |
| Other hexanes     | <b>0.2872</b>    | 86.18                         | 6.524E-04                |
| Heptanes          | <b>0.0720</b>    | 100.20                        | 1.902E-04                |
| Methylcyclohexane | <b>0.0556</b>    | 98.19                         | 1.439E-04                |
| Isooctane         | <b>0.0028</b>    | 100.21                        | 7.396E-06                |
| Benzene           | <b>0.0123</b>    | 78.11                         | 2.532E-05                |
| Toluene           | <b>0.0165</b>    | 92.14                         | 4.007E-05                |
| Ethylbenzene      | <b>0.0002</b>    | 106.17                        | 5.597E-07                |
| Xylenes           | <b>0.0024</b>    | 106.17                        | 6.716E-06                |
| C8+ Heavies       | <b>0.0187</b>    | 110.00                        | 5.422E-05                |
| Total             | 100.0001         |                               |                          |
| Total VOC         |                  |                               | 1.307E-02                |

Gas stream composition obtained from **Los Mestenos** extended gas analysis dated **05/06/2021**

Emission Factors (lb/scf) = (% / 100) x lb/lb-mole / 379.4 scf/lb-mole

## **Section 5.9**

### **Produced Water Storage Tank (Unit T3)**

#### **Written Description**

### ***Produced Water Storage Tank (Unit T3)***

Emissions from the produced water storage tanks were calculated using a throughput of 840 bbl/yr and emission factors from the Colorado Department of Public Health and Environment (CDPHE) and the Texas Commission on Environmental Quality (TCEQ).

In this application, there are no changes to the calculations as they were presented in both previous applications.

Calculations demonstrate that the produced water storage tanks are insignificant sources. Therefore, actual emissions were not calculated.

#### **Response to EPA request for additional information:**

- Explain the use of emission factors from Colorado, meteorological data from Colorado, etc. instead of New Mexico.

New Mexico has not yet developed emission factors for produced water. The AP-42 Chapter 7 equations/algorithms are not applicable to tanks without roofs. Even if a tank has some sort of roof, the composition of the water is not typically known. The only known emissions factors from states around New Mexico come from the CDPHE and TCEQ.

#### **Response to EPA request for additional information:**

- Provide explanation for using 2010 TCEQ guidance for produced water emission factor and not more recent information. Also, use NMED guidance instead of, i.e., information specific to area where facility is located.

New Mexico has not yet developed emission factors for produced water. The only known emissions factors from states around New Mexico come from the CDPHE and TCEQ. We have found nothing more recent.



## **Section 5.9**

### **Produced Water Storage Tank (Unit T3)**

#### **PTE Emission Calculations**

## Produced Water Storage Tank PTE Emissions Calculations

Unit Number: **T3**

Description: Produced Water Tank

Note: The data on this worksheet applies to each individual emissions unit identified above.

### Throughput

**70** bbl/turnover**12** turnover/yr

840 bbl/yr

Tank capacity

Turnovers per year

Annual liquid throughput

Harvest Four Corners, LLC

Harvest Four Corners, LLC

bbl/turnover x turnover/yr

### Emission Rates

| Pollutant    | Emission Factor, lb/bbl | Uncontrolled, Emission Rate, tpy |
|--------------|-------------------------|----------------------------------|
| VOC          | <b>0.262</b>            | 1.10E-01                         |
| Benzene      | <b>0.007</b>            | 2.94E-03                         |
| Ethylbenzene | <b>0.0007</b>           | 2.94E-04                         |
| n-Hexane     | <b>0.022</b>            | 9.24E-03                         |
| Toluene      | <b>0.009</b>            | 3.78E-03                         |
| Xylene       | <b>0.006</b>            | 2.52E-03                         |

VOC, Benzene, and n-Hexane emission factors are taken from the CDPHE PS Memo 09-02

(Oil &amp; Gas Produced Water Tank Batteries - Regulatory Definitions &amp; Permitting Guidance)

Ethylbenzene, toluene, and xylene emissions factors (Non-Texas) are taken from the TCEQ

Project 2010-29 (Emission Factor Determination for Produced Water Storage Tanks) report

Uncontrolled Emission Rates (tpy) = lb/bbl x bbl/yr / 2,000 lb/ton

## PS Memo 09-02

**To:** Stationary Sources Program, Local Agencies, and Regulated Community  
**From:** Chris Laplante and Roland C. Hea, Colorado Air Pollution Control Division  
**Date:** February 8, 2010  
**Subject:** Oil & Gas Produced Water Tank Batteries  
Regulatory Definitions and Permitting Guidance

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This guidance document is intended to answer frequently asked questions concerning oil and gas industry produced water tank batteries. This document does not address any other equipment types that may be part of a common facility with a tank battery. Nothing in this guidance should be construed regarding Air Pollution Control Division (Division) permitting of evaporation ponds or water treatment facilities. Please consult with the Division for information regarding the permitting of evaporation ponds or water treatment facilities.

### Revision History

|                  |   |
|------------------|---|
| October 1, 2009  | Initial issuance.   |
| February 8, 2010 | First revision. This guidance document replaces the October 1, 2009 version. Revised language to clarify APEN fee structure, definition of modification, APEN submittals, and produced water exemption. |

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### 3. EMISSION FACTORS AND SITE SPECIFIC SAMPLING Q&A

#### 3.1. *What are the State approved default emission factors for produced water tanks?*

| County  | Produced Water Tank Default Emission Factors <sup>1</sup> (lb/bbl) <sup>2</sup> |         |          |
|---|---|---------|----------|
|   | VOC   | Benzene | n-Hexane |
| Adams, Arapahoe, Boulder, Broomfield, Denver, Douglas, Jefferson, Larimer, & Weld | 0.262   | 0.007   | 0.022    |
| Garfield, Mesa, Rio Blanco, & Moffat  | 0.178   | 0.004   | 0.010    |
| Remainder of Colorado <sup>3</sup>  | 0.262   | 0.007   | 0.022    |

<sup>1</sup> Testing may be performed at any site to determine site-specific emissions factors. These default emission factors may be revised by the Division in the future, pending approved data and testing results.

<sup>2</sup> Units of lb/bbl means pounds of emissions per barrel of produced water throughput

<sup>3</sup> For counties not listed in this table, use the emissions factors listed as a conservative measure or perform testing to determine a site-specific emission factor

#### 3.2. *What type of emissions are included in the produced water tank state default emission factors?*

State default emission factors for produced water tanks include flash, working, and breathing losses.

#### 3.3. *Are there limits as to when produced water tank state default emission factors may be used?*

State default emission factors may be used at all oil and gas industry tank batteries. The Division intends to work with industry to refine emission factors and may develop separate emission factors for E&P and non-E&P sites.

#### 3.4. *When are site-specific emission factors required for tank batteries?*

Site-specific emission factors may be developed and used on a voluntary basis for any tank battery. The Division reserves the authority to require site-specific emission factors at any time. Site-specific emission factors may only be applied at the tank battery for which they were developed, unless otherwise approved by the Division.

#### 3.5. *How is a site-specific emission factor developed?*

A site-specific emission factor for tank batteries is developed by performing a Division approved stack test. A test protocol must be submitted and approved by the Division prior to performing the test. Once a test protocol has been approved by the Division, subsequent testing may be performed following the approved protocol without submittal to the Division.

The Division must be notified of the site specific testing at least 30-days prior to the actual test date.



Emission Factor  
Determination for Produced  
Water Storage Tanks

TCEQ Project 2010-29

Prepared for:  
**Texas Commission on Environmental Quality**  
**Austin, Texas**

Prepared by:  
**ENVIRON International Corporation**  
**Novato, California**

Date:  
**August 2010**

ENVIRON Project Number:  
**06-17477T**

Document source:

<https://www.tceq.texas.gov/assets/public/implementation/air/am/contracts/reports/ei/5820784005FY1024-20100830-environ-%20EmissionFactorDeterminationForProducedWaterStorageTanks.pdf>

## Executive Summary

The overall purpose of this Study is to evaluate volatile organic compounds (VOC), speciated VOC and hazardous air pollutant (HAP) emissions from produced water and/or saltwater storage tanks servicing oil and gas wells and to develop appropriate VOC and HAP emission factors. The emission factors are to be used for emission inventory development purposes.

The primary source of information for this study was testing conducted by the Texas Commission on Environmental Quality (TCEQ) under Work Order 522-7-84005-FY10-25, *Upstream Oil & Gas Tank Measurements*, TCEQ Project 2010-39. As part of this referenced testing project, pressurized produced water samples were taken at seven different tank batteries located in Johnson, Wise and Tarrant Counties, Texas (all part of the Eastern Barnett Shale region) and analyzed for flash gas volume and composition. The sample collection and analysis conducted as part of TCEQ Project 2010-39 was done according to strict sampling and quality assurance procedures. In addition to TCEQ Project 2010-39 data, a thorough review of publically-available information sources identified a limited amount of data on produced water emissions. This was supplemented by data provided by two natural gas producers and one petroleum engineering services company. Other than TCEQ Project 2010-39 data, however, it could not be confirmed that any of the data had undergone a rigorous quality assurance process and therefore is considered secondary data, used to support conclusions drawn using the primary data but not used directly in deriving the produced water emission factors.

Emissions from produced water storage tanks consist of flash emissions, working losses and breathing losses. Flash emissions are determined using flash gas analysis. Working and breathing losses are estimated using EPA TANKS 4.09d software. Using this approach and the assumptions detailed within this report, it is determined that working and breathing losses associated with primary data source sites are very small compared to flash emissions and can be ignored without affecting the overall emission factor determination.

Table ES-1 presents the recommended emission factors for VOC and four HAPs – benzene, toluene, ethylbenzene and xylenes – derived from the primary data source sites. For comparative purposes, average emissions from Texas and non-Texas secondary sites are also presented in Table ES-1.

**Table ES-1. Recommended Emission Factors and Comparative Data**

| Pollutant    | Average Produced Water Emission Factor by Data Set (lb/bbl) |                        |                            |
|--------------|---|------------------------|----------------------------|
|              | Recommended Emission Factor                                 | Secondary Data – Texas | Secondary Data – Non-Texas |
| VOC          | 0.01  | 0.012                  | 0.18                       |
| Benzene      | 0.0001  | 0.0012                 | 0.004                      |
| Toluene      | 0.0003  | 0.0012                 | 0.009                      |
| Ethylbenzene | 0.000006  | 0.0001                 | 0.0007                     |
| Xylenes      | 0.00006   | 0.0003                 | 0.006                      |

## **Section 5.10**

**Produced Water Truck Loading (Unit L2)**

**Written Description**

### ***Produced Water Truck Loading (L-2)***

Emissions from produced water truck loading were calculated using the annual produced water throughput and the emission factor equation from AP-42, Section 5.2, *Transportation and Marketing of Petroleum Liquids*. The emission factor was calculated using Antoine's equation to calculate the true vapor pressure, the molecular weight of water, and an estimated average temperature of the liquid. Please see the calculations on the Produced Water Truck Loading Emissions Calculations spreadsheet.

PTE emissions were calculated assuming a throughput of 840 bbl/yr

In this application, there are no changes to the calculations as they were presented in both previous applications.

Calculations demonstrate that produced water truck loading is an insignificant source. Therefore, actual emissions were not calculated.



## **Section 5.10**

**Produced Water Truck Loading (Unit L2)**

**PTE Emission Calculations**

## Produced Water Truck Loading PTE Emissions Calculations

Unit Number: **L2**

Description: Truck Loading

### Emission Factor

|                                       |                                  |   |
|---------------------------------------|----------------------------------|---|
| <b>0.6</b>                            | Saturation factor, S             | AP-42, Table 5.2-1 (submerged loading & dedicated service)  |
| 0.3045 psia (average)                 | True vapor pressure of liquid, P | Estimated using Antoine's Equation (see calculations below) |
| <b>18.02</b> lb/lb-mole               | Molecular weight of vapors, M    | TANKS 4.0 Database  |
| 65 °F (average)                       | Temperature of liquid            | Estimated (see calculations below)                          |
| 524.67 °R (average)                   | Temperature of liquid, T         | °F + 459.67   |
| 0.08 lb/10 <sup>3</sup> gal (average) | Emission factor, L               | AP-42, Section 5.2, $L = 12.46 \frac{SPM}{T}$               |

### Production Rate

|                                     |                                |                           |
|-------------------------------------|--------------------------------|---------------------------|
| <b>35.28</b> 10 <sup>3</sup> gal/yr | Maximum annual production rate | Harvest Four Corners, LLC |
|-------------------------------------|--------------------------------|---------------------------|

### Steady-State Emission Rates

| Pollutant | Emission Rates, tpy |
|-----------|---------------------|
| VOC       | 1.38E-03            |

Uncontrolled Emission Rate (tpy) = lb/10<sup>3</sup> gal x 10<sup>3</sup> gal/yr / 2,000 lb/ton

| Pollutants   | Mass Fraction | Emission Rates, tpy |
|--------------|---------------|---------------------|
| Benzene      | <b>0.0267</b> | 3.69E-07            |
| Ethylbenzene | <b>0.0027</b> | 3.69E-08            |
| n-Hexane     | <b>0.0840</b> | 1.16E-06            |
| Toluene      | <b>0.0344</b> | 4.74E-07            |
| m-Xylene     | <b>0.0229</b> | 3.16E-07            |

HAP mass fractions are estimated from the produced water tank emission factors

HAP Mass Fraction = HAP Emission Factor (lb/bbl) / VOC Emission Factor (lb/bbl)

Emission Rates (tpy) = VOC Emission Rate (tpy) x HAP Mass Fraction

### Vapor Pressure of Produced Water:

It is estimated that the true vapor pressure of produced water is approximately equal to the true vapor pressure of pure water. An estimate of the true vapor pressure for water is calculated using Antoine's equation (see AP-42, Section 7.1, Equation 1-25).

#### Maximum:

Temperature = **77** °F

$$\log P = A - (B / (C + T))$$

$$A = 8.07131$$

$$B = 1730.63$$

$$C = 233.426$$

$$T = 25.00 \text{ }^{\circ}\text{C}$$

$$P = \text{mmHg}$$

$$P = 10^{(A - (B / (C + T)))}$$

$$P = 23.69 \text{ mmHg}$$

$$P = 0.4581 \text{ psi}$$

Note: 760 mmHg = 14.7 psia

#### Average:

Temperature = **65** °F

$$\log P = A - (B / (C + T))$$

$$A = 8.07131$$

$$B = 1730.63$$

$$C = 233.426$$

$$T = 18.33 \text{ }^{\circ}\text{C}$$

$$P = \text{mmHg}$$

$$P = 10^{(A - (B / (C + T)))}$$

$$P = 15.75 \text{ mmHg}$$

$$P = 0.3045 \text{ psi}$$

## **Section 5.11**

### **Miscellaneous Storage Tanks (Units T4 – T7)**

#### **Written Description**

### ***Miscellaneous Storage Tank (Unit T4 – T7)***

Residual oil #6 was used as an estimate for lubrication oil. As the vapor pressure of residual oil #6 is less than 0.2 psia, the tanks containing lubrication and used oil were assumed to be Title V insignificant sources. No calculations are provided.

Ambitrol is an inhibited ethylene or propylene glycol coolant (antifreeze) containing ethylene or propylene glycol, water, and less than 5% dipotassium hydrogen phosphate. Since the vapor pressures of ethylene glycol and propylene glycol are less than 0.2 psia, the tank containing Ambitrol was assumed to be a Title V insignificant source. No calculations are provided.

VOC emissions from the methanol storage tank were calculated using TANKS 4.0.9d. As emissions were only 44.79 pounds per year, the tank is a Title V insignificant source. A copy of the TANKS output file is provided.

In this application, there are no changes to the calculations as they were presented in both previous applications.

## **Section 5.11**

**Miscellaneous Storage Tanks (Units T4 – T7)**

**PTE Emission Calculations**

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Tank Identification and Physical Characteristics**

**Identification**

|                      |                                  |
|----------------------|----------------------------------|
| User Identification: | Los Mestenos - T7 - Methanol     |
| City:                | Gavilan                          |
| State:               | New Mexico                       |
| Company:             | Harvest Four Corners, LLC        |
| Type of Tank:        | Horizontal Tank                  |
| Description:         | 500 Gallon Methanol Storage Tank |

**Tank Dimensions**

|                            |          |
|----------------------------|----------|
| Shell Length (ft):         | 6.00     |
| Diameter (ft):             | 4.00     |
| Volume (gallons):          | 500.00   |
| Turnovers:                 | 12.00    |
| Net Throughput(gal/yr):    | 6,000.00 |
| Is Tank Heated (y/n):      | N        |
| Is Tank Underground (y/n): | N        |

**Paint Characteristics**

|                    |             |
|--------------------|-------------|
| Shell Color/Shade: | Gray/Medium |
| Shell Condition    | Good        |

**Breather Vent Settings**

|                          |       |
|--------------------------|-------|
| Vacuum Settings (psig):  | -0.03 |
| Pressure Settings (psig) | 0.03  |

Meterological Data used in Emissions Calculations: Albuquerque, New Mexico (Avg Atmospheric Pressure = 12.15 psia)

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Liquid Contents of Storage Tank**

**Los Mestenos - T7 - Methanol - Horizontal Tank**  
**Gavilan, New Mexico**

| Mixture/Component | Month | Daily Liquid Surf.<br>Temperature (deg F) |       |       | Liquid<br>Bulk<br>Temp<br>(deg F) | Vapor Pressure (psia) |        |        | Vapor<br>Mol.<br>Weight | Liquid<br>Mass<br>Fract. | Vapor<br>Mass<br>Fract. | Mol.<br>Weight | Basis for Vapor Pressure<br>Calculations |
|-------------------|-------|---|-------|-------|-----------------------------------|-----------------------|--------|--------|-------------------------|--------------------------|-------------------------|----------------|--|
|                   |       | Avg.                                      | Min.  | Max.  |                                   | Avg.                  | Min.   | Max.   |                         |                          |                         |                |  |
| Methyl alcohol    | All   | 67.36                                     | 53.93 | 80.79 | 59.23                             | 1.8115                | 1.1881 | 2.6951 | 32.0400                 |                          |                         | 32.04          | Option 2: A=7.897, B=1474.08, C=229.13   |

## TANKS 4.0.9d

### Emissions Report - Detail Format

### Detail Calculations (AP-42)

#### Los Mestenos - T7 - Methanol - Horizontal Tank Gavilan, New Mexico

|   |            |
|---|------------|
| <b>Annual Emission Calculations</b>       |            |
| Standing Losses (lb):                     | 36.5024    |
| Vapor Space Volume (cu ft):               | 48.0243    |
| Vapor Density (lb/cu ft):                 | 0.0103     |
| Vapor Space Expansion Factor:             | 0.2419     |
| Vented Vapor Saturation Factor:           | 0.8389     |
| <b>Tank Vapor Space Volume:</b>           |            |
| Vapor Space Volume (cu ft):               | 48.0243    |
| Tank Diameter (ft):                       | 4.0000     |
| Effective Diameter (ft):                  | 5.5293     |
| Vapor Space Outage (ft):                  | 2.0000     |
| Tank Shell Length (ft):                   | 6.0000     |
| <b>Vapor Density</b>                      |            |
| Vapor Density (lb/cu ft):                 | 0.0103     |
| Vapor Molecular Weight (lb/lb-mole):      | 32.0400    |
| Vapor Pressure at Daily Average Liquid    |            |
| Surface Temperature (psia):               | 1.8115     |
| Daily Avg. Liquid Surface Temp. (deg. R): | 527.0322   |
| Daily Average Ambient Temp. (deg. F):     | 56.1542    |
| Ideal Gas Constant R                      |            |
| (psia cu ft / (lb-mol-deg R)):            | 10.731     |
| Liquid Bulk Temperature (deg. R):         | 518.9042   |
| Tank Paint Solar Absorptance (Shell):     | 0.6800     |
| Daily Total Solar Insulation              |            |
| Factor (Btu/sqft day):                    | 1,765.3167 |
| <b>Vapor Space Expansion Factor</b>       |            |
| Vapor Space Expansion Factor:             | 0.2419     |
| Daily Vapor Temperature Range (deg. R):   | 53.7176    |
| Daily Vapor Pressure Range (psia):        | 1.5070     |
| Breather Vent Press. Setting Range(psia): | 0.0600     |
| Vapor Pressure at Daily Average Liquid    |            |
| Surface Temperature (psia):               | 1.8115     |
| Vapor Pressure at Daily Minimum Liquid    |            |
| Surface Temperature (psia):               | 1.1881     |
| Vapor Pressure at Daily Maximum Liquid    |            |
| Surface Temperature (psia):               | 2.6951     |
| Daily Avg. Liquid Surface Temp. (deg R):  | 527.0322   |
| Daily Min. Liquid Surface Temp. (deg R):  | 513.6028   |
| Daily Max. Liquid Surface Temp. (deg R):  | 540.4617   |
| Daily Ambient Temp. Range (deg. R):       | 27.9250    |
| <b>Vented Vapor Saturation Factor</b>     |            |
| Vented Vapor Saturation Factor:           | 0.8389     |
| Vapor Pressure at Daily Average Liquid:   |            |
| Surface Temperature (psia):               | 1.8115     |
| Vapor Space Outage (ft):                  | 2.0000     |
| <b>Working Losses (lb):</b>               |            |
| Working Losses (lb):                      | 8.2917     |
| Vapor Molecular Weight (lb/lb-mole):      | 32.0400    |
| Vapor Pressure at Daily Average Liquid    |            |
| Surface Temperature (psia):               | 1.8115     |
| Annual Net Throughput (gal/yr.):          | 6,000.0000 |
| Annual Turnovers:                         | 12.0000    |
| Turnover Factor:                          | 1.0000     |



|                              |         |
|------------------------------|---------|
| Tank Diameter (ft):          | 4.0000  |
| Working Loss Product Factor: | 1.0000  |
|                              |         |
| Total Losses (lb):           | 44.7941 |

**TANKS 4.0.9d**  
**Emissions Report - Detail Format**  
**Individual Tank Emission Totals**

**Emissions Report for: Annual**

**Los Mestenos - T7 - Methanol - Horizontal Tank**  
**Gavilan, New Mexico**

|                | Losses(lbs)  |                |                 |
|----------------|--------------|----------------|-----------------|
| Components     | Working Loss | Breathing Loss | Total Emissions |
| Methyl alcohol | 8.29         | 36.50          | 44.79           |

## **Section 5.12**

### **GHG Emissions**

#### **Written Description**

### ***GHG Emissions***

CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub>O exhaust emissions were calculated using emission factors from 40 Code of Federal Regulations (CFR), Part C, Tables C-1 & C-2 and the combustion source higher heating value (HHV) design heat rates.

The SSM CO<sub>2</sub> and CH<sub>4</sub> emissions were calculated from the annual blowdown volumes and gas composition.

CO<sub>2</sub> and CH<sub>4</sub> equipment leaks emissions were calculated using Subpart W emission factors and gas stream composition.

Four extended gas analyses (collected during the last five years, 2017 - 2021) were available for use in the application: April 2017, April 2018, October 2019, and May 2021. Harvest calculated SSM, Pigging and equipment leak emissions using the analysis that predicted the highest VOC emission rates, the May 2021 analysis.

Condensate tank CO<sub>2</sub> and CH<sub>4</sub> emissions were calculated from throughput and composition data in the VMGSim output file.

## **Section 5.12**

### **GHG Emissions**

#### **PTE Emission Calculations**

## Green House Gas Emissions Data and Calculations

| Sources                         | Facility Total Emissions |                       |                       |          |                        |
|---------------------------------|--------------------------|-----------------------|-----------------------|----------|------------------------|
|                                 | CO <sub>2</sub> , tpy    | CH <sub>4</sub> , tpy | N <sub>2</sub> O, tpy | GHG, tpy | CO <sub>2</sub> e, tpy |
| Engine & Turbine Exhaust        | 5,575.80                 | 1.06E-01              | 1.07E-02              | 5,575.92 | 5581.63                |
| SSM Blowdowns                   | 9.10E-01                 | 30.26                 | --                    | 31.17    | 757.30                 |
| Equipment Leaks                 | 1.69E-01                 | 5.61                  | --                    | 5.78     | 140.45                 |
| Storage Tanks (Flash Emissions) | 7.34E-01                 | 10.69                 | --                    | 11.43    | 268.06                 |
| Total                           | 5,577.61                 | 46.67                 | 1.07E-02              | 5,624.29 | 6,747.45               |

### Engine & Turbine Exhaust Emissions

| Unit Numbers | Description        | Emission Factors           |                            |                            | Emission Rates        |                       |                       |
|--------------|--------------------|----------------------------|----------------------------|----------------------------|-----------------------|-----------------------|-----------------------|
|              |                    | CO <sub>2</sub> , kg/MMBtu | CH <sub>4</sub> , kg/MMBtu | N <sub>2</sub> O, kg/MMBtu | CO <sub>2</sub> , tpy | CH <sub>4</sub> , tpy | N <sub>2</sub> O, tpy |
| 1            | Solar Saturn T1200 | 53.06                      | 1.00E-03                   | 1.00E-04                   | 5,544.61              | 1.04E-01              | 1.04E-02              |
| 3            | Scania DS11        | 73.96                      | 3.00E-03                   | 6.00E-04                   | 31.19                 | 1.27E-03              | 2.53E-04              |
|              | Total              |                            |                            |                            | 5,575.80              | 1.06E-01              | 1.07E-02              |

The emissions factors are taken from 40 CFR 98, Subpart C, Tables C-1 & C-2

Emission Rates (tpy) = kg/MMBtu x 2.2 lb/kg x MMBtu/yr / 2,000 lb/ton

| Unit Numbers | Description        | Fuel Types | Operating Times, hr/yr | LHV Design Heat Rates, MMBtu/hr | HHV                         |                       |
|--------------|--------------------|------------|------------------------|---------------------------------|-----------------------------|-----------------------|
|              |                    |            |                        |                                 | Design Heat Rates, MMBtu/hr | Fuel Usages, MMBtu/yr |
| 1            | Solar Saturn T1200 | Nat. Gas   | 8,760                  | 9.76                            | 10.84                       | 94,997                |
| 3            | Scania DS11        | Diesel     | 500                    | 0.69                            | 0.77                        | 383                   |

The fuel types and operating times are provided by Harvest

The LHV design heat rates are taken from manufacturers data

HHV Design Heat Rates (MMBtu/hr) = LHV Design Heat Rates (MMBtu/hr) / 0.9 LHV/HHV

HHV Fuel Usages (MMBtu/yr) = HHV Design Heat Rates (MMBtu/hr) x hr/yr

### SSM Blowdown Emissions

| Unit Numbers | Description   | Total Gas Losses, scf/yr | CO <sub>2</sub> Emission Factors, lb/scf | CH <sub>4</sub> Emission Factors, lb/scf | Emission Rates        |                       |
|--------------|---------------|--------------------------|--|--|-----------------------|-----------------------|
|              |               |                          |  |  | CO <sub>2</sub> , tpy | CH <sub>4</sub> , tpy |
| SSM          | SSM Blowdowns | 1,818,000                | 0.0010                                   | 0.0333                                   | 0.91                  | 30.26                 |

The annual blowdown volumes are calculated from data provided by Harvest

The CO<sub>2</sub> and CH<sub>4</sub> emission factors are calculated from the facility extended gas analysis

Emission Rates (tpy) = scf/yr x lb/scf / 2,000 lb/ton

### Equipment Leaks Emissions

| Unit Numbers | Description            | Emission Rates        |                       |
|--------------|------------------------|-----------------------|-----------------------|
|              |                        | CO <sub>2</sub> , tpy | CH <sub>4</sub> , tpy |
| NA           | Valves                 | 1.3E-01               | 4.45                  |
| NA           | Connectors             | 1.4E-02               | 4.6E-01               |
| NA           | Open-Ended Lines       | 9.9E-03               | 3.3E-01               |
| NA           | Pressure Relief Valves | 1.1E-02               | 3.7E-01               |
|              | Total                  | 1.7E-01               | 5.61                  |

A combination of equations W-31 & W-36 (Subpart W) is used to calculate uncombusted CO<sub>2</sub> & CH<sub>4</sub> emissions

Since the CO<sub>2</sub>e is not being calculated in this table, it is not necessary to include the global warming potential from equation W-36

CO<sub>2</sub> Emission Rate (tpy) = # x scf/hr/component x (CO<sub>2</sub> Content (mole %) / 100) x hr/yr x CO<sub>2</sub> Density (kg/scf)

x (2,204.6 lb/tonne / 2,000 lb/ton) / 1,000 kg/tonne

CH<sub>4</sub> Emission Rate (tpy) = # x scf/hr/component x (CH<sub>4</sub> Content (mole %) / 100) x hr/yr x CH<sub>4</sub> Density (kg/scf)

x (2,204.6 lb/tonne / 2,000 lb/ton) / 1,000 kg/tonne

## Green House Gas Emissions Data and Calculations

| Unit Numbers | Description            | Number of Components, # | Emission Factors, scf/hr /component | CO2 Contents, mole % | CH4 Contents, mole % | Operating Times, hr/yr | CO2 Density, kg/scf | CH4 Density, kg/scf |
|--------------|------------------------|-------------------------|-------------------------------------|----------------------|----------------------|------------------------|---------------------|---------------------|
| NA           | Valves                 | 252                     | 0.121                               | 0.86                 | 78.73                | 8,760                  | 0.0526              | 0.0192              |
| NA           | Connectors             | 187                     | 0.017                               | 0.86                 | 78.73                | 8,760                  | 0.0526              | 0.0192              |
| NA           | Open-Ended Lines       | 73                      | 0.031                               | 0.86                 | 78.73                | 8,760                  | 0.0526              | 0.0192              |
| NA           | Pressure Relief Valves | 13                      | 0.193                               | 0.86                 | 78.73                | 8,760                  | 0.0526              | 0.0192              |

The number of sources are calculated based on the number of compressors and dehydrators at the station (see criteria pollutant and HAP equipment leaks calculations)

The emission factors are taken from Subpart W, Table W-1A (Western U.S. - Gas Service)

The facility CO2 and CH4 contents are taken from the facility extended gas analysis

The operating times are provided by Harvest (default is the entire year)

The CO2 & CH4 densities are taken from Subpart W, Paragraph 98.233(v)

### Storage Tanks (Flash Emissions)

| Unit Number | Description     | Emission Rates |          |
|-------------|-----------------|----------------|----------|
|             |                 | CO2, tpy       | CH4, tpy |
| T1          | Condensate Tank | 7.34E-01       | 10.69    |
| T2          | Condensate Tank | --             | --       |
|             | Total           | 7.34E-01       | 10.69    |

Emission rates calculated from VMGSym results

### Gas Stream Composition

| Components             | Mole Percents, % | Molecular Weights, lb/lb-mole | Component Weights, lb/lb-mole | Weight Percent of Total, % | Emission Factors, lb/scf |
|------------------------|------------------|-------------------------------|-------------------------------|----------------------------|--------------------------|
| Carbon Dioxide         | 0.8632           | 44.01                         | 0.38                          | 1.7805                     | 0.0010                   |
| Hydrogen Sulfide       | 0.0000           | 34.07                         | 0.00                          | 0.0000                     | 0.0000                   |
| Nitrogen               | 0.4462           | 28.01                         | 0.12                          | 0.5857                     | 0.0003                   |
| Methane                | 78.7294          | 16.04                         | 12.63                         | 59.1848                    | 0.0333                   |
| Ethane                 | 10.7901          | 30.07                         | 3.24                          | 15.2064                    | 0.0086                   |
| Propane                | 5.0734           | 44.09                         | 2.24                          | 10.4835                    | 0.0059                   |
| IsoButane              | 0.8940           | 58.12                         | 0.52                          | 2.4352                     | 0.0014                   |
| Normal Butane          | 1.5609           | 58.12                         | 0.91                          | 4.2518                     | 0.0024                   |
| IsoPentane             | 0.5577           | 72.15                         | 0.40                          | 1.8858                     | 0.0011                   |
| Normal Pentane         | 0.4298           | 72.15                         | 0.31                          | 1.4534                     | 0.0008                   |
| Cyclopentane           | 0.0189           | 70.14                         | 0.01                          | 0.0621                     | 0.0000                   |
| n-Hexane               | 0.1299           | 86.17                         | 0.11                          | 0.5246                     | 0.0003                   |
| Cyclohexane            | 0.0389           | 84.16                         | 0.03                          | 0.1534                     | 0.0001                   |
| Other Hexanes          | 0.2872           | 86.18                         | 0.25                          | 1.1600                     | 0.0007                   |
| Heptanes               | 0.0720           | 100.20                        | 0.07                          | 0.3381                     | 0.0002                   |
| Methylcyclohexane      | 0.0556           | 98.19                         | 0.05                          | 0.2559                     | 0.0001                   |
| 2,2,4-Trimethylpentane | 0.0028           | 100.21                        | 0.00                          | 0.0132                     | 0.0000                   |
| Benzene                | 0.0123           | 78.11                         | 0.01                          | 0.0450                     | 0.0000                   |
| Toluene                | 0.0165           | 92.14                         | 0.02                          | 0.0713                     | 0.0000                   |
| Ethylbenzene           | 0.0002           | 106.17                        | 0.00                          | 0.0010                     | 0.0000                   |
| Xylenes                | 0.0024           | 106.17                        | 0.00                          | 0.0119                     | 0.0000                   |
| C8+ heavies            | 0.0187           | 110.00                        | 0.02                          | 0.0964                     | 0.0001                   |
| Total                  | 100.0001         |                               | 21.34                         | 100.0000                   | 0.0562                   |
| VOC                    |                  |                               | 4.96                          | --                         | 0.0131                   |

Gas stream composition obtained from Los Mestenos extended gas analysis dated 05/06/2021

Component Weights (lb/lb-mole) = [Mole Percents (%) / 100] x Molecular Weights (lb/lb-mole)

Weight Percent of Total (%) = 100 x Component Weights (lb/lb-mole) / Total Component Weight (lb/lb-mole)

Emission Factors (lb/scf) = [Mole Percents (%) / 100] x Molecular Weights (lb/lb-mole) / 379.4 scf/lb-mole

Table A-1 to Subpart A of Part 98—Global Warming Potentials

## GLOBAL WARMING POTENTIALS

[100-Year Time Horizon]

| Name                                  | CAS No.     | Chemical formula   | Global warming potential<br>(100 yr.) |
|---------------------------------------|-------------|--|---------------------------------------|
| Carbon dioxide                        | 124-38-9    | CO <sub>2</sub>  | 1                                     |
| Methane                               | 74-82-8     | CH <sub>4</sub>  | <sup>a</sup> 25                       |
| Nitrous oxide                         | 10024-97-2  | N <sub>2</sub> O   | <sup>a</sup> 298                      |
| HFC-23                                | 75-46-7     | CHF <sub>3</sub>   | <sup>a</sup> 14,800                   |
| HFC-32                                | 75-10-5     | CH <sub>2</sub> F <sub>2</sub>   | <sup>a</sup> 675                      |
| HFC-41                                | 593-53-3    | CH <sub>3</sub> F  | <sup>a</sup> 92                       |
| HFC-125                               | 354-33-6    | C <sub>2</sub> HF <sub>5</sub>   | <sup>a</sup> 3,500                    |
| HFC-134                               | 359-35-3    | C <sub>2</sub> H <sub>2</sub> F <sub>4</sub>                                       | <sup>a</sup> 1,100                    |
| HFC-134a                              | 811-97-2    | CH <sub>2</sub> FCF <sub>3</sub>   | <sup>a</sup> 1,430                    |
| HFC-143                               | 430-66-0    | C <sub>2</sub> H <sub>3</sub> F <sub>3</sub>                                       | <sup>a</sup> 353                      |
| HFC-143a                              | 420-46-2    | C <sub>2</sub> H <sub>3</sub> F <sub>3</sub>                                       | <sup>a</sup> 4,470                    |
| HFC-152                               | 624-72-6    | CH <sub>2</sub> FCH <sub>2</sub> F   | 53                                    |
| HFC-152a                              | 75-37-6     | CH <sub>3</sub> CHF <sub>2</sub>   | <sup>a</sup> 124                      |
| HFC-161                               | 353-36-6    | CH <sub>3</sub> CH <sub>2</sub> F  | 12                                    |
| HFC-227ea                             | 431-89-0    | C <sub>3</sub> HF <sub>7</sub>   | <sup>a</sup> 3,220                    |
| HFC-236cb                             | 677-56-5    | CH <sub>2</sub> FCF <sub>2</sub> CF <sub>3</sub>                                   | 1,340                                 |
| HFC-236ea                             | 431-63-0    | CHF <sub>2</sub> CHFCF <sub>3</sub>  | 1,370                                 |
| HFC-236fa                             | 690-39-1    | C <sub>3</sub> H <sub>2</sub> F <sub>6</sub>                                       | <sup>a</sup> 9,810                    |
| HFC-245ca                             | 679-86-7    | C <sub>3</sub> H <sub>3</sub> F <sub>5</sub>                                       | <sup>a</sup> 693                      |
| HFC-245fa                             | 460-73-1    | CHF <sub>2</sub> CH <sub>2</sub> CF <sub>3</sub>                                   | 1,030                                 |
| HFC-365mfc                            | 406-58-6    | CH <sub>3</sub> CF <sub>2</sub> CH <sub>2</sub> CF <sub>3</sub>                    | 794                                   |
| HFC-43-10mee                          | 138495-42-8 | CF <sub>3</sub> CFHCFHCF <sub>2</sub> CF <sub>3</sub>                              | <sup>a</sup> 1,640                    |
| Sulfur hexafluoride                   | 2551-62-4   | SF <sub>6</sub>  | <sup>a</sup> 22,800                   |
| Trifluoromethyl sulphur pentafluoride | 373-80-8    | SF <sub>5</sub> CF <sub>3</sub>  | 17,700                                |
| Nitrogen trifluoride                  | 7783-54-2   | NF <sub>3</sub>  | 17,200                                |
| PFC-14 (Perfluoromethane)             | 75-73-0     | CF <sub>4</sub>  | <sup>a</sup> 7,390                    |
| PFC-116 (Perfluoroethane)             | 76-16-4     | C <sub>2</sub> F <sub>6</sub>  | <sup>a</sup> 12,200                   |
| PFC-218 (Perfluoropropane)            | 76-19-7     | C <sub>3</sub> F <sub>8</sub>  | <sup>a</sup> 8,830                    |
| Perfluorocyclopropane                 | 931-91-9    | C-C <sub>3</sub> F <sub>6</sub>  | 17,340                                |
| PFC-3-1-10 (Perfluorobutane)          | 355-25-9    | C <sub>4</sub> F <sub>10</sub>   | <sup>a</sup> 8,860                    |
| PFC-318 (Perfluorocyclobutane)        | 115-25-3    | C-C <sub>4</sub> F <sub>8</sub>  | <sup>a</sup> 10,300                   |
| PFC-4-1-12 (Perfluoropentane)         | 678-26-2    | C <sub>5</sub> F <sub>12</sub>   | <sup>a</sup> 9,160                    |
| PFC-5-1-14 (Perfluorohexane, FC-72)   | 355-42-0    | C <sub>6</sub> F <sub>14</sub>   | <sup>a</sup> 9,300                    |
| PFC-9-1-18                            | 306-94-5    | C <sub>10</sub> F <sub>18</sub>  | 7,500                                 |
| HCFE-235da2 (Isoflurane)              | 26675-46-7  | CHF <sub>2</sub> OCHClCF <sub>3</sub>  | 350                                   |
| HFE-43-10pccc (H-Galden 1040x, HG-11) | E1730133    | CHF <sub>2</sub> OCF <sub>2</sub> OC <sub>2</sub> F <sub>4</sub> OCHF <sub>2</sub> | 1,870                                 |



|   |             |  |        |
|---|-------------|--|--------|
| HFE-125   | 3822-68-2   | CHF <sub>2</sub> OCF <sub>3</sub>  | 14,900 |
| HFE-134 (HG-00)                                 | 1691-17-4   | CHF <sub>2</sub> OCHF <sub>2</sub>   | 6,320  |
| HFE-143a  | 421-14-7    | CH <sub>3</sub> OCF <sub>3</sub>   | 756    |
| HFE-227ea                                       | 2356-62-9   | CF <sub>3</sub> CHFOCF <sub>3</sub>  | 1,540  |
| HFE-236ca12 (HG-10)                             | 78522-47-1  | CHF <sub>2</sub> OCF <sub>2</sub> OCHF <sub>2</sub>                                    | 2,800  |
| HFE-236ea2 (Desflurane)                         | 57041-67-5  | CHF <sub>2</sub> OCHF <sub>2</sub> CF <sub>3</sub>                                     | 989    |
| HFE-236fa                                       | 20193-67-3  | CF <sub>3</sub> CH <sub>2</sub> OCF <sub>3</sub>                                       | 487    |
| HFE-245cb2                                      | 22410-44-2  | CH <sub>3</sub> OCF <sub>2</sub> CF <sub>3</sub>                                       | 708    |
| HFE-245fa1                                      | 84011-15-4  | CHF <sub>2</sub> CH <sub>2</sub> OCF <sub>3</sub>                                      | 286    |
| HFE-245fa2                                      | 1885-48-9   | CHF <sub>2</sub> OCH <sub>2</sub> CF <sub>3</sub>                                      | 659    |
| HFE-254cb2                                      | 425-88-7    | CH <sub>3</sub> OCF <sub>2</sub> CHF <sub>2</sub>                                      | 359    |
| HFE-263fb2                                      | 460-43-5    | CF <sub>3</sub> CH <sub>2</sub> OCH <sub>3</sub>                                       | 11     |
| HFE-329mcc2                                     | 134769-21-4 | CF <sub>3</sub> CF <sub>2</sub> OCF <sub>2</sub> CHF <sub>2</sub>                      | 919    |
| HFE-338mcf2                                     | 156053-88-2 | CF <sub>3</sub> CF <sub>2</sub> OCH <sub>2</sub> CF <sub>3</sub>                       | 552    |
| HFE-338pcc13 (HG-01)                            | 188690-78-0 | CHF <sub>2</sub> OCF <sub>2</sub> CF <sub>2</sub> OCHF <sub>2</sub>                    | 1,500  |
| HFE-347mcc3 (HFE-7000)                          | 375-03-1    | CH <sub>3</sub> OCF <sub>2</sub> CF <sub>2</sub> CF <sub>3</sub>                       | 575    |
| HFE-347mcf2                                     | 171182-95-9 | CF <sub>3</sub> CF <sub>2</sub> OCH <sub>2</sub> CHF <sub>2</sub>                      | 374    |
| HFE-347pcf2                                     | 406-78-0    | CHF <sub>2</sub> CF <sub>2</sub> OCH <sub>2</sub> CF <sub>3</sub>                      | 580    |
| HFE-356mec3                                     | 382-34-3    | CH <sub>3</sub> OCF <sub>2</sub> CHF <sub>2</sub> CF <sub>3</sub>                      | 101    |
| HFE-356pcc3                                     | 160620-20-2 | CH <sub>3</sub> OCF <sub>2</sub> CF <sub>2</sub> CHF <sub>2</sub>                      | 110    |
| HFE-356pcf2                                     | 50807-77-7  | CHF <sub>2</sub> CH <sub>2</sub> OCF <sub>2</sub> CHF <sub>2</sub>                     | 265    |
| HFE-356pcf3                                     | 35042-99-0  | CHF <sub>2</sub> OCH <sub>2</sub> CF <sub>2</sub> CHF <sub>2</sub>                     | 502    |
| HFE-365mcf3                                     | 378-16-5    | CF <sub>3</sub> CF <sub>2</sub> CH <sub>2</sub> OCH <sub>3</sub>                       | 11     |
| HFE-374pc2                                      | 512-51-6    | CH <sub>3</sub> CH <sub>2</sub> OCF <sub>2</sub> CHF <sub>2</sub>                      | 557    |
| HFE-449s1 (HFE-7100)                            | 163702-07-6 | C <sub>4</sub> F <sub>9</sub> OCH <sub>3</sub>   | 297    |
| Chemical blend                                  | 163702-08-7 | (CF <sub>3</sub> ) <sub>2</sub> CFCF <sub>2</sub> OCH <sub>3</sub>                     |        |
| HFE-569sf2 (HFE-7200)                           | 163702-05-4 | C <sub>4</sub> F <sub>9</sub> OC <sub>2</sub> H <sub>5</sub>                           | 59     |
| Chemical blend                                  | 163702-06-5 | (CF <sub>3</sub> ) <sub>2</sub> CFCF <sub>2</sub> OC <sub>2</sub> H <sub>5</sub>       |        |
| Sevoflurane (HFE-347mmz1)                       | 28523-86-6  | CH <sub>2</sub> FOCH(CF <sub>3</sub> ) <sub>2</sub>                                    | 345    |
| HFE-356mm1                                      | 13171-18-1  | (CF <sub>3</sub> ) <sub>2</sub> CHOCH <sub>3</sub>                                     | 27     |
| HFE-338mmz1                                     | 26103-08-2  | CHF <sub>2</sub> OCH(CF <sub>3</sub> ) <sub>2</sub>                                    | 380    |
| (Octafluorotetramethyl-ene) hydroxymethyl group | NA          | X-(CF <sub>2</sub> ) <sub>4</sub> CH(OH)-X   | 73     |
| HFE-347mmy1                                     | 22052-84-2  | CH <sub>3</sub> OCF(CF <sub>3</sub> ) <sub>2</sub>                                     | 343    |
| Bis(trifluoromethyl)-methanol                   | 920-66-1    | (CF <sub>3</sub> ) <sub>2</sub> CHOH   | 195    |
| 2,2,3,3,3-pentafluoropropanol                   | 422-05-9    | CF <sub>3</sub> CF <sub>2</sub> CH <sub>2</sub> OH                                     | 42     |
| PPFMIE (HT-70)                                  | NA          | CF <sub>3</sub> OCF(CF <sub>3</sub> )CF <sub>2</sub> OCF <sub>2</sub> OCF <sub>3</sub> | 10,300 |

<sup>a</sup>The GWP for this compound is different than the GWP in the version of Table A-1 to subpart A of part 98 published on October 30, 2009.

**Table C-1 to Subpart C of Part 98—Default CO<sub>2</sub> Emission Factors and High Heat Values for Various Types of Fuel**

**DEFAULT CO<sub>2</sub> EMISSION FACTORS AND HIGH HEAT VALUES FOR VARIOUS TYPES OF FUEL**

| <b>Fuel type</b>                             | <b>Default high heat value</b> | <b>Default CO<sub>2</sub> emission factor</b> |
|--|--------------------------------|---|
| <b>Coal and coke</b>                         | <b>mmBtu/short ton</b>         | <b>kg CO<sub>2</sub>/mmBtu</b>                |
| Anthracite                                   | 25.09                          | 103.69  |
| Bituminous                                   | 24.93                          | 93.28   |
| Subbituminous                                | 17.25                          | 97.17   |
| Lignite                                      | 14.21                          | 97.72   |
| Coal Coke                                    | 24.80                          | 113.67  |
| Mixed (Commercial sector)                    | 21.39                          | 94.27   |
| Mixed (Industrial coking)                    | 26.28                          | 93.90   |
| Mixed (Industrial sector)                    | 22.35                          | 94.67   |
| Mixed (Electric Power sector)                | 19.73                          | 95.52   |
| <b>Natural gas</b>                           | <b>mmBtu/scf</b>               | <b>kg CO<sub>2</sub>/mmBtu</b>                |
| (Weighted U.S. Average)                      | $1.026 \times 10^{-3}$         | 53.06   |
| <b>Petroleum products</b>                    | <b>mmBtu/gallon</b>            | <b>kg CO<sub>2</sub>/mmBtu</b>                |
| Distillate Fuel Oil No. 1                    | 0.139                          | 73.25   |
| Distillate Fuel Oil No. 2                    | 0.138                          | 73.96   |
| Distillate Fuel Oil No. 4                    | 0.146                          | 75.04   |
| Residual Fuel Oil No. 5                      | 0.140                          | 72.93   |
| Residual Fuel Oil No. 6                      | 0.150                          | 75.10   |
| Used Oil                                     | 0.138                          | 74.00   |
| Kerosene                                     | 0.135                          | 75.20   |
| Liquefied petroleum gases (LPG) <sup>1</sup> | 0.092                          | 61.71   |
| Propane <sup>1</sup>                         | 0.091                          | 62.87   |
| Propylene <sup>2</sup>                       | 0.091                          | 67.77   |
| Ethane <sup>1</sup>                          | 0.068                          | 59.60   |
| Ethanol                                      | 0.084                          | 68.44   |
| Ethylene <sup>2</sup>                        | 0.058                          | 65.96   |
| Isobutane <sup>1</sup>                       | 0.099                          | 64.94   |
| Isobutylene <sup>1</sup>                     | 0.103                          | 68.86   |
| Butane <sup>1</sup>                          | 0.103                          | 64.77   |
| Butylene <sup>1</sup>                        | 0.105                          | 68.72   |
| Naphtha (<401 deg F)                         | 0.125                          | 68.02   |
| Natural Gasoline                             | 0.110                          | 66.88   |
| Other Oil (>401 deg F)                       | 0.139                          | 76.22   |
| Pentanes Plus                                | 0.110                          | 70.02   |

|  |                          |                           |
|--|--------------------------|---------------------------|
| Petrochemical Feedstocks                         | 0.125                    | 71.02                     |
| Petroleum Coke                                   | 0.143                    | 102.41                    |
| Special Naphtha                                  | 0.125                    | 72.34                     |
| Unfinished Oils                                  | 0.139                    | 74.54                     |
| Heavy Gas Oils                                   | 0.148                    | 74.92                     |
| Lubricants                                       | 0.144                    | 74.27                     |
| Motor Gasoline                                   | 0.125                    | 70.22                     |
| Aviation Gasoline                                | 0.120                    | 69.25                     |
| Kerosene-Type Jet Fuel                           | 0.135                    | 72.22                     |
| Asphalt and Road Oil                             | 0.158                    | 75.36                     |
| Crude Oil  | 0.138                    | 74.54                     |
| Other fuels—solid                                | mmBtu/short ton          | kg CO <sub>2</sub> /mmBtu |
| Municipal Solid Waste                            | 9.95 <sup>3</sup>        | 90.7                      |
| Tires  | 28.00                    | 85.97                     |
| Plastics   | 38.00                    | 75.00                     |
| Petroleum Coke                                   | 30.00                    | 102.41                    |
| Other fuels—gaseous                              | mmBtu/scf                | kg CO <sub>2</sub> /mmBtu |
| Blast Furnace Gas                                | 0.092 × 10 <sup>-3</sup> | 274.32                    |
| Coke Oven Gas                                    | 0.599 × 10 <sup>-3</sup> | 46.85                     |
| Propane Gas                                      | 2.516 × 10 <sup>-3</sup> | 61.46                     |
| Fuel Gas <sup>4</sup>                            | 1.388 × 10 <sup>-3</sup> | 59.00                     |
| Biomass fuels—solid                              | mmBtu/short ton          | kg CO <sub>2</sub> /mmBtu |
| Wood and Wood Residuals (dry basis) <sup>5</sup> | 17.48                    | 93.80                     |
| Agricultural Byproducts                          | 8.25                     | 118.17                    |
| Peat   | 8.00                     | 111.84                    |
| Solid Byproducts                                 | 10.39                    | 105.51                    |
| Biomass fuels—gaseous                            | mmBtu/scf                | kg CO <sub>2</sub> /mmBtu |
| Landfill Gas                                     | 0.485 × 10 <sup>-3</sup> | 52.07                     |
| Other Biomass Gases                              | 0.655 × 10 <sup>-3</sup> | 52.07                     |
| Biomass Fuels—Liquid                             | mmBtu/gallon             | kg CO <sub>2</sub> /mmBtu |
| Ethanol  | 0.084                    | 68.44                     |
| Biodiesel (100%)                                 | 0.128                    | 73.84                     |
| Rendered Animal Fat                              | 0.125                    | 71.06                     |
| Vegetable Oil                                    | 0.120                    | 81.55                     |

<sup>1</sup>The HHV for components of LPG determined at 60 °F and saturation pressure with the exception of ethylene.

<sup>2</sup>Ethylene HHV determined at 41 °F (5 °C) and saturation pressure.

<sup>3</sup>Use of this default HHV is allowed only for: (a) Units that combust MSW, do not generate steam, and are allowed to use Tier 1; (b) units that derive no more than 10 percent of their annual heat input from MSW and/or tires; and (c) small batch incinerators that combust no more than 1,000 tons of MSW per year.

<sup>4</sup>Reporters subject to subpart X of this part that are complying with §98.243(d) or subpart Y of this part may only use the default HHV and the default CO<sub>2</sub> emission factor for fuel gas combustion under the conditions prescribed in §98.243(d)(2)(i) and (d)(2)(ii) and §98.252(a)(1) and (a)(2), respectively. Otherwise, reporters subject to subpart X or subpart Y shall use either Tier 3 (Equation C-5) or Tier 4.

<sup>5</sup>Use the following formula to calculate a wet basis HHV for use in Equation C-1:  $HHV_w = ((100 - M)/100) * HHV_d$  where  $HHV_w$  = wet basis HHV, M = moisture content (percent) and  $HHV_d$  = dry basis HHV from Table C-1.

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**Table C-2 to Subpart C of Part 98—Default CH<sub>4</sub> and N<sub>2</sub>O Emission Factors for Various Types of Fuel**

| Fuel type   | Default CH <sub>4</sub> emission factor (kg CH <sub>4</sub> /mmBtu) | Default N <sub>2</sub> O emission factor (kg N <sub>2</sub> O/mmBtu) |
|---|---|--|
| Coal and Coke (All fuel types in Table C-1)                                       | $1.1 \times 10^{-02}$   | $1.6 \times 10^{-03}$  |
| Natural Gas   | $1.0 \times 10^{-03}$   | $1.0 \times 10^{-04}$  |
| Petroleum (All fuel types in Table C-1)   | $3.0 \times 10^{-03}$   | $6.0 \times 10^{-04}$  |
| Fuel Gas  | $3.0 \times 10^{-03}$   | $6.0 \times 10^{-04}$  |
| Municipal Solid Waste   | $3.2 \times 10^{-02}$   | $4.2 \times 10^{-03}$  |
| Tires   | $3.2 \times 10^{-02}$   | $4.2 \times 10^{-03}$  |
| Blast Furnace Gas   | $2.2 \times 10^{-05}$   | $1.0 \times 10^{-04}$  |
| Coke Oven Gas   | $4.8 \times 10^{-04}$   | $1.0 \times 10^{-04}$  |
| Biomass Fuels—Solid (All fuel types in Table C-1, except wood and wood residuals) | $3.2 \times 10^{-02}$   | $4.2 \times 10^{-03}$  |
| Wood and wood residuals   | $7.2 \times 10^{-03}$   | $3.6 \times 10^{-03}$  |
| Biomass Fuels—Gaseous (All fuel types in Table C-1)                               | $3.2 \times 10^{-03}$   | $6.3 \times 10^{-04}$  |
| Biomass Fuels—Liquid (All fuel types in Table C-1)                                | $1.1 \times 10^{-03}$   | $1.1 \times 10^{-04}$  |

Note: Those employing this table are assumed to fall under the IPCC definitions of the “Energy Industry” or “Manufacturing Industries and Construction”. In all fuels except for coal the values for these two categories are identical. For coal combustion, those who fall within the IPCC “Energy Industry” category may employ a value of 1g of CH<sub>4</sub>/mmBtu.

**Table W-1A of Subpart W of Part 98—Default Whole Gas Emission Factors for Onshore Petroleum and Natural Gas Production**

| Onshore petroleum and natural gas production                                       | Emission factor (scf/hour/component) |
|--|--------------------------------------|
| <b>Eastern U.S.</b>  |                                      |
| <b>Population Emission Factors—All Components, Gas Service<sup>1</sup></b>         |                                      |
| Valve  | 0.027                                |
| Connector  | 0.003                                |
| Open-ended Line  | 0.061                                |
| Pressure Relief Valve  | 0.040                                |
| Low Continuous Bleed Pneumatic Device Vents <sup>2</sup>                           | 1.39                                 |
| High Continuous Bleed Pneumatic Device Vents <sup>2</sup>                          | 37.3                                 |
| Intermittent Bleed Pneumatic Device Vents <sup>2</sup>                             | 13.5                                 |
| Pneumatic Pumps <sup>3</sup>   | 13.3                                 |
| <b>Population Emission Factors—All Components, Light Crude Service<sup>4</sup></b> |                                      |
| Valve  | 0.05                                 |
| Flange   | 0.003                                |
| Connector  | 0.007                                |
| Open-ended Line  | 0.05                                 |
| Pump   | 0.01                                 |
| Other <sup>5</sup>   | 0.30                                 |
| <b>Population Emission Factors—All Components, Heavy Crude Service<sup>6</sup></b> |                                      |
| Valve  | 0.0005                               |
| Flange   | 0.0009                               |
| Connector (other)  | 0.0003                               |
| Open-ended Line  | 0.006                                |
| Other <sup>5</sup>   | 0.003                                |
| <b>Western U.S.</b>  |                                      |
| <b>Population Emission Factors—All Components, Gas Service<sup>1</sup></b>         |                                      |
| Valve  | 0.121                                |
| Connector  | 0.017                                |
| Open-ended Line  | 0.031                                |
| Pressure Relief Valve  | 0.193                                |
| Low Continuous Bleed Pneumatic Device Vents <sup>2</sup>                           | 1.39                                 |
| High Continuous Bleed Pneumatic Device Vents <sup>2</sup>                          | 37.3                                 |
| Intermittent Bleed Pneumatic Device Vents <sup>2</sup>                             | 13.5                                 |
| Pneumatic Pumps <sup>3</sup>   | 13.3                                 |
| <b>Population Emission Factors—All Components, Light Crude Service<sup>4</sup></b> |                                      |
| Valve  | 0.05                                 |
| Flange   | 0.003                                |

|  |        |
|--|--------|
| Connector (other)  | 0.007  |
| Open-ended Line  | 0.05   |
| Pump   | 0.01   |
| Other <sup>5</sup>   | 0.30   |
| <b>Population Emission Factors—All Components, Heavy Crude Service<sup>6</sup></b> |        |
| Valve  | 0.0005 |
| Flange   | 0.0009 |
| Connector (other)  | 0.0003 |
| Open-ended Line  | 0.006  |
| Other <sup>5</sup>   | 0.003  |

<sup>1</sup>For multi-phase flow that includes gas, use the gas service emissions factors.

<sup>2</sup>Emission Factor is in units of “scf/hour/device.”

<sup>3</sup>Emission Factor is in units of “scf/hour/pump.”

<sup>4</sup>Hydrocarbon liquids greater than or equal to 20°API are considered “light crude.”

<sup>5</sup>“Others” category includes instruments, loading arms, pressure relief valves, stuffing boxes, compressor seals, dump lever arms, and vents.

<sup>6</sup>Hydrocarbon liquids less than 20°API are considered “heavy crude.”

## Section 6

### Federal Regulations Applicability

| <u>FEDERAL<br/>REGU-<br/>LATIONS</u><br>CITATION | Title  | Applies<br>to<br>Entire<br>Facility | Applies to<br>Unit<br>No(s). | Does<br>Not<br>Apply | JUSTIFICATION:  |
|--|--|-------------------------------------|------------------------------|----------------------|---|
| 40 CFR 50  | NAAQS  | ✓                                   |                              |                      | This regulation is applicable because it applies to all sources in the United States.   |
| NSPS 40 CFR 60, Subpart A                        | General Provisions   |                                     | 1                            |                      | This regulation is applicable because 40 CFR Part 60 Subpart GG is applicable.  |
| NSPS<br>40 CFR 60,<br>Subpart K                  | Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced After June 11, 1973, and Prior to May 19, 1978                |                                     |                              | ✓                    | This regulation is not applicable because the petroleum liquids storage tanks at the facility have capacities less than the minimum applicability threshold capacity of 40,000 gallons (see §60.110(a)).  |
| NSPS<br>40 CFR 60,<br>Subpart Ka                 | Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced After May 18, 1978, and Prior to July 23, 1984                |                                     |                              | ✓                    | This regulation is not applicable because the storage tanks at the facility have capacities less than the minimum applicability threshold capacity of 40,000 gallons (see §60.110a(a)).   |
| NSPS<br>40 CFR 60,<br>Subpart Kb                 | Standards of Performance for Volatile Organic Liquid Storage Vessels (Including Petroleum Liquid Storage Vessels) for Which Construction, Reconstruction, or Modification Commenced After July 23, |                                     |                              | ✓                    | This regulation is not applicable because all storage tanks at the facility have capacities less than the minimum applicability threshold capacity of 75 cubic meters (19,812 gallons), or they have a capacity between 75 and 151 cubic meters (40,000 gallons) and store a liquid with a maximum true vapor pressure less than 15.0 kPa (2.2 psi), or store petroleum prior to custody transfer (see §60.110b(a) & §60.110b(b) & §60.110b(d)(4)). |

| <b><u>FEDERAL<br/>REGU-<br/>LATIONS</u><br/>CITATION</b> | <b>Title</b>  | <b>Applies<br/>to<br/>Entire<br/>Facility</b> | <b>Applies to<br/>Unit<br/>No(s).</b> | <b>Does<br/>Not<br/>Apply</b> | <b>JUSTIFICATION:</b>   |
|--|---|---|---------------------------------------|-------------------------------|---|
|  | 1984  |   |                                       |                               |   |
| NSPS<br>40 CFR,<br>Subpart GG                            | Standards of<br>Performance for<br>Stationary Gas<br>Turbines   |   | 1                                     |                               | The regulation is applicable as the facility is equipped with a stationary gas turbine with heat input equal to 10 MMBtu/hour or greater, installed on or after October 3, 1977.  |
| NSPS<br>40 CFR 60,<br>Subpart<br>KKK                     | Standards of<br>Performance for<br>Equipment<br>Leaks of VOC<br>from Onshore<br>Gas Plants                          |   |                                       | ✓                             | This regulation is not applicable because the facility is not an onshore natural gas processing plant as defined by the subpart (see §60.630(a)(1)). Natural gas processing plant (gas plant) means any processing site engaged in the extraction of natural gas liquids from field gas, fractionation of mixed natural gas liquids to natural gas products, or both (see §60.631).   |
| NSPS<br>40 CFR Part<br>60 Subpart<br>LLL                 | Standards of<br>Performance for<br>Onshore Natural<br>Gas Processing:<br>SO <sub>2</sub> Emissions                  |   |                                       | ✓                             | This regulation is not applicable because the facility is not a natural gas processing plant as defined by the subpart. It is not equipped with a sweetening unit (see §60.640(a)).   |
| NSPS<br>40 CFR 60,<br>Subpart IIII                       | Standards of<br>Performance for<br>Stationary<br>Compression<br>Ignition Internal<br>Combustion<br>Engines          |   |                                       | ✓                             | This regulation is not applicable because the facility is not equipped with stationary compression ignition (CI) internal combustion engines (ICE) that commenced construction after July 11, 2005 and were manufactured after April 1, 2006 (see §60.4200(a)(2)(i)).<br><br>For the purpose of this subpart, construction commences on the date the engine is ordered by the owner or operator (see §60.4200(a)).  |
| NSPS<br>40 CFR 60<br>Subpart JJJJ                        | Standards of<br>Performance for<br>Stationary<br>Spark Ignition<br>Internal<br>Combustion<br>Engines                |   |                                       | ✓                             | This regulation is not applicable because the facility is not equipped with spark ignition (SI) internal combustion engines (ICE) constructed, modified, or reconstructed after June 12, 2006.<br><br>Unit 3 was constructed prior to the applicability date and has not been modified or reconstructed.<br><br>See the definitions of construction, modification, and reconstruction referenced in Subpart OOOO below.   |
| NSPS<br>40 CFR 60<br>Subpart<br>OOOO                     | Standards of<br>Performance for<br>Crude Oil and<br>Natural Gas<br>Production,<br>Transmission,<br>and Distribution |   |                                       | ✓                             | This regulation is not applicable because the facility is not equipped with “affected” sources that commenced construction, modification or reconstruction after August 23, 2011 and on or before September 18, 2015: gas wells, centrifugal or reciprocating compressors, pneumatic controllers, and storage vessels (see §60.5365).<br><br>Note that the facility is not a natural gas processing plant as defined by the subpart (see §60.5430).<br><br>Commenced construction means a continuous program of fabrication, erection or installation (see §60.2).<br><br>Modification means any physical change in or change in the method of operation of an existing facility which increases emissions or results in new emissions (see §60.2). The following, by themselves, are not modifications: routine maintenance, repair or replacement, production increase without capital expenditure, increase in hours of operation, addition of emission controls, or the relocation or change in |



| <b><u>FEDERAL<br/>REGU-<br/>LATIONS</u><br/>CITATION</b> | <b>Title</b>  | <b>Applies<br/>to<br/>Entire<br/>Facility</b> | <b>Applies to<br/>Unit<br/>No(s).</b> | <b>Does<br/>Not<br/>Apply</b> | <b>JUSTIFICATION:</b>  |
|--|---|---|---------------------------------------|-------------------------------|--|
|  |   |   |                                       |                               | ownership of an existing facility (see §60.14).<br><br>Reconstruction means the replacement of components of an existing facility such that the fixed capital cost of the new components exceeds 50 % of the fixed capital cost required to construct a comparable entirely new facility. Fixed capital cost means the capital needed to provide all the depreciable components (see §60.15).  |
| NPS<br>40 CFR 60,<br>Subpart<br>OOOOa                    | Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced After September 18, 2015 |   |                                       | ✓                             | This regulation is not applicable because the facility is not equipped with “affected” sources that commenced construction, modification or reconstruction after September 18, 2015: gas wells, centrifugal or reciprocating compressors, pneumatic controllers, storage vessels, sweetening units, pneumatic pumps, and equipment leaks (see §60.5365a).<br><br>In general, this regulation may apply if existing affected equipment is replaced or new affected equipment is installed.<br><br>In particular, this regulation will apply to fugitive emissions components at the facility if any engines and compressors are installed. Fugitive components monitoring is required if a compressor station is modified. For the purpose of fugitive components monitoring as required by this subpart, modification of a compressor station is the addition of a compressor or replacement of a compressor with a larger unit (greater total horsepower) (see §60.5365a(j)).<br><br>Note that the facility is not a natural gas processing plant as defined by the subpart (see §60.5430a).<br><br>See the definitions of construction, modification, and reconstruction referenced in Subpart OOOO above. |
| NESHAP<br>40 CFR 61<br>Subpart A                         | General Provisions  |   |                                       | ✓                             | This regulation is not applicable because no other 40 CFR Part 61 subparts apply (see §61.01(c)).  |
| NESHAP<br>40 CFR 61<br>Subpart V                         | National Emission Standards for Equipment Leaks (Fugitive Emission Sources)   |   |                                       | ✓                             | This regulation is not applicable because none of the listed equipment at the facility is in VHAP service.<br><br>The provisions of this subpart apply to each of the following sources that are intended to operate in volatile hazardous air pollutant (VHAP) service: pumps, compressors, pressure relief devices, sampling connection systems, open-ended valves or lines, valves, connectors, surge control vessels, bottoms receivers, and control devices or systems required by this subpart (see §61.240(a)). VHAP service means a piece of equipment either contains or contacts a fluid (liquid or gas) that is at least 10 percent by weight of VHAP. VHAP means a substance regulated under this subpart for which a standard for equipment leaks of the substance has been promulgated (see §61.241).  |
| MACT<br>40 CFR 63,<br>Subpart A                          | General Provisions  |   | 3                                     |                               | This regulation is applicable because 40 CFR 63 Subpart ZZZZ applies (see §63.1(b)).   |

| <b><u>FEDERAL<br/>REGU-<br/>LATIONS<br/>CITATION</u></b> | <b>Title</b>   | <b>Applies<br/>to<br/>Entire<br/>Facility</b> | <b>Applies to<br/>Unit<br/>No(s).</b> | <b>Does<br/>Not<br/>Apply</b> | <b>JUSTIFICATION:</b>  |
|--|--|---|---------------------------------------|-------------------------------|--|
| MACT<br>40 CFR<br>63.760<br>Subpart HH                   | National<br>Emission<br>Standards for<br>Hazardous Air<br>Pollutants For<br>Oil and Natural<br>Gas Production<br>Facilities                                  |   |                                       | ✓                             | <p>This regulation is not applicable because the facility is not equipped with affected equipment.</p> <p>The facility is an area HAP source. Note that since it is a production field facility (located prior to the point of custody transfer), only HAP emissions from glycol dehydration units and storage vessels are aggregated for a major source determination. Storage vessels include crude oil tanks, condensate tanks, intermediate hydrocarbon liquid tanks, and produced water tanks (see §63.761).</p> <p>At area HAP facilities, the regulation is only applicable to dehydrators (see §63.760(b)(2)).</p> |
| MACT<br>40 CFR 63,<br>Subpart<br>HHH                     | National<br>Emission<br>Standards for<br>Hazardous Air<br>Pollutants From<br>Natural Gas<br>Transmission<br>and Storage<br>Facilities                        |   |                                       | ✓                             | <p>This regulation is not applicable because the facility is not a natural gas transmission and storage facility as defined by the subpart.</p> <p>A compressor station that transports natural gas prior to the point of custody transfer or to a natural gas processing plant (if present) are not considered a part of the natural gas transmission and storage source category (see §63.1270(a)).</p>  |
| MACT<br>40 CFR 63<br>Subpart<br>YYYY                     | National<br>Emissions<br>Standards for<br>Hazardous Air<br>Pollutants for<br>Stationary<br>Combustion<br>Turbines  |   |                                       | ✓                             | <p>This regulation is not applicable, as the facility is an area HAP source (see §63.6080).</p>  |
| MACT<br>40 CFR 63<br>Subpart<br>ZZZZ                     | National<br>Emissions<br>Standards for<br>Hazardous Air<br>Pollutants for<br>Stationary<br>Reciprocating<br>Internal<br>Combustion<br>Engines (RICE<br>MACT) |   | 3                                     |                               | <p>This regulation is applicable because the facility is equipped with an affected source.</p> <p>The station is an area HAP source as defined by the subpart. For production field facilities, only HAP emissions from engines, turbines, dehydrators, and storage vessels with the potential for flash emissions are aggregated for the HAP major source determination (see §63.6675).</p> <p>Unit 3 is an emergency generator as defined by the Subpart.</p>  |
| NESHAP<br>40 CFR 64                                      | Compliance<br>Assurance<br>Monitoring  |   |                                       | ✓                             | <p>This regulation is not applicable because no equipment at the facility requires a control device to achieve compliance with emission limits or standards where pre control emissions equal or exceed the major source threshold (100 tons per year). (see §64.2(a)).</p>  |
| NESHAP<br>40 CFR 68                                      | Chemical<br>Accident<br>Prevention   |   |                                       | ✓                             | <p>This regulation is not applicable because the facility does not store any of the identified toxic and flammable substances in quantities exceeding the applicability thresholds (see §68.10(a), §68.115(a), and §68.130 Tables 1-4).</p>  |
| Title V –<br>40 CFR 70                                   | State Operating<br>Permit<br>Programs  |   |                                       | ✓                             | <p>This regulation is not applicable because the facility is located within the exterior boundaries of the Jicarilla Apache Indian Reservation, and therefore not within the jurisdiction of the State of New Mexico Environment Department.</p>   |

| <b><u>FEDERAL<br/>REGU-<br/>LATIONS</u><br/>CITATION</b> | <b>Title</b>   | <b>Applies<br/>to<br/>Entire<br/>Facility</b> | <b>Applies to<br/>Unit<br/>No(s).</b> | <b>Does<br/>Not<br/>Apply</b> | <b>JUSTIFICATION:</b>  |
|--|--|---|---------------------------------------|-------------------------------|--|
| Title V –<br>40 CFR 71                                   | Federal<br>Operating<br>Permit<br>Programs                       | ✓   |                                       |                               | This regulation is applicable because the facility is located within the exterior boundaries of the Jicarilla Apache Indian Reservation.   |
| Title IV –<br>Acid Rain<br>40 CFR 72                     | Acid Rain  |   |                                       | ✓                             | This regulation is not applicable because the facility does not operate a source subject to Title IV of the Clean Air Act (CAA).   |
| Title IV –<br>Acid Rain<br>40 CFR 73                     | Sulfur Dioxide<br>Allowance<br>Emissions                         |   |                                       | ✓                             | This regulation is not applicable because the facility does not operate a source subject to Title IV of the Clean Air Act (CAA).   |
| Title IV –<br>Acid Rain<br>40 CFR 76                     | Acid Rain<br>Nitrogen Oxides<br>Emission<br>Reduction<br>Program |   |                                       | ✓                             | This regulation is not applicable to the facility because it does not operate a source subject to Title IV of the Clean Air Act (CAA).   |
| Title VI –<br>40 CFR 82                                  | Protection of<br>Stratospheric<br>Ozone                          |   |                                       | ✓                             | This regulation is not applicable to the facility because it does not produce, manufacture, transform, destroy, import, or export ozone-depleting substances; does not maintain or service motor vehicle air conditioning units or refrigeration equipment; and does not sell, distribute, or offer for sale or distribution any product that contains ozone-depleting substances. |

# **Section 7**

## **Alternative Operating Scenarios**

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No alternative operating scenarios are proposed by Harvest for the facility.

# **Section 8**

## **Additional Information**

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Copies of the additional information previously requested by and provided to EPA, and not elsewhere addressed in this application, are included in this Section.

EPA REVIEW COMMENTS CAA TRIBAL PERMIT APPLICATION  
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- Include the custody transfer point on the facility diagram or process flow diagram, whether upstream of or at the facility property boundary (e.g., upstream of pigging unit?) and provide copies of current contracts for amount of material transferred to the facility for processing (i.e., should coincide with representative throughputs provided in the permit application, with contingencies identified for possible future increase in throughput).
  - Custody transfer occurs upstream of the facility at individual natural gas wells. No custody transfer occurs at the facility. Natural gas from this facility is discharged to another Harvest compressor station.
  - There are no contracts for the amount of material that can be transferred to the facility. The facility is limited on how much material it can process by the compression capability of the site, which is limited to the single Solar turbine. With the current facility configuration, it can compress approximately 20 MMscf/day (see *Los Mestenos Maximum Facility Throughput*). Harvest cannot increase this capacity without construction that would need to be approved through the NSR program.
  - Harvest has put together the facility condensate throughput data from 2017 – 2022. The maximum 12-month rolling total at the facility over the last 5 years occurred in 2017 and was 9,109 bbls. The most recent 12-month rolling total was 4,181 bbls. The emissions model was run at a worst-case emissions scenario of 22,141 bbls. There are no plans to make any changes to the site that would increase the facility throughput above what the model was ran at. Any increase in throughput above the model inputs presented in the application would need to be approved by the EPA through the NSR program.

**Example of Missing Info for Emission Units and Control Devices**

**{Please complete filling in missing information and confirm information provided from current application below:}**

| Emission Unit No. | Type of Unit Serial No.                         | Manufacturer Model No. Design Heat Input | Operating Range or Size of Unit | Date of Installation and Construction   | Primary Use                 | Control Equipment |
|-------------------|---|--|---------------------------------|---|-----------------------------|-------------------|
| T-1               | Condensate Storage Tank Serial Number? 2874     | American Tank & Steel                    | 400 bbl                         | Install – Unknown Constructed – 06/1965 | Condensate Storage          | None              |
| T-2               | Condensate Storage Tank Serial Number? 831-2918 | American Tank & Steel                    | 400 bbl                         | Installed – 2014 Constructed – 10/1965  | Overflow Condensate Storage | None              |

|     |   |     |     |     |                    |      |
|-----|---|-----|-----|-----|--------------------|------|
| F-1 | Valves,<br>Flanges,<br>Seals, etc.<br>Unknown         | N/A | N/A | N/A | N/A                | None |
| MSS | Maintenance,<br>Startup, and<br>Shutdown<br>Emissions | N/A | N/A | N/A | Pressure<br>relief | None |

**Insignificant Emissions**

**{Please complete filling in missing information and confirm information provided from current application below:}**

| Emission Unit ID No. | Unit Description             | Size                                 | Exemptions to Federal Requirements   |
|----------------------|------------------------------|--------------------------------------|--|
| Unit 4               | Fuel Gas Heater              | 0.3 MMBtu/hr                         | <ul style="list-style-type: none"> <li>&lt; 2 tpy regulated pollutants and &lt; 0.5 tpy HAPs</li> <li>Provide what method, simulation, etc. used to calculate emissions, e.g., VMGSym, etc.</li> <li>Emission factors from AP-42 and GRI HapCalc (pg. 62-66 of the application)</li> <li>Provide Federal citation for exemption</li> <li>40 CFR 71.5(c)(11)(ii)</li> </ul> |
| Unit 5               | Tank Heater                  | 0.012 MM Btu/hr                      | Emission factors from AP-42 and GRI HAPCalc<br>Insignificant emission unit (71.5(c)(11)(ii))   |
| L1                   | Truck Loading Condensate     | XX bbl or # of events<br>22,141 bbls | Emissions calculated using AP-42 and EPA TANKS 4.0<br>Insignificant emission unit (71.5(c)(11)(ii))  |
| L2                   | Truck Loading Produced Water | 840 bbls                             | Emissions calculated using AP-42 and EPA TANKS 4.0<br>Insignificant emission unit (71.5(c)(11)(ii))  |
| T3                   | Produced Water Storage Tank  | 70 bbl                               | Emissions calculated using emission factors developed for produced water by Colorado Department of Public Health and Environment (CDPHE) and   |

| Emission Unit ID No. | Unit Description      | Size    | Exemptions to Federal Requirements  |
|----------------------|-----------------------|---------|---|
|                      |                       |         | the Texas Commission on Environmental Quality (TCEQ)<br>Insignificant emission unit<br>40 CFR 71.5(c)(11)(ii) |
| T4                   | Lube Oil Storage Tank | 500 gal | Emissions calculated using EPA TANKS 4.0<br>Insignificant emission unit<br>40 CFR 71.5(c)(11)(ii)             |
| T5                   | Lube Oil Storage Tank | 500 gal | Emissions calculated using EPA TANKS 4.0<br>Insignificant emission unit<br>40 CFR 71.5(c)(11)(ii)             |
| T6                   | Ambitrol Storage Tank | 350 gal | Emissions calculated using EPA TANKS 4.0<br>Insignificant emission unit<br>40 CFR 71.5(c)(11)(ii)             |
| T7                   | Methanol Storage Tank | 500 gal | Emissions calculated using EPA TANKS 4.0<br>Insignificant emission unit<br>40 CFR 71.5(c)(11)(ii)             |

- What is the pressure relief valve settings for the condensate tanks? Where does the gas go after flashing? Is it routed back to the process or gas line, if so, where? Please indicate all atmospheric vents on the process flow diagram appropriately.
  - Pressure relief setting – 0.4 oz
  - Flash gas vents to atmosphere
- Is the Equipment Leaks an actual and recent count of components?
  - Component counts are conservatively estimated. Harvest has evaluated some of its more complex sites and developed a component count per equipment type. This is used to estimate component counts for its facilities. In addition, Harvest adds the following to make its estimated count more conservative:
    - 1 valve for each open ended line
    - 2 connectors for each flow meter
    - 2 valves, 2 connectors, and 1 open-end line for each level gauge
    - 1 connector for each pressure gauge

**{Please complete filling in missing information and confirm information provided from current application below:}**



| Unit   | Make /Model                | Serial Number | Date of construction and installation       | Operating Range or Size HP (Also include: 2 or 4 stroke, rich or lean burn?) | Fuel Type   | Engine use                 | Pollution Control |
|--------|----------------------------|---------------|---|--|-------------|----------------------------|-------------------|
| Unit 1 | Solar Saturn Turbine T1200 | OHC18-S4468   | Constructed – 1979<br>Installed – 1989      | 1200 HP<br>NA for turbines   | Natural gas | Natural gas compression    | None              |
| Unit 3 | Scania F674DSU-DS11A06     | 951674        | Constructed – 1970-1995<br>Installed – 2019 | 250 HP<br>N/A;<br>Compression Ignition                                       | Diesel      | Emergency power generation | None              |

- Harvest has stated that the concentration of the condensate has changed, and these specific changes have decreased the flash emissions from the condensate tanks that would result in an overall emission limit decrease. However, substantiation of such changes to throughput and complete characterization *changes* need to be a part of the permit application. Data that is provided should match up to contracts currently in place vs historically in place, or onsite characterization efforts need to match up with historical vs current data analyses for all streams coming into the facility at specified throughput rates.
  - Harvest did not change the modeled throughput from the previous Title V permit renewal application. Emission models for both renewal applications were run assuming 22,141 barrels of annual condensate throughput. Using the PTE calculation methodology specified in EPA's OOOOa guidance and at 60.5365a, PTE for the tank would be determined using the maximum daily average throughput. Going back over 5 years of condensate throughput data (found in the *Los Mestenos Historic Condensate Throughputs 2017-2022* document), the highest monthly sum of condensate at the facility is 1,362.04 barrels, in February of 2017. This equates to 48.64 barrels per day (1,362.04/28) and 17,755.16 barrels per year (48.64\*365). The maximum average daily throughput over the last 5 years is 4,385.84 barrels less than what the model was ran at, making the model output an extra conservative figure.
  - Condensate compositions from 2017, 2018, 2019, and 2021 can be found in the *Los Mestenos Compressor Station Condensate Compositions 2017-2021* document. As the document and the supporting analyses show, C3 and C4 concentrations, the main drivers of VOC flash emissions, have decreased from year to year. Again, Harvest has no contracts that specify the amounts or constituents of material that can be sent to the facility. It has an operational design limit of approximately 20 MMscf/day based on its current configuration. There are no plans on changing anything at the site that would result in an increase in

throughputs. Any such changes that would result in an emissions increase or that would result in an increase above the model inputs in the application would be required to be approved by EPA through the NSR program prior to construction.

- Harvest has stated that sampling only occurs “as needed” and no more frequently than once per year. Is this condensate sample retrieved at the same time of year? Are there seasonal changes in material coming into the site? Would the constituents in the sample that is collected in Nov/Dec be different than a sample collected in June/July? Would the sample profile be different? Is there a seasonal effect on flash emissions from the condensate tanks? Is there more flashing in the condensate tanks in the summertime?
  - There is some variability with the amount of material that comes into the site during the different seasons. The sample constituents are the same regardless of the time of year. A condensate sample profile has the potential to change from month to month and year to year, but with sampling occurring on an annual basis, we get a good picture of what material is being collected at the facility. Harvest typically has condensate samples taken during the winter months when liquid flows are higher. With the higher flows, Harvest feels that these samples give us the most conservative estimate for emission modeling, as they also contain the highest amount of C3 and C4 constituents.
  - There are higher flash emissions from the tanks during the summer months with the higher temperatures and lower flash emissions from the tanks during the winter months with the lower temperatures. This is accounted for in the emission model by using average annual temperatures for the local geographic area.
- Are the changes to the condensate concentration permanent changes and indicative of current operations?
  - The 2021 Los Mestenos condensate sample has a higher concentration of heavier components than the sample used in the previous Title V permit renewal application. The available data shows that condensate at the facility has become increasingly heavier from year to year, which will result in lower amounts of flash emissions. In addition, the amount of condensate that is received at the facility has also decreased over the years, going from 8,622.64 barrels in 2017 to 3,667.8 barrels in 2021. This also significantly reduces the amount of actual flash emissions. The most recent condensate data included in this additional information request are indicative of current operations.
- Verify sample location of condensate and indicate on process flow diagram
  - Condensate samples are taken from the facility liquids receiver (VR-1013 on the process flow diagram)

# Los Mestenios Condensate Compositions 2017-2021

|                        | 2021-08 |         | 2019-12 |         | 2018-12 |         | 2017-12 |         |
|------------------------|---------|---------|---------|---------|---------|---------|---------|---------|
| % of C3 and C4         | 6.7039  | 3.6217  | 11.9060 | 7.1220  | 13.8160 | 8.9030  | 14.5590 | 8.9790  |
| Components             | Mol %   | Wt. %   | Mol %   | Wt %    | Mol %   | Wt %    | Mol %   | Wt %    |
| Nitrogen               | 0.1226  | 0.0326  | NIL     | NIL     | 0.038   | 0.013   | NIL     | NIL     |
| Methane                | 4.9619  | 0.7550  | 1.0550  | 0.1910  | 2.1260  | 0.4160  | 1.6910  | 0.3160  |
| Carbon Dioxide         | 0.0114  | 0.0048  | 0.0520  | 0.0260  | 0.0580  | 0.0310  | 0.0800  | 0.0410  |
| Ethane                 | 1.0136  | 0.2891  | 1.9140  | 0.6490  | 2.5110  | 0.9200  | 2.5430  | 0.8910  |
| Propane                | 0.5570  | 0.2330  | 4.3440  | 2.1620  | 5.1710  | 2.7790  | 5.3860  | 2.7670  |
| I-Butane               | 1.6575  | 0.9138  | 2.0950  | 1.3740  | 2.4170  | 1.7120  | 2.5680  | 1.7390  |
| n-Butane               | 4.4894  | 2.4749  | 5.4670  | 3.5860  | 6.2280  | 4.4120  | 6.6050  | 4.4730  |
| I-Pentane              | 5.2977  | 3.6254  | 5.2840  | 4.3020  | 5.9790  | 5.2580  | 6.2280  | 5.2350  |
| n-Pentane              | 4.6814  | 3.2036  | 5.6470  | 4.5980  | 6.4790  | 5.6980  | 6.6290  | 5.5720  |
| Cyclopentane           | 0.0459  | 0.0305  |         |         |         |         |         |         |
| Hexanes                | 5.1819  | 4.1803  | 8.9550  | 8.5520  | 14.2170 | 14.6040 | 8.1720  | 8.0590  |
| n-Hexane               | 4.5147  | 3.6904  | 6.5170  | 6.3370  | 9.2150  | 9.6840  | 6.1350  | 6.1600  |
| 2,2,4 Trimethylpentane | 0.2871  | 0.3110  |         |         |         |         | 0.1010  | 0.1350  |
| Benzene                | 1.1103  | 0.8226  | 1.0410  | 0.9180  | 1.1160  | 1.0620  | 1.3000  | 1.1830  |
| Cyclohexane            | 3.9759  | 3.1738  | 4.3870  | 4.1660  | 4.5650  | 4.6830  |         |         |
| Heptanes               | 15.3366 | 14.3883 | 13.6290 | 14.6350 | 16.7680 | 19.1490 | 23.1100 | 25.2440 |
| n-Heptane              | 5.7726  | 5.4862  | 5.3470  | 6.0460  | 4.2200  | 5.1540  |         |         |
| Toluene                | 0.4231  | 0.3698  | 3.9200  | 4.0760  | 2.3330  | 2.6200  | 3.8320  | 4.1140  |
| Octanes                | 6.0212  | 6.4994  | 17.4840 | 20.9670 | 12.5370 | 16.0710 | 16.9520 | 20.9500 |
| n-Octane               | 4.3860  | 4.7521  | 2.5010  | 3.2230  | 1.0540  | 1.4670  |         |         |
| Ethylbenzene           | 0.4533  | 0.4564  | 0.3160  | 0.3780  | 0.1200  | 0.1550  | 0.2310  | 0.2860  |
| m+P Xylenes            | 2.1677  | 2.1827  | 2.8290  | 3.3890  | 0.8200  | 1.0610  | 1.8080  | 2.2370  |
| o-Xylene               | 0.9768  | 0.9836  |         |         |         |         |         |         |
| Nonanes                | 4.7222  | 5.4973  | 4.1860  | 5.7950  | 1.6200  | 2.4090  | 3.1220  | 4.4840  |
| n-Nonane               | 4.3392  | 5.1956  | 0.7340  | 1.0620  | 0.2030  | 0.3170  |         |         |
| I-Decanes              |         |         | 1.7050  | 2.5600  | 0.2050  | 0.3250  |         |         |
| Decanes Plus           | 17.4928 | 30.4486 | 0.5910  | 1.0080  | NIL     | NIL     | 3.507   | 6.114   |

### Los Mestenios Historic Condensate Data

| Date     | bbl     | 12-Month<br>Rolling<br>Total |
|----------|---------|------------------------------|
| 01/16/17 | 963.82  | 8786.98                      |
| 02/16/17 | 1362.04 | 9023.40                      |
| 03/16/17 | 958.91  | 8769.19                      |
| 04/16/17 | 1088.53 | 8830.14                      |
| 05/16/17 | 864.60  | 9109.79                      |
| 06/16/17 | 554.33  | 8916.12                      |
| 07/16/17 | 197.41  | 8940.46                      |
| 08/16/17 | 347.69  | 8931.72                      |
| 09/16/17 | 206.14  | 8754.51                      |
| 10/16/17 | 415.95  | 8647.17                      |
| 11/16/17 | 713.28  | 8447.20                      |
| 12/16/17 | 949.94  | 8622.64                      |
| 01/16/18 | 1213.61 | 8872.43                      |
| 02/16/18 | 1073.67 | 8584.06                      |
| 03/16/18 | 1181.14 | 8806.29                      |
| 04/16/18 | 782.85  | 8500.61                      |
| 05/16/18 | 757.31  | 8393.32                      |
| 06/16/18 | 395.24  | 8234.23                      |
| 07/16/18 | 580.68  | 8617.50                      |
| 08/16/18 | 388.74  | 8658.55                      |
| 09/16/18 | 214.93  | 8667.34                      |
| 10/16/18 | 402.99  | 8654.38                      |
| 11/16/18 | 610.66  | 8551.76                      |
| 12/16/18 | 795.01  | 8396.83                      |
| 01/16/19 | 807.21  | 7990.43                      |
| 02/16/19 | 772.56  | 7689.32                      |
| 03/16/19 | 1103.18 | 7611.36                      |
| 04/16/19 | 824.02  | 7652.53                      |
| 05/16/19 | 787.59  | 7682.81                      |
| 06/16/19 | 579.32  | 7866.89                      |
| 07/16/19 | 396.81  | 7683.02                      |
| 08/16/19 | 200.14  | 7494.42                      |
| 09/16/19 | 205.62  | 7485.11                      |
| 10/16/19 | 398.18  | 7480.30                      |
| 11/16/19 | 181.62  | 7051.26                      |
| 12/16/19 | 566.91  | 6823.16                      |
| 01/16/20 | 938.29  | 6954.24                      |
| 02/16/20 | 575.09  | 6756.77                      |
| 03/16/20 | 587.54  | 6241.13                      |
| 04/16/20 | 385.50  | 5802.61                      |
| 05/16/20 | 163.35  | 5178.37                      |
| 06/16/20 | 0.00    | 4599.05                      |
| 07/16/20 | 0.00    | 4202.24                      |

### Los Mestenios Historic Condensate Data

| Date     | bbl    | 12-Month<br>Rolling<br>Total |
|----------|--------|------------------------------|
| 08/31/20 | 0.00   | 4002.10                      |
| 09/30/20 | 0.00   | 3796.48                      |
| 10/31/20 | 182.85 | 3581.15                      |
| 11/30/20 | 0.00   | 3399.53                      |
| 12/31/20 | 200.62 | 3033.24                      |
| 01/31/21 | 386.61 | 2481.56                      |
| 02/28/21 | 214.68 | 2121.15                      |
| 03/31/21 | 405.50 | 1939.11                      |
| 04/30/21 | 369.54 | 1923.15                      |
| 05/31/21 | 388.46 | 2148.26                      |
| 06/30/21 | 367.70 | 2515.96                      |
| 07/31/21 | 188.48 | 2704.44                      |
| 08/31/21 | 0.00   | 2704.44                      |
| 09/30/21 | 365.55 | 3069.99                      |
| 10/31/21 | 211.25 | 3098.39                      |
| 11/30/21 | 368.17 | 3466.56                      |
| 12/31/21 | 401.86 | 3667.80                      |
| 01/31/22 | 618.45 | 3899.64                      |
| 02/28/22 | 410.07 | 4095.03                      |
| 03/31/22 | 718.78 | 4408.31                      |
| 04/30/22 | 366.57 | 4405.34                      |
| 05/31/22 | 351.32 | 4368.20                      |
| 06/30/22 | 180.56 | 4181.06                      |

## Condensate (bbl)

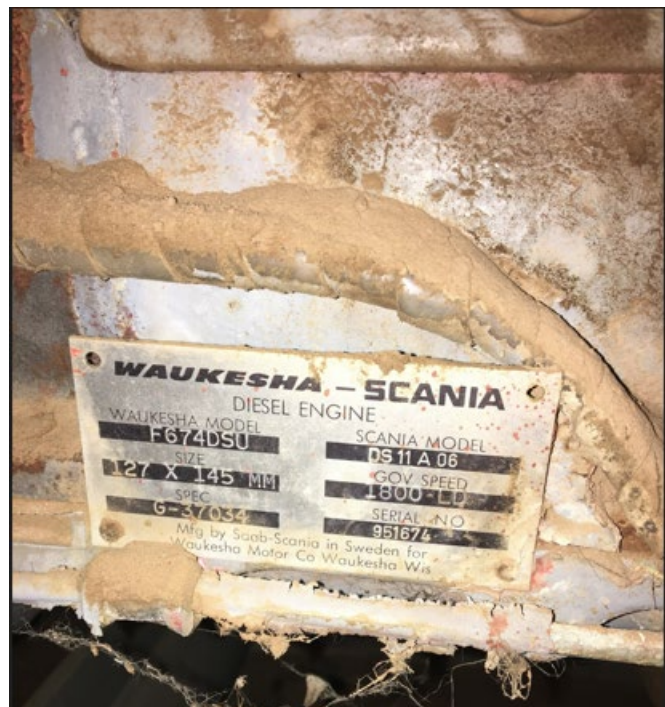
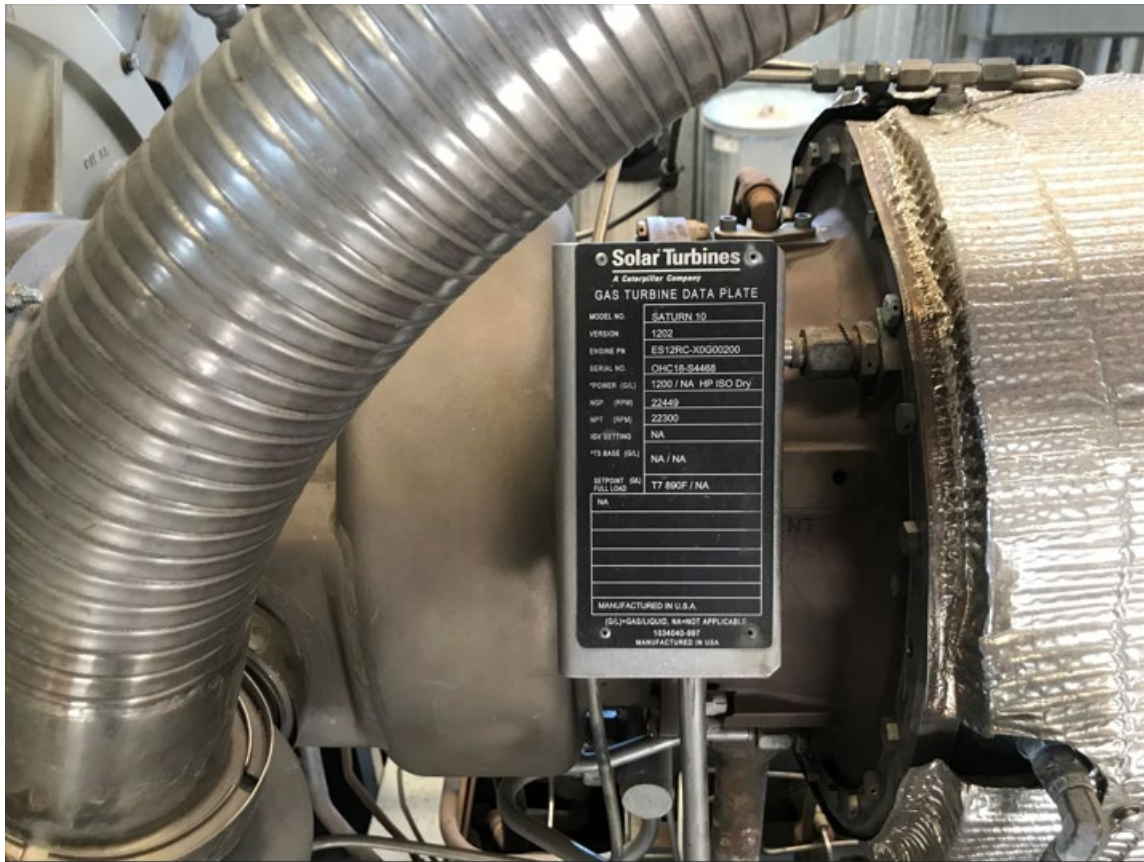
### Environmental - Tank Flash

Report Run Date:

| Date       | Los Mestenos,<br>Condensate (bbl) |
|------------|-----------------------------------|
| 01/31/2021 | 386.61                            |
| 02/28/2021 | 214.68                            |
| 03/31/2021 | 405.50                            |
| 04/30/2021 | 369.54                            |
| 05/31/2021 | 388.46                            |
| 06/30/2021 | 367.70                            |
| 07/31/2021 | 188.48                            |
| 08/31/2021 | 0.00                              |
| 09/30/2021 | 365.55                            |
| 10/31/2021 | 211.25                            |
| 11/30/2021 | 368.17                            |
| 12/31/2021 | 401.86                            |
| Sum        | 3,667.80                          |

### Los Mestenios 2021 Pigging Events

| Area  | Pig Name                        | Date/Time | Facility      |
|-------|---------------------------------|-----------|---------------|
| North | Trunk W South - Trk W South 10" | 01/05/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 02/10/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 03/19/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 04/27/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 05/20/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 06/14/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 07/13/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 01/13/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 01/25/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 02/11/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 02/16/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 03/02/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 03/15/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 03/29/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 04/06/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 04/13/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 05/10/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 05/24/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 06/08/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 06/22/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 06/30/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 07/07/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 07/13/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 07/22/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 08/04/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 08/19/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 08/31/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 09/01/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 09/14/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 09/27/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 10/18/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 10/19/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 10/25/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 11/01/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 11/15/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 11/15/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 11/22/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 12/07/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 12/07/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 12/14/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 12/20/21  | Los Mestenios |
| North | Trunk W South - Trk W South 10" | 12/27/21  | Los Mestenios |
| North | Trunk W South - Trk W South 8"  | 12/28/21  | Los Mestenios |





# Solar Turbines

A Caterpillar Company

## PREDICTED ENGINE PERFORMANCE

|   |  |
|---|--|
| Customer<br><b>Williams</b>                 |  |
| Job ID<br><b>TBD</b>                        |  |
| Run By<br><b>Michael E Clay</b>             | Date Run<br><b>28-Dec-07</b>               |
| Engine Performance Code<br><b>REV. 3.40</b> | Engine Performance Data<br><b>REV. 0.0</b> |

|                                    |
|------------------------------------|
| Model<br><b>SATURN 10-1200</b>     |
| Package Type<br><b>CS/MD</b>       |
| Match<br><b>STANDARD</b>           |
| Fuel System<br><b>GAS</b>          |
| Fuel Type<br><b>SD NATURAL GAS</b> |

### DATA FOR MINIMUM PERFORMANCE

|              |        |      |
|--------------|--------|------|
| Elevation    | feet   | 6700 |
| Inlet Loss   | in H2O | 2.2  |
| Exhaust Loss | in H2O | 3.3  |

|                          |           | 1      | 2      | 3      | 4      | 5      | 6      |
|--------------------------|-----------|--------|--------|--------|--------|--------|--------|
| Engine Inlet Temperature | deg F     | 0      | 20.0   | 40.0   | 60.0   | 80.0   | 100.0  |
| Relative Humidity        | %         | 60.0   | 60.0   | 60.0   | 60.0   | 60.0   | 60.0   |
| Driven Equipment Speed   | RPM       | 22300  | 22300  | 22289  | 22224  | 22050  | 21624  |
| Specified Load           | HP        | FULL   | FULL   | FULL   | FULL   | FULL   | FULL   |
| Net Output Power         | HP        | 960    | 942    | 914    | 881    | 837    | 771    |
| Fuel Flow                | mmBtu/hr  | 10.84  | 10.64  | 10.37  | 10.07  | 9.75   | 9.28   |
| Heat Rate                | Btu/HP-hr | 11295  | 11296  | 11351  | 11437  | 11645  | 12036  |
| Therm Eff                | %         | 22.526 | 22.524 | 22.415 | 22.247 | 21.850 | 21.139 |
| Engine Exhaust Flow      | lbm/hr    | 42233  | 41050  | 39871  | 38645  | 37142  | 35087  |
| Exhaust Temperature      | deg F     | 766    | 794    | 818    | 841    | 863    | 887    |

|                                       |                        |        |
|---------------------------------------|------------------------|--------|
| Fuel Gas Composition (Volume Percent) | Methane (CH4)          | 92.79  |
|                                       | Ethane (C2H6)          | 4.16   |
|                                       | Propane (C3H8)         | 0.84   |
|                                       | N-Butane (C4H10)       | 0.18   |
|                                       | N-Pentane (C5H12)      | 0.04   |
|                                       | Hexane (C6H14)         | 0.04   |
|                                       | Carbon Dioxide (CO2)   | 0.44   |
|                                       | Hydrogen Sulfide (H2S) | 0.0001 |
|                                       | Nitrogen (N2)          | 1.51   |

|                     |               |       |                  |        |                    |        |
|---------------------|---------------|-------|------------------|--------|--------------------|--------|
| Fuel Gas Properties | LHV (Btu/Scf) | 939.2 | Specific Gravity | 0.5970 | Wobbe Index at 60F | 1215.6 |
|---------------------|---------------|-------|------------------|--------|--------------------|--------|

This performance was calculated with a basic inlet and exhaust system. Special equipment such as low noise silencers, special filters, heat recovery systems or cooling devices will affect engine performance. Performance shown is "Expected" performance at the pressure drops stated, not guaranteed.

Notes

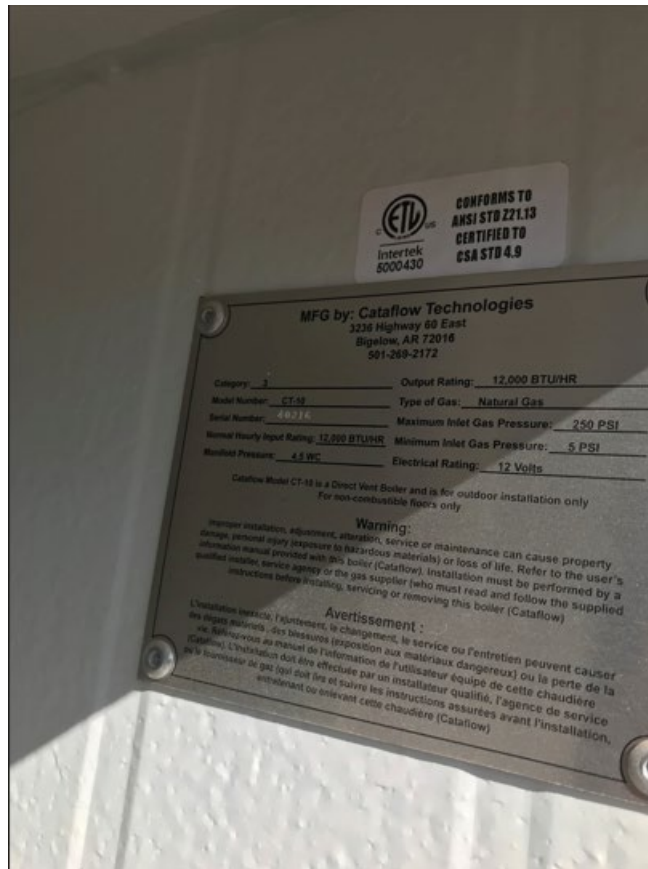
Los Mestenos



Unit T1



Unit T2



ETL  
Intertek  
5000430  
CONFORMS TO  
ANSI STD Z21.13  
CERTIFIED TO  
CSA STD 4.9

MFG by: Cataflow Technologies  
3238 Highway 68 East  
Bogalou, AR 72016  
501-269-2172

|   |                                     |
|---|-------------------------------------|
| Category: 1                               | Output Rating: 12,000 BTU/HR        |
| Model Number: CT-18                       | Type of Gas: Natural Gas            |
| Serial Number: 46234                      | Maximum Inlet Gas Pressure: 250 PSI |
| Normal Hourly Input Rating: 12,000 BTU/HR | Minimum Inlet Gas Pressure: 5 PSI   |
| Working Pressure: 4.5 WC                  | Electrical Rating: 12 Volts         |

Cataflow Model CT-18 is a Direct Vent Boiler and is for outdoor installation only  
For non-combustible fibers only

**Warning:**

Improper installation, adjustment, alteration, service or maintenance can cause property damage, personal injury (exposure to hazardous materials) or loss of life. Refer to the user's information manual provided with this boiler (Cataflow). Installation must be performed by a qualified installer, service agency or the gas supplier (who must read and follow the supplied instructions before installing, servicing or removing this boiler (Cataflow)).

**Avertissement :**

L'installation, service, l'ajustement, le changement, le service ou l'entretien peuvent causer des dégâts matériels, des blessures (exposition aux matériaux dangereux) ou la perte de la vie. Référez-vous au manuel de l'utilisateur de cette chaudière (Cataflow). L'installation doit être effectuée par un installateur qualifié, l'agence de service ou le fournisseur de gaz (qui doit lire et suivre les instructions assurées avant l'installation, entretient ou ôtant cette chaudière (Cataflow)).

Tank Heater



Caterpillar Engine Discharge - Air Gapped and Blind Flanged

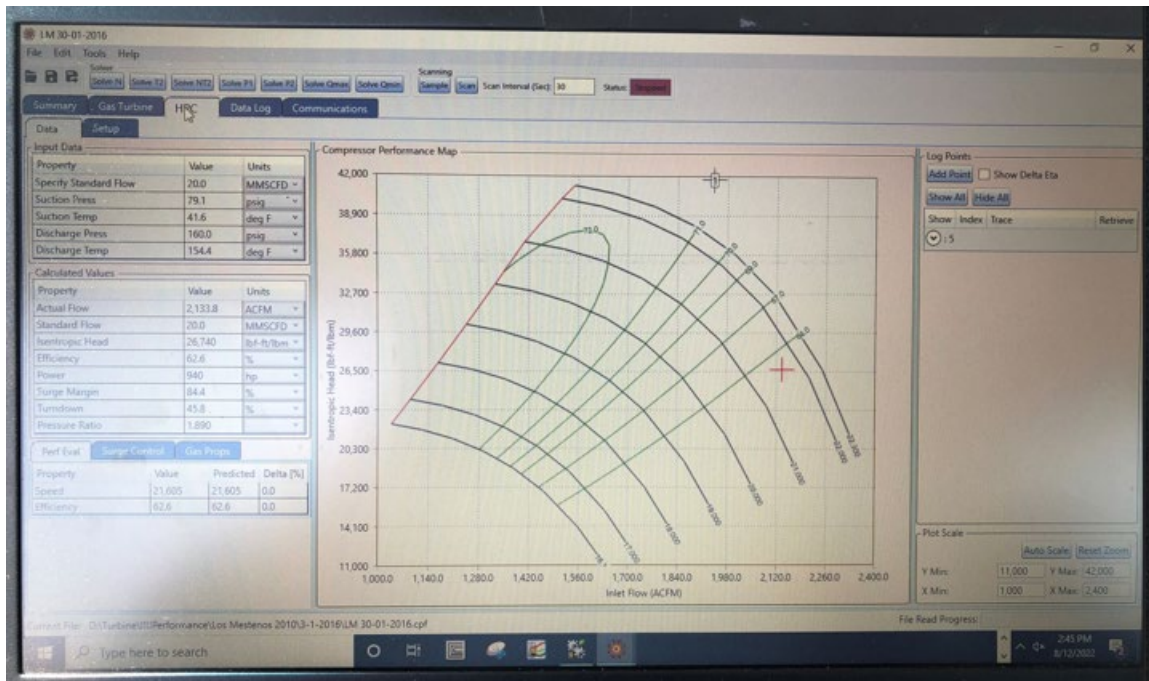


Caterpillar Engine Inlet - Air Gapped





Caterpillar Engine Fuel Gas Line – Air Gapped



Maximum Facility Throughput.



Williams Four Corners LLC  
Environmental Services  
1755 Arroyo Drive  
Bloomfield, NM 87413  
(505) 632-4700

March 29, 2018

U.S. EPA, Region 6  
Air Enforcement Section, 6EN-A  
1445 Ross Avenue  
Dallas, TX 75202-2733

re: Title V Part 71 Annual Fee - 2017  
Permit R6FOP-NM-04-R2 – Los Mestenos Compressor Station

Dear Madam/Sir,

In accordance with condition 4.15 of the Part 71 operating permit number R6FOP-NM-04-R2 for Williams Four Corners LLC's Los Mestenos Compressor Station, please find enclosed an annual report containing the hours of operation of the facility and the calculated annual emissions. Note that there were no periods of non-compliance to report.

The annual permit fee and associated forms (Form FEE – Fee Calculation Worksheet for pollutants emitted during the calendar year 2017 and the Form FF - Fee Filing Form) are being submitted concurrently with this report, in accordance with condition 5.1.2 of the permit.

If you have any questions, please call me at (505) 632-4708.

Sincerely,

A handwritten signature in blue ink, appearing to read "Mitch Morris".

Mitch Morris  
Environmental Specialist

Attachments



Federal Operating Permit Program (40 CFR Part 71)  
**FEE CALCULATION WORKSHEET (FEE)**

Use this form initially, or thereafter on an annual basis, to calculate part 71 fees.

**A. General Information**

Type of fee (Check one): ☐ Initial ☒ Annual

Deadline for submitting fee calculation worksheet 04 / 01 / 2018

For initial fees, emissions are based on (Check one):

☒ Actual emissions for the preceding calendar year. (Required in most circumstances.)

☐ Estimates of actual emissions for the current calendar year. (Required when operations commenced during the preceding calendar year.)

Date commenced operations      /      /     

☐ Estimates of actual emissions for the preceding calendar year. (Optional after a part 71 permit was issued to replace a part 70 permit, but only if initial fee payment is due between January 1 and March 31; otherwise use actual emissions for the preceding calendar year.)

For annual fee payment, you are required to use actual emissions for the preceding calendar year.

**B. Source Information:** Complete this section only if you are paying fees but not applying for a permit.

Source or facility name Williams Four Corners LLC's Los Mestenos Compressor Station

Mailing address: Street or P.O. Box 1755 Arroyo Drive

City: Bloomfield State: NM ZIP 87413 -     

Contact person: Mitch Morris Title: Environmental Specialist

Telephone (505) 632 - 4708 Ext      Part 71 permit no. R6FOP-NM-04-R2

**C. Certification of Truth, Accuracy and Completeness:** Only needed if not submitting a separate form CTAC.

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in this submittal (form and attachments) are true, accurate and complete.

Name (signed) 

Name (typed) Glen Jasek Date: 3 / 29 / 18

**D. Annual Emissions Report for Fee Calculation Purposes -- Non-HAP**

You may use this to report actual emissions (tons per year) of regulated pollutants (for fee calculation) on a calendar-year basis for both initial and annual fee calculation purposes. Section E is designed to report HAP emissions. Quantify all actual emissions, including fugitives, but do not include insignificant emissions and certain regulated air pollutants that are not counted for fee purposes, such as CO and GHGs (see instructions). Sum the emissions in each column to calculate subtotals. Subtotals should be reported to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000 for that column.

This data is for 2017 (year)

| Emission Unit ID  | NOx  | VOC  | SO2 | PM10 | Lead | Other |
|-------------------|------|------|-----|------|------|-------|
| 1                 | 14.3 | 0.4  |     |      |      |       |
| 2                 | 0.0  | 0.0  |     |      |      |       |
| Tk-1              | 0.0  | 49.7 |     |      |      |       |
| F-1               | 0.0  | 3.5  |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
| <b>SUBTOTALS:</b> | 14.3 | 53.6 |     |      |      |       |

**E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

HAP Identification. Identify individual HAP emitted at the facility, identify the CAS number, and assign a unique identifier for use in the second table in this section. Whenever assigning identifier codes, use "HAP1" for the first, "HAP2" for the second, and so on.

| Name of HAP  | CAS No    | Identifier   |
|--------------|-----------|--------------|
| Acetaldehyde | 75-07-0   | HAP <u>1</u> |
| Formaldehyde | 50-00-0   | HAP <u>2</u> |
| Benzene      | 71-43-2   | HAP <u>3</u> |
| Toluene      | 108-88-3  | HAP <u>4</u> |
| Ethylbenzene | 100-41-4  | HAP <u>5</u> |
| Xylenes      | 1330-20-7 | HAP <u>6</u> |
| n-Hexane     | 110-54-3  | HAP <u>7</u> |

HAP Emissions. Report the actual emissions of individual HAP identified above. Use the identifiers assigned in the table above. Include all emissions, including fugitives, and do not include insignificant emissions. Sum the emissions in each column to calculate subtotals. Report subtotals to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000.

This data is for 2017 (year)

| Emissions Unit ID | Actual Emissions (Tons/Year) |        |        |        |        |        |        |       |
|-------------------|------------------------------|--------|--------|--------|--------|--------|--------|-------|
|                   | HAP_1_                       | HAP_2_ | HAP_3_ | HAP_4_ | HAP_5_ | HAP_6_ | HAP_7_ | HAP__ |
| 1                 | 0.2                          | 0.3    |        |        |        |        |        |       |
| 2                 | 0.0                          | 0.0    |        |        |        |        |        |       |
| Tk-1              |                              |        | 0.5    | 1.9    | 0.1    | 1.0    | 6.8    |       |
| F-1               |                              |        |        |        |        |        | 0.0    |       |
|                   |                              |        |        |        |        |        |        |       |
|                   |                              |        |        |        |        |        |        |       |
|                   |                              |        |        |        |        |        |        |       |
| <b>SUBTOTALS:</b> | 0.2                          | 0.3    | 0.5    | 1.9    | 0.1    | 1.0    | 6.8    |       |



## F. Fee Calculation Worksheet

This worksheet is used to calculate the total fee owed (including the emissions-based fee and the GHG fee adjustment) for both initial and annual fee payment purposes. Reconciliation is only for cases where you are paying the annual fee and you used any type of estimate of actual emissions when you calculated the initial fee. If you do not need to reconcile fees, complete line 1-5 (emissions summary) and then skip down to line 21 (emission calculation). See instructions for more detailed explanation.

### EMISSIONS SUMMARY

|  |      |
|--|------|
| 1. Sum the subtotals from section D of this form (non-HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 67.9 |
| 2. Sum the subtotals from section E of this form (HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 10.7 |
| 3. Sum lines 1 and 2.  | 78.6 |
| 4. Enter the emissions that were counted twice. If none, enter "0."  | 10.7 |
| 5. Subtract line 4 from line 3, round to the nearest ton, and enter the result here. This is the <b>total emissions</b> that count for fees purposes.  | 67.9 |
| <p style="text-align: center;"><b>RECONCILIATION</b><br/> <b>(WHEN INITIAL FEES WERE BASED ON ESTIMATES</b><br/> <b>FOR THE "CURRENT" CALENDAR YEAR)</b></p> <p>Only complete lines 6-10 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year in which you paid initial fees; otherwise skip to line 11 or to line 21.</p> |      |
| 6. Enter the total estimated actual emissions for the year the initial fee was paid (previously reported on line 5 of the initial fee form).   |      |
| 7. If line 5 is greater than line 6, subtract line 6 from line 5, and enter the result. Otherwise enter "0."   |      |
| 8. If line 6 is greater than line 5, subtract line 5 from line 6, and enter the result. Otherwise enter "0."   |      |
| 9. If line 7 is greater than 0, multiply line 7 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment. Go to line 21.   |      |
| 10. If line 8 is greater than 0, multiply line 8 by last year's fee rate (\$/ton) and enter the result here. This is the overpayment. Go to line 21.   |      |

**RECONCILIATION  
(WHEN INITIAL FEES WERE BASED ON ESTIMATES  
FOR THE "PRECEDING" CALENDAR YEAR)**

Only complete lines 11-20 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year preceding initial fee payment; otherwise skip to line 21. If completing this section, you will also need to complete sections D and E to report actual emissions for the calendar year preceding initial fee payment.

|  |           |
|--|-----------|
| 11. Sum the actual emissions from section D (non-HAP) for the calendar year preceding initial fee payment and enter the result here.   |           |
| 12. Sum the actual emissions from section E (HAP) for the calendar year preceding initial fee payment and enter the result here.   |           |
| 13. Add lines 11 and 12 and enter the total here. These are total actual emissions for the calendar year preceding initial fee payment.  |           |
| 14. Enter double counted emission from line 13 here. If none, enter "0."   |           |
| 15. Subtract line 14 from line 13, round to the nearest ton, and enter the result here.  |           |
| 16. Enter the total estimated actual emissions previously reported on line 5 of the initial fee form. These are estimated actual emissions for the calendar year preceding initial fee payment.  |           |
| 17. If line 15 is greater than line 16, subtract line 16 from line 15, and enter the result here. Otherwise enter "0."   |           |
| 18. If line 16 is greater than line 15, subtract line 15 from line 16, and enter the result here. Otherwise enter "0."   |           |
| 19. If line 17 is greater than 0, multiply line 17 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment.   |           |
| 20. If line 18 is greater than 0, multiply line 18 by last year's fee rate (\$/ton) and enter the result on this line. This is the overpayment.  |           |
| <b>EMISSION FEE CALCULATION</b>  |           |
| 21. Multiply line 5 (tons) by the current fee rate (\$/ton) and enter the result here. This is the unadjusted emissions fee. Continue on to line 23.   | \$3500.92 |
| <b>GHG FEE ADJUSTMENT</b>  |           |
| 22. If you are submitting an initial permit application and this is the first time you are paying fees, enter \$2,236, otherwise enter "0". [Note that any updates to the initial application are covered under this one-time charge.] | 0         |
| 23. Enter the number of permit modifications (or related permit actions) you have submitted to the permitting authority since you last paid fees. If none, skip to line 25.  | 0         |
| 24. Multiply the number in line 23 by \$365 and enter the result.  | 0         |

|  |         |
|--|---------|
| 25. If you have submitted a permit renewal application since the last time you paid fees enter \$520, otherwise enter "0"  | 0       |
| 26. Sum line 22, 24, and 25 and enter the result. This is the GHG fee adjustment   | 0       |
| <b>OTHER ADJUSTMENTS</b>   |         |
| 27. Add the total on line 21 and the total on line 26 and enter the result.  | 3500.92 |
| 28. Enter any underpayment from line 9 or 19 here. Otherwise enter "0."  | 0       |
| 29. Enter any overpayment from line 10 or 20 here. Otherwise enter "0."  | 0       |
| 30. If line 28 is greater than "0," add it to line 27 and enter the result here. If line 29 is greater than "0," subtract this from line 27 and enter the result here. Otherwise enter the amount on line 27 here. This is the fee adjusted for over/underpayment. | 3500.92 |
| 31. Enter any credit for fee assessment error here. Otherwise, enter "0."  | 0       |
| 32. Subtract line 31 from line 30 and enter the result here. Stop here. This is the <b>TOTAL FEE (AFTER ADJUSTMENTS)</b> that you must remit to EPA.   | 3500.92 |



**Williams Four Corners LLC Los Mestenos Compressor Station  
2017 Actual Emissions**

|             | hours | NOx - lb/hr | NOx - tpy | VOC - lb/hr | VOC - tpy |
|-------------|-------|-------------|-----------|-------------|-----------|
| Solar       | 8438  | 3.4         | 14.3      | 0.1         | 0.4       |
| Caterpillar | 0.0   | 18.8        | 0.0       | 13.5        | 0.00      |
| Tk-1 flash  | 8760  |             |           |             | 46.7      |
| Tk-1 W&B    | 8760  |             |           |             | 3.0       |
| F-1         | 8760  |             |           | PTE         | 3.5       |
|             |       |             | 14.3      |             | 53.6      |

turbine NOx emission rates = 9/1/10 EPA method test results (max of three test dates)

engine NOx emission rates = 5/11/10 EPA method test results (max of three test dates)

turbine VOC emission rates = 2010 TV PTE equiv allowables

(5/11/10 & 8/31/10 VOC test results = 0.0 ppmvd NMEOC & 0.0 lb/hr VOC)

engine VOC emission rates = 5/11/10 EPA method test results (max of three test dates)

tank flash VOC emissions = 2017 ProMax calc

tank W&B VOC emissions from 2017 Tanks4.09d calc.

fugitive VOC emissions = TV app emissions w/o SF

**FEE CALCULATION**

Year 2017 tons of pollutant = 67.9

2017 annual fee at \$51.56/ton = \$3,500.92

hours from monthly fuel use (bob3) report - fuel meter #10030-30

|        | Solar | Caterpillar |
|--------|-------|-------------|
| Jan-17 | 743.9 | 0           |
| Feb-17 | 668.8 | 0           |
| Mar-17 | 731.0 | 0           |
| Apr-17 | 521.2 | 0           |
| May-17 | 728.8 | 0           |
| Jun-17 | 719.9 | 0           |
| Jul-17 | 675.5 | 0           |
| Aug-17 | 736.1 | 0           |
| Sep-17 | 707.5 | 0           |
| Oct-17 | 743.4 | 0           |
| Nov-17 | 720.0 | 0           |
| Dec-17 | 742.4 | 0           |
|        | 8438  | 0.0         |

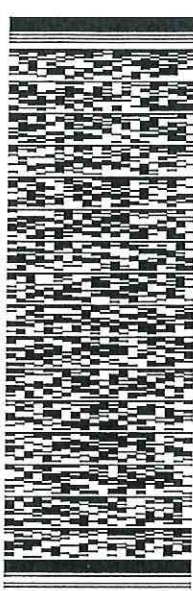
ORIGIN ID:FMNA (505) 632-4500  
TRISTEN RIVERA  
WILLIAMS FOUR CORNERS LLC  
1155 ARROYO DRIVE  
BLOOMFIELD, NM 87413  
UNITED STATES US

SHIP DATE: 30MAR18  
ACTWGT: 0.50 LB  
CAD: 105020064/NET3980  
BILL SENDER

TO AIR ENFORCEMENT SECTION, 6EN-A  
USEPA REGION 6  
1445 ROSS AVE

DALLAS TX 75202

REF: (000) 000-0000  
INV: PO: DEPT:

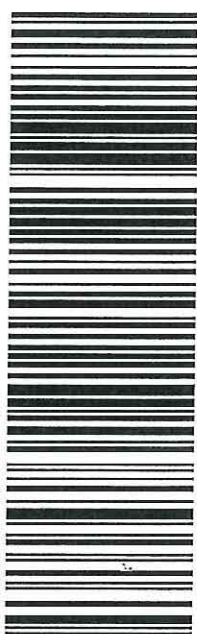


TRK# 7718 7807 9840  
0201

MON - 02 APR 10:30A  
PRIORITY OVERNIGHT

XH KIPA

75202  
TX-US DFW



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**Warning: Use only the printed original label for shipping. Using a photocopy of this label for shipping purposes is fraudulent and could result in additional billing charges, along with the cancellation of your FedEx account number.**

Use of this system constitutes your agreement to the service conditions in the current FedEx Service Guide, available on [fedex.com](http://fedex.com). FedEx will not be responsible for any claim in excess of \$100 per package, whether the result of loss, damage, delay, non-delivery, misdelivery, or misinformation, unless you declare a higher value, pay an additional charge, document your actual loss and file a timely claim. Limitations found in the current FedEx Service Guide apply. Your right to recover from FedEx for any loss, including intrinsic value of the package, loss of sales, income interest, profit, attorney's fees, costs, and other forms of damage whether direct, incidental, consequential, or special is limited to the greater of \$100 or the authorized declared value. Recovery cannot exceed actual documented loss. Maximum for items of extraordinary value is \$1,000, e.g. jewelry, precious metals, negotiable instruments and other items listed in our ServiceGuide. Written claims must be filed within strict time limits, see current FedEx Service Guide.



## Ruybalid, Tristen

**From:** TrackingUpdates@fedex.com  
**Sent:** Monday, April 02, 2018 9:06 AM  
**To:** Ruybalid, Tristen  
**Subject:** [EXTERNAL] FedEx Shipment 771878079840 Delivered

# Your package has been delivered

Tracking # 771878079840

Ship date:

**Fri, 3/30/2018**

**Tristen Ruybalid**

Williams Four Corners LLC  
BLOOMFIELD, NM 87413  
US



Delivery date:

**Mon, 4/2/2018 9:56 am**

**Air Enforcement Section,  
6EN-A**

USEPA Region 6  
1445 ROSS AVE  
DALLAS, TX 75202  
US

## Personalized Message

Los Mestenos

## Shipment Facts

Our records indicate that the following package has been delivered.

**Tracking number:** [771878079840](#)

**Status:** Delivered: 04/02/2018 09:56 AM  
Signed for By: C.LEWIS

**Signed for by:** C.LEWIS

**Delivery location:** DALLAS, TX

**Delivered to:** Receptionist/Front Desk

**Service type:** FedEx Priority Overnight

**Packaging type:** FedEx Envelope

**Number of pieces:** 1

**Weight:** 0.50 lb.

**Special handling/Services:** Deliver Weekday

**Standard transit:** 4/2/2018 by 10:30 am

## This tracking update has been requested by:


**Company name:** Williams Four Corners LLC

**Name:** Tristen Ruybalid



**Email:**

Mitch.Morris@williams.com

 Please do not respond to this message. This email was sent from an unattended mailbox. This report was generated at approximately 10:05 AM CDT on 04/02/2018.

All weights are estimated.

To track the latest status of your shipment, click on the tracking number above.

This tracking update has been sent to you by FedEx on behalf of the Requestor Mitch.Morris@williams.com. FedEx does not validate the authenticity of the requestor and does not validate, guarantee or warrant the authenticity of the request, the requestor's message, or the accuracy of this tracking update.

Standard transit is the date and time the package is scheduled to be delivered by, based on the selected service, destination and ship date. Limitations and exceptions may apply. Please see the FedEx Service Guide for terms and conditions of service, including the FedEx Money-Back Guarantee, or contact your FedEx Customer Support representative.

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Thank you for your business.



Williams Four Corners LLC  
Environmental Services  
1755 Arroyo Drive  
Bloomfield, NM 87413  
(505) 632-4700

March 29, 2018

U.S. Bank  
Government Lockbox 979078  
US EPA FOIA & Misc. Payments  
1005 Convention Plaza  
SL-MO-C2-GL  
St. Louis, MO 63101

re: Title V Part 71 Annual Fee - 2017  
Permit R6FOP-NM-04-R2 – Los Mestenios Compressor Station

Dear Madam/Sir,

In accordance with condition 5.1 of the Part 71 operating permit number R6FOP-NM-04-R2 for Williams Four Corners LLC's Los Mestenios Compressor Station, please find enclosed the Form FEE – Fee Calculation Worksheet for pollutants emitted during the calendar year 2017, and Form FF for the filing of payment for these emissions. Also enclosed is check number 4000198507 in the amount of \$3,500.92 for the annual permit fee for operations during calendar year 2017.

If you have any questions, please call me at (505) 632-4708.

Sincerely,

A handwritten signature in blue ink, appearing to read "Mitch Morris".

Mitch Morris  
Environmental Specialist

Attachments

Xc: U.S. EPA Region VI  
Air Permits Section, 6PD-R  
1445 Ross Avenue  
Dallas, TX 75202-2733

**Federal Operating Permit Program (40 CFR Part 71)  
FEE FILING FORM (FF)**

The purpose of this form is to ensure that fee payments made by check are credited to the proper facility and to the proper government account. Send this form, along with form **FEE** and the check, to the appropriate lockbox bank address listed on the following page. This form is required whenever you pay by check, including for initial and annual fee payments. Part 71 fees may be paid by check or electronically, and further information on making payments by check or electronically is provided on the following page.

Source or Facility Name Williams Four Corners LLC's Los Mestenos Compressor StationSource Location Rio Arriba County, New MexicoEPA Region where Source Located Region 6

## Mailing Address:

Street/P.O. Box 1755 Arroyo DriveCity BloomfieldState NM ZIP 87413 - Contact Person: Mitch MorrisTitle Environmental SpecialistTelephone ( 505 ) 632 - 4708 Ext. **Total Fee Payment Remitted:** \$ 3500.92

WILLIAMS FIELD SERVICES GROUP LLC  
PO BOX 21218  
TULSA, OK 74121-1218

COMPANY NUMBER: 4000

CHECK NUMBER: 4000198507

| PAY DATE  | SUPPLIER NO. | SUPPLIER NAME                      | CHECK TOTAL |
|-----------|--------------|------------------------------------|-------------|
| 08-MAR-18 | 400605       | US ENVIRONMENTAL PROTECTION AGENCY | 3,500.92    |

[illegible]

**Supplier Support 1-866-778-2665**

VERIFY THE AUTHENTICITY OF THIS MULTI-TONE SECURITY DOCUMENT.

CHECK BACKGROUND AREA CHANGES COLOR GRADUALLY FROM TOP TO BOTTOM.



WILLIAMS FIELD SERVICES GROUP LLC  
PO BOX 21218  
TULSA, OK 74121-1218  
Company Number: 4000

JPMorgan Chase Bank, N.A. 70-2322/719  
Chicago, IL

Check Number: 4000198507

Check Date: 08-MAR-18

**Three Thousand Five Hundred Dollars And Ninety-Two Cents**

**Pay To The Order Of:**

US ENVIRONMENTAL PROTECTION AGENCY  
US BANK - GOVT LOCKBOX 979078  
US EPA FOIA & MISC PAYMENTS  
1005 CONVENTION PLAZA, SL-MO-C2-GL  
ST LOUIS, MO 63101 United States

|           |            |
|-----------|------------|
| PAY (USD) | \$3,500.92 |
|-----------|------------|

Authorized Signature

11400019850711 1207192322612

00101312711



## TWO PAYMENT OPTIONS FOR PART 71 FEES:

### OPTION 1 - CHECK PAYMENT VIA U.S. POSTAL SERVICE

- Fee payment shall be in U.S. currency drawn on a U.S. bank.
- Check should be made out to the order of the "U.S. Environmental Protection Agency."
- Indicate on the check that the payment is for "Part 71 Fee Payment."
- Make a photocopy of the check.
- **Send the following to the EPA region (or delegate agency):**
  - ✓ Form *FEE* (EPA Form 5900-03) and
  - ✓ Photocopy of check
- **Send the following to one of the addresses below:**
  - ✓ Form *FF* (EPA Form 5900-06) and
  - ✓ Original check

| <b><i>Address for Regular Mail<br/>(U.S. Postal Service):</i></b>   | <b><i>Address for Express Delivery<br/>(or If Physical Address is Required):</i></b>   |
|---|--|
| U.S. EPA<br>FOIA and Misc. Payments<br>Cincinnati Finance Center<br>PO Box 979078<br>St. Louis, MO 63197-9000 | U.S. Bank<br>Government Lockbox 979078<br>US EPA FOIA & Misc. Payments<br>1005 Convention Plaza<br>Mail Station SL-MO-C2-GL<br>St. Louis, MO 63101 |

- **Tips for Completing form FF (Fee Filing Form)**
  - **Source Location:** Physical location - Street address (if any), City, County, and State.
  - **Mailing Address:** Address for the EPA to send correspondence. This address may be different from the source location, such as a corporate office.
  - **EPA Region:** EPA region in which the source is located (e.g., EPA Region 8).
  - **Contact:** Person that can best answer questions concerning fee payment.

### OPTION 2 – ONLINE PAYMENT

- Part 71 fees can be paid online at [www.pay.gov](http://www.pay.gov) using form "**SFO 1.1 (EPA Miscellaneous Payments - Cincinnati Finance Center)**." *Note that EPA Form 5900-06 cannot be used for online payments.*
- **Tips for completing online form SFO 1.1:**
  - From the "Type of Payment" drop down menu, select "Other/Miscellaneous"
  - On the "Bill# or description" line, enter "Part 71 Fee Payment"
  - In the "Comments" box, enter the source or facility name and the part 71 permit number associated with this payment.
- **After submitting payment online, send the following to the EPA region (or delegate agency):**
  - Form *FEE* (EPA Form 5900-03) and
  - Copy of the electronic payment confirmation generated by the online payment system.
- **FOR MORE INFORMATION:** The following link provides detailed information on how to make payments to EPA for part 71 fees, penalties, and interest, including contact information for EPA's Accounts Receivable Branch in Cincinnati <https://www.epa.gov/financial/makepayment>

**Contacts:** Craig Steffen (US EPA Finance): 513-487-2091  
Natalie Pearson (U.S. Bank): 314-418-4087

Federal Operating Permit Program (40 CFR Part 71)  
**CERTIFICATION OF TRUTH, ACCURACY, AND COMPLETENESS (CTAC)**

This form must be completed, signed by the "Responsible Official" designated for the facility or emission unit, and sent with each submission of documents (i.e., application forms, updates to applications, reports, or any information required by a part 71 permit).

**A. Responsible Official**

Name: (Last) Jasek (First) Glen (MI)

Title Vice President and General Manager, Four Corners Area

Street or P.O. Box 1755 Arroyo Drive

City Bloomfield State NM ZIP 87413 -

Telephone ( 505 ) 632 - 4628 Ext.  Facsimile ( 505 ) 632 - 4781

**B. Certification of Truth, Accuracy and Completeness** (to be signed by the responsible official)

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in these documents are true, accurate and complete.

Name (signed) 

Name (typed) Glen Jasek Date: 3 / 29 / 18



ORIGIN ID: FAMA (505) 632-4600  
TRISTEN RUTBAID  
WILLIAMS FOUR CORNERS LLC  
1755 ARROYO DRIVE  
BLOOMFIELD, NM 87413  
UNITED STATES US

SHIP DATE: 30MAR18  
ACTWG: 0.50 LB  
CAD: 105020064/INET3980

BILL SENDER

TO US EPA FOIA & MISC. PAYMENTS

US BANK - GOVNMNT LOCKBOX 979078

1005 CONVENTION PLAZA

SL-MO-C2-GL

SAINT LOUIS MO 63101

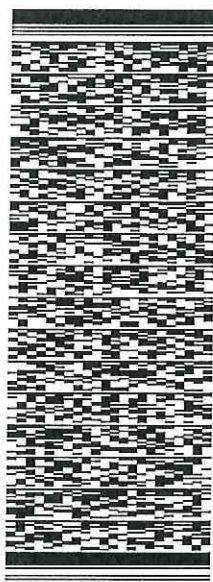
(000) 000-0000

REF:

PO:

DEPT:

552J107F5/DC/5



J181118012601ur

TRK# 7718 7816 9338  
0201

MON - 02 APR 10:30A  
PRIORITY OVERNIGHT

XX CPSA

63101  
MO-US STL



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2. Fold the printed page along the horizontal line.
3. Place label in shipping pouch and affix it to your shipment so that the barcode portion of the label can be read and scanned.

**Warning: Use only the printed original label for shipping. Using a photocopy of this label for shipping purposes is fraudulent and could result in additional billing charges, along with the cancellation of your FedEx account number.**

Use of this system constitutes your agreement to the service conditions in the current FedEx Service Guide, available on [fedex.com](http://fedex.com). FedEx will not be responsible for any claim in excess of \$100 per package, whether the result of loss, damage, delay, non-delivery, misdelivery, or misinformation, unless you declare a higher value, pay an additional charge, document your actual loss and file a timely claim. Limitations found in the current FedEx Service Guide apply. Your right to recover from FedEx for any loss, including intrinsic value of the package, loss of sales, income interest, profit, attorney's fees, costs, and other forms of damage whether direct, incidental, consequential, or special is limited to the greater of \$100 or the authorized declared value. Recovery cannot exceed actual documented loss. Maximum for items of extraordinary value is \$1,000, e.g. jewelry, precious metals, negotiable instruments and other items listed in our ServiceGuide. Written claims must be filed within strict time limits, see current FedEx Service Guide.



## Ruybalid, Tristen

**From:** TrackingUpdates@fedex.com  
**Sent:** Monday, April 02, 2018 7:47 AM  
**To:** Ruybalid, Tristen  
**Subject:** [EXTERNAL] FedEx Shipment 771878169338 Delivered

# Your package has been delivered

Tracking # 771878169338

Ship date:

**Fri, 3/30/2018**

**Tristen Ruybalid**

Williams Four Corners LLC

BLOOMFIELD, NM 87413

US

Delivery date:

**Mon, 4/2/2018 8:41 am**

**US EPA FOIA & Misc.**

**Payments**

US Bank - Govnmnt Lockbox  
979078

1005 Convention Plaza

SL-MO-C2-GL

SAINT LOUIS, MO 63101

US



## Personalized Message

Los Mestenios

## Shipment Facts

Our records indicate that the following package has been delivered.

**Tracking number:** [771878169338](#)

**Status:** Delivered: 04/02/2018 08:41 AM  
Signed for By: M.KINDIN

**Signed for by:** M.KINDIN

**Delivery location:** SAINT LOUIS, MO

**Delivered to:** Mailroom

**Service type:** FedEx Priority Overnight

**Packaging type:** FedEx Envelope

**Number of pieces:** 1

**Weight:** 0.50 lb.


**Special handling/Services:** Deliver Weekday

**Standard transit:** 4/2/2018 by 10:30 am

**This tracking update has been requested by:**

**Company name:** Williams Four Corners LLC

**Name:** Tristen Ruybalid  
**Email:** Mitch.Morris@williams.com

 Please do not respond to this message. This email was sent from an unattended mailbox. This report was generated at approximately 8:46 AM CDT on 04/02/2018.

All weights are estimated.

To track the latest status of your shipment, click on the tracking number above.

This tracking update has been sent to you by FedEx on behalf of the Requestor Mitch.Morris@williams.com. FedEx does not validate the authenticity of the requestor and does not validate, guarantee or warrant the authenticity of the request, the requestor's message, or the accuracy of this tracking update.

Standard transit is the date and time the package is scheduled to be delivered by, based on the selected service, destination and ship date. Limitations and exceptions may apply. Please see the FedEx Service Guide for terms and conditions of service, including the FedEx Money-Back Guarantee, or contact your FedEx Customer Support representative.

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Thank you for your business.



1755 Arroyo Drive  
Bloomfield, NM 87413  
Phone 505-632-4600  
Fax 505-632-4682  
harvestmidstream.com

July 17, 2019

U.S. EPA, Region 6  
Air and Radiation Division Air Permits Section (ARPE)  
1201 Elm Street, Suite 500  
Dallas, TX 75270

re: Title V Part 71 Annual Fee - 2018  
Permit R6FOP-NM-04-R2 – Los Mestenios Compressor Station

Dear Madam/Sir,

In accordance with condition 4.15 of the Part 71 operating permit number R6FOP-NM-04-R2 for Harvest Four Corners, LLC's Los Mestenios Compressor Station, please find enclosed an annual report containing the hours of operation of the facility and the calculated annual emissions. Note that except for the late submittal of the annual report addressed below, there were no periods of non-compliance to report.

The annual permit fee and associated forms (Form FEE – Fee Calculation Worksheet for pollutants emitted during the calendar year 2018 and the Form FF - Fee Filing Form) will be submitted no later than July 20, 2019 in accordance with condition 5.1.2 of the permit.

Note that due to the Fall 2018 change in ownership and initiation of a new compliance tracking system, this annual report was not submitted by the April 1, 2019 as required by the permit. The fee is being paid within the appropriate timeline. This deviation will be noted in the next six-month report.

If you have any questions, please call me at (505) 632-4625 or Bobby Myers of Cirrus Consulting at (801) 484-4412.

Sincerely,

Monica Smith  
Environmental Specialist

Attachments

**Federal Operating Permit Program (40 CFR Part 71)  
FEE CALCULATION WORKSHEET (FEE)**

Use this form initially, or thereafter on an annual basis, to calculate part 71 fees.

**A. General Information**

Type of fee (Check one): ☐ Initial ☒ Annual

Deadline for submitting fee calculation worksheet 04 / 01 / 2019

For initial fees, emissions are based on (Check one):

☒ Actual emissions for the preceding calendar year. (Required in most circumstances.)

☐ Estimates of actual emissions for the current calendar year. (Required when operations commenced during the preceding calendar year.)

Date commenced operations      /      /     

☐ Estimates of actual emissions for the preceding calendar year. (Optional after a part 71 permit was issued to replace a part 70 permit, but only if initial fee payment is due between January 1 and March 31; otherwise use actual emissions for the preceding calendar year.)

For annual fee payment, you are required to use actual emissions for the preceding calendar year.

**B. Source Information:** Complete this section only if you are paying fees but not applying for a permit.

Source or facility name Harvest Four Corners, LLC's Los Mestenos Compressor Station

Mailing address: Street or P.O. Box 1755 Arroyo Drive

City: Bloomfield State: NM ZIP 87413 -     

Contact person: Monica Smith Title: Environmental Specialist

Telephone ( 505 ) 632 - 4625 Ext      Part 71 permit no. R6FOP-NM-04-R2

**C. Certification of Truth, Accuracy and Completeness:** Only needed if not submitting a separate form CTAC.

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in this submittal (form and attachments) are true, accurate and complete.

Name (signed) 

Name (typed) Travis Jones Date: 7 / 15 / 2019

**E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

**HAP Identification.** Identify individual HAP emitted at the facility, identify the CAS number, and assign a unique identifier for use in the second table in this section. Whenever assigning identifier codes, use "HAP1" for the first, "HAP2" for the second, and so on.

| Name of HAP  | CAS No    | Identifier |
|--------------|-----------|------------|
| Acetaldehyde | 75-07-0   | HAP __1__  |
| Formaldehyde | 50-00-0   | HAP __2__  |
| Benzene      | 71-43-2   | HAP __3__  |
| Toluene      | 108-88-3  | HAP __4__  |
| Ethylbenzene | 100-41-4  | HAP __5__  |
| Xylenes      | 1330-20-7 | HAP __6__  |
| n-Hexane     | 110-54-3  | HAP __7__  |

**HAP Emissions.** Report the actual emissions of individual HAP identified above. Use the identifiers assigned in the table above. Include all emissions, including fugitives, and do not include insignificant emissions. Sum the emissions in each column to calculate subtotals. Report subtotals to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000.

This data is for \_2018\_ (year)

| Emissions Unit ID | Actual Emissions (Tons/Year) |         |         |         |         |         |         |         |
|-------------------|------------------------------|---------|---------|---------|---------|---------|---------|---------|
|                   | HAP_1__                      | HAP_2__ | HAP_3__ | HAP_4__ | HAP_5__ | HAP_6__ | HAP_7__ | HAP____ |
| 1                 | 0.2                          | 0.3     |         |         |         |         |         |         |
| 2                 | 0.0                          | 0.0     |         |         |         |         |         |         |
| Tk-1              |                              |         | 0.3     | 0.2     | 0.0     | 0.0     | 7.0     |         |
| F-1               |                              |         |         |         |         |         | 0.5     |         |
|                   |                              |         |         |         |         |         |         |         |
|                   |                              |         |         |         |         |         |         |         |
|                   |                              |         |         |         |         |         |         |         |
| <b>SUBTOTALS:</b> | 0.2                          | 0.3     | 0.3     | 0.2     | 0.0     | 0.0     | 7.5     |         |

## F. Fee Calculation Worksheet

This worksheet is used to calculate the total fee owed (including the emissions-based fee and the GHG fee adjustment) for both initial and annual fee payment purposes. Reconciliation is only for cases where you are paying the annual fee and you used any type of estimate of actual emissions when you calculated the initial fee. If you do not need to reconcile fees, complete line 1-5 (emissions summary) and then skip down to line 21 (emission calculation). See instructions for more detailed explanation.

### EMISSIONS SUMMARY

|  |      |
|--|------|
| 1. Sum the subtotals from section D of this form (non-HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 72.1 |
| 2. Sum the subtotals from section E of this form (HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 8.5  |
| 3. Sum lines 1 and 2.  | 80.6 |
| 4. Enter the emissions that were counted twice. If none, enter "0."  | 8.5  |
| 5. Subtract line 4 from line 3, round to the nearest ton, and enter the result here. This is the <b>total emissions</b> that count for fees purposes.  | 72.1 |
| <p style="text-align: center;"><b>RECONCILIATION</b><br/> <b>(WHEN INITIAL FEES WERE BASED ON ESTIMATES</b><br/> <b>FOR THE "CURRENT" CALENDAR YEAR)</b></p> <p>Only complete lines 6-10 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year in which you paid initial fees; otherwise skip to line 11 or to line 21.</p> |      |
| 6. Enter the total estimated actual emissions for the year the initial fee was paid (previously reported on line 5 of the initial fee form).   |      |
| 7. If line 5 is greater than line 6, subtract line 6 from line 5, and enter the result. Otherwise enter "0."   |      |
| 8. If line 6 is greater than line 5, subtract line 5 from line 6, and enter the result. Otherwise enter "0."   |      |
| 9. If line 7 is greater than 0, multiply line 7 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment. Go to line 21.   |      |
| 10. If line 8 is greater than 0, multiply line 8 by last year's fee rate (\$/ton) and enter the result here. This is the overpayment. Go to line 21.   |      |

**RECONCILIATION  
(WHEN INITIAL FEES WERE BASED ON ESTIMATES  
FOR THE "PRECEDING" CALENDAR YEAR)**

Only complete lines 11-20 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year preceding initial fee payment; otherwise skip to line 21. If completing this section, you will also need to complete sections D and E to report actual emissions for the calendar year preceding initial fee payment.

|   |  |
|---|--|
| 11. Sum the actual emissions from section D (non-HAP) for the calendar year preceding initial fee payment and enter the result here.  |  |
| 12. Sum the actual emissions from section E (HAP) for the calendar year preceding initial fee payment and enter the result here.  |  |
| 13. Add lines 11 and 12 and enter the total here. These are total actual emissions for the calendar year preceding initial fee payment.   |  |
| 14. Enter double counted emission from line 13 here. If none, enter "0."  |  |
| 15. Subtract line 14 from line 13, round to the nearest ton, and enter the result here.   |  |
| 16. Enter the total estimated actual emissions previously reported on line 5 of the initial fee form. These are estimated actual emissions for the calendar year preceding initial fee payment. |  |
| 17. If line 15 is greater than line 16, subtract line 16 from line 15, and enter the result here. Otherwise enter "0."  |  |
| 18. If line 16 is greater than line 15, subtract line 15 from line 16, and enter the result here. Otherwise enter "0."  |  |
| 19. If line 17 is greater than 0, multiply line 17 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment.  |  |
| 20. If line 18 is greater than 0, multiply line 18 by last year's fee rate (\$/ton) and enter the result on this line. This is the overpayment.   |  |

**EMISSION FEE CALCULATION**

|  |           |
|--|-----------|
| 21. Multiply line 5 (tons) by the current fee rate (\$/ton) and enter the result here. This is the unadjusted emissions fee. Continue on to line 23. | \$3807.60 |
|--|-----------|

**GHG FEE ADJUSTMENT**

|  |   |
|--|---|
| 22. If you are submitting an initial permit application and this is the first time you are paying fees, enter \$2,236, otherwise enter "0". [Note that any updates to the initial application are covered under this one-time charge.] | 0 |
| 23. Enter the number of permit modifications (or related permit actions) you have submitted to the permitting authority since you last paid fees. If none, skip to line 25.  | 0 |
| 24. Multiply the number in line 23 by \$365 and enter the result.  | 0 |

|  |         |
|--|---------|
| 25. If you have submitted a permit renewal application since the last time you paid fees enter \$520, otherwise enter "0"  | 0       |
| 26. Sum line 22, 24, and 25 and enter the result. This is the GHG fee adjustment   | 0       |
| <b>OTHER ADJUSTMENTS</b>   |         |
| 27. Add the total on line 21 and the total on line 26 and enter the result.  | 3807.60 |
| 28. Enter any underpayment from line 9 or 19 here. Otherwise enter "0."  | 0       |
| 29. Enter any overpayment from line 10 or 20 here. Otherwise enter "0."  | 0       |
| 30. If line 28 is greater than "0," add it to line 27 and enter the result here. If line 29 is greater than "0," subtract this from line 27 and enter the result here. Otherwise enter the amount on line 27 here. This is the fee adjusted for over/underpayment. | 3807.60 |
| 31. Enter any credit for fee assessment error here. Otherwise, enter "0."  | 0       |
| 32. Subtract line 31 from line 30 and enter the result here. Stop here. This is the <b>TOTAL FEE (AFTER ADJUSTMENTS)</b> that you must remit to EPA.   | 3807.60 |



## INSTRUCTIONS FOR FEE FEE CALCULATION WORKSHEET

### Information Collection Burden Estimates

The public reporting and recordkeeping burden for this collection of information is estimated to average 247 hours per respondent per year. Send comments on the Agency's need for this information, the accuracy of the provided burden estimates, and any suggested methods for minimizing respondent burden, including through the use of automated collection techniques to the Director, Collection Strategies Division, U.S. Environmental Protection Agency (2822T), 1200 Pennsylvania Ave., NW, Washington, D.C. 20460. Include the OMB control number in any correspondence. Do not send the completed form to this address.

### DETAILED INSTRUCTIONS

Use this form to initially or annually calculate fees. This form is for paying fees to EPA or a delegate agency (such as a State or tribe) under a part 71 operating permit program. The requirements for paying fees under part 71 programs, as well as the forms and instructions contained herein, are based on the requirements of 40 CFR 71.9

There may be cases, under a part 71 program, when you are not required to complete this form or pay the EPA fee rate (where the part 71 program has been delegated and EPA's fee has been suspended because EPA incurs no administrative costs). In such cases, the delegate agency will instruct you on how to calculate fees and how to pay them. If in doubt, contact your permitting authority.

#### General Rules for Fee Calculation under Part 71:

- Use the fee rate in effect at the time you pay the fee regardless of the time period that the emissions data represents. For example, if the annual fee for the current year is due July 1, you would use the fee rate in effect for the current year and the actual emissions for the previous calendar year.
- Do not prorate initial or annual fees. Pay full fees for the entire calendar year regardless of how many days you operated or were subject to the program during the previous or current year.
- Do not hesitate to contact the permitting authority if you have any doubt about how to calculate fees, especially if you have an unusual set of circumstances not addressed specifically by these forms or whenever the permit requirements appear to conflict with these forms (however, always assume the permit requirements take precedence in such cases).

### Section A. General Information

The deadline for submitting the fee form and paying the fee for initial fee payment purposes for most sources is the same deadline as for submitting all other forms required for the initial permit application. Other deadlines apply for initial fee payment in certain limited circumstances:

- When a source is subject to part 71 because of an unresolved EPA objection to a part 70 permit, fees are not due with the part 71 application, but are due 3 months following the date of the issuance of the part 71 permit.
- When EPA withdraws approval of a part 70 program and implements a part 71 programs, fees are submitted according to a schedule based on the source's SIC code (within 6 to 9 months of the effective date of the part 71 program).

The deadline for submitting the fee form and paying the fee for annual fee payment purposes is the anniversary date of initial fee payment. This is required whether or not a permit has been issued. If you were required to pay initial fees between January 1 and March 31, the regulations allow for submittal of annual fees no later than April 1.

Whether you are paying initial or annual fees see the instructions for sections D and E for more information on which calendar-year emission data to use (preceding or current year) and how to quantify such emissions (actual emissions or estimates of actual emissions).

### **Section B. Source Information**

Complete this section only if you are preparing this form for submittal at a different time than for the other portions of an initial application or for annual fee purposes.

### **Section C. Certification of Truth, Accuracy and Completeness**

This form and any other document required by a permit must be signed by a responsible official certifying truth, accuracy and completeness of the information. If you are submitting a separate **CTAC** form, there is no need to complete this section of the form. If you complete this section, there is no need to submit form **CTAC** separately.

### **Section D. Annual Emissions Report for Fee Calculation Purposes – Non-HAP**

Calculate actual emissions of regulated pollutants (for fee calculation), except for HAP, on a calendar-year basis for the facility in this section. Section E is provided to report actual emissions of HAP. Note the phrase "regulated pollutant (for fee calculation)" is any "regulated air pollutant" except carbon monoxide (CO), and pollutants regulated solely because they are: 1) subject to regulation under section 112(r) of the Act, or 2) a class I or II substance under title VI of the Act. **Note that GHG emissions are not counted for fee purposes.**

If more than one year of data is being submitted with the fee calculation worksheet, copy this page and complete a separate table for each year. If you are submitting an initial application, you may use emissions data already reported on form **EMISS**, provided this is the same data you would otherwise report in sections D and E of this form. If using **EMISS** in this manner, please note this on the fee calculation form. Also, sources must submit attachments to this form to show (at a minimum) examples of the calculations used to determine these values.

Show actual emissions for each listed air pollutant for each emission unit. Values should be reported to the nearest tenth (0.1) of a ton.

The column for "other" is for other regulated pollutants (for fee calculation) not already listed on the form. Write in the name of the pollutant in the proximity of the "other" column. If more than one such pollutant, show the pollutants, and the totals on an attachment.

Actual emissions must be calculated using actual operating hours, production rates, in-place control equipment, and types of materials processed, stored, or combusted over the preceding calendar year. Sources that have been issued title V permits are required to compute actual emissions using compliance methods required by the permits, such as monitoring or source testing data. If this is not possible, actual emissions should be determined using other federally recognized procedures.

For initial fee calculation purposes, most sources are required to use actual emissions for the preceding calendar year. However, there are certain exceptions where estimates of actual emissions are either required or allowed in place of actual emissions for the preceding calendar year (see table below):

| Exception  | Emission Data   |
|--|---|
| When the source commenced operation during the preceding calendar year.  | Estimates of actual emissions for the "current" calendar year are required  |
| When EPA withdraws approval of a part 70 program and implements a part 71 program, and the source pays initial part 71 fees between January 1 and March                        | Either estimates of actual emissions for the "preceding" calendar year or actual emissions for the preceding calendar year may be used. |
| When a part 71 permit was issued following an unresolved objection to a part 70 permit, and the source is required to pay initial part 71 fees between January 1 and March 31. | Either estimates of actual emissions for the "preceding" calendar year or actual emissions for the preceding calendar year may be used. |

For annual fee purposes, fee calculation should be based on actual emissions for the preceding calendar year in all cases.

In most cases you will only need to report one set of emission data using sections D and E of this form (the data that is the basis of the initial or annual fee being paid as explained above). This data is subsequently carried over to lines 1 and 2 of section F (Fee Calculation Worksheet) of the form.

However, there is one exception where you would be required to report two different sets of emissions data using sections D and E – when paying the first annual fee and reconciliation is required because the initial fee was based on estimated actual emissions for the "preceding" calendar year (the year preceding initial fee payment). In this case, the two data sets would be:

- actual emissions for the year initial fees paid (for annual fee purposes in lines 1-5 of section F of the form), and
- actual emissions for the year preceding initial fee payment (for reconciliation in lines 11-20 of the form)

Whenever reconciliation is required as part of annual fee payment, you will also need a copy of the fee forms you previously submitted with initial fee payment in order to obtain the value of estimated actual emissions.

Include all fugitive emissions in the calculation of actual emissions, including those that do not count for applicability. Do not include any insignificant emissions identified on form IE.

The subtotal line in section D of the form is provided at the bottom of each column to enter total emissions for each pollutant reported above. Each subtotal should be reported to the nearest tenth (0.1) of a ton. If any subtotal exceeds 4,000 tons, enter 4,000 tons for that column.

Any necessary adjustments for double counting of emissions will be performed later in section F.

#### **Section E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

List the actual emissions of individual HAP from each emission unit. If you are initially applying for a permit, you may use the emissions of HAP reported on form **EMISS**, instead of completing this section of this form, provided these emissions are the same as you would otherwise report using this section of the form. If you are doing this, please note it on the form.

This section is composed of two tables. The first table is to identify individual HAP emitted at each emission unit. Assign a unique identifier for use in the second table. Please use "HAP1" for the first

one, "HAP2" for the second one, and so on. The second table is to calculate the actual emission of individual HAP at each emission unit. Use the identifiers assigned in the first table to label the column headers for the second table. You may round and report these emissions to the nearest tenth (0.1) of a ton. Sum the values in each column and enter the subtotals at the bottom of the table. If any subtotal exceeds 4,000 tons, enter 4,000 for that column.

See instructions for section D for more information on reporting emissions data.

### **Section F. Fee Calculation Worksheet**

This worksheet is used to sum the total tons of actual emissions subject to fees, adjust for double counting of emissions, perform certain reconciliations for underpayment and overpayment of fees and adjust for fee assessment errors, if needed, and ultimately to determine the total fee to be paid.

A detailed explanation of Section F follows (separated into six parts):

#### **Emissions Summary**

The subtotals for each pollutant listed in Sections D and E (or from form **EMISS**) are added together to calculate the total emissions (in tons per year) for the facility.

The emissions that are reported here will vary for initial fee payment purposes, depending on the specific circumstances, but will always be actual emissions for the preceding calendar year for annual fee purposes. See the instructions for section D for more on the emissions data you should use in the part of the form.

The total emissions are adjusted for double counting and are rounded to the nearest ton. For example, double counting may occur where a pollutant is defined as HAP and VOC. If you adjust for double counting, attach an explanation for this.

#### **Reconciliation (When Initial Emission Fees Were Based on Estimates for the Current Calendar Year)**

This section is only used by sources paying their first annual fee when their initial fee was based on estimates of calendar-year emissions for the "current" year (the same year that initial fees were paid). This reconciliation is done by comparing the actual emissions for the "current" year provided in sections D and E of this submittal with the estimate of those emissions previously provided with initial fee payment. There may have been overpayment or underpayment of the initial fee. The fee you are paying now will be adjusted for this difference later.

#### **Reconciliation (When Initial Emission Fees Were Based on Estimates for the Preceding Calendar Year)**

This section is only used by sources paying their first annual fee when their initial fee was based on estimates of calendar-year emissions for the year preceding initial fee payment, provided the source was required to pay its initial fee between January 1 and March 31, and EPA issued the Part 71 permit to replace a Part 70 permit. This reconciliation is done by comparing the actual emissions for the "preceding" year provided in sections D and E of this submittal with the estimate of those emissions provided with initial fee payment. There may have been overpayment or underpayment of the initial fee. The fee you are paying now will be adjusted for this difference later.

## **Emission Fee Calculation**

Calculate the emission-based fee using the emissions from line 5 (tons) multiplied by the fee rate (\$/ton) in effect at the time the fee is paid.

## **GHG Fee Adjustment**

The part 71 rule was amended in 2015 to require the fees to be increased by a GHG fee adjustment. The GHG adjustment must be calculated by each source that is required to pay fees. The adjustment is based on the burden for the permitting authority to conduct certain GHG evaluations or reviews related to the source, rather than on emissions. Set fees are charged for certain activities that have occurred at the source since the last time fees were paid. For an initial application, the set fee is a one-time charge that includes the costs of processing application updates. The term "permit modification" refers to any significant and minor modifications, but not to administrative amendments. The number of permit modifications must be multiplied by the set fee for modifications to determine the total GHG adjustment for modifications. The set fee for a permit renewal also includes any permit modifications that may be processed at the same time as the renewal. Note that you may need to check with the permitting authority to determine if they are holding any permit modification requests you have submitted for processing with an upcoming permit renewal.

## **Other Adjustments**

The purpose of this section is to adjust the emissions-based to determine the total fee (after adjustments) that is due to the EPA. The emissions fee determined on line 21 is adjusted by the GHG fee adjustment, any amounts of overpayment or underpayment related to a previous fee submittal, and to correct for any fee assessment errors.

Fee assessment errors occur when the permitting authority determines that the source has calculated the fee incorrectly. If this occurs, you will be notified of the error. Any overpayment will be credited against the next fee owed. In the case of underpayment, you will be billed for the corrected fee and you will have 30 days to remit the amount. If you think the assessed fee is in error, you may submit a written explanation of the alleged error, but you must pay the fee. The permitting authority will provide a determination in 90 days. If the assessment of underpayment is in error, your account will be credited.

## **Fee Payment**

See form FF (the Fee Filing form) for instructions on how to make fee payment to the EPA.

## **Penalties and Interest**

The permitting authority will bill sources for appropriate penalties and interest for late payment or excessive underpayment of fees. Interest will be assessed on payments received later than the due date. Penalties shall be assessed if payment is not paid within 30 days of the due date. For sources issued with issued permits, penalties and interest shall be assessed for excessive underpayment of the annual fee amount.

**END**



# Harvest Midstream Company

P.O. Box 61229  
Houston TX 77208-1229



| Owner:    | 1070478   | Check Date:                         | 07/16/2019 | Check Number: | 0062048394 |
|-----------|-----------|-------------------------------------|------------|---------------|------------|
| Invoice # | Inv. Date | Description                         | Amount     | Discount      | Net Amount |
| 070119    | 7/1/2019  | PERMIT R6FOP-NM-04-R2 LOS MESTENIOS | \$3,807.60 | \$0.00        | \$3,807.60 |

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1005 CONVENTIONAL PLAZA

ST LOUIS MO 63101

*Colleen Elkins*

Authorized Signature

0062048394 113011258 53267652

|  |  |  |
|--|--|--|
| ORIGIN ID#FMAA (505) 634-4316<br>TRISTEN RUYBALD<br>HARVEST FOUR CORNERS, LLC<br>1755 ARROYO DRIVE<br>BLOOMFIELD, NM 87413<br>UNITED STATES US                 |  | SHIP DATE: 19 JUL 19<br>ACTWGT: 0.50 LB<br>CAD: 113465079/INET4160 |
| TO AIR & RADIATION DIV/AIR PERMITS SEC<br>US EPA REGION-6, ARPE<br>1201 ELM STREET<br>SUITE 500<br>DALLAS TX 75270<br>(000) 000-0000<br>INV. REF:<br>PO. DEPT: |  | BILL SENDER  |

|  |  |
|--|--|
| TRK# 7757 8927 2381<br>0201<br>XH KIPA<br>TX-US DFW<br>75270 | MON - 22 JUL 3:00P<br>STANDARD OVERNIGHT |
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Tristen Ruybalid

---

From: TrackingUpdates@fedex.com  
Sent: Monday, July 22, 2019 9:05 AM  
To: Tristen Ruybalid  
Subject: [EXTERNAL] FedEx Shipment 775789272381 Delivered

## Your package has been delivered

Tracking # 775789272381

Ship date:

**Fri, 7/19/2019**

**Tristen Ruybalid**

Harvest Four Corners, LLC

Bloomfield, NM 87413

US

Delivery date:

**Mon, 7/22/2019 9:57  
am**

**Air & Radiation Div/Air**

**Permits Sec**

US EPA Region-6, ARPE

1201 Elm Street

Suite 500

DALLAS, TX 75270

US



### Personalized Message

E&H Receiver & Los Mestenios TV Part 71 Annual Fees

### Shipment Facts

Our records indicate that the following package has been delivered.

**Tracking number:** [775789272381](#)

**Status:** Delivered: 07/22/2019 09:57  
AM Signed for By: G.GRIBBS

**Signed for by:** G.GRIBBS

**Delivery location:** DALLAS, TX

**Delivered to:** Guard/Security Station

**Service type:** FedEx Standard Overnight®

**Packaging type:** FedEx® Envelope

**Number of pieces:** 1

**Weight:** 0.50 lb.





**Special handling/Services:** Deliver Weekday

**Standard transit:** 7/22/2019 by 3:00 pm


---

**This tracking update has been requested by:**

**Company name:** Harvest Four Corners, LLC

**Name:** Tristen Ruybalid

**Email:** truybalid@harvestmidstream.com

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All weights are estimated.

To track the latest status of your shipment, click on the tracking number above.

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Thank you for your business.



1755 Arroyo Drive  
Bloomfield, NM 87413  
Phone 505-632-4600  
Fax 505-632-4682  
harvestmidstream.com

July 17, 2019

U.S. Bank  
Government Lockbox 979078  
US EPA FOIA & Misc. Payments  
1005 Convention Plaza  
SL-MO-C2-GL  
St. Louis, MO 63101

re: Title V Part 71 Annual Fee - 2018  
Permit R6FOP-NM-04-R2 – Los Mestenos Compressor Station

Dear Madam/Sir,

In accordance with condition 5.1 of the Part 71 operating permit number R6FOP-NM-04-R2 for Harvest Four Corners LLC's Los Mestenos Compressor Station, please find enclosed the Form FEE – Fee Calculation Worksheet for pollutants emitted during the calendar year 2018, and Form FF for the filing of payment for these emissions. Also enclosed is check number 0062048394 in the amount of \$3,807.60 for the annual permit fee for operations during calendar year 2018.

If you have any questions, please call me at (505) 632-4625 or Bobby Myers of Cirrus Consulting at (801) 484-4412.

Sincerely,

Monica Smith  
Environmental Specialist

Attachments

**Federal Operating Permit Program (40 CFR Part 71)  
FEE FILING FORM (FF)**

The purpose of this form is to ensure that fee payments made by check are credited to the proper facility and to the proper government account. Send this form, along with form FEE and the check, to the appropriate lockbox bank address listed on the following page. This form is required whenever you pay by check, including for initial and annual fee payments. Part 71 fees may be paid by check or electronically, and further information on making payments by check or electronically is provided on the following page.

Source or Facility Name \_Harvest Four Corners, LLC's Los Mestenos Compressor Station\_

Source Location \_Rio Arriba County, New Mexico\_

EPA Region where Source Located \_Region 6\_

**Mailing Address:**

Street/P.O. Box \_1755 Arroyo Drive\_

City \_Bloomfield\_

State \_NM\_ ZIP \_87413\_ -     

Contact Person: \_Monica Smith\_

Title \_Environmental Specialist\_

Telephone ( \_505\_ ) \_632\_ - \_4625\_ Ext.     

**Total Fee Payment Remitted: \$ \_3807.60\_**



# Harvest Midstream Company

P.O. Box 61229  
Houston TX 77208-1229

| Owner:    | 1070478   | Check Date:                         | 07/16/2019 | Check Number: | 0062048394 |
|-----------|-----------|-------------------------------------|------------|---------------|------------|
| Invoice # | Inv. Date | Description                         | Amount     | Discount      | Net Amount |
| 070119    | 7/1/2019  | PERMIT R6FOP-NM-04-R2 LOS MESTENIOS | \$3,807.60 | \$0.00        | \$3,807.60 |

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| Check No   | Check Date | Check Amount    |
|------------|------------|-----------------|
| 0062048394 | 7/16/2019  | *****\$3,807.60 |

PAY

Three Thousand Eight Hundred Seven Dollars and Sixty Cents

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THE  
ORDER  
OF

US ENVIRONMENTAL PROTECTION AGENCY  
GOVERNMENT LOCKBOX 979078  
1005 CONVENTIONAL PLAZA

ST LOUIS MO 63101

*Colleen Elkins*

Authorized Signature

0062048394 113011258 53267652

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|------------------------------------|--|
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| <b>Security Screen:</b>            | Absence of "Original Document" Verbiage on back of check                     |
| <b>Micro-Printing - "MP"</b>       | Small type under endorsement area and surrounding                            |
| <b>Chemically Sensitive Paper:</b> | Fullback Security box appears blurred if copied or scanned.                  |
| <b>Fluorescent Fibers:</b>         | High Polarity Solvents, Low Polarity Solvents, Oxidizing Acids and Alkalies. |
| <b>Visible Fibers:</b>             | Appearance of brown and/or blue stains may indicate alterations.             |
| <b>Fourdrinier Watermark:</b>      | Invisible unless exposed to ultraviolet light.                               |
|                                    | Absence of visible red and/or blue fibers may indicate alteration.           |
|                                    | True watermark visible from both sides, absence indicates alteration.        |



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| TO <b>US EPA FOIA &amp; MISC. PAYMENTS</b><br><b>U.S. BANK GOVERNMENT LOCKBOX 979078</b><br><b>1005 CONVENTION PLAZA</b><br><b>SL-MO-C2-GL</b><br><b>ST. LOUIS MO 63101</b><br>(000) 000-0000 |          | BILL SENDER<br>UNITED STATES US                                    |
| REF: DEPT:  | PO: INV: |  |

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|                                      |   |
|--------------------------------------|---|
| <b>XX CPSA</b><br>MO-US STL<br>63101 |  |
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567.J2/A6F9.05A2

**After printing this label:**

1. Use the 'Print' button on this page to print your label to your laser or inkjet printer.
2. Fold the printed page along the horizontal line.
3. Place label in shipping pouch and affix it to your shipment so that the barcode portion of the label can be read and scanned.

**Warning:** Use only the printed original label for shipping. Using a photocopy of this label for shipping purposes is fraudulent and could result in additional billing charges, along with the cancellation of your FedEx account number.

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Tristen Ruybalid

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From: TrackingUpdates@fedex.com  
Sent: Monday, July 22, 2019 8:48 AM  
To: Tristen Ruybalid  
Subject: [EXTERNAL] FedEx Shipment 775789389791 Delivered

## Your package has been delivered

Tracking # 775789389791

Ship date:

**Fri, 7/19/2019**

**Tristen Ruybalid**

Harvest Four Corners, LLC

Bloomfield, NM 87413

US

Delivery date:

**Mon, 7/22/2019 9:40 am**

**US EPA FOIA & Misc.**

**Payments**

U.S. Bank Government

Lockbox 979078

1005 Convention Plaza

SL-MO-C2-GL

SAINT LOUIS, MO 63101

US



### Personalized Message

Los Mestenos TV Part 71 Annual Fee Payment

### Shipment Facts

Our records indicate that the following package has been delivered.

**Tracking number:** [775789389791](#)

**Status:** Delivered: 07/22/2019 09:40 AM  
Signed for By: P.PATTERSON

**Signed for by:** P.PATTERSON

**Delivery location:** ST. LOUIS, MO

**Delivered to:** Mailroom

**Service type:** FedEx Standard Overnight®

**Packaging type:** FedEx® Envelope




|                                   |                      |
|-----------------------------------|----------------------|
| <b>Number of pieces:</b>          | 1                    |
| <b>Weight:</b>                    | 0.50 lb.             |
| <b>Special handling/Services:</b> | Deliver Weekday      |
| <b>Standard transit:</b>          | 7/22/2019 by 3:00 pm |

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**This tracking update has been requested by:**

**Company name:** Harvest Four Corners, LLC  
**Name:** Tristen Ruybalid  
**Email:** truybalid@harvestmidstream.com

 Please do not respond to this message. This email was sent from an unattended mailbox. This report was generated at approximately 9:48 AM CDT on 07/22/2019.

All weights are estimated.

To track the latest status of your shipment, click on the tracking number above.

This tracking update has been sent to you by FedEx on behalf of the Requestor truybalid@harvestmidstream.com. FedEx does not validate the authenticity of the requestor and does not validate, guarantee or warrant the authenticity of the request, the requestor's message, or the accuracy of this tracking update.

Standard transit is the date and time the package is scheduled to be delivered by, based on the selected service, destination and ship date. Limitations and exceptions may apply. Please see the FedEx Service Guide for terms and conditions of service, including the FedEx Money-Back Guarantee, or contact your FedEx Customer Support representative.

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Thank you for your business.





1755 Arroyo Drive  
Bloomfield, NM 87413  
Phone 505-632-4600  
Fax 505-632-4682  
harvestmidstream.com

March 12, 2020

U.S. EPA, Region 6  
Air and Radiation Division Air Permits Section (ARPE)  
1201 Elm Street, Suite 500  
Dallas, TX 75270

re: Title V Part 71 Annual Fee Form FEE - 2019  
Permit R6FOP-NM-04-R2 – Los Mestenos Compressor Station

Dear Madam/Sir,

In accordance with condition 4.15 of the Part 71 operating permit number R6FOP-NM-04-R2 for Harvest Four Corners LLC's Los Mestenos Compressor Station, please find enclosed the Form FEE – Fee Calculation Worksheet, for the quantification for pollutants emitted during the calendar year 2019. Also enclosed is a photocopy of check number 0062053521-in the amount of \$2,071.69 for the annual operating permit fee.

If you have any questions, please call me at (505) 632-4625 or Bobby Myers of Cirrus Consulting at (801) 484-4412.

Sincerely,

Monica Smith  
Environmental Specialist

Attachments

**Federal Operating Permit Program (40 CFR Part 71)  
FEE CALCULATION WORKSHEET (FEE)**

Use this form initially, or thereafter on an annual basis, to calculate part 71 fees.

**A. General Information**

Type of fee (Check one): ☐ Initial ☒ Annual

Deadline for submitting fee calculation worksheet 04 / 01 / 2020

For initial fees, emissions are based on (Check one):

☒ Actual emissions for the preceding calendar year. (Required in most circumstances.)

☐ Estimates of actual emissions for the current calendar year. (Required when operations commenced during the preceding calendar year.)

Date commenced operations      /      /     

☐ Estimates of actual emissions for the preceding calendar year. (Optional after a part 71 permit was issued to replace a part 70 permit, but only if initial fee payment is due between January 1 and March 31; otherwise use actual emissions for the preceding calendar year.)

For annual fee payment, you are required to use actual emissions for the preceding calendar year.

**B. Source Information:** Complete this section only if you are paying fees but not applying for a permit.

Source or facility name Harvest Four Corners, LLC's Los Mestenos Compressor Station

Mailing address: Street or P.O. Box 1755 Arroyo Drive

City: Bloomfield State: NM ZIP 87413 -     

Contact person: Monica Smith Title: Environmental Specialist

Telephone (505) 632 - 4625 Ext      Part 71 permit no. R6FOP-NM-04-R2

**C. Certification of Truth, Accuracy and Completeness:** Only needed if not submitting a separate form CTAC.

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in this submittal (form and attachments) are true, accurate and complete.

Name (signed) 

Name (typed) Travis Jones Date: 3 / 3 / 2020

**D. Annual Emissions Report for Fee Calculation Purposes -- Non-HAP**

You may use this to report actual emissions (tons per year) of regulated pollutants (for fee calculation) on a calendar-year basis for both initial and annual fee calculation purposes. Section E is designed to report HAP emissions. Quantify all actual emissions, including fugitives, but do not include insignificant emissions and certain regulated air pollutants that are not counted for fee purposes, such as CO and GHGs (see instructions). Sum the emissions in each column to calculate subtotals. Subtotals should be reported to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000 for that column.

This data is for 2019 (year)

| Emission Unit ID  | NOx  | VOC  | SO2 | PM10 | Lead | Other |
|-------------------|------|------|-----|------|------|-------|
| 1                 | 14.8 | 0.4  |     |      |      |       |
| 2                 | 0.0  | 0.0  |     |      |      |       |
| Tk-1              |      | 19.3 |     |      |      |       |
| F-1               |      | 0.5  |     |      |      |       |
|                   |      | 3.5  |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
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|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
| <b>SUBTOTALS:</b> | 14.8 | 23.7 |     |      |      |       |

**E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

**HAP Identification.** Identify individual HAP emitted at the facility, identify the CAS number, and assign a unique identifier for use in the second table in this section. Whenever assigning identifier codes, use "HAP1" for the first, "HAP2" for the second, and so on.

| Name of HAP  | CAS No    | Identifier   |
|--------------|-----------|--------------|
| Acetaldehyde | 75-07-0   | HAP <u>1</u> |
| Formaldehyde | 50-00-0   | HAP <u>2</u> |
| Benzene      | 71-43-2   | HAP <u>3</u> |
| Toluene      | 108-88-3  | HAP <u>4</u> |
| Ethylbenzene | 100-41-4  | HAP <u>5</u> |
| Xylenes      | 1330-20-7 | HAP <u>6</u> |
| n-Hexane     | 110-54-3  | HAP <u>7</u> |

**HAP Emissions.** Report the actual emissions of individual HAP identified above. Use the identifiers assigned in the table above. Include all emissions, including fugitives, and do not include insignificant emissions. Sum the emissions in each column to calculate subtotals. Report subtotals to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000.

This data is for 2019 (year)

| Emissions Unit ID | Actual Emissions (Tons/Year) |        |        |        |        |        |        |       |
|-------------------|------------------------------|--------|--------|--------|--------|--------|--------|-------|
|                   | HAP_1_                       | HAP_2_ | HAP_3_ | HAP_4_ | HAP_5_ | HAP_6_ | HAP_7_ | HAP__ |
| 1                 | 0.2                          | 0.3    |        |        |        |        |        |       |
| 2                 | 0.0                          | 0.0    |        |        |        |        |        |       |
| Tk-1              |                              |        | 0.1    | 0.1    | 0      | 0      | 1.4    |       |
| F-1               |                              |        |        |        |        |        | 0.1    |       |
|                   |                              |        |        |        |        |        |        |       |
|                   |                              |        |        |        |        |        |        |       |
|                   |                              |        |        |        |        |        |        |       |
| <b>SUBTOTALS:</b> | 0.2                          | 0.3    | 0.1    | 0.1    | 0      | 0      | 1.5    | 2.2   |

## F. Fee Calculation Worksheet

This worksheet is used to calculate the total fee owed (including the emissions-based fee and the GHG fee adjustment) for both initial and annual fee payment purposes. Reconciliation is only for cases where you are paying the annual fee and you used any type of estimate of actual emissions when you calculated the initial fee. If you do not need to reconcile fees, complete line 1-5 (emissions summary) and then skip down to line 21 (emission calculation). See instructions for more detailed explanation.

### EMISSIONS SUMMARY

|  |      |
|--|------|
| 1. Sum the subtotals from section D of this form (non-HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 38.5 |
| 2. Sum the subtotals from section E of this form (HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 2.1  |
| 3. Sum lines 1 and 2.  | 40.6 |
| 4. Enter the emissions that were counted twice. If none, enter "0."  | 2.1  |
| 5. Subtract line 4 from line 3, round to the nearest ton, and enter the result here. This is the <b>total emissions</b> that count for fees purposes.  | 38.5 |
| <p style="text-align: center;"><b>RECONCILIATION</b><br/> <b>(WHEN INITIAL FEES WERE BASED ON ESTIMATES</b><br/> <b>FOR THE "CURRENT" CALENDAR YEAR)</b></p> <p>Only complete lines 6-10 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year in which you paid initial fees; otherwise skip to line 11 or to line 21.</p> |      |
| 6. Enter the total estimated actual emissions for the year the initial fee was paid (previously reported on line 5 of the initial fee form).   |      |
| 7. If line 5 is greater than line 6, subtract line 6 from line 5, and enter the result. Otherwise enter "0."   |      |
| 8. If line 6 is greater than line 5, subtract line 5 from line 6, and enter the result. Otherwise enter "0."   |      |
| 9. If line 7 is greater than 0, multiply line 7 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment. Go to line 21.   |      |
| 10. If line 8 is greater than 0, multiply line 8 by last year's fee rate (\$/ton) and enter the result here. This is the overpayment. Go to line 21.   |      |

**RECONCILIATION  
(WHEN INITIAL FEES WERE BASED ON ESTIMATES  
FOR THE "PRECEDING" CALENDAR YEAR)**

Only complete lines 11-20 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year preceding initial fee payment; otherwise skip to line 21. If completing this section, you will also need to complete sections D and E to report actual emissions for the calendar year preceding initial fee payment.

|   |  |
|---|--|
| 11. Sum the actual emissions from section D (non-HAP) for the calendar year preceding initial fee payment and enter the result here.  |  |
| 12. Sum the actual emissions from section E (HAP) for the calendar year preceding initial fee payment and enter the result here.  |  |
| 13. Add lines 11 and 12 and enter the total here. These are total actual emissions for the calendar year preceding initial fee payment.   |  |
| 14. Enter double counted emission from line 13 here. If none, enter "0."  |  |
| 15. Subtract line 14 from line 13, round to the nearest ton, and enter the result here.   |  |
| 16. Enter the total estimated actual emissions previously reported on line 5 of the initial fee form. These are estimated actual emissions for the calendar year preceding initial fee payment. |  |
| 17. If line 15 is greater than line 16, subtract line 16 from line 15, and enter the result here. Otherwise enter "0."  |  |
| 18. If line 16 is greater than line 15, subtract line 15 from line 16, and enter the result here. Otherwise enter "0."  |  |
| 19. If line 17 is greater than 0, multiply line 17 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment.  |  |
| 20. If line 18 is greater than 0, multiply line 18 by last year's fee rate (\$/ton) and enter the result on this line. This is the overpayment.   |  |

**EMISSION FEE CALCULATION**

|  |           |
|--|-----------|
| 21. Multiply line 5 (tons) by the current fee rate (\$/ton) and enter the result here. This is the unadjusted emissions fee. Continue on to line 23. | \$2071.69 |
|--|-----------|

**GHG FEE ADJUSTMENT**

|  |   |
|--|---|
| 22. If you are submitting an initial permit application and this is the first time you are paying fees, enter \$2,236, otherwise enter "0". [Note that any updates to the initial application are covered under this one-time charge.] | 0 |
| 23. Enter the number of permit modifications (or related permit actions) you have submitted to the permitting authority since you last paid fees. If none, skip to line 25.  | 0 |
| 24. Multiply the number in line 23 by \$365 and enter the result.  | 0 |

|  |           |
|--|-----------|
| 25. If you have submitted a permit renewal application since the last time you paid fees enter \$520, otherwise enter "0"  | 0         |
| 26. Sum line 22, 24, and 25 and enter the result. This is the GHG fee adjustment   | 0         |
| <b>OTHER ADJUSTMENTS</b>   |           |
| 27. Add the total on line 21 and the total on line 26 and enter the result.  | \$2071.69 |
| 28. Enter any underpayment from line 9 or 19 here. Otherwise enter "0."  | 0         |
| 29. Enter any overpayment from line 10 or 20 here. Otherwise enter "0."  | 0         |
| 30. If line 28 is greater than "0," add it to line 27 and enter the result here. If line 29 is greater than "0," subtract this from line 27 and enter the result here. Otherwise enter the amount on line 27 here. This is the fee adjusted for over/underpayment. | \$2071.69 |
| 31. Enter any credit for fee assessment error here. Otherwise, enter "0."  | 0         |
| 32. Subtract line 31 from line 30 and enter the result here. Stop here. This is the <b>TOTAL FEE (AFTER ADJUSTMENTS)</b> that you must remit to EPA.   | \$2071.69 |

## INSTRUCTIONS FOR FEE FEE CALCULATION WORKSHEET

### Information Collection Burden Estimates

The public reporting and recordkeeping burden for this collection of information is estimated to average 247 hours per respondent per year. Send comments on the Agency's need for this information, the accuracy of the provided burden estimates, and any suggested methods for minimizing respondent burden, including through the use of automated collection techniques to the Director, Collection Strategies Division, U.S. Environmental Protection Agency (2822T), 1200 Pennsylvania Ave., NW, Washington, D.C. 20460. Include the OMB control number in any correspondence. Do not send the completed form to this address.

### DETAILED INSTRUCTIONS

Use this form to initially or annually calculate fees. This form is for paying fees to EPA or a delegate agency (such as a State or tribe) under a part 71 operating permit program. The requirements for paying fees under part 71 programs, as well as the forms and instructions contained herein, are based on the requirements of 40 CFR 71.9

There may be cases, under a part 71 program, when you are not required to complete this form or pay the EPA fee rate (where the part 71 program has been delegated and EPA's fee has been suspended because EPA incurs no administrative costs). In such cases, the delegate agency will instruct you on how to calculate fees and how to pay them. If in doubt, contact your permitting authority.

#### General Rules for Fee Calculation under Part 71:

- Use the fee rate in effect at the time you pay the fee regardless of the time period that the emissions data represents. For example, if the annual fee for the current year is due July 1, you would use the fee rate in effect for the current year and the actual emissions for the previous calendar year.
- Do not prorate initial or annual fees. Pay full fees for the entire calendar year regardless of how many days you operated or were subject to the program during the previous or current year.
- Do not hesitate to contact the permitting authority if you have any doubt about how to calculate fees, especially if you have an unusual set of circumstances not addressed specifically by these forms or whenever the permit requirements appear to conflict with these forms (however, always assume the permit requirements take precedence in such cases).

### Section A. General Information

The deadline for submitting the fee form and paying the fee for initial fee payment purposes for most sources is the same deadline as for submitting all other forms required for the initial permit application. Other deadlines apply for initial fee payment in certain limited circumstances:

- When a source is subject to part 71 because of an unresolved EPA objection to a part 70 permit, fees are not due with the part 71 application, but are due 3 months following the date of the issuance of the part 71 permit.
- When EPA withdraws approval of a part 70 program and implements a part 71 program, fees are submitted according to a schedule based on the source's SIC code (within 6 to 9 months of the effective date of the part 71 program).

The deadline for submitting the fee form and paying the fee for annual fee payment purposes is the anniversary date of initial fee payment. This is required whether or not a permit has been issued. If you were required to pay initial fees between January 1 and March 31, the regulations allow for submittal of annual fees no later than April 1.



Whether you are paying initial or annual fees see the instructions for sections D and E for more information on which calendar-year emission data to use (preceding or current year) and how to quantify such emissions (actual emissions or estimates of actual emissions).

### **Section B. Source Information**

Complete this section only if you are preparing this form for submittal at a different time than for the other portions of an initial application or for annual fee purposes.

### **Section C. Certification of Truth, Accuracy and Completeness**

This form and any other document required by a permit must be signed by a responsible official certifying truth, accuracy and completeness of the information. If you are submitting a separate CTAC form, there is no need to complete this section of the form. If you complete this section, there is no need to submit form CTAC separately.

### **Section D. Annual Emissions Report for Fee Calculation Purposes – Non-HAP**

Calculate actual emissions of regulated pollutants (for fee calculation), except for HAP, on a calendar-year basis for the facility in this section. Section E is provided to report actual emissions of HAP. Note the phrase "regulated pollutant (for fee calculation)" is any "regulated air pollutant" except carbon monoxide (CO), and pollutants regulated solely because they are: 1) subject to regulation under section 112(r) of the Act, or 2) a class I or II substance under title VI of the Act. **Note that GHG emissions are not counted for fee purposes.**

If more than one year of data is being submitted with the fee calculation worksheet, copy this page and complete a separate table for each year. If you are submitting an initial application, you may use emissions data already reported on form **EMISS**, provided this is the same data you would otherwise report in sections D and E of this form. If using **EMISS** in this manner, please note this on the fee calculation form. Also, sources must submit attachments to this form to show (at a minimum) examples of the calculations used to determine these values.

Show actual emissions for each listed air pollutant for each emission unit. Values should be reported to the nearest tenth (0.1) of a ton.

The column for "other" is for other regulated pollutants (for fee calculation) not already listed on the form. Write in the name of the pollutant in the proximity of the "other" column. If more than one such pollutant, show the pollutants, and the totals on an attachment.

Actual emissions must be calculated using actual operating hours, production rates, in-place control equipment, and types of materials processed, stored, or combusted over the preceding calendar year. Sources that have been issued title V permits are required to compute actual emissions using compliance methods required by the permits, such as monitoring or source testing data. If this is not possible, actual emissions should be determined using other federally recognized procedures.

For initial fee calculation purposes, most sources are required to use actual emissions for the preceding calendar year. However, there are certain exceptions where estimates of actual emissions are either required or allowed in place of actual emissions for the preceding calendar year (see table below):

| <b>Exception</b>   | <b>Emission Data</b>  |
|--|---|
| When the source commenced operation during the preceding calendar year.  | Estimates of actual emissions for the "current" calendar year are required  |
| When EPA withdraws approval of a part 70 program and implements a part 71 program, and the source pays initial part 71 fees between January 1 and March                        | Either estimates of actual emissions for the "preceding" calendar year or actual emissions for the preceding calendar year may be used. |
| When a part 71 permit was issued following an unresolved objection to a part 70 permit, and the source is required to pay initial part 71 fees between January 1 and March 31. | Either estimates of actual emissions for the "preceding" calendar year or actual emissions for the preceding calendar year may be used. |

For annual fee purposes, fee calculation should be based on actual emissions for the preceding calendar year in all cases.

In most cases you will only need to report one set of emission data using sections D and E of this form (the data that is the basis of the initial or annual fee being paid as explained above). This data is subsequently carried over to lines 1 and 2 of section F (Fee Calculation Worksheet) of the form.

However, there is one exception where you would be required to report two different sets of emissions data using sections D and E – when paying the first annual fee and reconciliation is required because the initial fee was based on estimated actual emissions for the "preceding" calendar year (the year preceding initial fee payment). In this case, the two data sets would be:

- actual emissions for the year initial fees paid (for annual fee purposes in lines 1-5 of section F of the form), and
- actual emissions for the year preceding initial fee payment (for reconciliation in lines 11-20 of the form)

Whenever reconciliation is required as part of annual fee payment, you will also need a copy of the fee forms you previously submitted with initial fee payment in order to obtain the value of estimated actual emissions.

Include all fugitive emissions in the calculation of actual emissions, including those that do not count for applicability. Do not include any insignificant emissions identified on form IE.

The subtotal line in section D of the form is provided at the bottom of each column to enter total emissions for each pollutant reported above. Each subtotal should be reported to the nearest tenth (0.1) of a ton. If any subtotal exceeds 4,000 tons, enter 4,000 tons for that column.

Any necessary adjustments for double counting of emissions will be performed later in section F.

### **Section E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

List the actual emissions of individual HAP from each emission unit. If you are initially applying for a permit, you may use the emissions of HAP reported on form **EMISS**, instead of completing this section of this form, provided these emissions are the same as you would otherwise report using this section of the form. If you are doing this, please note it on the form.

This section is composed of two tables. The first table is to identify individual HAP emitted at each emission unit. Assign a unique identifier for use in the second table. Please use "HAP1" for the first

one, "HAP2" for the second one, and so on. The second table is to calculate the actual emission of individual HAP at each emission unit. Use the identifiers assigned in the first table to label the column headers for the second table. You may round and report these emissions to the nearest tenth (0.1) of a ton. Sum the values in each column and enter the subtotals at the bottom of the table. If any subtotal exceeds 4,000 tons, enter 4,000 for that column.

See instructions for section D for more information on reporting emissions data.

### **Section F. Fee Calculation Worksheet**

This worksheet is used to sum the total tons of actual emissions subject to fees, adjust for double counting of emissions, perform certain reconciliations for underpayment and overpayment of fees and adjust for fee assessment errors, if needed, and ultimately to determine the total fee to be paid.

A detailed explanation of Section F follows (separated into six parts):

#### **Emissions Summary**

The subtotals for each pollutant listed in Sections D and E (or from form **EMISS**) are added together to calculate the total emissions (in tons per year) for the facility.

The emissions that are reported here will vary for initial fee payment purposes, depending on the specific circumstances, but will always be actual emissions for the preceding calendar year for annual fee purposes. See the instructions for section D for more on the emissions data you should use in the part of the form.

The total emissions are adjusted for double counting and are rounded to the nearest ton. For example, double counting may occur where a pollutant is defined as HAP and VOC. If you adjust for double counting, attach an explanation for this.

#### **Reconciliation (When Initial Emission Fees Were Based on Estimates for the Current Calendar Year)**

This section is only used by sources paying their first annual fee when their initial fee was based on estimates of calendar-year emissions for the "current" year (the same year that initial fees were paid). This reconciliation is done by comparing the actual emissions for the "current" year provided in sections D and E of this submittal with the estimate of those emissions previously provided with initial fee payment. There may have been overpayment or underpayment of the initial fee. The fee you are paying now will be adjusted for this difference later.

#### **Reconciliation (When Initial Emission Fees Were Based on Estimates for the Preceding Calendar Year)**

This section is only used by sources paying their first annual fee when their initial fee was based on estimates of calendar-year emissions for the year preceding initial fee payment, provided the source was required to pay its initial fee between January 1 and March 31, and EPA issued the Part 71 permit to replace a Part 70 permit. This reconciliation is done by comparing the actual emissions for the "preceding" year provided in sections D and E of this submittal with the estimate of those emissions provided with initial fee payment. There may have been overpayment or underpayment of the initial fee. The fee you are paying now will be adjusted for this difference later.

## **Emission Fee Calculation**

Calculate the emission-based fee using the emissions from line 5 (tons) multiplied by the fee rate (\$/ton) in effect at the time the fee is paid.

## **GHG Fee Adjustment**

The part 71 rule was amended in 2015 to require the fees to be increased by a GHG fee adjustment. The GHG adjustment must be calculated by each source that is required to pay fees. The adjustment is based on the burden for the permitting authority to conduct certain GHG evaluations or reviews related to the source, rather than on emissions. Set fees are charged for certain activities that have occurred at the source since the last time fees were paid. For an initial application, the set fee is a one-time charge that includes the costs of processing application updates. The term "permit modification" refers to any significant and minor modifications, but not to administrative amendments. The number of permit modifications must be multiplied by the set fee for modifications to determine the total GHG adjustment for modifications. The set fee for a permit renewal also includes any permit modifications that may be processed at the same time as the renewal. Note that you may need to check with the permitting authority to determine if they are holding any permit modification requests you have submitted for processing with an upcoming permit renewal.

## **Other Adjustments**

The purpose of this section is to adjust the emissions-based to determine the total fee (after adjustments) that is due to the EPA. The emissions fee determined on line 21 is adjusted by the GHG fee adjustment, any amounts of overpayment or underpayment related to a previous fee submittal, and to correct for any fee assessment errors.

Fee assessment errors occur when the permitting authority determines that the source has calculated the fee incorrectly. If this occurs, you will be notified of the error. Any overpayment will be credited against the next fee owed. In the case of underpayment, you will be billed for the corrected fee and you will have 30 days to remit the amount. If you think the assessed fee is in error, you may submit a written explanation of the alleged error, but you must pay the fee. The permitting authority will provide a determination in 90 days. If the assessment of underpayment is in error, your account will be credited.

## **Fee Payment**

See form FF (the Fee Filing form) for instructions on how to make fee payment to the EPA.

## **Penalties and Interest**

The permitting authority will bill sources for appropriate penalties and interest for late payment or excessive underpayment of fees. Interest will be assessed on payments received later than the due date. Penalties shall be assessed if payment is not paid within 30 days of the due date. For sources issued with issued permits, penalties and interest shall be assessed for excessive underpayment of the annual fee amount.

**END**



# Harvest Midstream Company

P.O. Box 61229  
Houston TX 77208-1229

|           |           |                                   |            |               |            |
|-----------|-----------|-----------------------------------|------------|---------------|------------|
| Owner:    | 1070478   | Check Date:                       | 03/10/2020 | Check Number: | 0062053521 |
| Invoice # | Inv. Date | Description                       | Amount     | Discount      | Net Amount |
| 030420    | 3/4/2020  | PART 71 FEE PAYMENT LOS MESTENIOS | \$2,071.69 | \$0.00        | \$2,071.69 |

PLEASE DETATCH AT PERFORATION BELOW

PLEASE DETATCH AT PERFORATION BELOW

THIS CHECK IS PRINTED ON CHEMICALLY REACTIVE PAPER THAT HAS VISIBLE FIBERS AND A WATERMARK – HOLD TO LIGHT TO VIEW

Harvest Midstream Company  
P.O. Box 61229  
Houston TX 77208-1229

AMEGY BANK

32-1125  
1130

Void After 90 Days

|            |            |                 |
|------------|------------|-----------------|
| Check No   | Check Date | Check Amount    |
| 0062053521 | 3/10/2020  | *****\$2,071.69 |

PAY *Two Thousand Seventy-One Dollars and Sixty-Nine Cents*

TO  
THE  
ORDER  
OF

US ENVIRONMENTAL PROTECTION AGENCY  
1300 PENNSYLVANIA AVE NW  
MAIL CODE 2733R  
WASHINGTON DC 20004

*Colleen Elkins*

Authorized Signature

0062053521 1130112581 53267652



|  |  |   |  |
|--|--|---|--|
| ORIGIN ID: FJNNA (505) 634-4316<br>TRISTEN RUYBALD<br>HARVEST FOUR CORNERS, LLC<br>1755 ARROYO DRIVE<br>BLOOMFIELD, NM 87413 |  | SHIP DATE: 13MAR20<br>ACTWTGT: 0.50 LB<br>CAD: 113465079/INET4220 |  |
| UNITED STATES US   |  | BILL SENDER   |  |
| <b>TO AIR &amp; RADIATION DIVAIR PERMITS SEC</b>   |  |   |  |
| <b>US EPA REGION-6, ARPE</b>   |  |   |  |
| <b>1201 ELM STREET</b>   |  |   |  |
| <b>SUITE 500</b>   |  |   |  |
| <b>DALLAS TX 75270</b>   |  |   |  |
| (000) 000-0000 REF:  |  | DEPT:   |  |
| PO:  |  | DEPT:   |  |




MON - 16 MAR 3:00P  
 STANDARD OVERNIGHT  
 75270  
 TX-US DFW

TRK# 7700 1481 3357  
 0201

**XH KIPA**


**After printing this label:**

1. Use the 'Print' button on this page to print your label to your laser or inkjet printer.
2. Fold the printed page along the horizontal line.
3. Place label in shipping pouch and affix it to your shipment so that the barcode portion of the label can be read and scanned.

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Use of this system constitutes your agreement to the service conditions in the current FedEx Service Guide, available on [fedex.com](http://fedex.com). FedEx will not be responsible for any claim in excess of \$100 per package, whether the result of loss, damage, delay, non-delivery, misdelivery, or misinformation, unless you declare a higher value, pay an additional charge, document your actual loss and file a timely claim. Limitations found in the current FedEx Service Guide apply. Your right to recover from FedEx for any loss, including intrinsic value of the package, loss of sales, income interest, profit, attorney's fees, costs, and other forms of damage whether direct, incidental, consequential, or special is limited to the greater of \$100 or the authorized declared value. Recovery cannot exceed actual documented loss. Maximum for items of extraordinary value is \$1,000, e.g. jewelry, precious metals, negotiable instruments and other items listed in our ServiceGuide. Written claims must be filed within strict time limits, see current FedEx Service Guide.

Kayleigh Ruybalid

---

From: TrackingUpdates@fedex.com  
Sent: Monday, March 16, 2020 8:30 AM  
To: Kayleigh Ruybalid  
Subject: [EXTERNAL] FedEx Shipment 770014813357 Delivered

## Your package has been delivered

Tracking # 770014813357

Ship date:

**Fri, 3/13/2020**

**Tristen Ruybalid**

Harvest Four Corners, LLC

Bloomfield, NM 87413

US

Delivery date:

**Mon, 3/16/2020 9:25 am**

**Air & Radiation Div**

**Permits Sec**

US EPA Region-6, ARPE

1201 Elm Street

Suite 500

DALLAS, TX 75270

US



### Personalized Message

Los Mestenos TV Part 71 Annual Fee Form FEE 2019

### Shipment Facts

Our records indicate that the following package has been delivered.

**Tracking number:** [770014813357](#)

**Status:** Delivered: 03/16/2020 09:25 AM  
Signed for By: S.MARTINEZ

**Signed for by:** S.MARTINEZ

**Delivery location:** DALLAS, TX

**Delivered to:** Guard/Security Station

**Service type:** FedEx Standard Overnight®

**Packaging type:** FedEx® Envelope

**Number of pieces:** 1




|                                   |                      |
|-----------------------------------|----------------------|
| <b>Weight:</b>                    | 0.50 lb.             |
| <b>Special handling/Services:</b> | Deliver Weekday      |
| <b>Standard transit:</b>          | 3/16/2020 by 3:00 pm |

---

### This tracking update has been requested by:

**Company name:** Harvest Four Corners, LLC  
**Name:** Tristen Ruybalid  
**Email:** truybalid@harvestmidstream.com

 Please do not respond to this message. This email was sent from an unattended mailbox. This report was generated at approximately 9:29 AM CDT on 03/16/2020.

All weights are estimated.

To track the latest status of your shipment, click on the tracking number above.

This tracking update has been sent to you by FedEx on behalf of the Requestor truybalid@harvestmidstream.com. FedEx does not validate the authenticity of the requestor and does not validate, guarantee or warrant the authenticity of the request, the requestor's message, or the accuracy of this tracking update.

Standard transit is the date and time the package is scheduled to be delivered by, based on the selected service, destination and ship date. Limitations and exceptions may apply. Please see the FedEx Service Guide for terms and conditions of service, including the FedEx Money-Back Guarantee, or contact your FedEx Customer Support representative.

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Thank you for your business.



## Kayleigh Ruybalid

---

**From:** Collier, Laura <collier.laura@epa.gov>  
**Sent:** Friday, November 6, 2020 8:40 AM  
**To:** Kayleigh Ruybalid; Church, Stacey  
**Cc:** Monica Smith  
**Subject:** [EXTERNAL] RE: Part 71 Fee Expired Check

Hello Kayleigh,

Please resubmit the check to the Cincinnati Finance Center (CFC) address below. Since our office has been teleworking due to the pandemic, initially we had not been receiving mail and were not able to process check payments. We have put interim procedures in place to have the CFC process checks for FCB. We apologize for any inconvenience you have experienced.

US EPA  
Cincinnati Finance Center  
1005 Convention Plaza  
Lockbox #979078  
St. Louis, MO 63101

Thank you

*Laura Collier*

*Lead Accountant*  
*Fees and Collections Branch*  
*Phone: 202-564-7593*  
*USEPA/OCFO/OC/ACAD/FCB*  
[OC SharePoint](#)

\*\*\*\*\*Privacy Act Notice\*\*\*\*\*

Information contained in this message may be subject to the Privacy Act (5 USC 522a) and should be treated accordingly.

---

**From:** Kayleigh Ruybalid <truybalid@harvestmidstream.com>  
**Sent:** Thursday, November 05, 2020 4:45 PM  
**To:** Church, Stacey <Church.Stacey@epa.gov>; Collier, Laura <collier.laura@epa.gov>  
**Cc:** Monica Smith <msmith@harvestmidstream.com>  
**Subject:** Part 71 Fee Expired Check

Hello,

We had submitted a Part 71 fee payment earlier this year in March to EPA, but our AP department alerted us that the check was never deposited by EPA.

We have a shipping confirmation that the check was delivered on 3/16/2020 to the following address:

Collections Team

US EPA OCFO/OC/ACAD/FCB  
1300 Pennsylvania Ave NW  
Mail Cod 2733R  
Washington, DC 20004

I have tried contacting both individuals copied on this e-mail and left voicemails, but have not received a response.

This check has been cancelled, but we will be happy to reissue and resubmit the payment if you would please provide where the check needs to be sent to ensure it is received and deposited in a timely manner.

Please advise at your earliest convenience.

Thank you,

**T. Kayleigh Ruybalid**  
EHS Compliance Administrator  
Harvest Midstream Company  
1755 Arroyo Drive | Bloomfield, NM | 87413  
O) 505-634-4316 | F) 505-632-4737  
[truybalid@harvestmidstream.com](mailto:truybalid@harvestmidstream.com)

---

The information contained in this email message is confidential and may be legally privileged and is intended only for the use of the individual or entity named above. If you are not an intended recipient or if you have received this message in error, you are hereby notified that any dissemination, distribution, or copy of this email is strictly prohibited. If you have received this email in error, please immediately notify us by return email or telephone if the sender's phone number is listed above, then promptly and permanently delete this message.

While all reasonable care has been taken to avoid the transmission of viruses, it is the responsibility of the recipient to ensure that the onward transmission, opening, or use of this message and any attachments will not adversely affect its systems or data. No responsibility is accepted by the company in this regard and the recipient should carry out such virus and other checks as it considers appropriate.

---

Harvest Midstream Company

VENDOR

1070478

CHECK DATE

11/13/2020

| INVOICE<br>NUMBER | INVOICE<br>DATE |                         | DISCOUNT<br>TAKEN | AMOUNT<br>PAID |
|-------------------|-----------------|-------------------------|-------------------|----------------|
| 030420A           | 03/04/2020      | Part 71 Fee Payment Los | 0.00              | 2,071.69       |
|                   |                 | Total:                  | 0.00              | 2,071.69       |

F94446

THIS CHECK IS PRINTED IN BLUE INK ON WHITE PAPER WITH A VOID SECURITY BACKGROUND AND MICROPRINT SIGNATURE LINE.

Harvest Midstream Company  
P.O. Box 61229  
Houston, Texas 77208-1229

AMEGY BANK  
5 POST OAK BLVD  
4400 POST OAK PARKWAY  
HOUSTON, TX 77027

35-1125/1130

CHECK NO.  
62058258

PAY Two Thousand Seventy One Dollars and Sixty Nine Cents  
TO THE ORDER OF:

US ENVIRONMENTAL PROTECTION AGENCY  
GOVERNMENT LOCKBOX 979078  
1005 CONVENTIONAL PLAZA  
ST LOUIS MO 63101

DATE  
11/13/2020

VOID AFTER 90 DAYS  
AMOUNT  
\*\*\*\*\*2,071.69

BY

*Colleen Elkins*

MP

⑈62058258⑈ ⑆113011258⑆ ⑈53267652⑈

Harvest Midstream Company  
P.O. Box 61229  
Houston, Texas 77208-1229

0133460



PD3DCV00100010 - 545981




US ENVIRONMENTAL PROTECTION AGENCY  
GOVERNMENT LOCKBOX 979078  
1005 CONVENTIONAL PLAZA  
ST LOUIS MO 63101

0001001010400 - PD3DCV00100010

ENDORSE

BEFORE CASHING  
THIS CHECK, PLEASE VERIFY THE FOLLOWING INFORMATION:  
1. THE CHECK IS FROM THE FEDERAL RESERVE BOARD OF GOVERNORS REG. CC

 The security features listed below are all as they are used.

Security features: Results of document authentication:

• Microprint: • Serial number: • Watermark: • Security features: • Absence of tampering: • Bank of America

• Federal Reserve Board of Governors Reg. CC



1755 Arroyo Drive  
Bloomfield, NM 87413  
Phone 505-632-4600  
Fax 505-632-4682  
harvestmidstream.com

March 12, 2020

U.S. EPA  
OCFO/OC/ACAD/FCB  
Attn: Collections Team  
1300 Pennsylvania Ave NW  
Mail Code 2733R  
Washington, DC 20004

re: Title V Part 71 Annual Fee Form FF - 2019  
Permit R6FOP-NM-04-R2 – Los Mestenos Compressor Station

Dear Madam/Sir,

In accordance with condition 5.1 of the Part 71 operating permit number R6FOP-NM-04-R2 for Harvest Four Corners LLC's Los Mestenos Compressor Station, please find enclosed the Fee Filing Form FF, for the payment for pollutants emitted during the calendar year 2019. Also enclosed is check number 0062053521 in the amount of \$2,071.69 for the annual operating permit fee.

If you have any questions, please call me at (505) 632-4625 or Bobby Myers of Cirrus Consulting at (801) 484-4412.

Sincerely,

Monica Smith  
Environmental Specialist

Attachments

**Federal Operating Permit Program (40 CFR Part 71)  
FEE FILING FORM (FF)**

The purpose of this form is to ensure that fee payments made by check are credited to the proper facility and to the proper government account. Send this form, along with form **FEE** and the check, to the appropriate lockbox bank address listed on the following page. This form is required whenever you pay by check, including for initial fee payment and to pay annual fees. Part 71 fees may be paid by check or electronically, and further information on making payments by check or electronically is provided on the following page.

Source or Facility Name Harvest Four Corners, LLC's Los Mestenos Compressor StationSource Location Rio Arriba County, New MexicoEPA Region where Source Located Region 6

## Mailing Address:

Street/P.O. Box 1755 Arroyo DriveCity BloomfieldState NM ZIP 87413 - Contact Person: Monica SmithTitle Environmental SpecialistTelephone ( 505 ) 632 - 4625 Ext. **Total Fee Payment Remitted: \$ 2071.69**



## TWO PAYMENT OPTIONS FOR PART 71 FEES:

### OPTION 1 - CHECK PAYMENT VIA U.S. POSTAL SERVICE

- Fee payment shall be in U.S. currency drawn on a U.S. bank.
- Check should be made out to the order of the "U.S. Environmental Protection Agency."
- Indicate on the check that the payment is for "Part 71 Fee Payment."
- Make a photocopy of the check.
- **Send the following to the EPA region (or delegate agency):**
  - ✓ Form *FEE* (EPA Form 5900-03) and
  - ✓ Photocopy of check
- **Send the following to the address below:**
  - ✓ Form *FF* (EPA Form 5900-06) and
  - ✓ Original check

|   |
|---|
| <b><i>Address for Regular Mail<br/>(U.S. Postal Service):</i></b>   |
| U.S. EPA<br>OCFO/OC/ACAD/FCB<br>Attn: Collections Team<br>1300 Pennsylvania Ave NW<br>Mail Code 2733R<br>Washington, DC 20004 |

- **Tips for Completing form FF (Fee Filing Form)**
  - **Source Location:** Physical location - Street address (if any), City, County, and State.
  - **Mailing Address:** Address for the EPA to send correspondence. This address may be different from the source location, such as a corporate office.
  - **EPA Region:** EPA region in which the source is located (e.g., EPA Region 8).
  - **Contact:** Person that can best answer questions concerning fee payment.

### OPTION 2 – ONLINE PAYMENT

- Part 71 fees can be paid online at [www.pay.gov](http://www.pay.gov) using form "SFO 1.1 (EPA Miscellaneous Payments - Cincinnati Finance Center)." *Note that EPA Form 5900-06 cannot be used for online payments.*
- **Tips for completing online form SFO 1.1:**
  - From the "Type of Payment" drop down menu, select "Other/Miscellaneous"
  - On the "Bill# or description" line, enter "Part 71 Fee Payment"
  - In the "Comments" box, enter the source or facility name and the part 71 permit number associated with this payment.
- **After submitting payment online, send the following to the EPA region (or delegate agency):**
  - Form *FEE* (EPA Form 5900-03) and
  - Copy of the electronic payment confirmation generated by the online payment system.
- **FOR MORE INFORMATION:** The following link provides detailed information on how to make payments to EPA for part 71 fees, penalties, and interest, including contact information for EPA's Accounts Receivable Branch in Cincinnati <https://www.epa.gov/financial/makepayment>
- Questions/inquiries may be sent to: [CollectionInquiryMailbox@epa.gov](mailto:CollectionInquiryMailbox@epa.gov)  
Laura Collier - [collier.laura@epa.gov](mailto:collier.laura@epa.gov)  
Stacey Church - [church.stacey@epa.gov](mailto:church.stacey@epa.gov)

ORIGIN ID:FMNA (505) 634-4316  
TRISTEN RUYBALD  
HARVEST FOUR CORNERS, LLC  
1755 ARROYO DRIVE

SHIP DATE: 17NOV20  
ACTWTG: 0.50 LB  
CAD: 113465079/INET4280

BLOOMFIELD, NM 87413  
UNITED STATES US

BILL SENDER

TO CINCINNATI FINANCE CENTER

US EPA

1005 CONVENTION PLAZA

LOCKBOX #979078

ST. LOUIS MO 63101

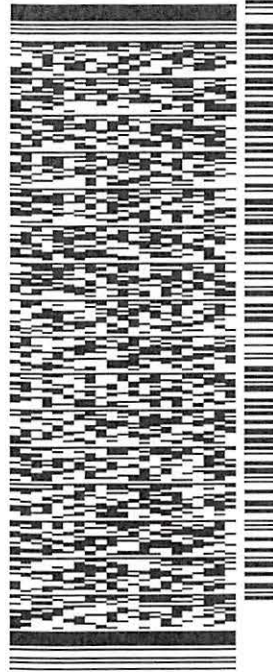
(202) 564-7593

REF:

PO:

DEPT:

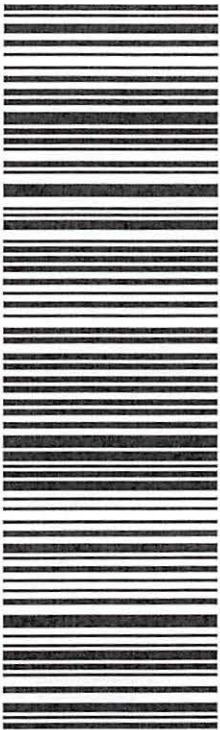
56BJ5/BA9/B766



TRK# 7721 0524 0388  
0201

WED - 18 NOV 4:30P  
STANDARD OVERNIGHT

XX CPSA 63101  
MO-US STL



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**Warning:** Use only the printed original label for shipping. Using a photocopy of this label for shipping purposes is fraudulent and could result in additional billing charges, along with the cancellation of your FedEx account number.

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Kayleigh Ruybalid

---

From: TrackingUpdates@fedex.com  
Sent: Wednesday, November 18, 2020 8:52 AM  
To: Kayleigh Ruybalid  
Subject: [EXTERNAL] FedEx Shipment 772105240388: Your package has been delivered



Hi. Your package was  
delivered Wed, 11/18/2020 at  
9:48am.



Delivered to 1005 CONVENTION PLZ, ST. LOUIS, MO 63101  
Received by J.EBLER

[OBTAIN PROOF OF DELIVERY](#)

---

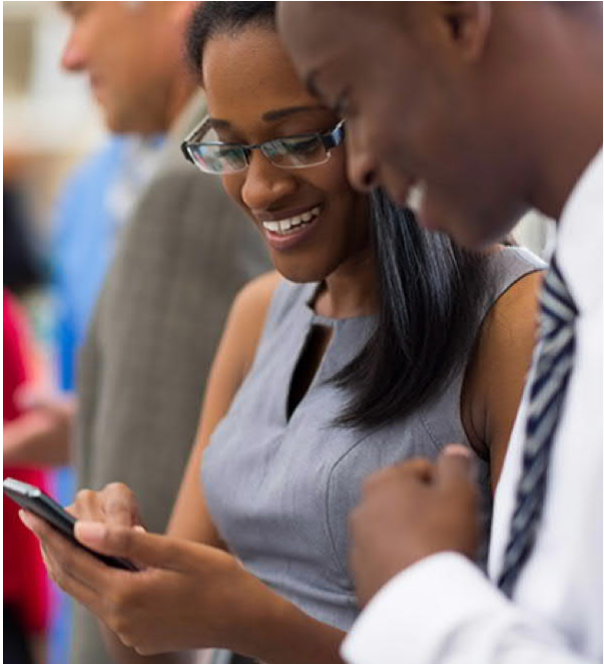
## Personal Message

Los Mestenos Part 71 Fee Payment Resubmittal

---

TRACKING NUMBER [772105240388](#)

|                              |   |
|------------------------------|---|
| <b>FROM</b>                  | Harvest Four Corners, LLC<br>1755 Arroyo Drive<br>Bloomfield, NM, US, 87413                                 |
| <b>TO</b>                    | US EPA<br>Cincinnati Finance Center<br>1005 Convention Plaza<br>Lockbox #979078<br>ST. LOUIS, MO, US, 63101 |
| <b>SHIP DATE</b>             | Tue 11/17/2020 04:42 PM   |
| <b>DELIVERED TO</b>          | Mailroom  |
| <b>PACKAGING TYPE</b>        | FedEx Envelope  |
| <b>ORIGIN</b>                | Bloomfield, NM, US, 87413   |
| <b>DESTINATION</b>           | ST. LOUIS, MO, US, 63101  |
| <b>NUMBER OF PIECES</b>      | 1   |
| <b>TOTAL SHIPMENT WEIGHT</b> | 0.50 LB   |
| <b>SERVICE TYPE</b>          | FedEx Standard Overnight  |



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[LEARN MORE](#)


This tracking update has been requested by:

**Company name:** Harvest Four Corners, LLC  
**Name:** Tristen Ruybalid  
**Email:** truybalid@harvestmidstream.com

---

**FOLLOW FEDEX**



 Please do not respond to this message. This email was sent from an unattended mailbox. This report was generated at approximately 9:51 AM CST 11/18/2020.

All weights are estimated.

To track the latest status of your shipment, click on the tracking number above.

Standard transit is the date and time the package is scheduled to be delivered by, based on the selected service, destination and ship date. Limitations and exceptions may apply. Please see the FedEx Service Guide for terms and conditions of service, including the FedEx Money-Back Guarantee, or contact your FedEx Customer Support representative.

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Thank you for your business.



1755 Arroyo Drive  
Bloomfield, NM 87413  
Phone 505-632-4600  
Fax 505-632-4682  
harvestmidstream.com

May 10, 2021

U.S. EPA  
OCFO/OC/ACAD/FCB  
Attn: Collections Team  
1300 Pennsylvania Ave NW  
Mail Code 2733R  
Washington, DC 20004

re: Title V Part 71 Annual Fee Form FF - 2020  
Permit R6FOP-NM-04-R2 – Los Mestenos Compressor Station

Dear Madam/Sir,

In accordance with condition 5.1 of the Part 71 operating permit number R6FOP-NM-04-R2 for Harvest Four Corners LLC's Los Mestenos Compressor Station, please find enclosed the Fee Filing Form FF, for the payment for pollutants emitted during the calendar year 2020. Also enclosed is check number 46001066 in the amount of \$1,561.56 for the annual operating permit fee.

If you have any questions, please call me at (505) 632-4625 or Bobby Myers of Cirrus Consulting at (801) 484-4412.

Sincerely,

Monica Smith  
Environmental Specialist

Attachments

**Federal Operating Permit Program (40 CFR Part 71)  
FEE FILING FORM (FF)**

The purpose of this form is to ensure that fee payments made by check are credited to the proper facility and to the proper government account. Send this form, along with form **FEE** and the check, to the appropriate lockbox bank address listed on the following page. This form is required whenever you pay by check, including for initial fee payment and to pay annual fees. Part 71 fees may be paid by check or electronically, and further information on making payments by check or electronically is provided on the following page.

Source or Facility Name Harvest Four Corners, LLC's Los Mestenos Compressor StationSource Location Rio Arriba County, New MexicoEPA Region where Source Located Region 6**Mailing Address:**Street/P.O. Box 1755 Arroyo DriveCity BloomfieldState NM ZIP 87413 - Contact Person: Monica SmithTitle Environmental SpecialistTelephone ( 505 ) 632 - 4625 Ext. **Total Fee Payment Remitted: \$ 1561.56**

## TWO PAYMENT OPTIONS FOR PART 71 FEES:

### OPTION 1 - CHECK PAYMENT VIA U.S. POSTAL SERVICE

- Fee payment shall be in U.S. currency drawn on a U.S. bank.
- Check should be made out to the order of the "U.S. Environmental Protection Agency."
- Indicate on the check that the payment is for "Part 71 Fee Payment."
- Make a photocopy of the check.
- **Send the following to the EPA region (or delegate agency):**
  - ✓ Form *FEE* (EPA Form 5900-03) and
  - ✓ Photocopy of check
- **Send the following to the address below:**
  - ✓ Form *FF* (EPA Form 5900-06) and
  - ✓ Original check

|   |
|---|
| <b>Address for Regular Mail<br/>(U.S. Postal Service):</b>  |
| U.S. EPA<br>OCFO/OC/ACAD/FCB<br>Attn: Collections Team<br>1300 Pennsylvania Ave NW<br>Mail Code 2733R<br>Washington, DC 20004 |

- **Tips for Completing form FF (Fee Filing Form)**
  - **Source Location:** Physical location - Street address (if any), City, County, and State.
  - **Mailing Address:** Address for the EPA to send correspondence. This address may be different from the source location, such as a corporate office.
  - **EPA Region:** EPA region in which the source is located (e.g., EPA Region 8).
  - **Contact:** Person that can best answer questions concerning fee payment.

### OPTION 2 – ONLINE PAYMENT

- Part 71 fees can be paid online at [www.pay.gov](http://www.pay.gov) using form "**SFO 1.1 (EPA Miscellaneous Payments - Cincinnati Finance Center)**." *Note that EPA Form 5900-06 cannot be used for online payments.*
- **Tips for completing online form SFO 1.1:**
  - From the "*Type of Payment*" drop down menu, select "Other/Miscellaneous"
  - On the "*Bill# or description*" line, enter "Part 71 Fee Payment"
  - In the "*Comments*" box, enter the source or facility name and the part 71 permit number associated with this payment.
- **After submitting payment online, send the following to the EPA region (or delegate agency):**
  - Form *FEE* (EPA Form 5900-03) and
  - Copy of the electronic payment confirmation generated by the online payment system.
- **FOR MORE INFORMATION:** The following link provides detailed information on how to make payments to EPA for part 71 fees, penalties, and interest, including contact information for EPA's Accounts Receivable Branch in Cincinnati <https://www.epa.gov/financial/makepayment>
- Questions/inquiries may be sent to: [CollectionInquiryMailbox@epa.gov](mailto:CollectionInquiryMailbox@epa.gov)  
Laura Collier - [collier.laura@epa.gov](mailto:collier.laura@epa.gov)  
Stacey Church - [church.stacey@epa.gov](mailto:church.stacey@epa.gov)





# Harvest Midstream Company

P.O.Box 61529  
Houston TX 77002

|            |            |             |            |               |          |
|------------|------------|-------------|------------|---------------|----------|
| Owner:     | 40011027   | Check Date: | 04/09/2021 | Check Number: | 46001066 |
| Invoice No | Inv. Date  | Description | Discount   | Net Amount    |          |
| 1900002391 | 04/07/2021 | 032421      | \$0.00     | \$1,561.56    |          |

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*Colleen Elkman*

Authorized Signature

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|   |   |  |
|---|---|--|
| ORIGIN ID: FMNA (505) 634-4316<br>TRISTEN RUYBALD<br>HARVEST FOUR CORNERS, LLC<br>1755 ARROYO DRIVE<br>BLOOMFIELD, NM 87413<br>UNITED STATES US   |   | SHIP DATE: 10MAY21<br>ACTWGT: 0.50 LB<br>CAD: 113465079/IN/ET4340<br>BILL SENDER |
| <b>TO COLLECTIONS TEAM</b><br><b>US EPA OCF00CACADFCB</b><br><b>1300 PENNSYLVANIA AVE NW</b><br><b>MAIL CODE 2733R</b><br><b>WASHINGTON DC 20004</b><br>(202) 564-7593<br>INV: REF: DEPT: |   |  |
|                       |   |  |
| TRK# 7736 8225 0479<br>0201   | TUE - 11 MAY 4:30P<br>STANDARD OVERNIGHT  |  |
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**Kayleigh Ruybalid**

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**From:** TrackingUpdates@fedex.com  
**Sent:** Tuesday, May 11, 2021 9:58 AM  
**To:** Kayleigh Ruybalid  
**Subject:** [EXTERNAL] FedEx Shipment 773682250479: Your package has been delivered



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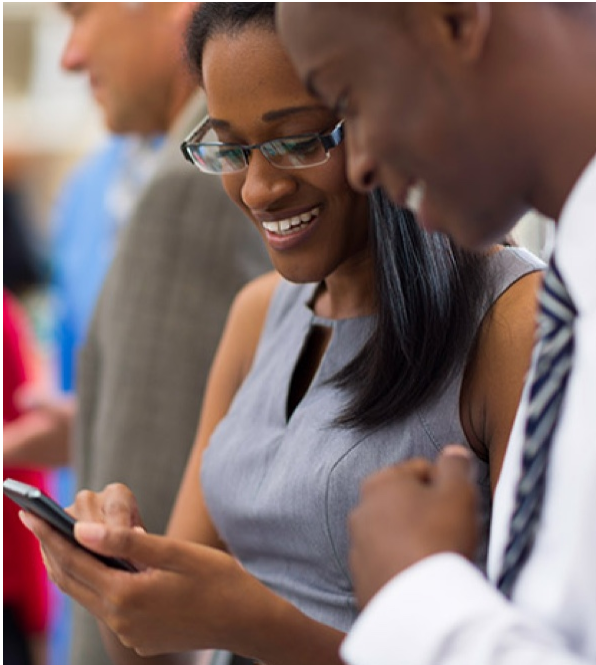
### Personal Message

Los Mestenos TV Part 71 Annual Fee Form FF 2020 Payment

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**TRACKING NUMBER** [773682250479](#)

|                              |  |
|------------------------------|--|
| <b>FROM</b>                  | Harvest Four Corners, LLC<br>1755 Arroyo Drive<br>Bloomfield, NM, US, 87413  |
| <b>TO</b>                    | US EPA OCFOOCACADFCB<br>Collections Team<br>1300 Pennsylvania Ave NW<br>Mail Code 2733R<br>WASHINGTON, DC, US, 20004 |
| <b>SHIP DATE</b>             | Mon 5/10/2021 04:36 PM   |
| <b>PACKAGING TYPE</b>        | FedEx Envelope   |
| <b>ORIGIN</b>                | Bloomfield, NM, US, 87413  |
| <b>DESTINATION</b>           | WASHINGTON, DC, US, 20004  |
| <b>SPECIAL HANDLING</b>      | Deliver Weekday  |
| <b>NUMBER OF PIECES</b>      | 1  |
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**Name:** Tristen Ruybalid  
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Thank you for your business.



1755 Arroyo Drive  
Bloomfield, NM 87413  
Phone 505-632-4600  
Fax 505-632-4682  
harvestmidstream.com

March 24, 2021

U.S. EPA, Region 6  
Air and Radiation Division Air Permits Section (ARPE)  
1201 Elm Street, Suite 500  
Dallas, TX 75270

re: Title V Part 71 Annual Fee Form FEE - 2020  
Permit R6FOP-NM-04-R2 – Los Mestenos Compressor Station

Dear Madam/Sir,

In accordance with condition 4.15 of the Part 71 operating permit number R6FOP-NM-04-R2 for Harvest Four Corners LLC's Los Mestenos Compressor Station, please find enclosed the Form FEE – Fee Calculation Worksheet, for the quantification for pollutants emitted during the calendar year 2020. In accordance with condition 5.1.2 of the operating permit, the Fee Filing Form FF and the annual operating permit fee in the amount of \$1,561.56 will be submitted no later than July 20, 2021, and a photocopy of the fee check and payment will be provided to you.

If you have any questions, please call me at (505) 632-4625 or Bobby Myers of Cirrus Consulting at (801) 484-4412.

Sincerely,

Monica Smith  
Environmental Specialist

Attachments

## Federal Operating Permit Program (40 CFR Part 71)

### FEE CALCULATION WORKSHEET (FEE)

Use this form initially, or thereafter on an annual basis, to calculate part 71 fees.

### A. General Information

Type of fee (Check one):      Initial   x   Annual

Deadline for submitting fee calculation worksheet 04 / 01 / 2021

For initial fees, emissions are based on (Check one):

x Actual emissions for the preceding calendar year. (Required in most circumstances.)

— Estimates of actual emissions for the current calendar year. (Required when operations commenced during the preceding calendar year.)

Date commenced operations        /        /

\_\_\_\_ Estimates of actual emissions for the preceding calendar year. (Optional after a part 71 permit was issued to replace a part 70 permit, but only if initial fee payment is due between January 1 and March 31; otherwise use actual emissions for the preceding calendar year.)

For annual fee payment, you are required to use actual emissions for the preceding calendar year.

**B. Source Information:** Complete this section only if you are paying fees but not applying for a permit.

Source or facility name Harvest Four Corners, LLC's Los Mestenios Compressor Station

Mailing address: Street or P.O. Box 1755 Arroyo Drive

City: Bloomfield State: NM ZIP 87413 -

Contact person: Monica Smith                      Title: Environmental Specialist

Telephone ( 505 ) 632 - 4625 Ext      Part 71 permit no. R6FOP-NM-04-R2

**C. Certification of Truth, Accuracy and Completeness:** Only needed if not submitting a separate form CTAC.

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in this submittal (form and attachments) are true, accurate and complete.

Name (signed) \_\_\_\_\_

Name (typed) Travis Jones Date:      /      /

**D. Annual Emissions Report for Fee Calculation Purposes -- Non-HAP**

You may use this to report actual emissions (tons per year) of regulated pollutants (for fee calculation) on a calendar-year basis for both initial and annual fee calculation purposes. Section E is designed to report HAP emissions. Quantify all actual emissions, including fugitives, but do not include insignificant emissions and certain regulated air pollutants that are not counted for fee purposes, such as CO and GHGs (see instructions). Sum the emissions in each column to calculate subtotals. Subtotals should be reported to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000 for that column.

This data is for 2020 (year)

| Emission Unit ID  | NOx  | VOC  | SO2 | PM10 | Lead | Other |
|-------------------|------|------|-----|------|------|-------|
| 1                 | 14.9 | 0.4  |     |      |      |       |
| 2                 | 0.0  | 0.0  |     |      |      |       |
| Tk-1              |      | 9.8  |     |      |      |       |
| F-1               |      | 3.5  |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
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|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
| <b>SUBTOTALS:</b> | 14.9 | 13.7 |     |      |      |       |

**E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

**HAP Identification.** Identify individual HAP emitted at the facility, identify the CAS number, and assign a unique identifier for use in the second table in this section. Whenever assigning identifier codes, use "HAP1" for the first, "HAP2" for the second, and so on.

| Name of HAP  | CAS No    | Identifier   |
|--------------|-----------|--------------|
| Acetaldehyde | 75-07-0   | HAP <u>1</u> |
| Formaldehyde | 50-00-0   | HAP <u>2</u> |
| Benzene      | 71-43-2   | HAP <u>3</u> |
| Toluene      | 108-88-3  | HAP <u>4</u> |
| Ethylbenzene | 100-41-4  | HAP <u>5</u> |
| Xylenes      | 1330-20-7 | HAP <u>6</u> |
| n-Hexane     | 110-54-3  | HAP <u>7</u> |

**HAP Emissions.** Report the actual emissions of individual HAP identified above. Use the identifiers assigned in the table above. Include all emissions, including fugitives, and do not include insignificant emissions. Sum the emissions in each column to calculate subtotals. Report subtotals to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000.

This data is for 2019 (year)

| Emissions Unit ID | Actual Emissions (Tons/Year) |        |        |        |        |        |        |       |
|-------------------|------------------------------|--------|--------|--------|--------|--------|--------|-------|
|                   | HAP_1_                       | HAP_2_ | HAP_3_ | HAP_4_ | HAP_5_ | HAP_6_ | HAP_7_ | HAP__ |
| 1                 | 0.2                          | 0.3    |        |        |        |        |        |       |
| 2                 | 0.0                          | 0.0    |        |        |        |        |        |       |
| Tk-1              |                              |        | 0.1    | 0.1    | 0.0    | 0.1    | 1.5    |       |
| F-1               |                              |        | 0.0    | 0.0    | 0.0    | 0.0    | 0.0    |       |
|                   |                              |        |        |        |        |        |        |       |
|                   |                              |        |        |        |        |        |        |       |
|                   |                              |        |        |        |        |        |        |       |
| <b>SUBTOTALS:</b> | 0.2                          | 0.3    | 0.0    | 0.1    | 0.0    | 0.0    | 1.5    | 2.1   |



## F. Fee Calculation Worksheet

This worksheet is used to calculate the total fee owed (including the emissions-based fee and the GHG fee adjustment) for both initial and annual fee payment purposes. Reconciliation is only for cases where you are paying the annual fee and you used any type of estimate of actual emissions when you calculated the initial fee. If you do not need to reconcile fees, complete line 1-5 (emissions summary) and then skip down to line 21 (emission calculation). See instructions for more detailed explanation.

### EMISSIONS SUMMARY

|  |      |
|--|------|
| 1. Sum the subtotals from section D of this form (non-HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 28.6 |
| 2. Sum the subtotals from section E of this form (HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 2.1  |
| 3. Sum lines 1 and 2.  | 30.7 |
| 4. Enter the emissions that were counted twice. If none, enter "0."  | 2.1  |
| 5. Subtract line 4 from line 3, round to the nearest ton, and enter the result here. This is the <b>total emissions</b> that count for fees purposes.  | 28.6 |
| <p style="text-align: center;"><b>RECONCILIATION</b><br/> <b>(WHEN INITIAL FEES WERE BASED ON ESTIMATES</b><br/> <b>FOR THE "CURRENT" CALENDAR YEAR)</b></p> <p>Only complete lines 6-10 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year in which you paid initial fees; otherwise skip to line 11 or to line 21.</p> |      |
| 6. Enter the total estimated actual emissions for the year the initial fee was paid (previously reported on line 5 of the initial fee form).   |      |
| 7. If line 5 is greater than line 6, subtract line 6 from line 5, and enter the result. Otherwise enter "0."   |      |
| 8. If line 6 is greater than line 5, subtract line 5 from line 6, and enter the result. Otherwise enter "0."   |      |
| 9. If line 7 is greater than 0, multiply line 7 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment. Go to line 21.   |      |
| 10. If line 8 is greater than 0, multiply line 8 by last year's fee rate (\$/ton) and enter the result here. This is the overpayment. Go to line 21.   |      |

**RECONCILIATION  
(WHEN INITIAL FEES WERE BASED ON ESTIMATES  
FOR THE "PRECEDING" CALENDAR YEAR)**

Only complete lines 11-20 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year preceding initial fee payment; otherwise skip to line 21. If completing this section, you will also need to complete sections D and E to report actual emissions for the calendar year preceding initial fee payment.

|  |           |
|--|-----------|
| 11. Sum the actual emissions from section D (non-HAP) for the calendar year preceding initial fee payment and enter the result here.   |           |
| 12. Sum the actual emissions from section E (HAP) for the calendar year preceding initial fee payment and enter the result here.   |           |
| 13. Add lines 11 and 12 and enter the total here. These are total actual emissions for the calendar year preceding initial fee payment.  |           |
| 14. Enter double counted emission from line 13 here. If none, enter "0."   |           |
| 15. Subtract line 14 from line 13, round to the nearest ton, and enter the result here.  |           |
| 16. Enter the total estimated actual emissions previously reported on line 5 of the initial fee form. These are estimated actual emissions for the calendar year preceding initial fee payment.  |           |
| 17. If line 15 is greater than line 16, subtract line 16 from line 15, and enter the result here. Otherwise enter "0."   |           |
| 18. If line 16 is greater than line 15, subtract line 15 from line 16, and enter the result here. Otherwise enter "0."   |           |
| 19. If line 17 is greater than 0, multiply line 17 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment.   |           |
| 20. If line 18 is greater than 0, multiply line 18 by last year's fee rate (\$/ton) and enter the result on this line. This is the overpayment.  |           |
| <b>EMISSION FEE CALCULATION</b>  |           |
| 21. Multiply line 5 (tons) by the current fee rate (\$/ton) and enter the result here. This is the unadjusted emissions fee. Continue on to line 23.   | \$1561.56 |
| <b>GHG FEE ADJUSTMENT</b>  |           |
| 22. If you are submitting an initial permit application and this is the first time you are paying fees, enter \$2,236, otherwise enter "0". [Note that any updates to the initial application are covered under this one-time charge.] | 0         |
| 23. Enter the number of permit modifications (or related permit actions) you have submitted to the permitting authority since you last paid fees. If none, skip to line 25.  | 0         |
| 24. Multiply the number in line 23 by \$365 and enter the result.  | 0         |

|  |           |
|--|-----------|
| 25. If you have submitted a permit renewal application since the last time you paid fees enter \$520, otherwise enter "0"  | 0         |
| 26. Sum line 22, 24, and 25 and enter the result. This is the GHG fee adjustment   | 0         |
| <b>OTHER ADJUSTMENTS</b>   |           |
| 27. Add the total on line 21 and the total on line 26 and enter the result.  | \$1561.56 |
| 28. Enter any underpayment from line 9 or 19 here. Otherwise enter "0."  | 0         |
| 29. Enter any overpayment from line 10 or 20 here. Otherwise enter "0."  | 0         |
| 30. If line 28 is greater than "0," add it to line 27 and enter the result here. If line 29 is greater than "0," subtract this from line 27 and enter the result here. Otherwise enter the amount on line 27 here. This is the fee adjusted for over/underpayment. | \$1561.56 |
| 31. Enter any credit for fee assessment error here. Otherwise, enter "0."  | 0         |
| 32. Subtract line 31 from line 30 and enter the result here. Stop here. This is the <b>TOTAL FEE (AFTER ADJUSTMENTS)</b> that you must remit to EPA.   | \$1561.56 |

## INSTRUCTIONS FOR FEE FEE CALCULATION WORKSHEET

### Information Collection Burden Estimates

The public reporting and recordkeeping burden for this collection of information is estimated to average 247 hours per respondent per year. Send comments on the Agency's need for this information, the accuracy of the provided burden estimates, and any suggested methods for minimizing respondent burden, including through the use of automated collection techniques to the Director, Collection Strategies Division, U.S. Environmental Protection Agency (2822T), 1200 Pennsylvania Ave., NW, Washington, D.C. 20460. Include the OMB control number in any correspondence. Do not send the completed form to this address.

### DETAILED INSTRUCTIONS

Use this form to initially or annually calculate fees. This form is for paying fees to EPA or a delegate agency (such as a State or tribe) under a part 71 operating permit program. The requirements for paying fees under part 71 programs, as well as the forms and instructions contained herein, are based on the requirements of 40 CFR 71.9

There may be cases, under a part 71 program, when you are not required to complete this form or pay the EPA fee rate (where the part 71 program has been delegated and EPA's fee has been suspended because EPA incurs no administrative costs). In such cases, the delegate agency will instruct you on how to calculate fees and how to pay them. If in doubt, contact your permitting authority.

#### General Rules for Fee Calculation under Part 71:

- Use the fee rate in effect at the time you pay the fee regardless of the time period that the emissions data represents. For example, if the annual fee for the current year is due July 1, you would use the fee rate in effect for the current year and the actual emissions for the previous calendar year.
- Do not prorate initial or annual fees. Pay full fees for the entire calendar year regardless of how many days you operated or were subject to the program during the previous or current year.
- Do not hesitate to contact the permitting authority if you have any doubt about how to calculate fees, especially if you have an unusual set of circumstances not addressed specifically by these forms or whenever the permit requirements appear to conflict with these forms (however, always assume the permit requirements take precedence in such cases).

### Section A. General Information

The deadline for submitting the fee form and paying the fee for initial fee payment purposes for most sources is the same deadline as for submitting all other forms required for the initial permit application. Other deadlines apply for initial fee payment in certain limited circumstances:

- When a source is subject to part 71 because of an unresolved EPA objection to a part 70 permit, fees are not due with the part 71 application, but are due 3 months following the date of the issuance of the part 71 permit.
- When EPA withdraws approval of a part 70 program and implements a part 71 programs, fees are submitted according to a schedule based on the source's SIC code (within 6 to 9 months of the effective date of the part 71 program).

The deadline for submitting the fee form and paying the fee for annual fee payment purposes is the anniversary date of initial fee payment. This is required whether or not a permit has been issued. If you were required to pay initial fees between January 1 and March 31, the regulations allow for submittal of annual fees no later than April 1.

Whether you are paying initial or annual fees see the instructions for sections D and E for more information on which calendar-year emission data to use (preceding or current year) and how to quantify such emissions (actual emissions or estimates of actual emissions).

### **Section B. Source Information**

Complete this section only if you are preparing this form for submittal at a different time than for the other portions of an initial application or for annual fee purposes.

### **Section C. Certification of Truth, Accuracy and Completeness**

This form and any other document required by a permit must be signed by a responsible official certifying truth, accuracy and completeness of the information. If you are submitting a separate **CTAC** form, there is no need to complete this section of the form. If you complete this section, there is no need to submit form **CTAC** separately.

### **Section D. Annual Emissions Report for Fee Calculation Purposes – Non-HAP**

Calculate actual emissions of regulated pollutants (for fee calculation), except for HAP, on a calendar-year basis for the facility in this section. Section E is provided to report actual emissions of HAP. Note the phrase “regulated pollutant (for fee calculation)” is any “regulated air pollutant” except carbon monoxide (CO), and pollutants regulated solely because they are: 1) subject to regulation under section 112(r) of the Act, or 2) a class I or II substance under title VI of the Act. **Note that GHG emissions are not counted for fee purposes.**

If more than one year of data is being submitted with the fee calculation worksheet, copy this page and complete a separate table for each year. If you are submitting an initial application, you may use emissions data already reported on form **EMISS**, provided this is the same data you would otherwise report in sections D and E of this form. If using **EMISS** in this manner, please note this on the fee calculation form. Also, sources must submit attachments to this form to show (at a minimum) examples of the calculations used to determine these values.

Show actual emissions for each listed air pollutant for each emission unit. Values should be reported to the nearest tenth (0.1) of a ton.

The column for "other" is for other regulated pollutants (for fee calculation) not already listed on the form. Write in the name of the pollutant in the proximity of the "other" column. If more than one such pollutant, show the pollutants, and the totals on an attachment.

Actual emissions must be calculated using actual operating hours, production rates, in-place control equipment, and types of materials processed, stored, or combusted over the preceding calendar year. Sources that have been issued title V permits are required to compute actual emissions using compliance methods required by the permits, such as monitoring or source testing data. If this is not possible, actual emissions should be determined using other federally recognized procedures.

For initial fee calculation purposes, most sources are required to use actual emissions for the preceding calendar year. However, there are certain exceptions where estimates of actual emissions are either required or allowed in place of actual emissions for the preceding calendar year (see table below):

| <b>Exception</b>   | <b>Emission Data</b>  |
|--|---|
| When the source commenced operation during the preceding calendar year.  | Estimates of actual emissions for the "current" calendar year are required  |
| When EPA withdraws approval of a part 70 program and implements a part 71 program, and the source pays initial part 71 fees between January 1 and March                        | Either estimates of actual emissions for the "preceding" calendar year or actual emissions for the preceding calendar year may be used. |
| When a part 71 permit was issued following an unresolved objection to a part 70 permit, and the source is required to pay initial part 71 fees between January 1 and March 31. | Either estimates of actual emissions for the "preceding" calendar year or actual emissions for the preceding calendar year may be used. |

For annual fee purposes, fee calculation should be based on actual emissions for the preceding calendar year in all cases.

In most cases you will only need to report one set of emission data using sections D and E of this form (the data that is the basis of the initial or annual fee being paid as explained above). This data is subsequently carried over to lines 1 and 2 of section F (Fee Calculation Worksheet) of the form.

However, there is one exception where you would be required to report two different sets of emissions data using sections D and E – when paying the first annual fee and reconciliation is required because the initial fee was based on estimated actual emissions for the "preceding" calendar year (the year preceding initial fee payment). In this case, the two data sets would be:

- actual emissions for the year initial fees paid (for annual fee purposes in lines 1-5 of section F of the form), and
- actual emissions for the year preceding initial fee payment (for reconciliation in lines 11-20 of the form)

Whenever reconciliation is required as part of annual fee payment, you will also need a copy of the fee forms you previously submitted with initial fee payment in order to obtain the value of estimated actual emissions.

Include all fugitive emissions in the calculation of actual emissions, including those that do not count for applicability. Do not include any insignificant emissions identified on form **IE**.

The subtotal line in section D of the form is provided at the bottom of each column to enter total emissions for each pollutant reported above. Each subtotal should be reported to the nearest tenth (0.1) of a ton. If any subtotal exceeds 4,000 tons, enter 4,000 tons for that column.

Any necessary adjustments for double counting of emissions will be performed later in section F.

### **Section E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

List the actual emissions of individual HAP from each emission unit. If you are initially applying for a permit, you may use the emissions of HAP reported on form **EMISS**, instead of completing this section of this form, provided these emissions are the same as you would otherwise report using this section of the form. If you are doing this, please note it on the form.

This section is composed of two tables. The first table is to identify individual HAP emitted at each emission unit. Assign a unique identifier for use in the second table. Please use "HAP1" for the first

one, "HAP2" for the second one, and so on. The second table is to calculate the actual emission of individual HAP at each emission unit. Use the identifiers assigned in the first table to label the column headers for the second table. You may round and report these emissions to the nearest tenth (0.1) of a ton. Sum the values in each column and enter the subtotals at the bottom of the table. If any subtotal exceeds 4,000 tons, enter 4,000 for that column.

See instructions for section D for more information on reporting emissions data.

### **Section F. Fee Calculation Worksheet**

This worksheet is used to sum the total tons of actual emissions subject to fees, adjust for double counting of emissions, perform certain reconciliations for underpayment and overpayment of fees and adjust for fee assessment errors, if needed, and ultimately to determine the total fee to be paid.

A detailed explanation of Section F follows (separated into six parts):

#### **Emissions Summary**

The subtotals for each pollutant listed in Sections D and E (or from form **EMISS**) are added together to calculate the total emissions (in tons per year) for the facility.

The emissions that are reported here will vary for initial fee payment purposes, depending on the specific circumstances, but will always be actual emissions for the preceding calendar year for annual fee purposes. See the instructions for section D for more on the emissions data you should use in the part of the form.

The total emissions are adjusted for double counting and are rounded to the nearest ton. For example, double counting may occur where a pollutant is defined as HAP and VOC. If you adjust for double counting, attach an explanation for this.

#### **Reconciliation (When Initial Emission Fees Were Based on Estimates for the Current Calendar Year)**

This section is only used by sources paying their first annual fee when their initial fee was based on estimates of calendar-year emissions for the "current" year (the same year that initial fees were paid). This reconciliation is done by comparing the actual emissions for the "current" year provided in sections D and E of this submittal with the estimate of those emissions previously provided with initial fee payment. There may have been overpayment or underpayment of the initial fee. The fee you are paying now will be adjusted for this difference later.

#### **Reconciliation (When Initial Emission Fees Were Based on Estimates for the Preceding Calendar Year)**

This section is only used by sources paying their first annual fee when their initial fee was based on estimates of calendar-year emissions for the year preceding initial fee payment, provided the source was required to pay its initial fee between January 1 and March 31, and EPA issued the Part 71 permit to replace a Part 70 permit. This reconciliation is done by comparing the actual emissions for the "preceding" year provided in sections D and E of this submittal with the estimate of those emissions provided with initial fee payment. There may have been overpayment or underpayment of the initial fee. The fee you are paying now will be adjusted for this difference later.

## **Emission Fee Calculation**

Calculate the emission-based fee using the emissions from line 5 (tons) multiplied by the fee rate (\$/ton) in effect at the time the fee is paid.

## **GHG Fee Adjustment**

The part 71 rule was amended in 2015 to require the fees to be increased by a GHG fee adjustment. The GHG adjustment must be calculated by each source that is required to pay fees. The adjustment is based on the burden for the permitting authority to conduct certain GHG evaluations or reviews related to the source, rather than on emissions. Set fees are charged for certain activities that have occurred at the source since the last time fees were paid. For an initial application, the set fee is a one-time charge that includes the costs of processing application updates. The term "permit modification" refers to any significant and minor modifications, but not to administrative amendments. The number of permit modifications must be multiplied by the set fee for modifications to determine the total GHG adjustment for modifications. The set fee for a permit renewal also includes any permit modifications that may be processed at the same time as the renewal. Note that you may need to check with the permitting authority to determine if they are holding any permit modification requests you have submitted for processing with an upcoming permit renewal.

## **Other Adjustments**

The purpose of this section is to adjust the emissions-based to determine the total fee (after adjustments) that is due to the EPA. The emissions fee determined on line 21 is adjusted by the GHG fee adjustment, any amounts of overpayment or underpayment related to a previous fee submittal, and to correct for any fee assessment errors.

Fee assessment errors occur when the permitting authority determines that the source has calculated the fee incorrectly. If this occurs, you will be notified of the error. Any overpayment will be credited against the next fee owed. In the case of underpayment, you will be billed for the corrected fee and you will have 30 days to remit the amount. If you think the assessed fee is in error, you may submit a written explanation of the alleged error, but you must pay the fee. The permitting authority will provide a determination in 90 days. If the assessment of underpayment is in error, your account will be credited.

## **Fee Payment**

See form **FF** (the Fee Filing form) for instructions on how to make fee payment to the EPA.

## **Penalties and Interest**

The permitting authority will bill sources for appropriate penalties and interest for late payment or excessive underpayment of fees. Interest will be assessed on payments received later than the due date. Penalties shall be assessed if payment is not paid within 30 days of the due date. For sources issued with issued permits, penalties and interest shall be assessed for excessive underpayment of the annual fee amount.

**END**



## Kayleigh Ruybalid

---

**From:** TrackingUpdates@fedex.com  
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**To:** Kayleigh Ruybalid  
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### Personal Message

Los Mestenios 2020 TV Part 71 Form FEE

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**TRACKING NUMBER** [773296798440](#)

|                              |  |
|------------------------------|--|
| <b>FROM</b>                  | Harvest Four Corners, LLC<br>1755 Arroyo Drive<br>Bloomfield, NM, US, 87413  |
| <b>TO</b>                    | US EPA Region-6, ARPE<br>Air & Radiation DivAir Permits Sec<br>1201 Elm Street<br>Suite 500<br>DALLAS, TX, US, 75270 |
| <b>SHIP DATE</b>             | Wed 3/31/2021 04:55 PM   |
| <b>DELIVERED TO</b>          | Mailroom   |
| <b>PACKAGING TYPE</b>        | FedEx Envelope   |
| <b>ORIGIN</b>                | Bloomfield, NM, US, 87413  |
| <b>DESTINATION</b>           | DALLAS, TX, US, 75270  |
| <b>SPECIAL HANDLING</b>      | Deliver Weekday  |
| <b>NUMBER OF PIECES</b>      | 1  |
| <b>TOTAL SHIPMENT WEIGHT</b> | 0.50 LB  |
| <b>SERVICE TYPE</b>          | FedEx Standard Overnight   |



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**Name:** Tristen Ruybalid

**Email:** [truybalid@harvestmidstream.com](mailto:truybalid@harvestmidstream.com)

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Thank you for your business.



1755 Arroyo Drive  
Bloomfield, NM 87413  
Phone 505-632-4600  
Fax 505-632-4682  
harvestmidstream.com

July 13, 2022

U.S. EPA  
OCFO/OC/ACAD/FCB  
Attn: Collections Team  
1300 Pennsylvania Ave NW  
Mail Code 2733R  
Washington, DC 20004

Re: Title V Part 71 Form FF (for 2021 inventory)  
Permit R6FOP-NM-04-R2 – Los Mestenos Compressor Station

Dear Madam/Sir,

In accordance with Condition 5.1 of the Part 71 operating permit, R6FOP-NM-04-R2, for the Harvest Four Corners, LLC – Los Mestenos Compressor Station, please find attached a check for the 2021 annual operating permit fee in the amount of \$1,945.56. Also attached are the required Form FF – Filing Fee and Form FEE – Fee Calculation Worksheet.

Thank you for your assistance. If you have any questions, please call me at (505) 632-4421.

Sincerely,

Oakley Hayes  
Environmental Specialist

Attachments

Check  
Form FF  
Form FEE

**Federal Operating Permit Program (40 CFR Part 71)**  
**FEE FILING FORM (FF)**

The purpose of this form is to ensure that fee payments made by check are credited to the proper facility and to the proper government account. Send this form, along with form **FEE** and the check, to the appropriate lockbox bank address listed on the following page. This form is required whenever you pay by check, including for initial fee payment and to pay annual fees. Part 71 fees may be paid by check or electronically, and further information on making payments by check or electronically is provided on the following page.

Source or Facility Name: Harvest Four Corners, LLC - Los Mestenos Compressor StationSource Location: Rio Arriba County, New MexicoEPA Region where Source Located: Region 6

## Mailing Address:

Street/P.O. Box: 1755 Arroyo DriveCity: BloomfieldState: NM ZIP: 87413 -       Contact Person: Oakley HayesTitle: Environmental SpecialistTelephone (505) 632 - 4421 Ext.       **Total Fee Payment Remitted: \$1,945.56**



# Harvest Midstream Company

P.O.Box 61529  
Houston TX 77208-1529

|            |            |             |            |               |          |
|------------|------------|-------------|------------|---------------|----------|
| Owner:     | 40011027   | Check Date: | 07/07/2022 | Check Number: | 46010523 |
| SAP Doc No | Inv. Date  | Invoice No  | Discount   | Net Amount    |          |
| 1900020727 | 07/06/2022 | 07062022    | \$0.00     | \$1,945.56    |          |

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Harvest Midstream Company  
P.O.Box 61529  
Houston TX 77208-1529

AMEGY BANK

32-1125  
1130

Void After 90 Days

|          |            |                 |
|----------|------------|-----------------|
| Check No | Check Date | Check Amount    |
| 46010523 | 07/07/2022 | *****\$1,945.56 |

PAY *One Thousand Nine Hundred Forty-Five Dollars And Fifty-Six Cents*

TO  
THE  
ORDER  
OF

US ENVIRONMENTAL PROTECTION AGENCY  
1300 PA AVE NW MAIL CODE 2733R  
WASHINGTON DC 20004

Authorized Signature

⑈46010523⑈ ⑆113011258⑆ 0053267652⑈



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Padlock Security box appears blurred if copied or scanned  
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Appearance of brown and/or blue stains may indicate alterations  
Invisible unless exposed to ultraviolet light  
Absence of visible red and/or blue fibers may indicate alteration  
True watermark visible from both sides, absence indicates alteration



Federal Operating Permit Program (40 CFR Part 71)  
**FEE CALCULATION WORKSHEET (FEE)**

Use this form initially, or thereafter on an annual basis, to calculate part 71 fees.

**A. General Information**

Type of fee (Check one): ☐ Initial ☒ Annual

Deadline for submitting fee calculation worksheet 07 / 20 / 2022

For initial fees, emissions are based on (Check one):

☒ Actual emissions for the preceding calendar year. (Required in most circumstances.)

☐ Estimates of actual emissions for the current calendar year. (Required when operations commenced during the preceding calendar year.)

Date commenced operations        /        /       

☐ Estimates of actual emissions for the preceding calendar year. (Optional after a part 71 permit was issued to replace a part 70 permit, but only if initial fee payment is due between January 1 and March 31; otherwise use actual emissions for the preceding calendar year.)

For annual fee payment, you are required to use actual emissions for the preceding calendar year.

**B. Source Information:** Complete this section only if you are paying fees but not applying for a permit.

Source or facility name Harvest Four Corners, LLC - Los Mestenos Compressor Station

Mailing address: Street or P.O. Box 1755 Arroyo Drive

City: Bloomfield State: NM ZIP: 87413 -       

Contact person: Oakley Hayes Title: Environmental Specialist

Telephone (505) 632 - 4421 Ext.:        Part 71 Permit No.: R6FOP-NM-04-R2

**C. Certification of Truth, Accuracy and Completeness:** Only needed if not submitting a separate form CTAC.

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in this submittal (form and attachments) are true, accurate and complete.

Name (signed) 

Name (typed): Travis Jones Date: 7 / 7 / 2022



**D. Annual Emissions Report for Fee Calculation Purposes -- Non-HAP**

You may use this to report actual emissions (tons per year) of regulated pollutants (for fee calculation) on a calendar-year basis for both initial and annual fee calculation purposes. Section E is designed to report HAP emissions. Quantify all actual emissions, including fugitives, but do not include insignificant emissions and certain regulated air pollutants that are not counted for fee purposes, such as CO and GHGs (see instructions). Sum the emissions in each column to calculate subtotals. Subtotals should be reported to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000 for that column.

This data is for 2021 (year)

| Emission Unit ID  | NOx  | VOC  | SO2 | PM10 | Lead | Other |
|-------------------|------|------|-----|------|------|-------|
| 1                 | 19.3 | 0.4  | 0.2 | 0.3  |      |       |
| 2                 | 0.0  | 0.0  | 0.0 | 0.0  |      |       |
| 3                 | 0.2  | 0.0  | 0.0 | 0.0  |      |       |
| SSM               |      | 0.0  |     |      |      |       |
| F1                |      | 3.8  |     |      |      |       |
| T1                |      | 9.1  |     |      |      |       |
| T2                |      | 1.3  |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
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|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
|                   |      |      |     |      |      |       |
| <b>SUBTOTALS:</b> | 19.5 | 14.6 | 0.2 | 0.3  |      |       |

**E. Annual Emissions Report for Fee Calculation Purposes -- HAP**

**HAP Identification.** Identify individual HAP emitted at the facility, identify the CAS number, and assign a unique identifier for use in the second table in this section. Whenever assigning identifier codes, use "HAP1" for the first, "HAP2" for the second, and so on.

| Name of HAP  | CAS No   | Identifier |
|--------------|----------|------------|
| Acetaldehyde | 75-07-0  | HAP __1__  |
| Benzene      | 71-43-2  | HAP __2__  |
| Formaldehyde | 50-00-0  | HAP __3__  |
| n-Hexane     | 110-54-3 | HAP __4__  |
|              |          |            |
|              |          |            |
|              |          |            |

**HAP Emissions.** Report the actual emissions of individual HAP identified above. Use the identifiers assigned in the table above. Include all emissions, including fugitives, and do not include insignificant emissions. Sum the emissions in each column to calculate subtotals. Report subtotals to the nearest tenth (0.1) of a ton at the bottom of the page. If any subtotal exceeds 4,000 tons, enter 4,000.

This data is for 2021 (year)

| Emissions Unit ID | Actual Emissions (Tons/Year) |         |         |         |         |         |         |         |
|-------------------|------------------------------|---------|---------|---------|---------|---------|---------|---------|
|                   | HAP_1__                      | HAP_2__ | HAP_3__ | HAP_4__ | HAP_5__ | HAP_6__ | HAP_7__ | HAP____ |
| 1                 | 0.2                          | 0.0     | 0.2     | 0.0     |         |         |         |         |
| 2                 | 0.0                          | 0.0     | 0.0     | 0.0     |         |         |         |         |
| 3                 | 0.0                          | 0.0     | 0.0     | 0.0     |         |         |         |         |
| SSM               | 0.0                          | 0.0     | 0.0     | 0.0     |         |         |         |         |
| F1                | 0.0                          | 0.0     | 0.0     | 0.1     |         |         |         |         |
| T1                | 0.0                          | 0.1     | 0.0     | 0.5     |         |         |         |         |
| T2                | 0.0                          | 0.0     | 0.0     | 0.1     |         |         |         |         |
| <b>SUBTOTALS:</b> | 0.2                          | 00.1    | 0.2     | 0.7     |         |         |         |         |

## F. Fee Calculation Worksheet

This worksheet is used to calculate the total fee owed (including the emissions-based fee and the GHG fee adjustment) for both initial and annual fee payment purposes. Reconciliation is only for cases where you are paying the annual fee and you used any type of estimate of actual emissions when you calculated the initial fee. If you do not need to reconcile fees, complete line 1-5 (emissions summary) and then skip down to line 21 (emission calculation). See instructions for more detailed explanation.

### EMISSIONS SUMMARY

|  |      |
|--|------|
| 1. Sum the subtotals from section D of this form (non-HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 34.6 |
| 2. Sum the subtotals from section E of this form (HAP) and enter the total, rounded to the nearest tenth (0.1) of a ton.   | 1.2  |
| 3. Sum lines 1 and 2.  | 35.8 |
| 4. Enter the emissions that were counted twice. If none, enter "0."  | 1.2  |
| 5. Subtract line 4 from line 3, round to the nearest ton, and enter the result here. This is the <b>total emissions</b> that count for fees purposes.  | 34.6 |
| <p style="text-align: center;"><b>RECONCILIATION</b><br/> <b>(WHEN INITIAL FEES WERE BASED ON ESTIMATES</b><br/> <b>FOR THE "CURRENT" CALENDAR YEAR)</b></p> <p>Only complete lines 6-10 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year in which you paid initial fees; otherwise skip to line 11 or to line 21.</p> |      |
| 6. Enter the total estimated actual emissions for the year the initial fee was paid (previously reported on line 5 of the initial fee form).   |      |
| 7. If line 5 is greater than line 6, subtract line 6 from line 5, and enter the result. Otherwise enter "0."   |      |
| 8. If line 6 is greater than line 5, subtract line 5 from line 6, and enter the result. Otherwise enter "0."   |      |
| 9. If line 7 is greater than 0, multiply line 7 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment. Go to line 21.   |      |
| 10. If line 8 is greater than 0, multiply line 8 by last year's fee rate (\$/ton) and enter the result here. This is the overpayment. Go to line 21.   |      |

**RECONCILIATION  
(WHEN INITIAL FEES WERE BASED ON ESTIMATES  
FOR THE "PRECEDING" CALENDAR YEAR)**

Only complete lines 11-20 if you are paying the first annual fee and initial fees were based on estimated actual emissions for the calendar year preceding initial fee payment; otherwise skip to line 21. If completing this section, you will also need to complete sections D and E to report actual emissions for the calendar year preceding initial fee payment.

|  |            |
|--|------------|
| 11. Sum the actual emissions from section D (non-HAP) for the calendar year preceding initial fee payment and enter the result here.   |            |
| 12. Sum the actual emissions from section E (HAP) for the calendar year preceding initial fee payment and enter the result here.   |            |
| 13. Add lines 11 and 12 and enter the total here. These are total actual emissions for the calendar year preceding initial fee payment.  |            |
| 14. Enter double counted emission from line 13 here. If none, enter "0."   |            |
| 15. Subtract line 14 from line 13, round to the nearest ton, and enter the result here.  |            |
| 16. Enter the total estimated actual emissions previously reported on line 5 of the initial fee form. These are estimated actual emissions for the calendar year preceding initial fee payment.  |            |
| 17. If line 15 is greater than line 16, subtract line 16 from line 15, and enter the result here. Otherwise enter "0."   |            |
| 18. If line 16 is greater than line 15, subtract line 15 from line 16, and enter the result here. Otherwise enter "0."   |            |
| 19. If line 17 is greater than 0, multiply line 17 by last year's fee rate (\$/ton) and enter the result here. This is the underpayment.   |            |
| 20. If line 18 is greater than 0, multiply line 18 by last year's fee rate (\$/ton) and enter the result on this line. This is the overpayment.  |            |
| <b>EMISSION FEE CALCULATION</b>  |            |
| 21. Multiply line 5 (tons) by the current fee rate (\$/ton) and enter the result here. This is the unadjusted emissions fee. Continue on to line 23.   | \$1,945.56 |
| <b>GHG FEE ADJUSTMENT</b>  |            |
| 22. If you are submitting an initial permit application and this is the first time you are paying fees, enter \$2,236, otherwise enter "0". [Note that any updates to the initial application are covered under this one-time charge.] | 0          |
| 23. Enter the number of permit modifications (or related permit actions) you have submitted to the permitting authority since you last paid fees. If none, skip to line 25.  | 0          |
| 24. Multiply the number in line 23 by \$365 and enter the result.  | 0          |

|  |            |
|--|------------|
| 25. If you have submitted a permit renewal application since the last time you paid fees enter \$520, otherwise enter "0"  | 0          |
| 26. Sum line 22, 24, and 25 and enter the result. This is the GHG fee adjustment   | 0          |
| <b>OTHER ADJUSTMENTS</b>   |            |
| 27. Add the total on line 21 and the total on line 26 and enter the result.  | \$1,945.56 |
| 28. Enter any underpayment from line 9 or 19 here. Otherwise enter "0."  | 0          |
| 29. Enter any overpayment from line 10 or 20 here. Otherwise enter "0."  | 0          |
| 30. If line 28 is greater than "0," add it to line 27 and enter the result here. If line 29 is greater than "0," subtract this from line 27 and enter the result here. Otherwise enter the amount on line 27 here. This is the fee adjusted for over/underpayment. | \$1,945.56 |
| 31. Enter any credit for fee assessment error here. Otherwise, enter "0."  | 0          |
| 32. Subtract line 31 from line 30 and enter the result here. Stop here. This is the <b>TOTAL FEE (AFTER ADJUSTMENTS)</b> that you must remit to EPA.   | \$1,945.56 |

ORIGIN ID:FMNA (505) 634-4316  
TRISTEN RUYBALD  
HARVEST FOUR CORNERS, LLC  
1755 ARROYO DRIVE

BLOOMFIELD, NM 87413  
UNITED STATES US

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ACTWGT: 0.50 LB  
CAD: 113465079/NMET4490

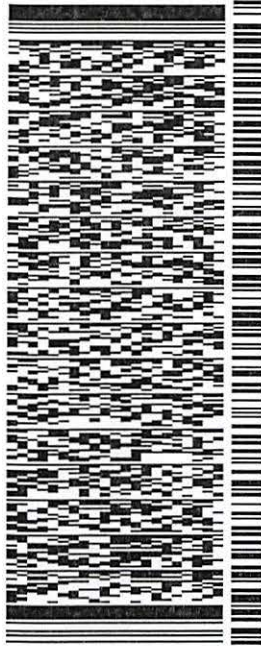
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## Personal Message

Los Mestenios TV Part 71 Form FF 2021 (Payment)

---

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Bloomfield, NM, US, 87413

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Collections Team  
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**Name:** Tristen Ruybalid

**Email:** truybalid@harvestmidstream.com



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## **Section 9**

### **Certification of Truth, Accuracy and Completeness**

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A certification of truth, accuracy and completeness is provided in this section. Please see the following page.

Federal Operating Permit Program (40 CFR Part 71)  
**CERTIFICATION OF TRUTH, ACCURACY, AND COMPLETENESS (CTAC)**

This form must be completed, signed by the "Responsible Official" designated for the facility or emission unit, and sent with each submission of documents (i.e., application forms, updates to applications, reports, or any information required by a part 71 permit).

**A. Responsible Official**

Name: (Last) Jones (First) Travis (MI) \_\_\_\_\_

Title EHS Manager

Street or P.O. Box 1111 Travis St

City Houston State TX ZIP 77002 - \_\_\_\_\_

Telephone (713) 289 - 2630 Ext. \_\_\_\_\_ Facsimile (\_\_\_\_) \_\_\_\_\_ - \_\_\_\_\_

**B. Certification of Truth, Accuracy and Completeness** (to be signed by the responsible official)

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in these documents are true, accurate and complete.

Name (signed) 

Name (typed) Travis Jones Date: 11 / 22 / 22